

# Thoughts of an Isovoluminetric Thermal Desorption Experiment

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IKIT/INR/MET (Maschinenbau)

- 1.: Motivation
- 2.: Description of setup and simplification
- 3.: Structure of Differential Equations
- 4.: Analytical outlook of solution
- 5.: Outlook to Open Foam Results
- 6.: Results of numerical Solution
- 7.: Isovoluminetric thermal Desorption Experiment as automotive application

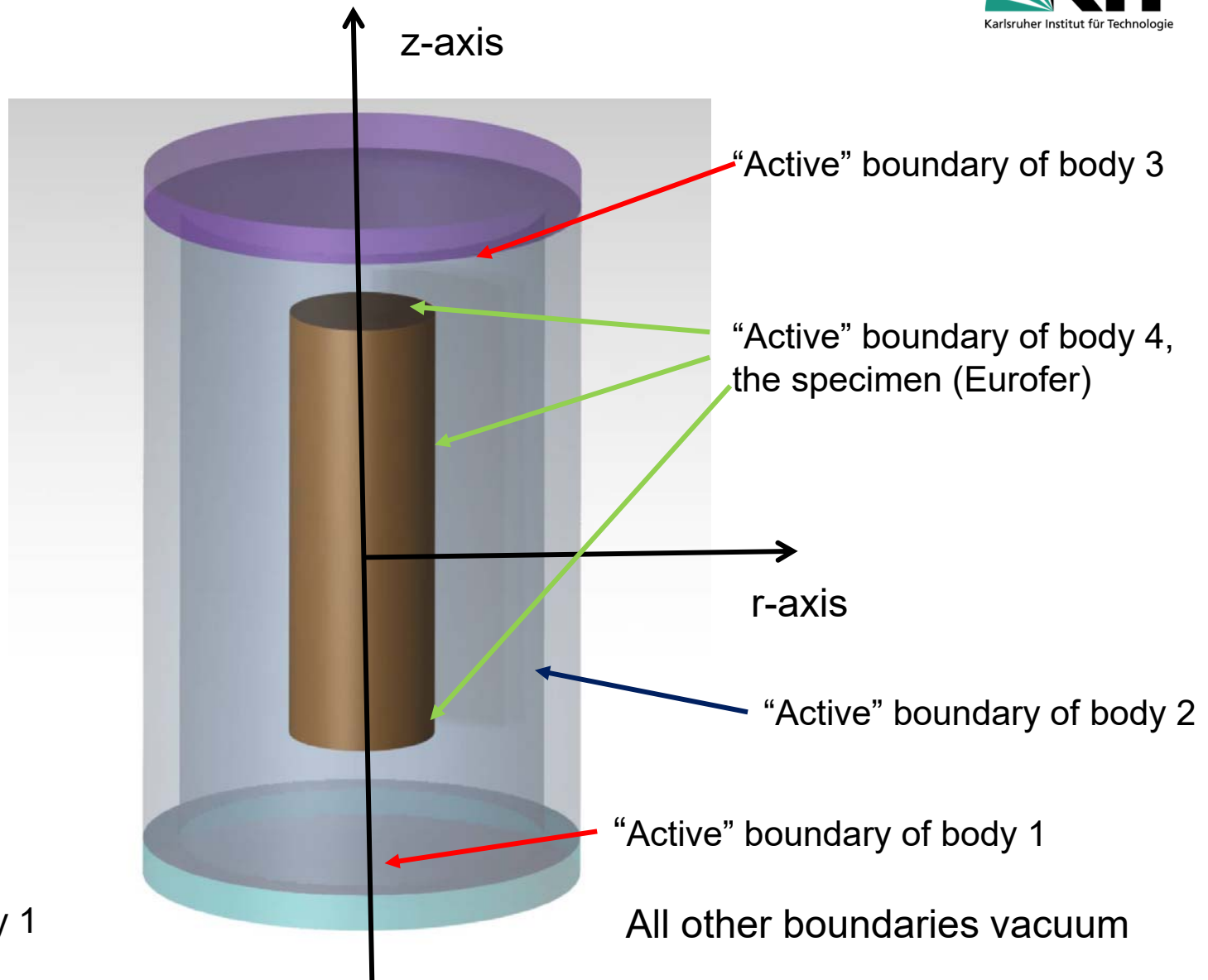
# 1.: Descripton of setup of an Isovolumetric Thermal Desorption Experiment

Upper cup, body 3

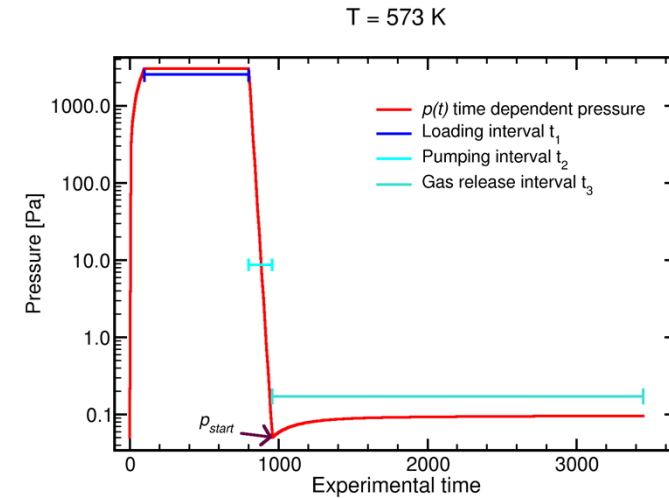
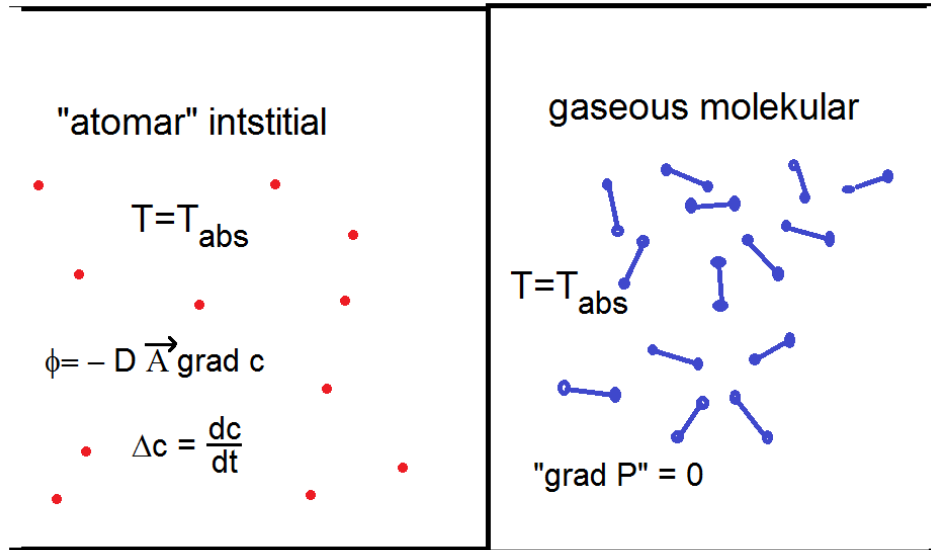
Specimen, cylinder, body 4

