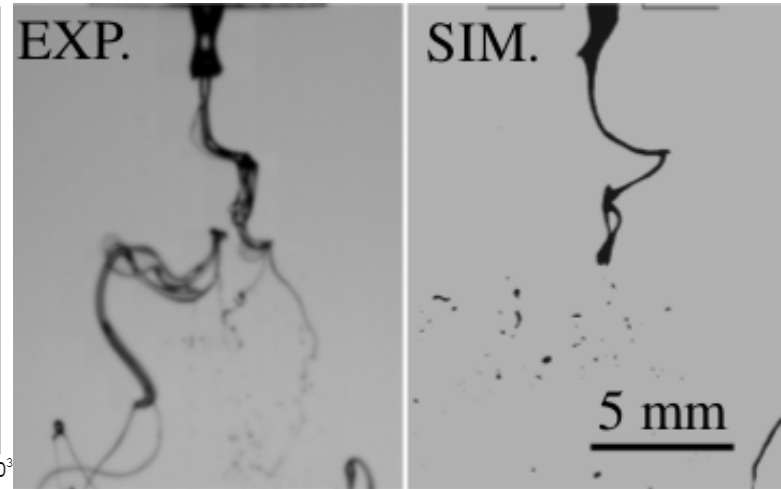
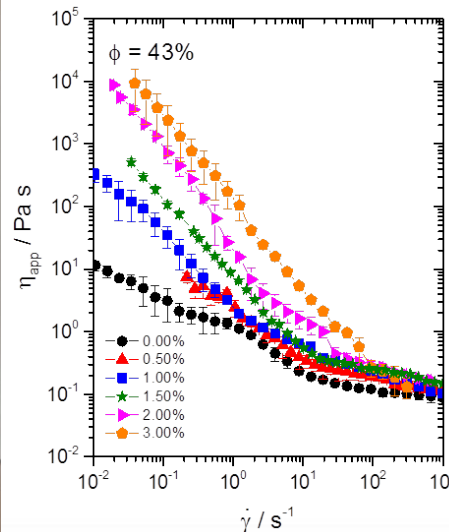
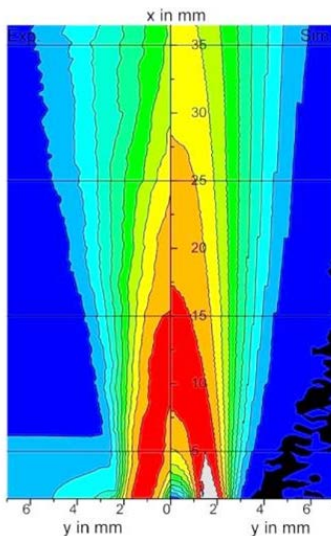


# Zerstäubung von biosyncrude

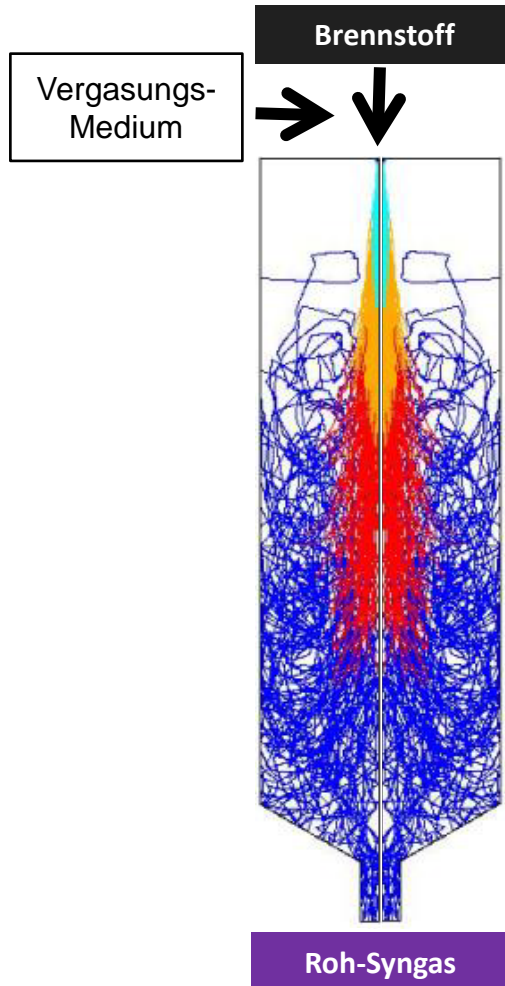
(Begleitforschung bioliq<sup>®</sup> 2)

KIT (ITC, EBI, ITS, MVM)

