



Sth International Conference on Structured Catalysts and Reactors

Catalyzed wall

Mass transfer and catalytic reaction in Taylor flow: parametric numerical study for frozen hydrodynamics

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Objectives

- Goal: Simulation of catalyzed hydrogenation of nitrobenzene to aniline within a Taylor flow in monolith reactor Periodic Periodic Flow driven by pressure drop condition condition Methodology Nitrobe Coupling two computer codes: TURBIT-VOF^[1] for the gas-liguid Catalyzed wal flows and DETCHEM^[2] for the reaction kinetics (Hydrogenation of nitrobenzene) Test conditions · Moving reference frame approach for mass transfer Temperature: 298K, pressure: 7bar, channel height: 100µm Langmuir-Hinshelwood type global reaction kinetics^[3] Reynolds number: 80~110, capillary number: 0.03~0.04 Numerical approaches Hydrodynamics Mass transfer in the moving frame · Velocity fields for different Reynolds and capillary number (case 1) Two-dimensional incompressible Navier-Stokes Solve concentration equations with frozen equation with Volume-of-fluid (VOF) method Axial velocity (u*) distribution hydrodynamics at quasi steady state Isothermal simulation : Computational domain > Flow Constant physical properties during calculation Fine mesh resolution near the boundary wall Comparison of film thickness with Halpern & Gaver relation^[4] Velocity in a fixed frame Halpern & Gaver relation Case 1: Ca= 0.0356 Case 2: Ca= 0.0394 Case 3: Ca= 0.0292 Fixed reference frame approach 0. Velocity in the frame of moving bubble $h_0 = h_0/H$ $= 0.417(1 - \exp(-1.69Ca^{0.5}))$ 0.01 L 1E-3 0.0 0.7 Moving reference frame approach Ca [-] Results of reactive mass transfer in the moving frame Temporal distributions of hydrogen and aniline Mean concentrations and mass transfer coefficient 1.2E-02 6 0E-10 0.05 Witho time= 1.0E-0 0.04 250 µs 8.0E-03 4.0E-10 **s** 0.03 ع⁵ 6.0E-0 3.0E-10 در 10.02 4.0E-0 2.0E-10 time Anilir 0.0 500 µ 2.0E-0 1.0E-10 ____00E+00 1000 0.0E+00 400 600 Time [μs] 800 1000 400 600 Time [μs] · Hydrogen mass transfer is largest at the rear part of the bubble time= 750 µ where the liquid film thickness is thinnest The aniline is mainly produced in rear part as well The mean concentration of hydrogen in liquid phase is increasing by mass transfer from the gas phase and that of aniline is also time=
- Conclusions
- The gas-liquid Taylor flow of nitrobenzene and hydrogen has been successfully computed with real viscosities and diffusivities
- Moving frame approach allows to save the computational time without loss of physical information
- The estimation of film region is most important to investigate the catalytic reaction within the Taylor flow

References

1 ms

[1] Onea et al., Chem. Eng. Sci., 64 (2009) 1416-1435 [4] Halpern et al., J Comput Phys, 115(2) (1994) 366-375 [2] Deutschmann et al, DETCHEM™ User Manual, 2012, http://www.detchem.com

increasing due to the reaction

The enhancement of mass transfer coefficient by reaction is small

[3] Höller et al., Chem. Eng. Technol. 23 (2000) 3, 251-255

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