Hollow cylinder, body 2

Lower cup, body 1



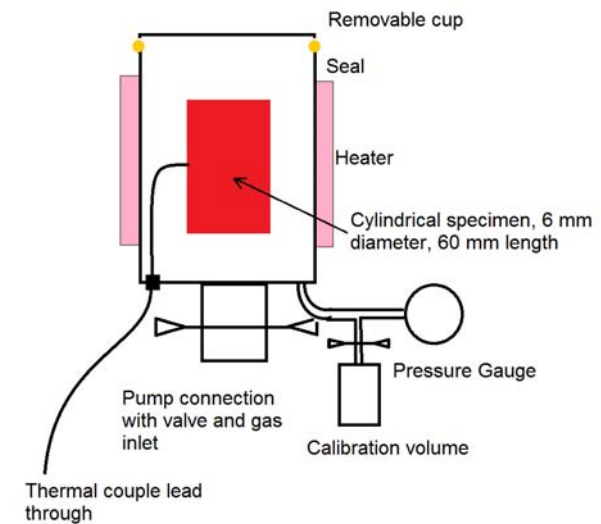
## 2.: Physical descripton



“Velocity” of mass transfer by diffusion constant D

Ratio of densities given by Sieverts' law  
(phase equilibrium)

$$c = k_s \sqrt{p_r}$$



# Simple analytical Solutions

Without re-diffusion, complete outgasing:

$$p_r \underset{t \rightarrow \infty}{=} \underbrace{p_{end}}_{\substack{\text{switching off} \\ \text{pump}}} + \frac{V_{sa} k_{s,sa} \sqrt{p_{load}} R T}{\left( \underbrace{V_c}_{\substack{\text{chamber}}} - \underbrace{V_{sa}}_{\substack{\text{sample}}} \right)^2}$$

With phase equilibrium, mass conservation (number of “hydrogens” in atomic interstitial and molecular gaseous state constant) and non interacting confinement condition:

$$0 = \frac{2(V_c - V_{sa})}{R T} (\sqrt{p_r})^2 + V_s k_{s,sa} \underbrace{\sqrt{p_r}}_{= "x"} - \left( V_s k_{s,sa} \sqrt{p_{end}} + \frac{2 p_{end} (V_c - V_{sa})}{R T} \right)$$

$$p_r \underset{t \rightarrow \infty}{=} \left( \frac{-1 \underset{\substack{\text{neg. sqrt}}}{+} \sqrt{1 + \left( \frac{8(V_c - V_{sa}) \sqrt{p_{load}}}{R T V_s k_{s,sa}} + \frac{16 p_{end} (V_c - V_{sa})^2}{(R T V_{sa} k_{s,sa})^2} \right)}}{\left( \frac{V_{sa} k_{s,sa} R T}{4 (V_c - V_{sa})} \right)^{-1}} \right)^2$$

### 3.: Structure of differential equations:

$$\frac{\partial c}{\partial t} = D_{sa} \Delta c \quad \frac{\partial d}{\partial t} = D_{cu} \Delta d(i), i = 1, 2, 3$$

$$\frac{\partial^2}{\partial r^2} + \frac{1}{r} \frac{\partial}{\partial r} + \frac{\partial^2}{\partial z^2}$$

$$c(0 \leq r \leq r_s, z = \pm z_s, \forall t) = k_{s,sa} \sqrt{p(t)}$$

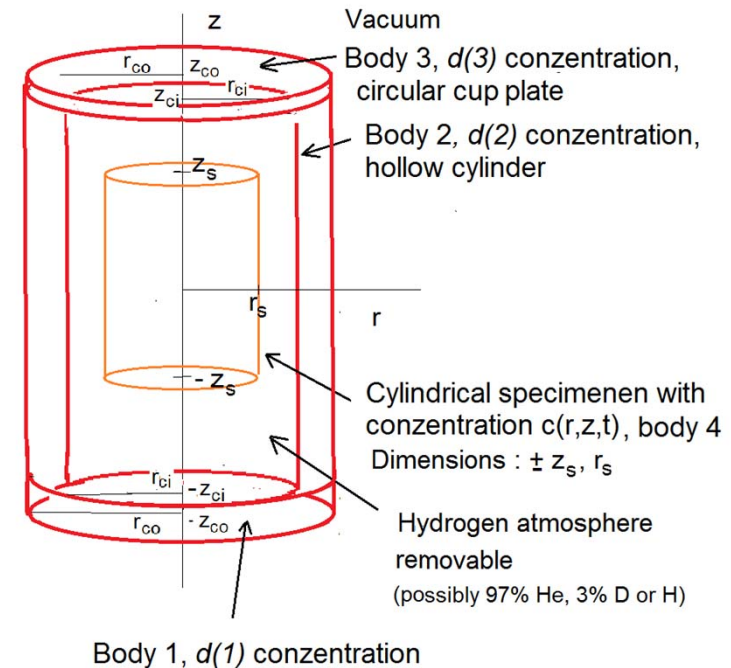
$$c(r = r_s, |z| \leq z_s, \forall t) = k_{s,sa} \sqrt{p(t)}$$

$$d(1)(r \leq r_{co}, z = -z_{ci}, \forall t) = k_{s,cu} \sqrt{p(t)}$$

$$d(2)(r = r_{ci}, -z_{ci} \leq z \leq z_{ci}, \forall t) = k_{s,cu} \sqrt{p(t)}$$

$$d(2)(r_{ci} \leq r \leq r_{co}, z = \pm z_{ci}, \forall t) = k_{s,cu} \sqrt{p(t)}$$

$$d(3)(r \leq r_{co}, z = z_{ci}, \forall t) = k_{s,cu} \sqrt{p(t)}$$



### 3. Structure of differential equations

$$\frac{dm}{dt} = - 2 \pi D_{sa} \int_0^{r_s} \underbrace{2}_{\text{symmetric}} r \frac{\partial}{\partial z} c(r, z = z_s, t) dr$$