Tobias Jakobs



# Prozessschritte der Flugstromvergasung



## Prozessschritte:

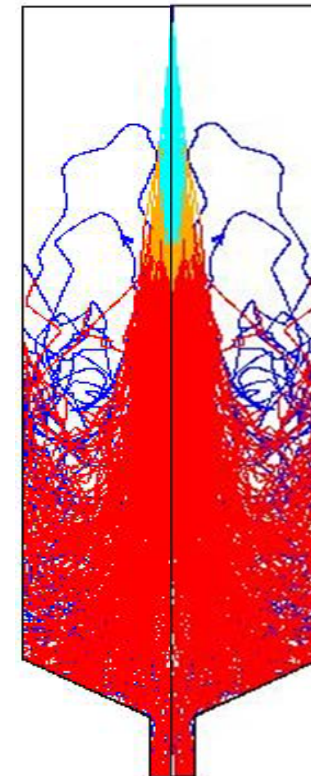
Zerstäubung

Verdampfung

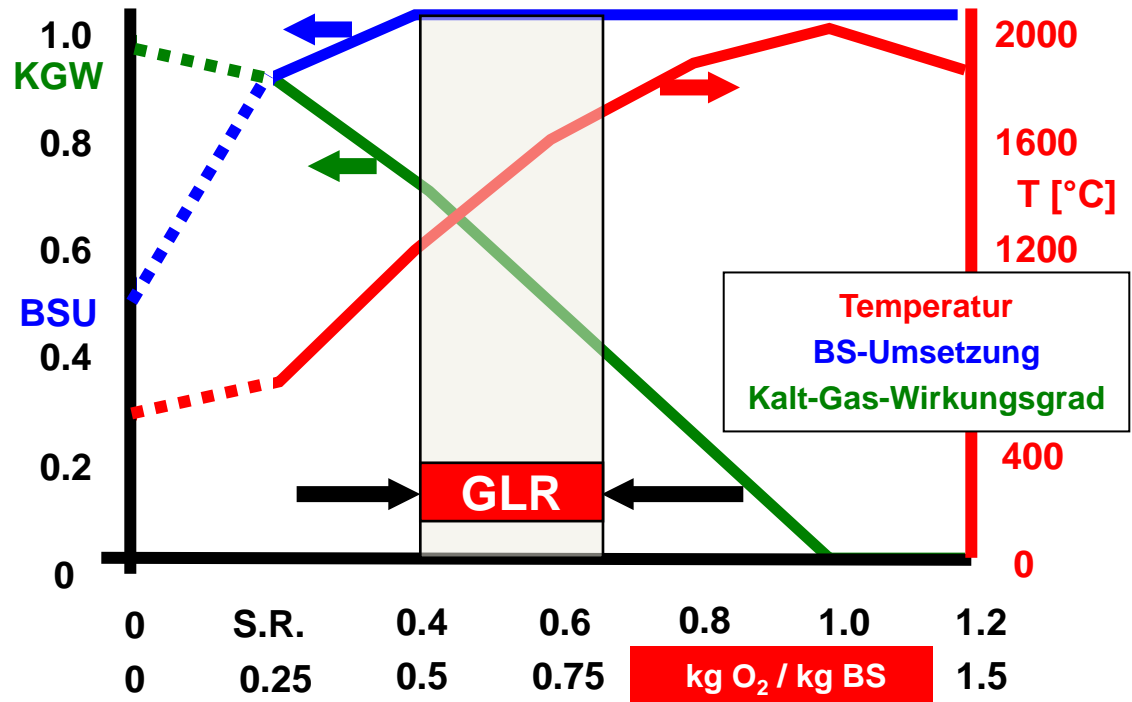
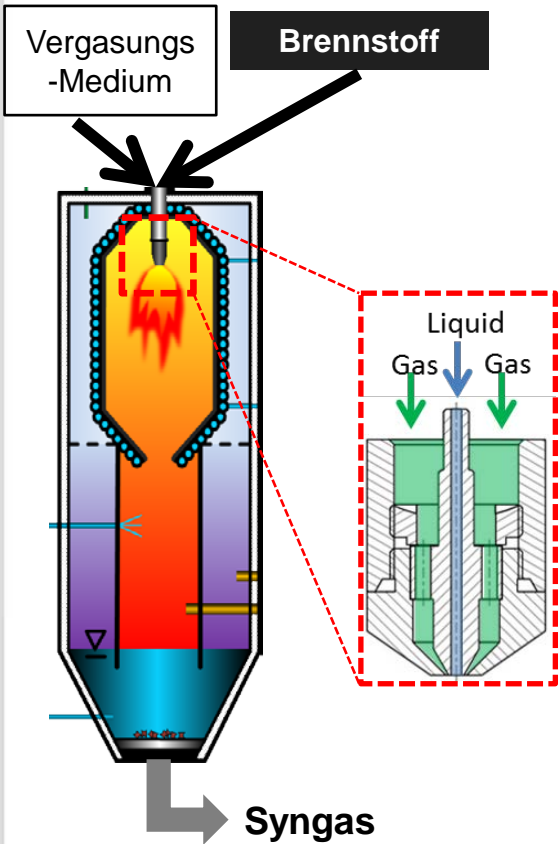
Partikelauflheizung

Vergasungsreaktionen

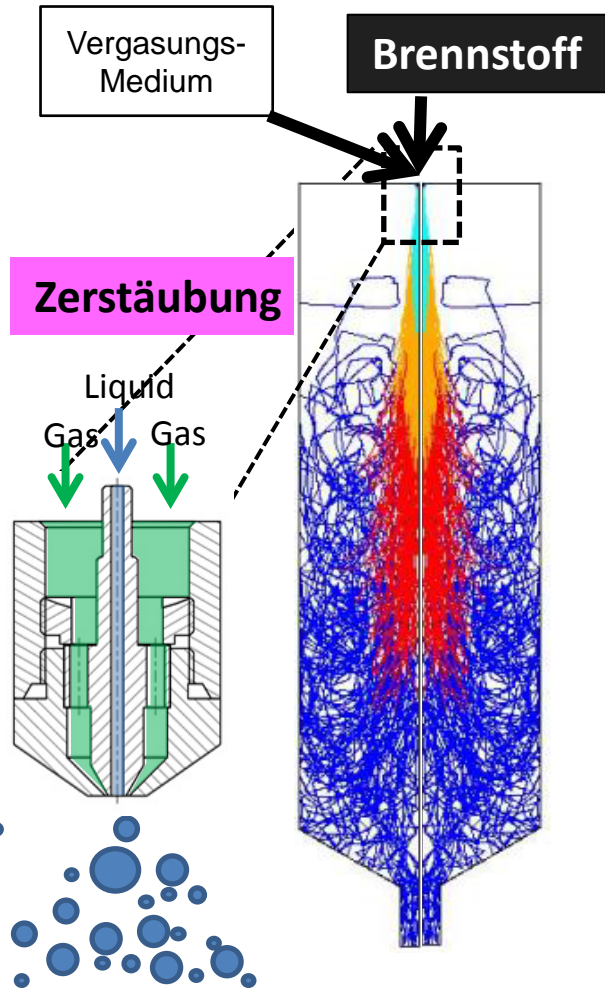
Inertmaterial (Asche, Schlacke)



# Zerstäubung ↔ Vergasung



$$GLR = \frac{\dot{M}_{Gas}}{\dot{M}_{Liq}} = \frac{\dot{M}_{Oxidizer}}{\dot{M}_{Fuel}} \propto S.R.$$





Experiment

Rheologie

Simulation

**ITC**

T. Jakobs      A. Sanger

**MVM**




L. Jampolski

**EBI**

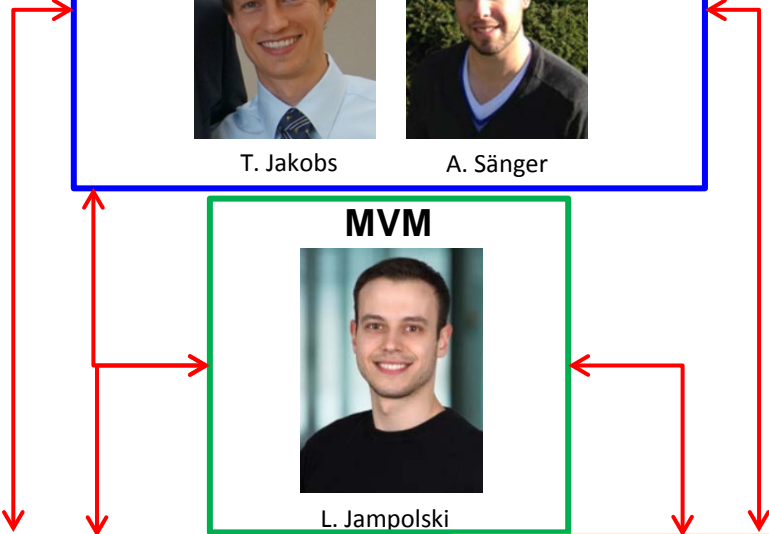


T. Muller

**ITS**



G. Chaussonnet



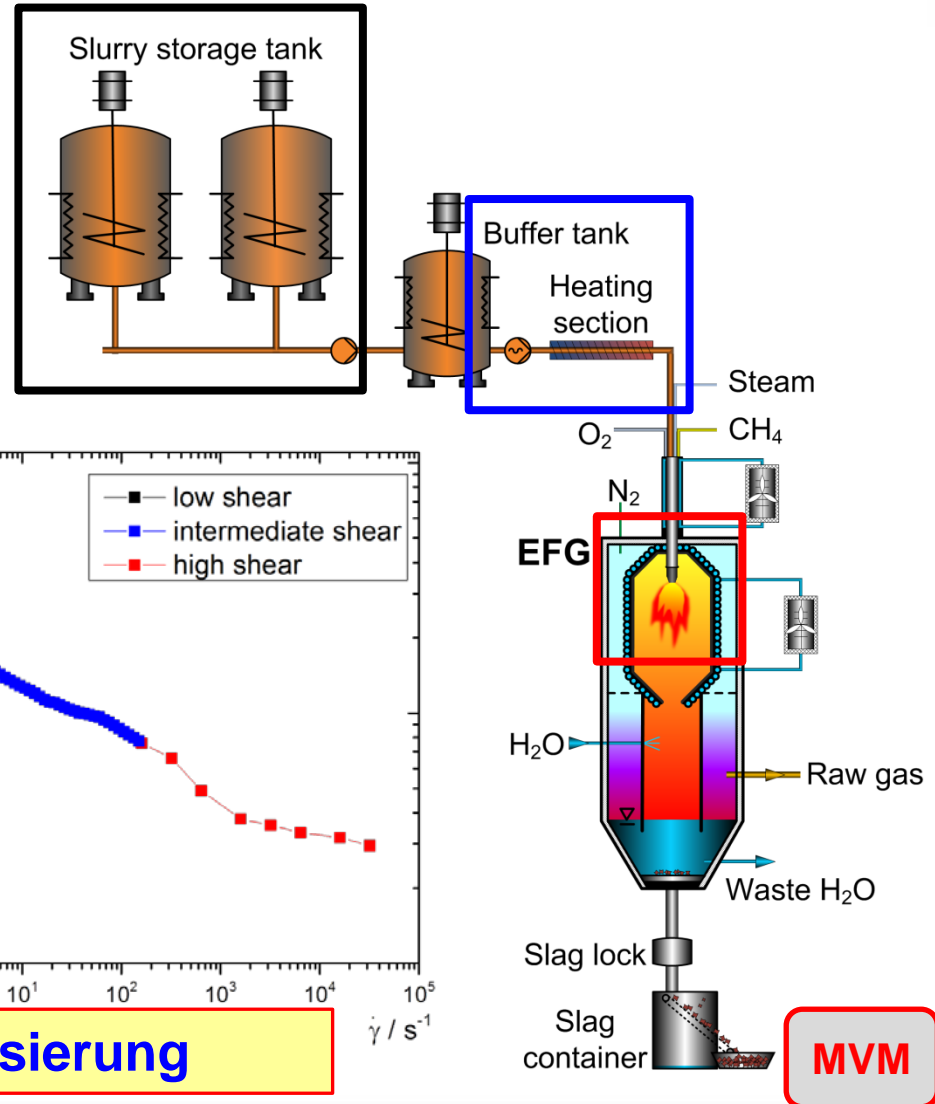
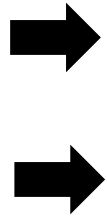
→ Brennerentwicklung & Modellierung der Zerstaubung

# Rheologische Untersuchung biosyncrude

biosyncrude:

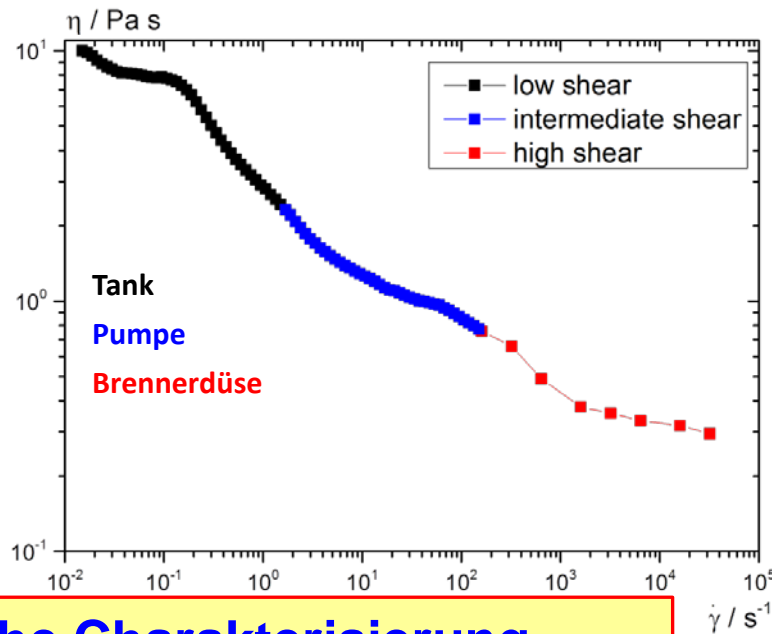


Brennstoff



## Rheologische Eigenschaften:

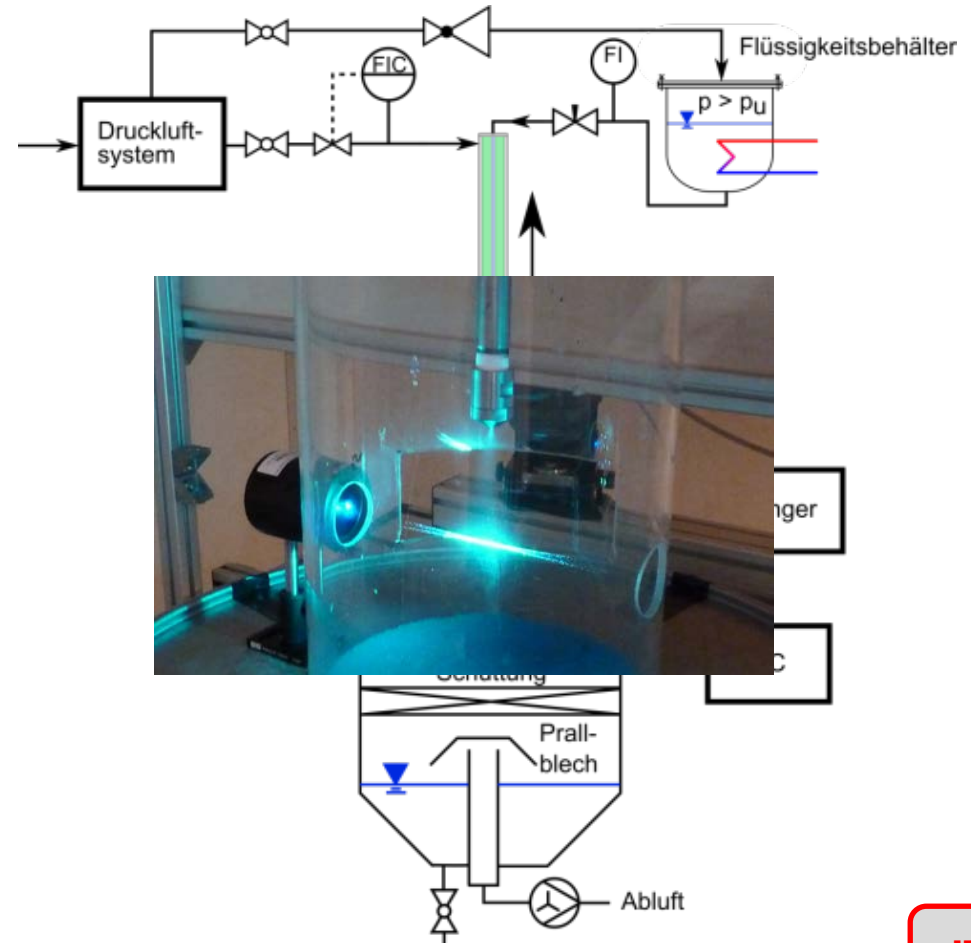
- Fließverhalten
- Viskosität (bis zu 10 Pa·s)