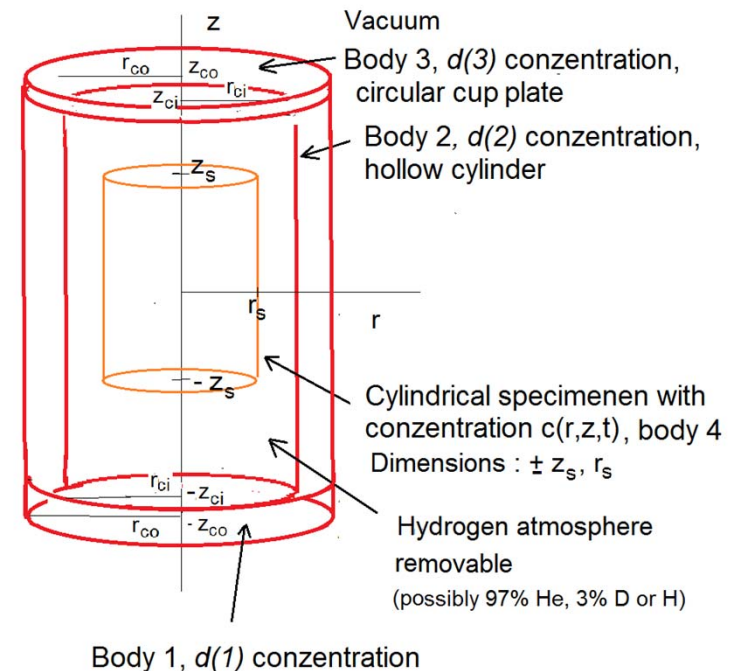
$$- \underbrace{2 \pi r_s D_{sa} \int_{-z_s}^{z_s} \frac{\partial}{\partial r} c(r = r_s, z, t) dz}_{\text{superficies surface of specimen}}$$

$$- \underbrace{2 \pi D_{cu} \int_0^{r_{co}} r \frac{\partial}{\partial z} d(1)(r, z = -z_{ci}, t) dr}_{\text{circular aerea of body 1}}$$

$$- 2 \pi r_{ci} D_{cu} \int_{-z_{ci}}^{z_{ci}} \frac{\partial}{\partial r} d(2)(r = r_{ci}, z, t) dz$$

*superficies surface of body 2*

$$- \underbrace{2 \pi D_{cu} \int_0^{r_{co}} r \frac{\partial}{\partial z} d(3)(r, z = z_{ci}, t) dr}_{\text{circular area of body3}}$$



$$p(t) = p_{start} + \frac{k_v}{RT_{abs}/V_{gas}} \int_{t_1+t_2}^t \underbrace{0.5}_{\text{gaseous} \leftrightarrow \text{interstitial}} \frac{dm}{dt} dt$$

## 4. Outlook to analytical solution

Die Lösung für die Diffusionsgleichung mit Zylinderkoordinaten ( $\varphi$ -unabhängig)

$$\frac{dc}{dt} = D_{sa} \left\{ \frac{\partial^2 c}{\partial r^2} + \frac{1}{r} \frac{\partial c}{\partial r} + \frac{\partial^2 c}{\partial z^2} \right\}$$

mit Randbedingung  $K_{s,sa} \sqrt{p}$  (Konstante) für

$$r = r_s, \quad |z| \leq z_s$$

und

$$0 \leq r \leq r_s, \quad z = \pm z_s$$

ist

$$c(r, z, t) = \sum_{k=1}^{\infty} \sum_{n=0}^{\infty} B_{kn} e^{-\mu_{kn} t} \cos\left(\frac{n\pi z}{2z_s}\right) J_0\left(\sqrt{\frac{\mu_{kn}}{D_{sa}} - \left(\frac{n\pi}{2z_s}\right)^2} r\right) + K_{s,sa} \sqrt{p},$$

wobei

$$B_{kn} = \frac{\int_{-z_s}^{z_s} \int_0^{r_s} (u(r, z, 0) - K_{s,sa} \sqrt{p}) \cos\left(\frac{n\pi z}{2z_s}\right) J_0\left(\sqrt{\frac{\mu_{kn}}{D_{sa}} - \left(\frac{n\pi}{2z_s}\right)^2} r\right) r dr dz}{\int_{-z_s}^{z_s} \int_0^{r_s} \cos^2\left(\frac{n\pi z}{2z_s}\right) J_0\left(\sqrt{\frac{\mu_{kn}}{D_{sa}} - \left(\frac{n\pi}{2z_s}\right)^2} r\right)^2 r dr dz}$$

und

$$\mu_{kn} = D_{sa} \left\{ \left(\frac{\alpha_k}{r_s}\right)^2 + \left(\frac{n\pi}{2z_s}\right)^2 \right\}$$

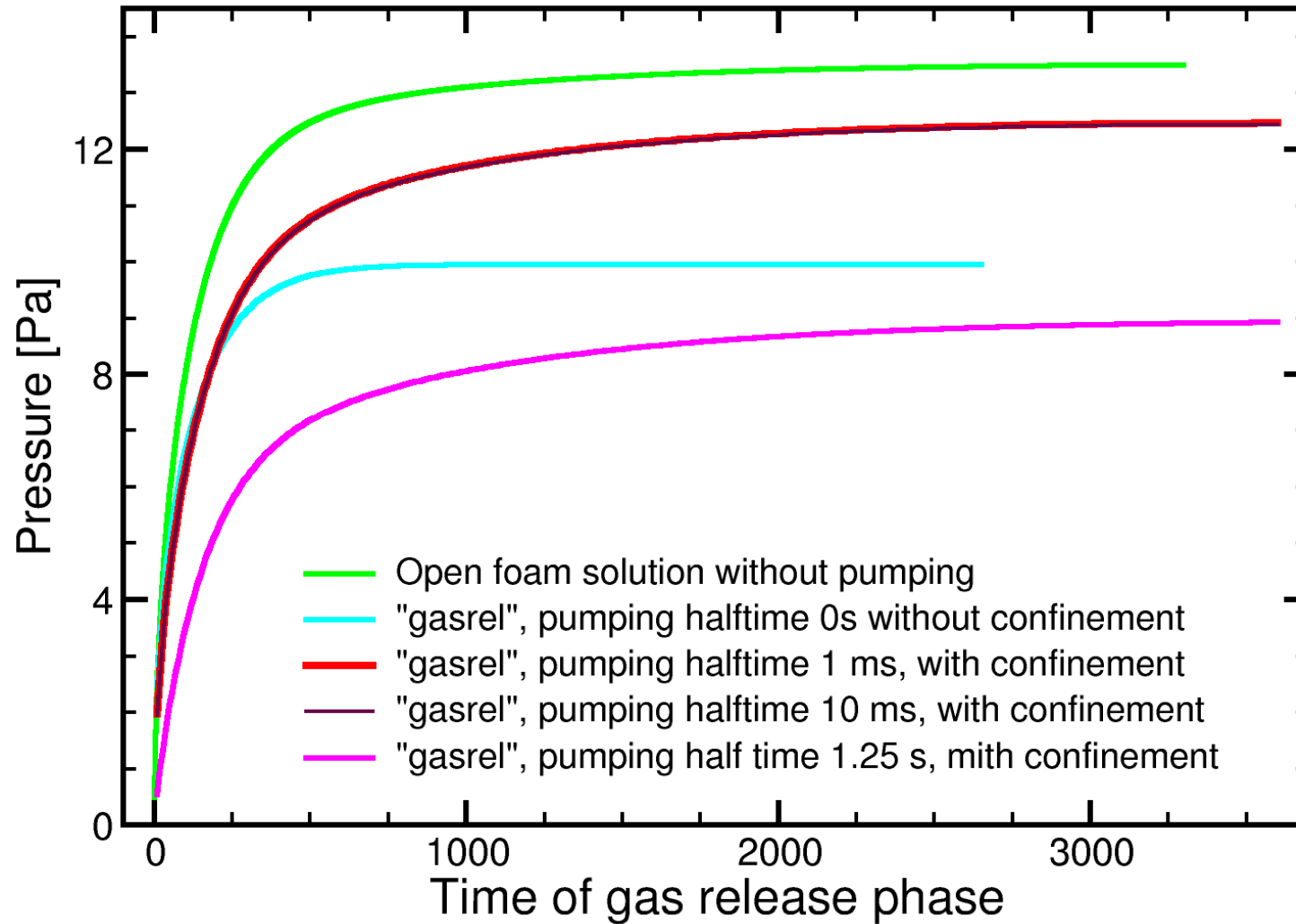
mit  $\alpha_k$ :  $k$ -te Nullstelle von Besselfunktion  $J_0$ .

Eine Symmetrie für  $z$ -Achse wurde vorausgesetzt.

Um Konstante  $B_{kn}$  zu berechnen, muss  $u(r, z, 0)$  durch eine gegebene Funktion (Anfangsbedingung) ersetzt werden.

# 5. Outlook to open foam results

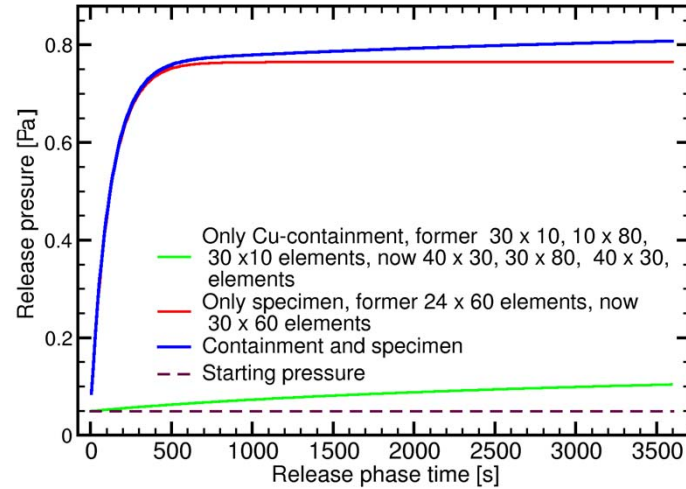
"gasrel" calculation with 6400 specimen element and 1800 elements  
14 halftimes reaching endpresure (0.1 Pa)





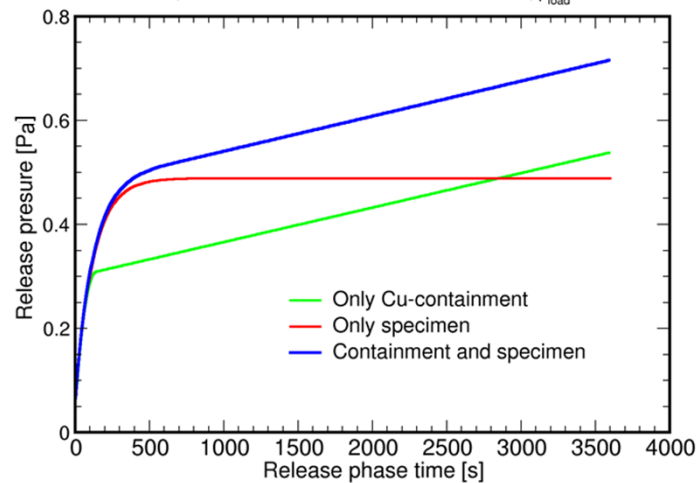
## 6.: Results of numerical solution

T=773 K, Cu containment with Optifer specimen, 13. 5.  
 chamber dimension 80 mm to 40 mm diameter,  $p_{load} = 3 \cdot 10^3$  Pa, improved gradient calculation



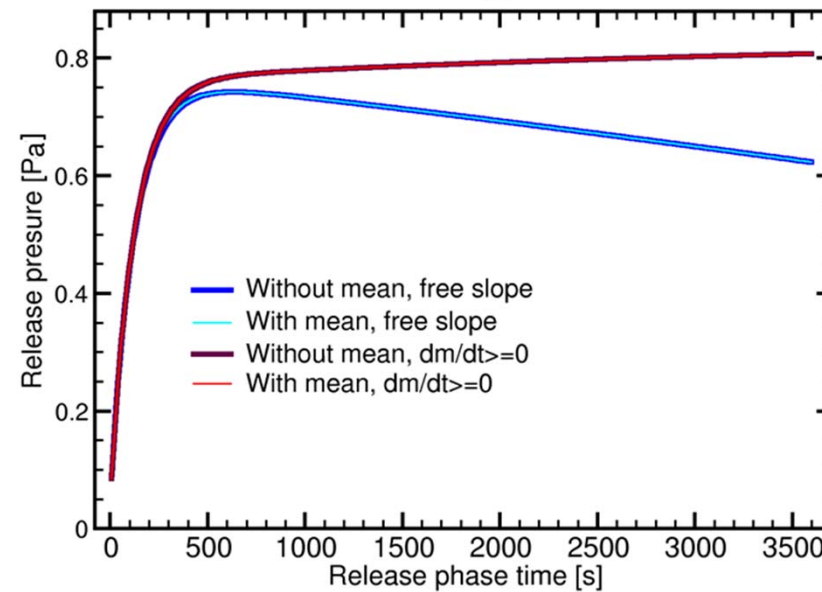
## Simple numerical gradient calculation

T=773 K, Cu containment with Optifer specimen  
 12. 5. 2019, chamber dimension 80 mm to 40 mm diameter,  $p_{load} = 3 \cdot 10^3$  Pa