→ Rheologische Charakterisierung

## Technische Daten:

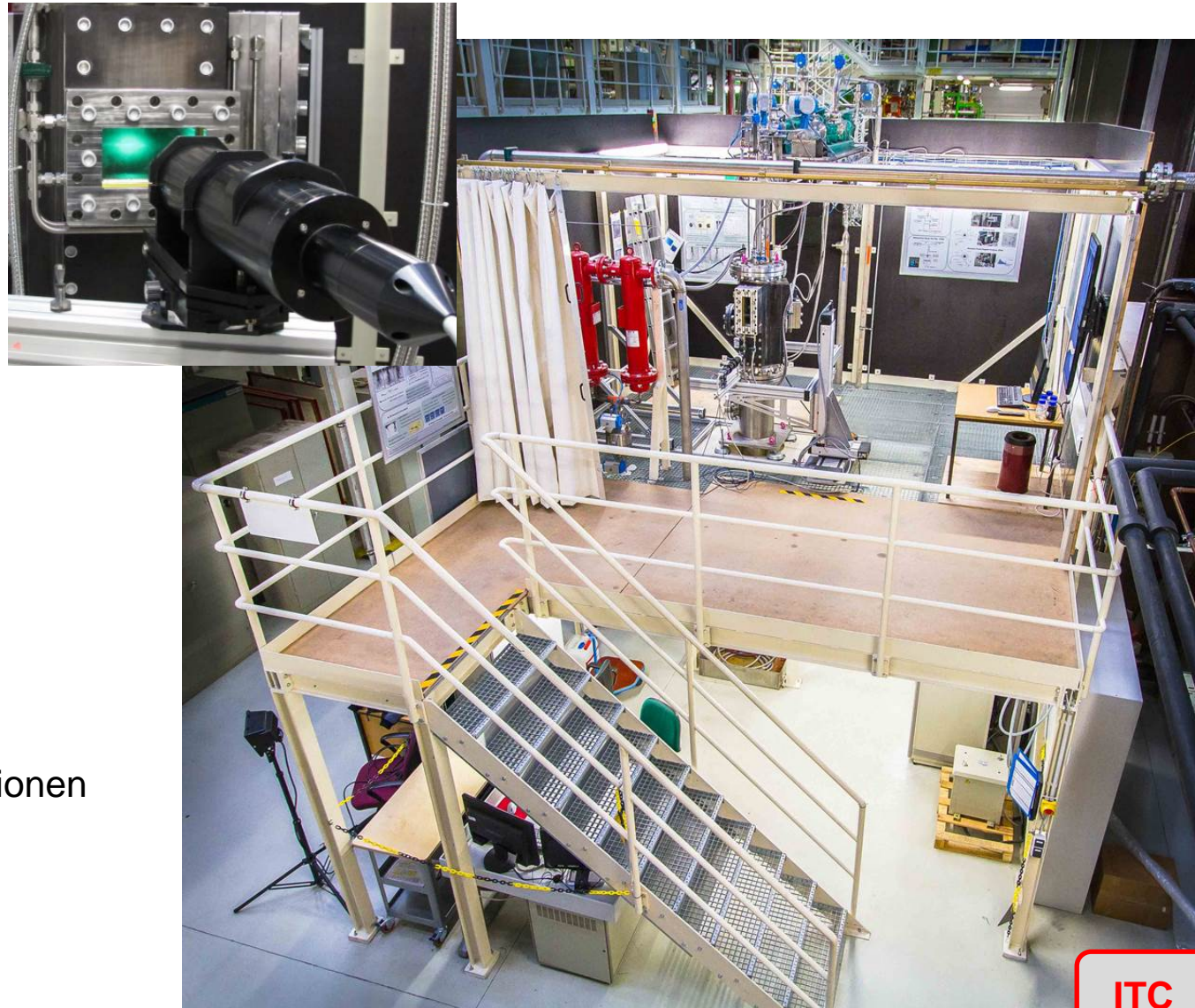
- $p = 1 \text{ bar}_{\text{abs}}$
- $\eta_{\text{liq,max}} = 1000 \text{ mPa s}$
- $T_{\text{liq}} = 10 - 50 \text{ }^\circ\text{C}$
- $\dot{m}_{\text{gas}} = 1 - 20 \text{ kg h}^{-1}$
- $\dot{m}_{\text{liq}} = 1 - 20 \text{ kg h}^{-1}$
- geeignet für Suspensionen
- Verschiedene Düsen





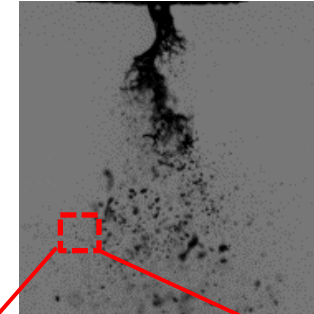
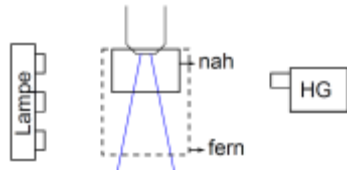
## Technische Daten:

- $p_{\text{reac}} = 1 - 21 \text{ bar}_{\text{abs}}$
- $\eta_{\text{liq,max}} = 1000 \text{ mPa s}$
- $T_{\text{liq}} = 10 - 50 \text{ }^\circ\text{C}$
- $\dot{m}_{\text{gas}} = 1 - 500 \text{ kg h}^{-1}$
- $\dot{m}_{\text{liq}} = 10 - 200 \text{ kg h}^{-1}$
  
- 3 optische Zugänge
- Scheibenreinigung
- geeignet für Suspensionen
- Verschiedene Düsen



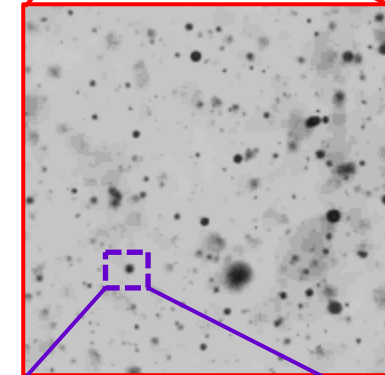
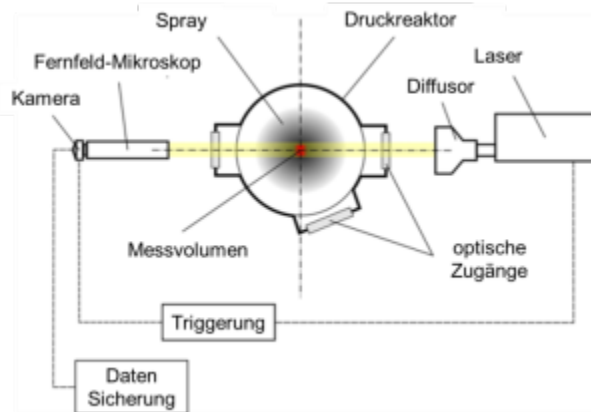
# Eingesetzte Messtechnik

## High Speed Camera



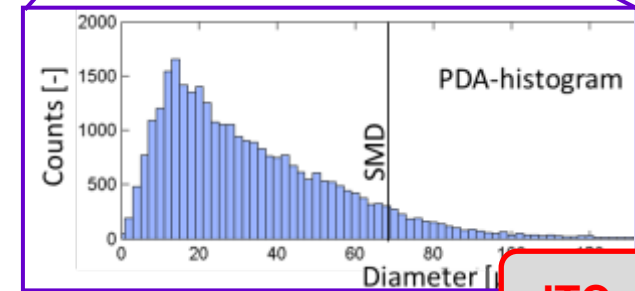
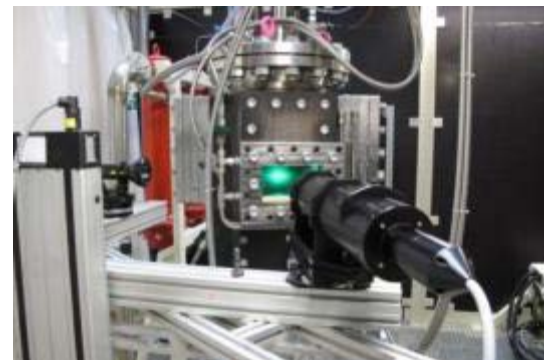
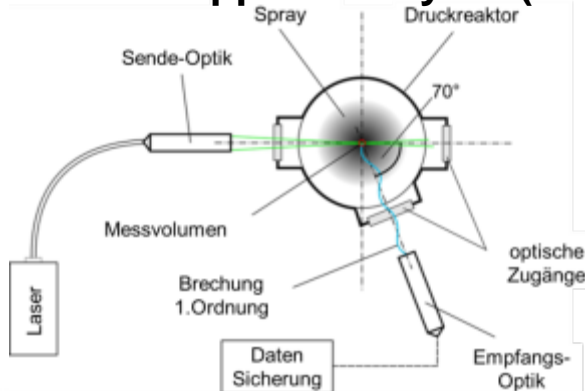
HG-Kamera