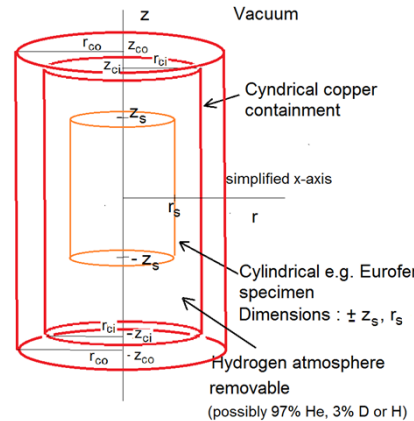
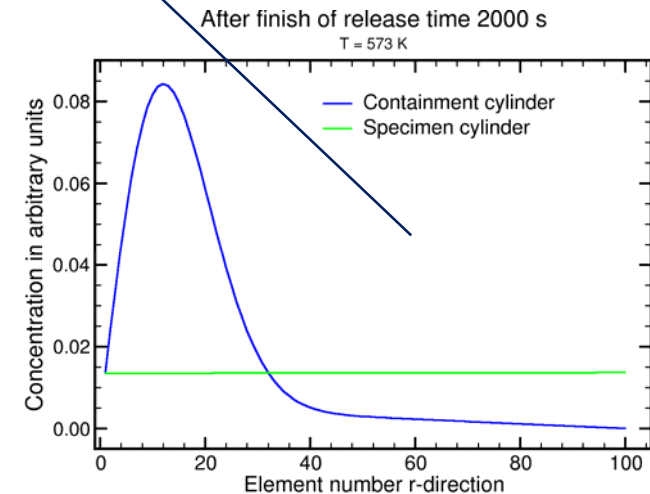
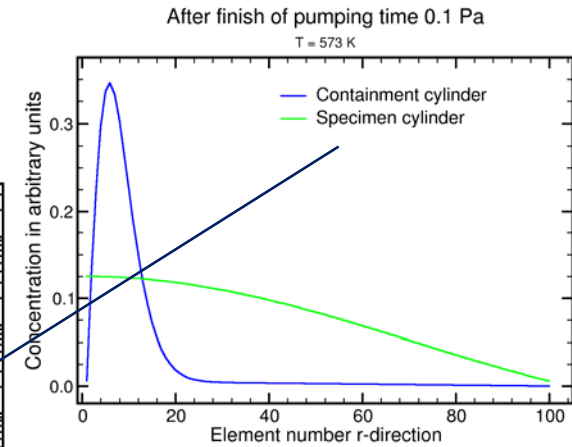
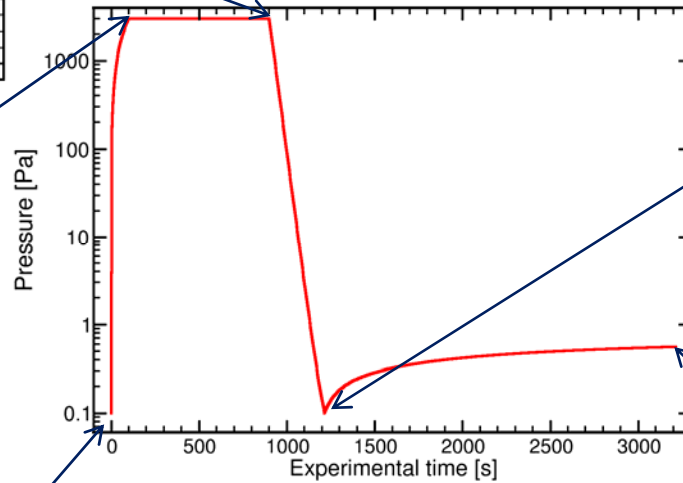
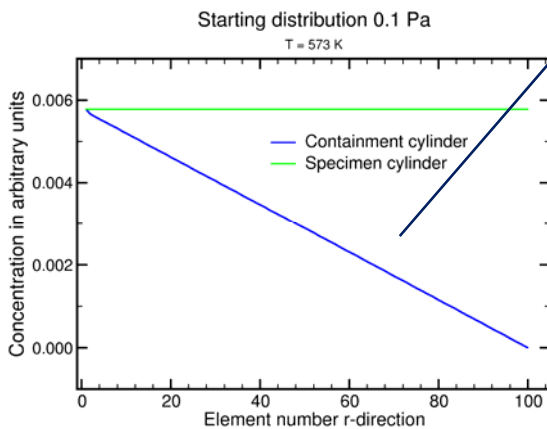
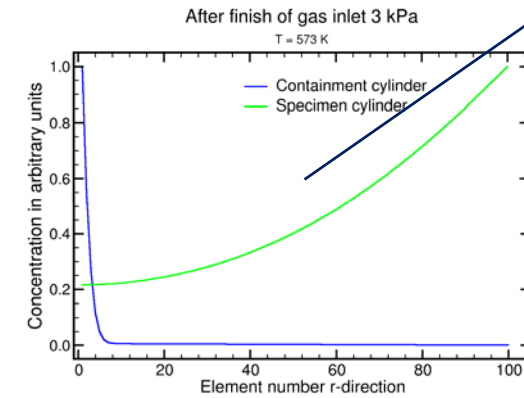
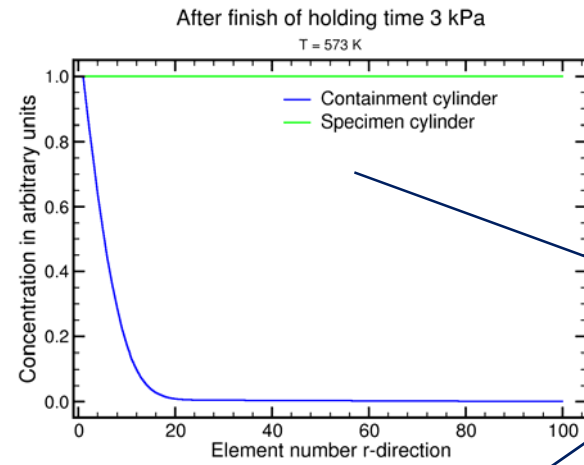
## Numerical artefacts

Development, T=773 K, Cu cont. with Optifer specimen  
 chamber dimension 80 mm to 40 mm diameter,  $p_{load} = 3 \cdot 10^3$  Pa, improved gradient calculation