## Shadow-Sizer



Fernfeldmikroskop

## Phase-Doppler-Analyzer (PDA / LDA)

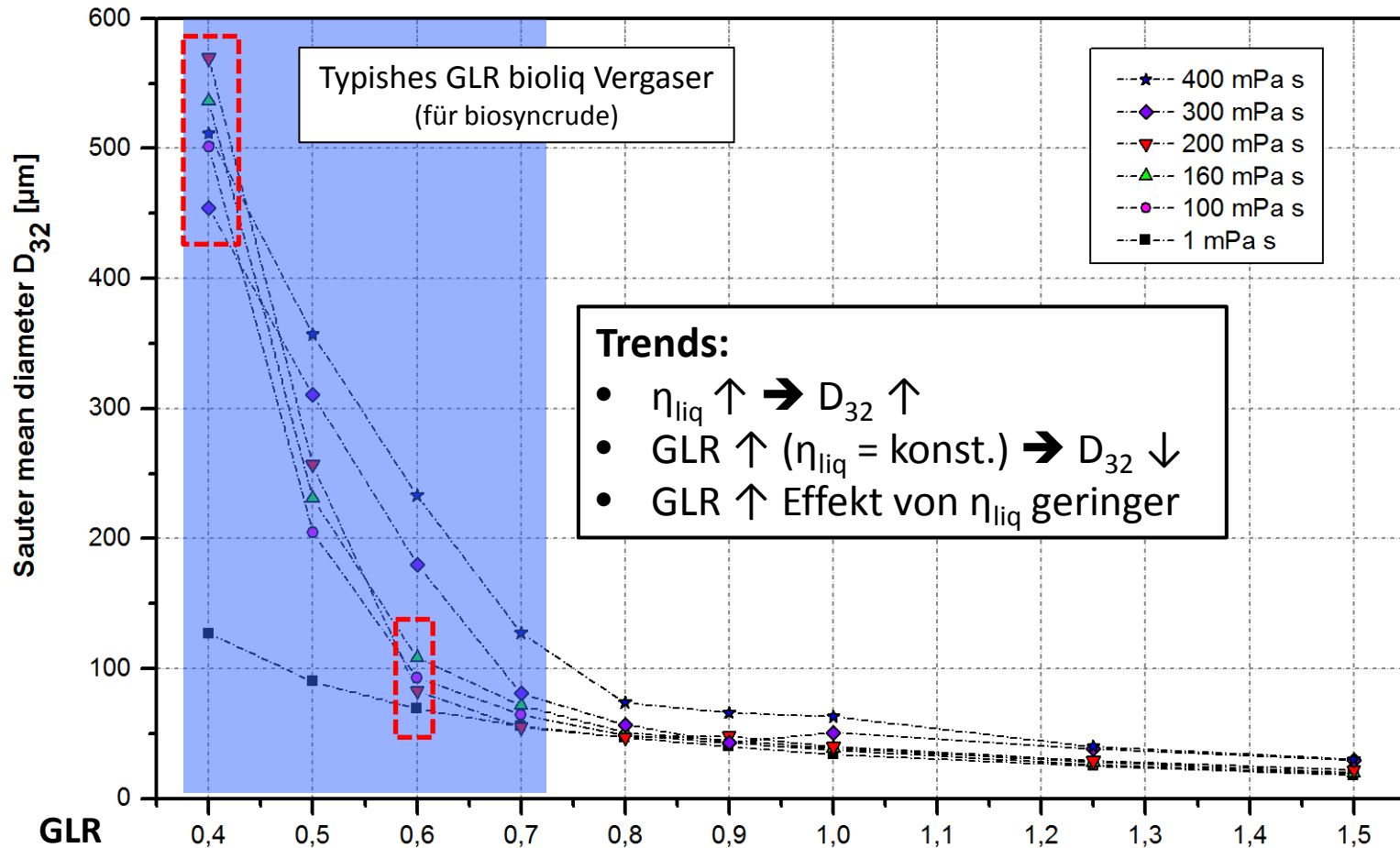


Lokale TGV





# Tropfengröße als Fkt. der Viskosität

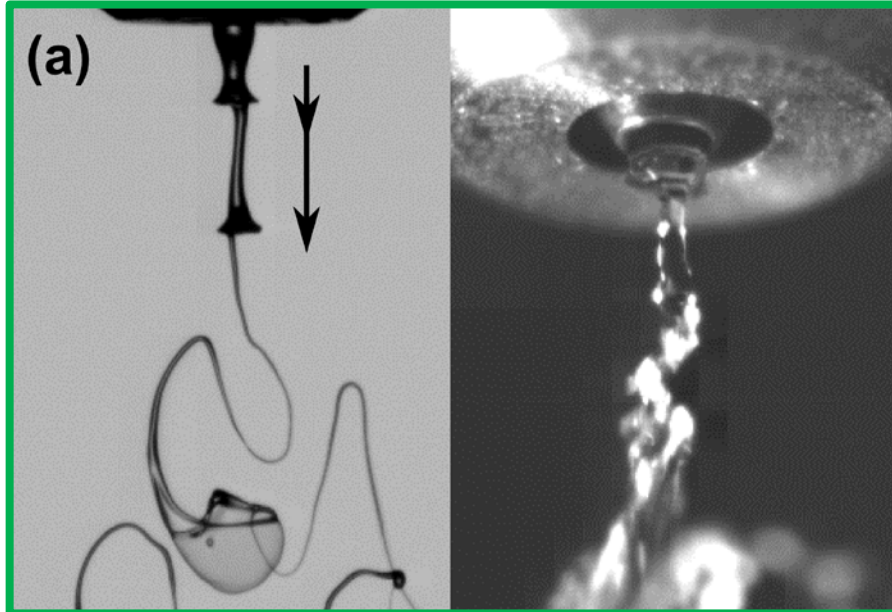


→ Unerwartetes Verhalten der Tropfengröße

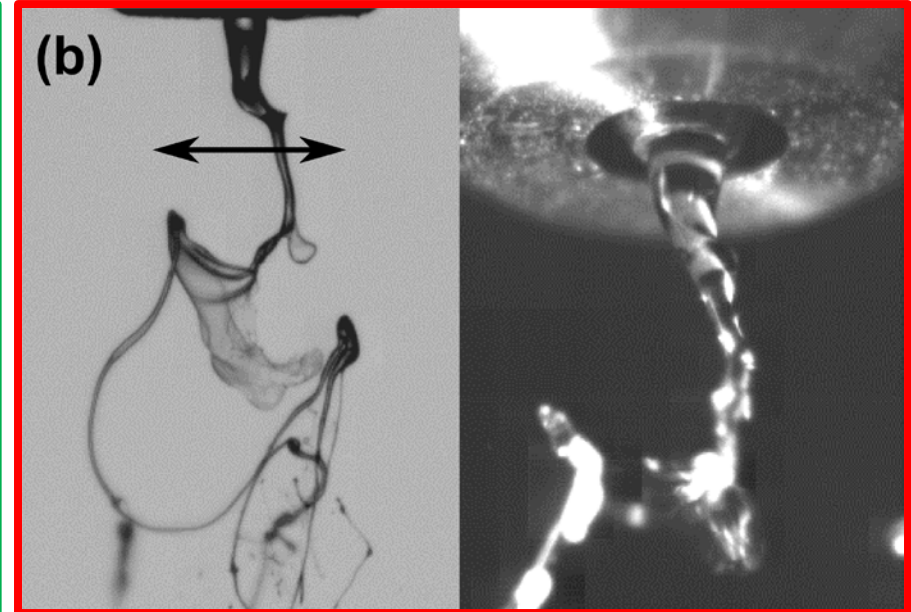
ITC

# Primärinstabilitäten „Pulsating / Flapping“

*Pulsating*



*Flapping*

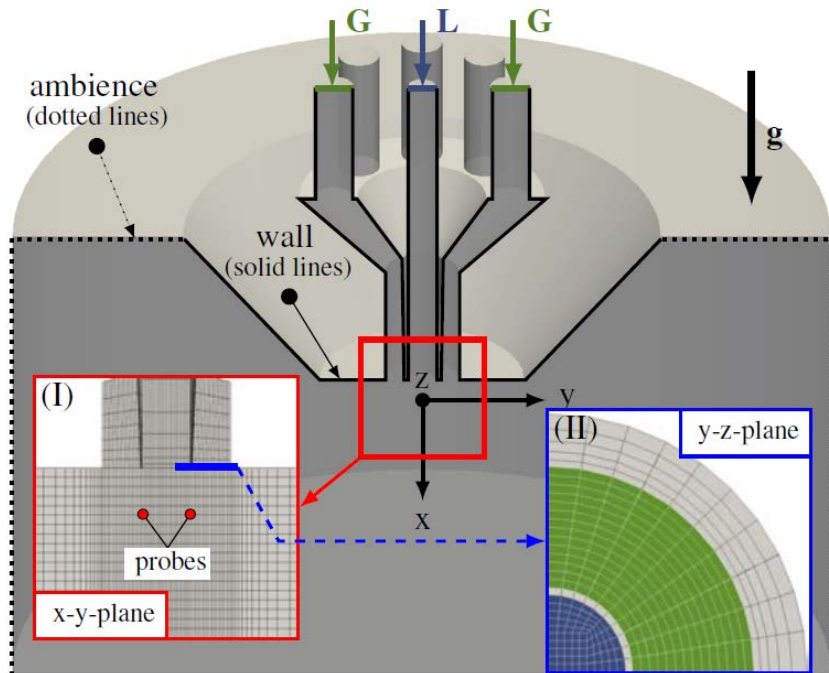


- Hohe aerodynamische Kräfte ( $GLR > 1.0$ ) → *Pulsating mode*
- Geringere aerodynamische Kräfte ( $GLR < 1.0$ ) und  $\eta_{liq} < 200 \text{ mPa}\cdot\text{s}$  → *Pulsating mode*
- Geringere aerodynamische Kräfte ( $GLR < 1.0$ ) und  $\eta_{liq} > 200 \text{ mPa}\cdot\text{s}$  → *Flapping mode*

→ **Flapping effektiver als Pulsating**

ITC

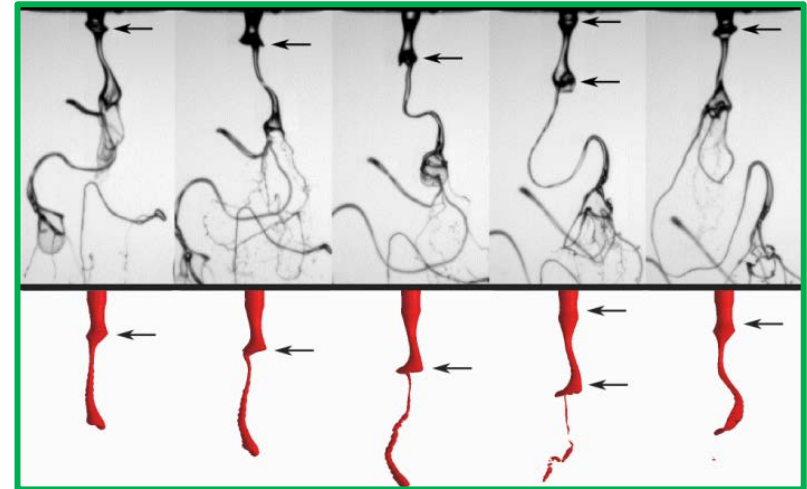
# VoF Modell – Gitter



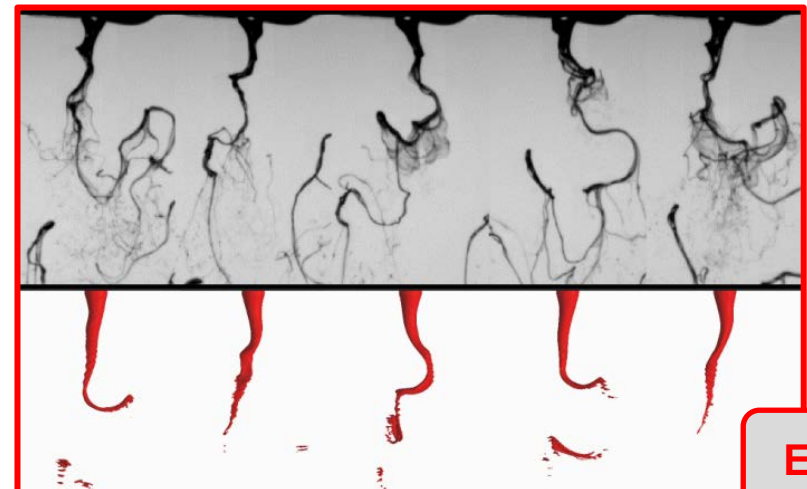
## Gitter:

6.6 Millionen Zellen  
 $50 \times 50 \times 50 \mu\text{m}^3$

## Pulsating

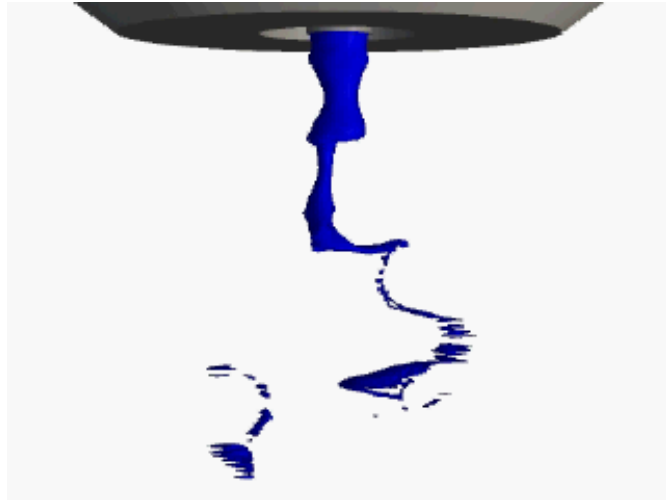


## Flapping



EBI

## Simulation



$$f_{\text{primär}} = 429 \text{ Hz}$$

## Experiment



$$f_{\text{primär}} = 426 \text{ Hz}$$

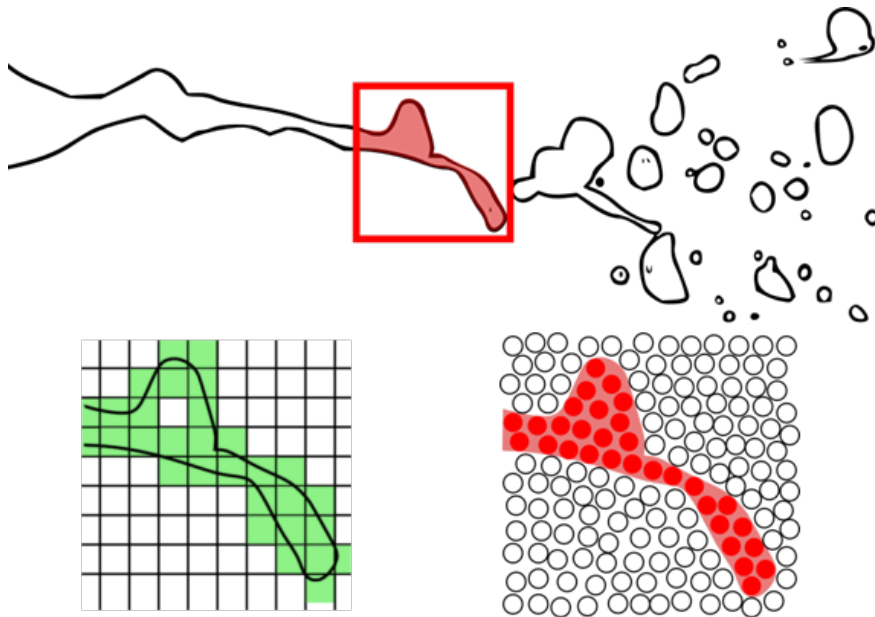
→ Gute Übereinstimmung für alle Betriebspunkte

EBI

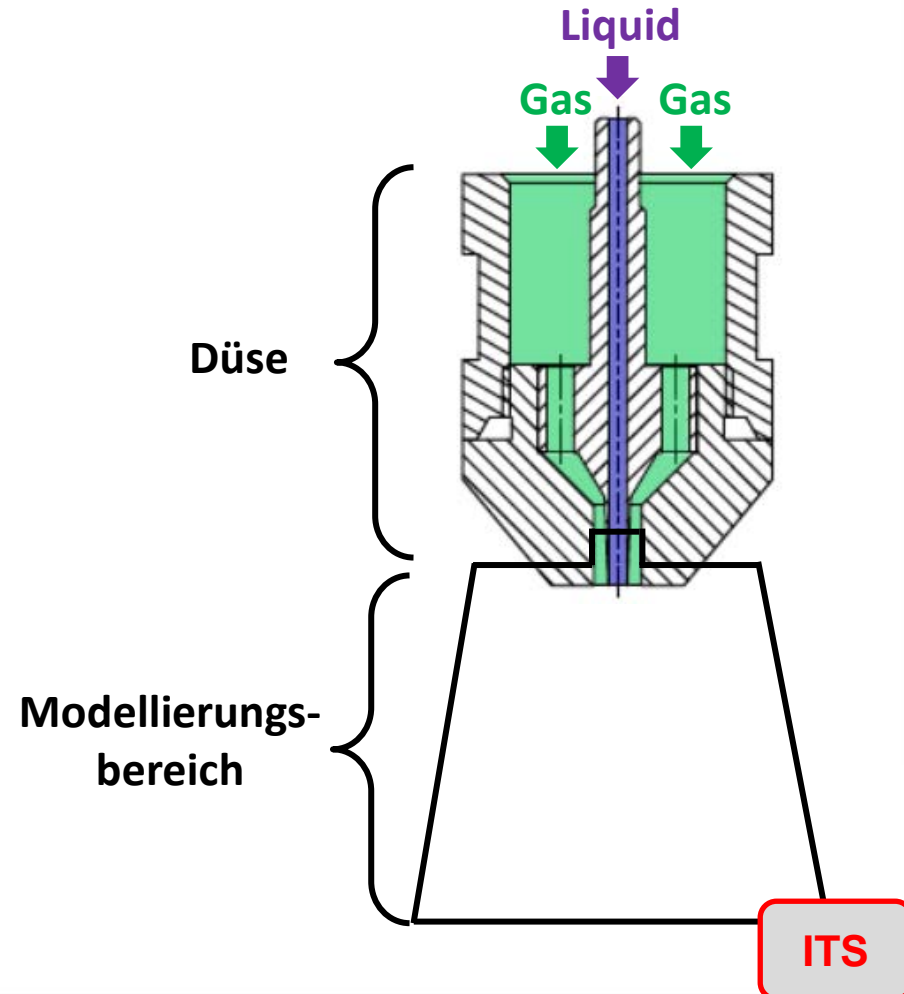


## Vorteil: Mehrphasen / Grenzflächen Handling:

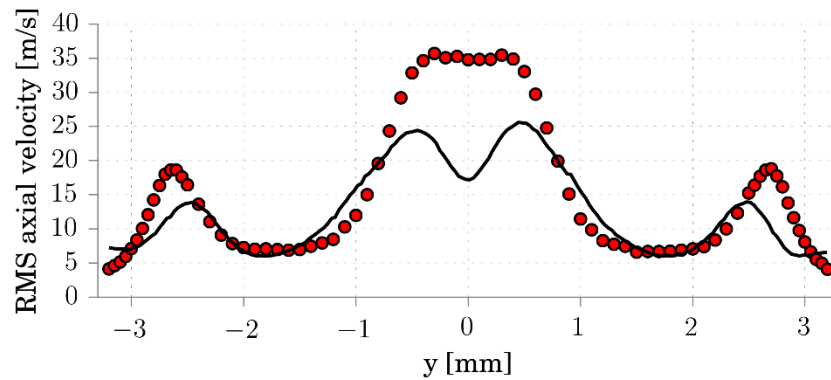
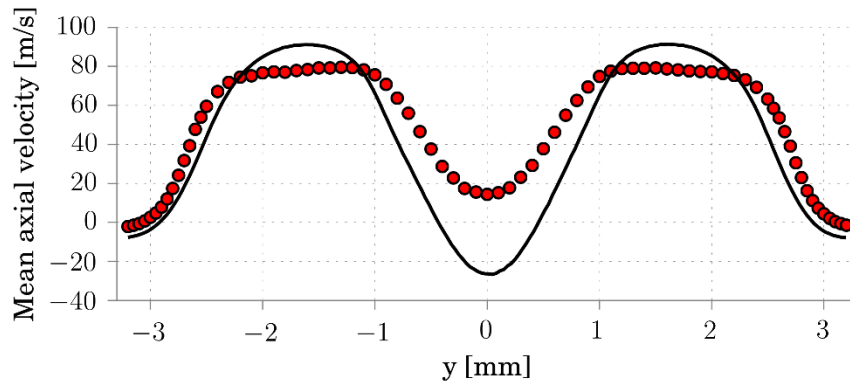
- Kein Gitter nötig
- Grenzfläche automatisch gegeben