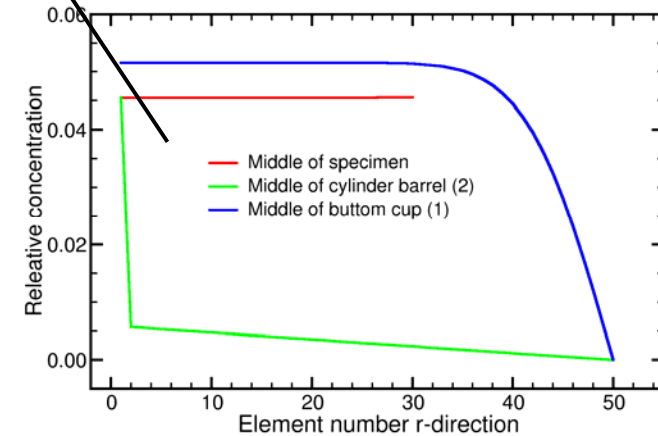
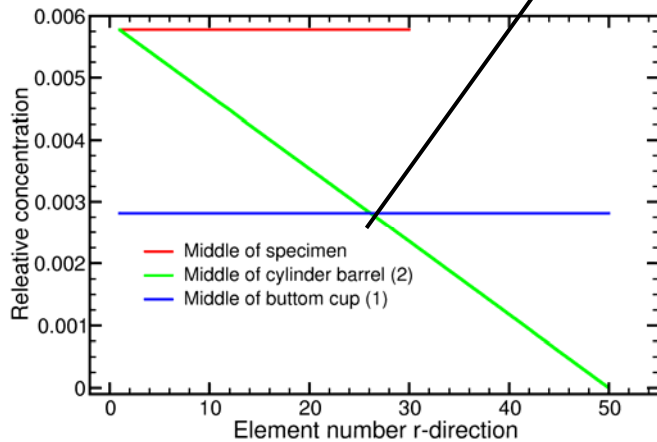
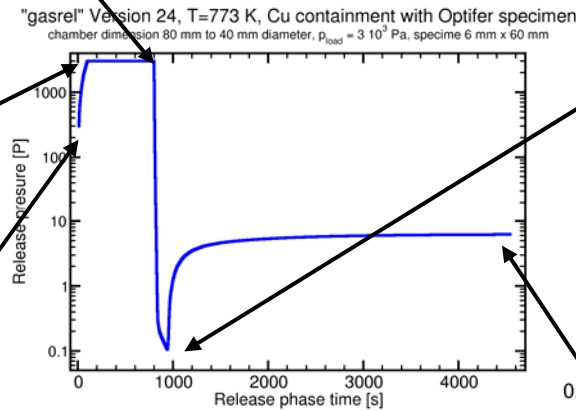
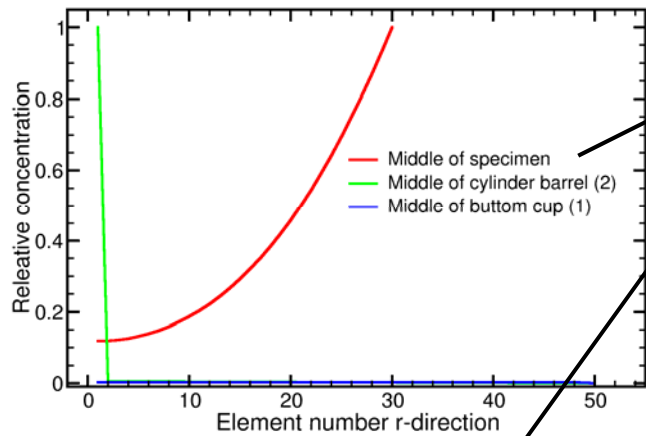
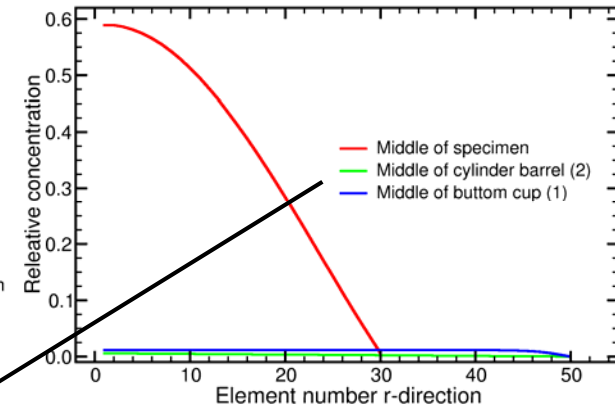
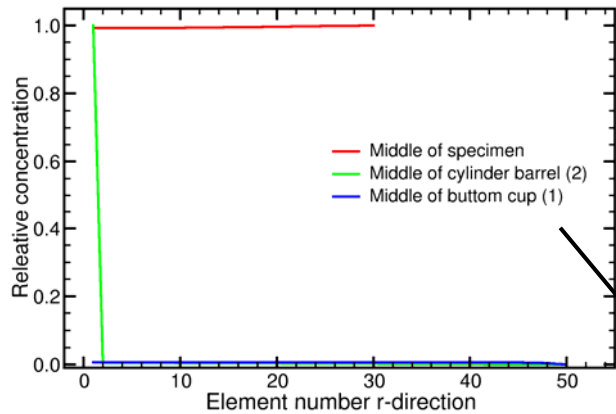


# Gas release Experiment, current status

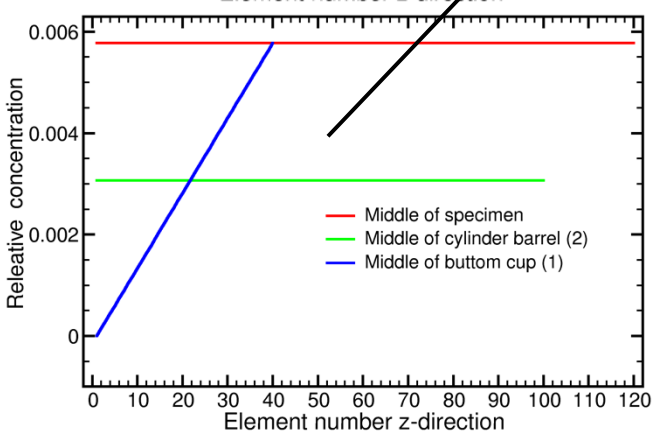
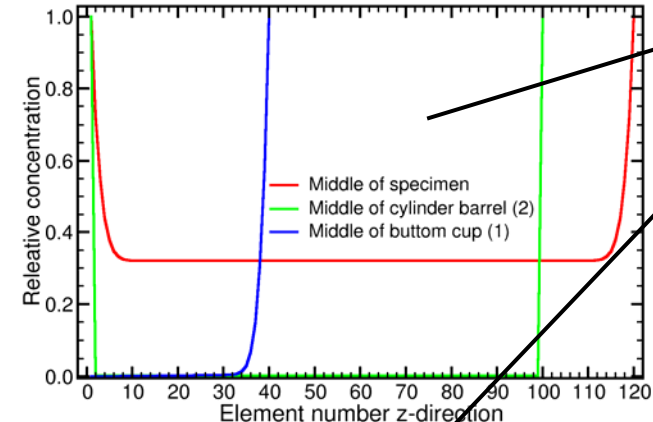
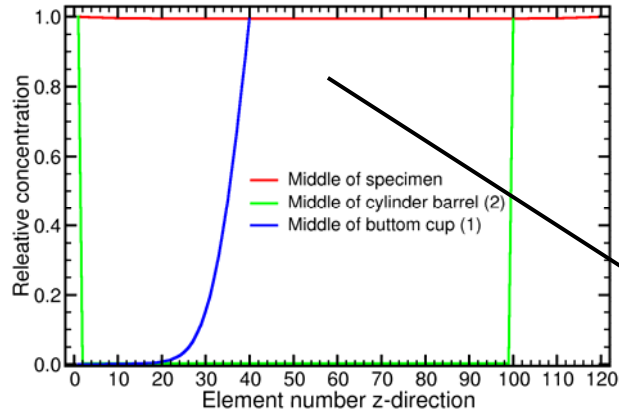
Result of 1D solver r-dependency.



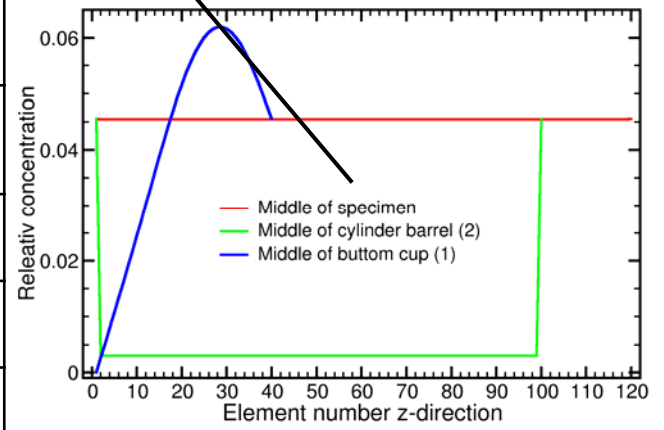
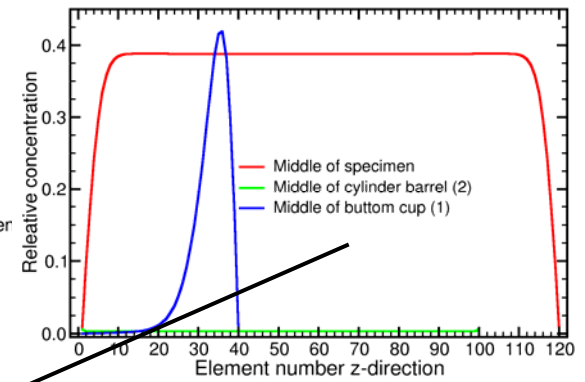
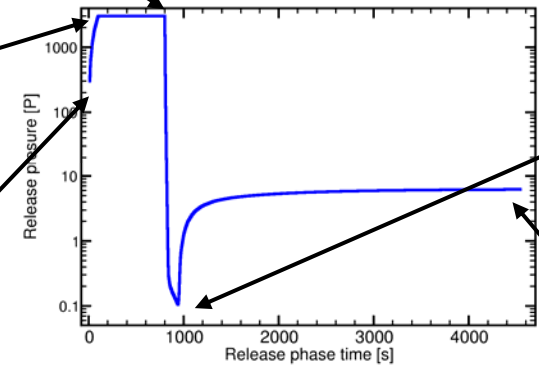
# Calculation time 2D 2 h, inverse problem approx. 920 h Uc1