## Numerisches Setup



## Simulation Gasströmung



→ Gute Übereinstimmung der Axialgeschwindigkeit

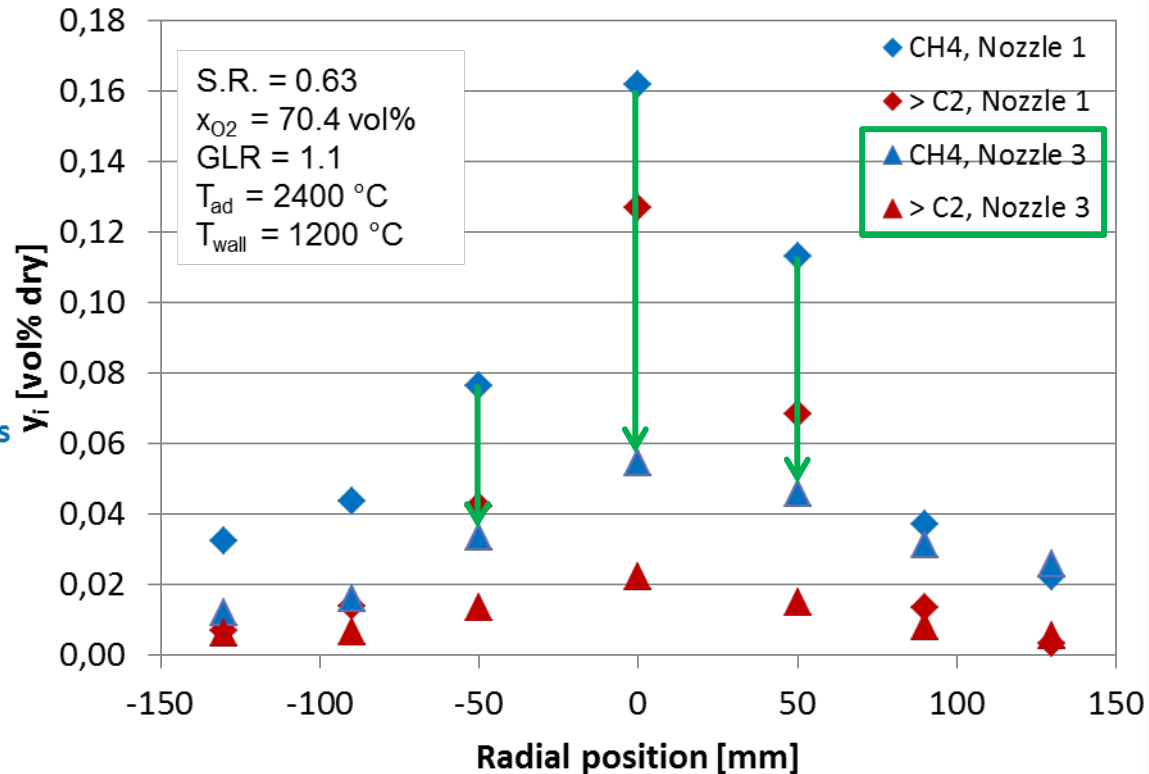
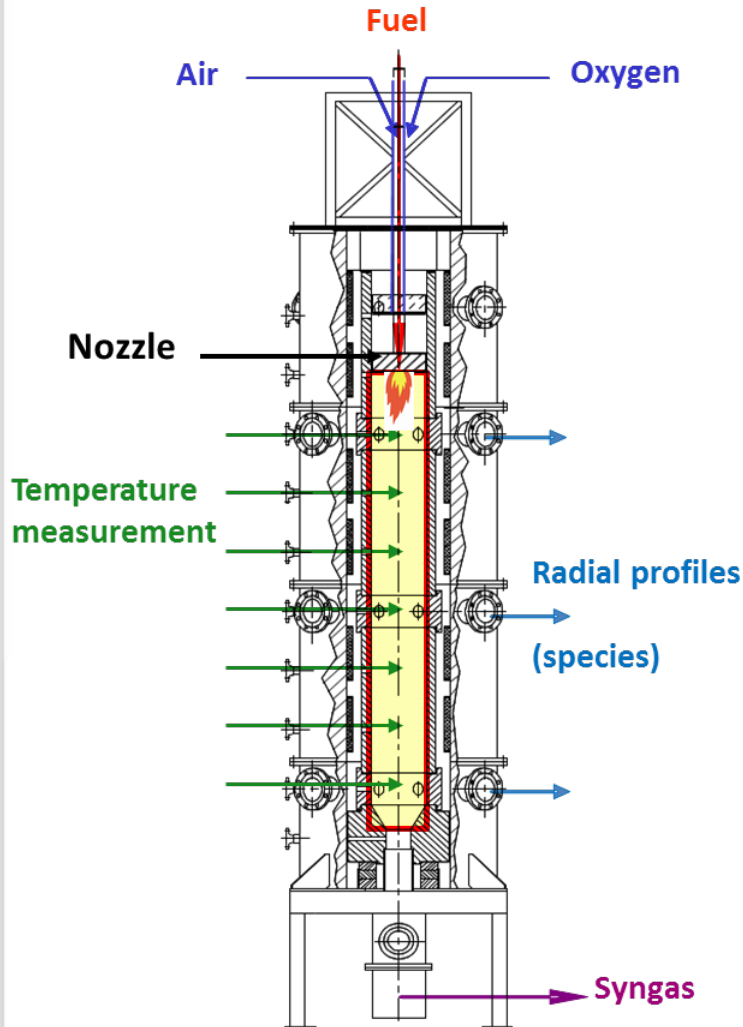
ITS

# Einfluss Druck – Zerstäubung hochviskos

32 P<sub>reac</sub>

ITC

# Einsatz neuer Brennerdüsen im Vergaser



→ Verbesserung der Syngas Qualität durch neue Düse

ITC

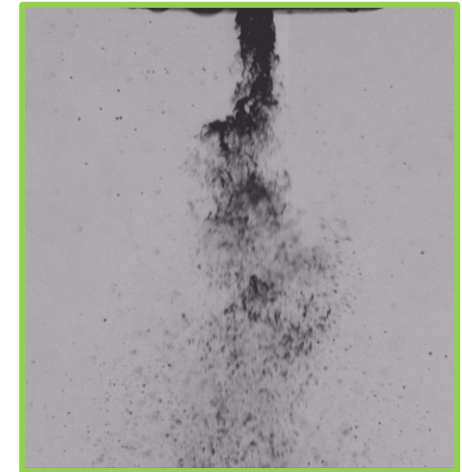
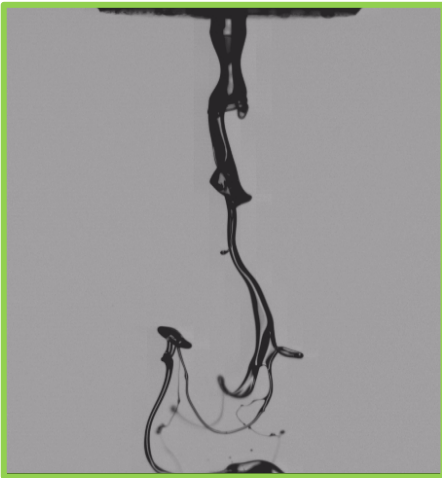


## Zusammenfassung

- Rheologische Charakterisierung biosyncrude
- Zerstäubung hochviskoser Brennstoffe bei 1 – 21 bar<sub>abs</sub>
- Numerische Simulation des Strahlzerfalls (VoF / SPH)
- Einsatz Brennerdüsen im Vergaser → Syngas-Qualität gesteigert

## Ausblick

- Optimale Sprayqualität für ein breites Brennstoffspektrum



# Danke!