# Calculation with 2D Version 24 with 12600 elements



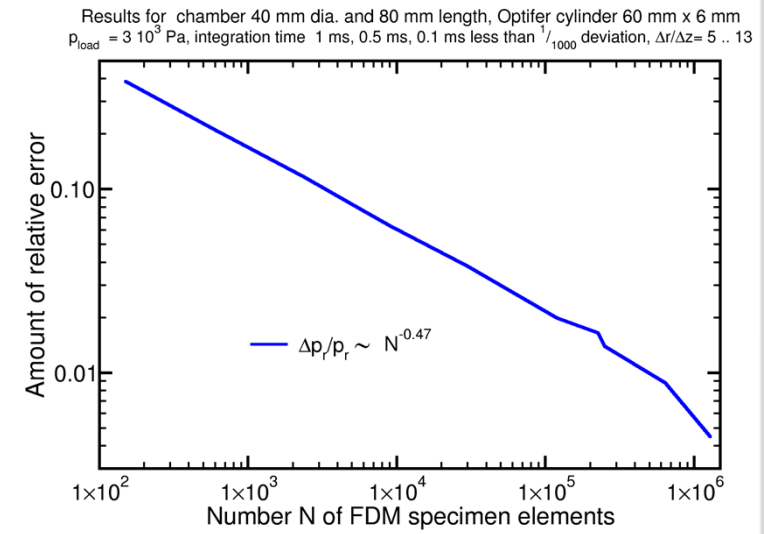
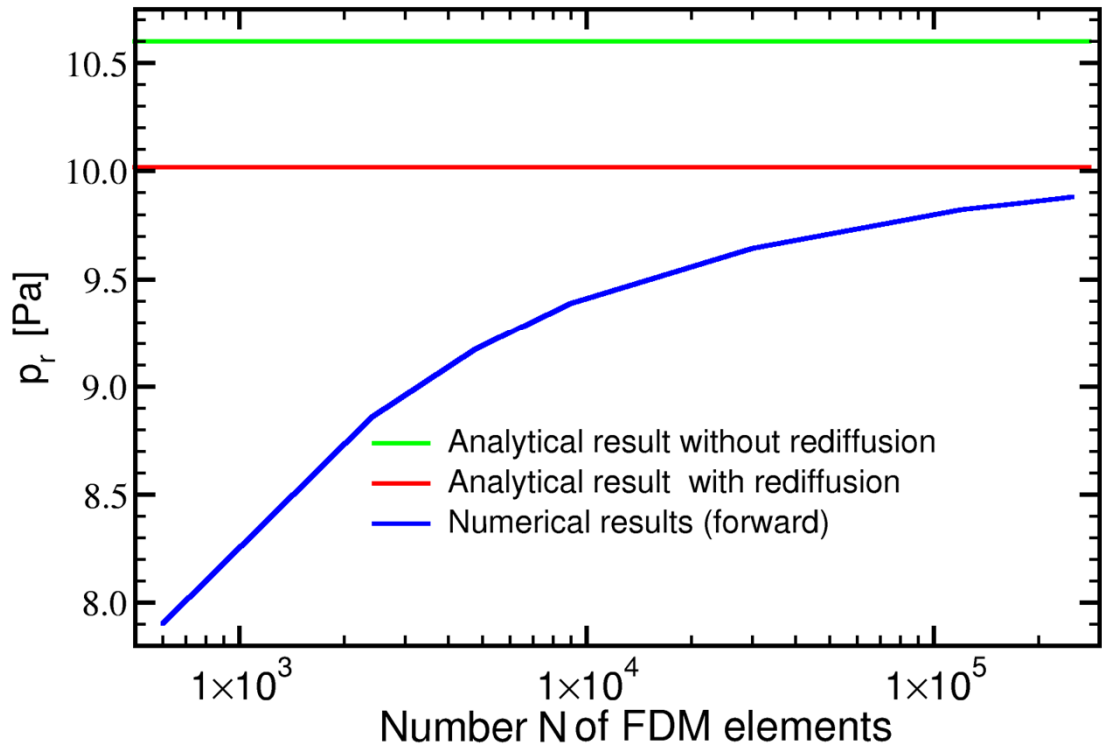
"gasrel" Version 24, T=773 K, Cu containment with Optifer specimen  
chamber dimension 80 mm to 40 mm diameter,  $p_{load} = 3 \cdot 10^3$  Pa, specime 6 mm x 60 mm



Body	R-elem	Z-elem
Specimen	30	120
1	50	40
2	50	100
3	50	40

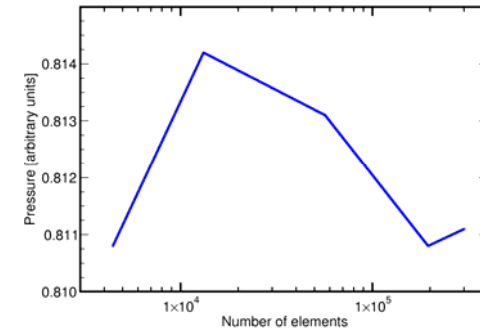
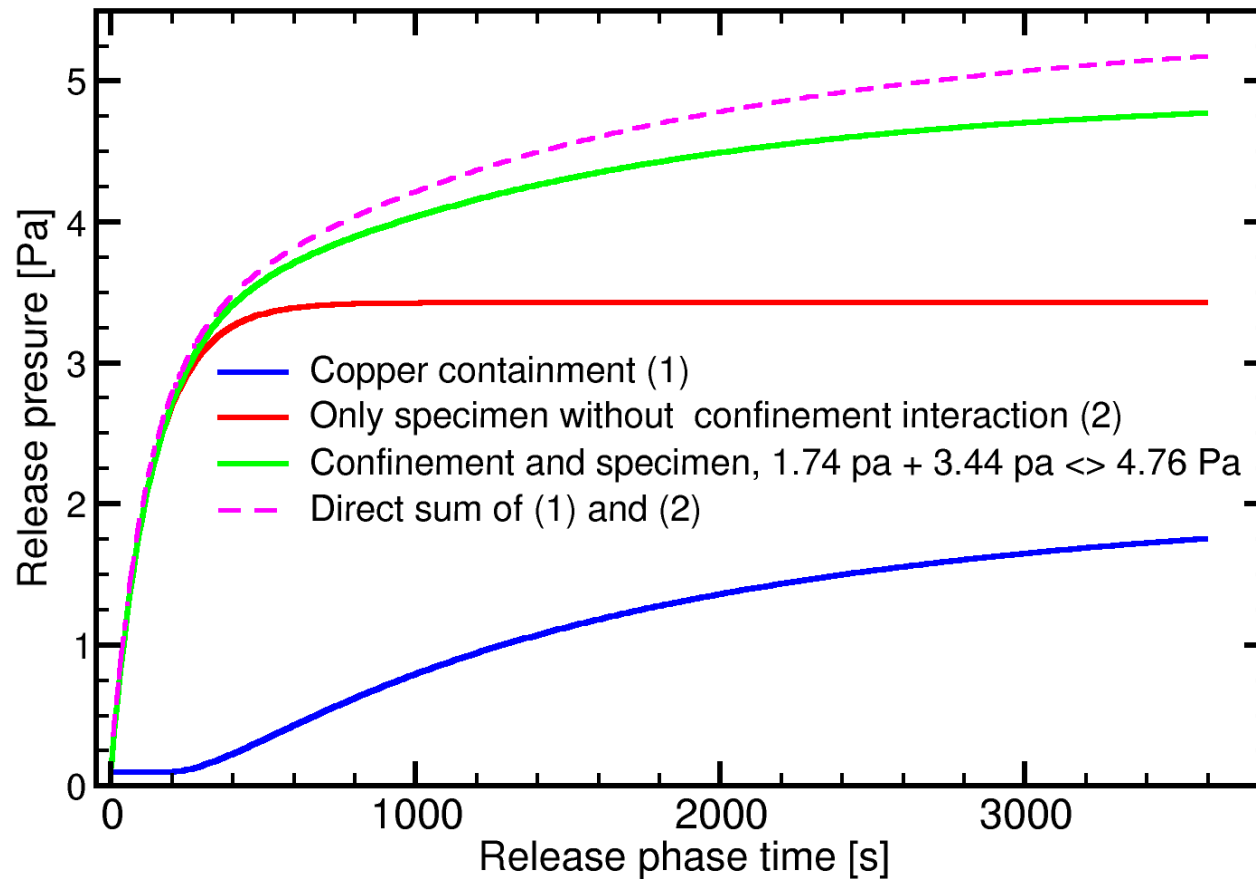
### Comparison with analytical solution:

Results for chamber 40 mm dia. and 80 mm length, Optifer  
 $p_{load} = 3 \cdot 10^3$  Pa, integration time checked 1 ms, 0.5 ms, 0.1 ms less than  $1/1000$  deviation

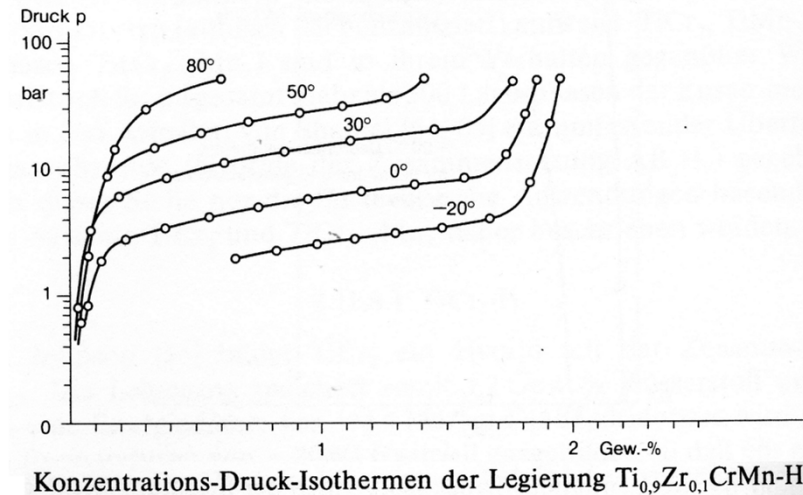
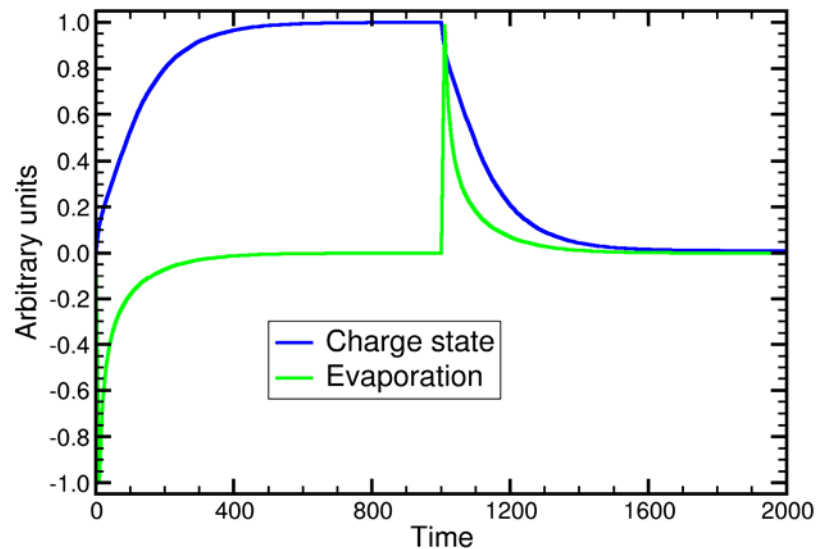


# Comparison to analytical solution

"gasrel24",  $T=773$  K, Cu containment with Optifer specimen, 24. 5.  
chamber dimension 80 mm to 40 mm diameter,  $p_{load} = 3 \cdot 10^3$  Pa, interstitial-molecular



# 7. Thermal desorption experiment as possible automotive application (energy storage)



	Thermal desorption, GR	Metal hydride storage	Lithiumorthosilicate tritium extraction
Pressure	3 kPa	$5 \cdot 10^5 - 10^6$ Pa	1 Pa
Extraction to	Hydrogen atmosphere		
Material	Sieverts'	Non linear	Isotope exchange
Temperature	300°C-500°C	20°C-30°C	> 500°C

# Acknowledgement:

The current talk summarizes results of two running projects:

*Main goal of the first one is the determination of transport parameters of hydrogen in structural metallic materials used for components in fusion power stations:*

*This work has been carried out within the framework of the EUROfusion Consortium, and has received funding from the Euratom research and training program 2014-2018 and 2019-2020 under grant agreement No 633053. The views and opinions expressed herein do not necessarily reflect those of the European Commission*

*The authors further acknowledge support and founding by the KIT center MathSEE in the frame of a second project:*

*Neue Lösungen der Kontinuitätsdifferentialgleichung mit Phasengleichgewicht zur Verbesserung der Ergebnisse bei der Auswertung von Experimenten.*