

# In situ probing of Pt/TiO<sub>2</sub> activity in low-temperature ammonia oxidation

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The improvement of the low-temperature activity of the supported platinum catalysts in selective ammonia oxidation to nitrogen is still a challenging task. The recent developments in *in situ/operando* characterization techniques allows to bring new insight into the properties of the systems in correlation with their catalytic activity. In this work, near ambient pressure X-ray photoelectron spectroscopy (NAP-XPS) and *operando* X-ray absorption spectroscopy (XAS) techniques were applied to study Pt/TiO<sub>2</sub> catalysts in ammonia oxidation (NH<sub>3</sub>+O<sub>2</sub> reaction). Several synthesis methods were used to obtain samples with different size of Pt particles, oxidation state of Pt, and morphology of the support. Metal platinum particles on titania prepared by pulsed laser ablation in liquids exhibited the highest activity at lower temperatures with the temperature of 50% conversion of NH<sub>3</sub> being 150°C. The low-temperature activity of the catalysts synthesized by impregnation can be improved by the reductive pretreatment. NAP-XPS and *operando* XANES data do not show formation of PtO<sub>x</sub> surface layers or PtO/PtO<sub>2</sub> oxides during NH<sub>3</sub>+O<sub>2</sub> reaction. Despite the differences in the oxidation state of platinum in the as-prepared catalysts, their treatment in the reaction mixture results in the formation of metallic platinum particles, which can serve as centers for stabilization of the adsorbed oxygen species. Stabilization of the bulk platinum oxide structures in the Pt/TiO<sub>2</sub> catalysts seems to be less favorable due to the metal-support interaction.

## Introduction

Pt-containing catalysts are important components of the complex systems used for the exhausts gas aftertreatment.<sup>1–4</sup> Supported platinum systems are utilized in diesel vehicles, among others, as a part of ammonia slip catalysts responsible for NH<sub>3</sub> oxidation to molecular nitrogen.<sup>5,6</sup>

Both model platinum systems – single-crystals, foils, and gauzes,<sup>7–12</sup> as well as supported platinum catalysts,<sup>13–20</sup> have been studied in detail as catalysts for the ammonia oxidation reaction, mostly within the Ostwald process for nitric acid production. DFT calculations<sup>21–25</sup> and kinetic modeling<sup>26–28</sup> were performed to gain more insight into the mechanism. However, ways to improve the low-temperature activity (T<250°C) of the catalysts and the selectivity of the reaction towards N<sub>2</sub> formation (required for exhaust gas aftertreatment) are still under discussion. For supported Pt systems, activity and selectivity of the catalysts are influenced by many factors: the size of the platinum particles, Pt oxidation state, the structure and nature of the support, metal-support interactions, etc. Also, the state of the active component can change during the reaction process, which requires special

experimental approaches to obtain relevant results. This makes it difficult to draw reliable conclusion on “structure” - “activity/selectivity” correlations.

The recent development of *in situ* and *operando* techniques opens new opportunities to get information about the systems under reaction conditions. *In situ* methods play a key role in studying reaction mechanisms and identifying the main factors affecting the activity and selectivity of the catalysts. Thus, *in situ* X-ray photoelectron spectroscopy (XPS) gives information about processes taking place on the surface of the catalysts during the reaction: the reaction intermediates formed on the surface can be identified; the change of the charge state of the active component can be analyzed. *In situ* XPS data for ammonia oxidation reaction on the surface of bulk platinum systems have already been reported.<sup>10</sup> The authors used stepped platinum surface which might to some extent simulate the structural heterogeneity of nanoparticles present in real powder catalysts. However, to obtain more relevant results, a further transition to the study of supported systems is necessary.

In this paper, we present a study of Pt/TiO<sub>2</sub> catalysts by *in situ/operando* methods in the ammonia oxidation reaction. The Pt/TiO<sub>2</sub> systems are less investigated for this reaction than the traditionally used Pt/Al<sub>2</sub>O<sub>3</sub>.<sup>29,30</sup> However, unlike the Pt/Al<sub>2</sub>O<sub>3</sub> catalysts, for the Pt/TiO<sub>2</sub> system, there is a possibility of the metal-support interaction, which can influence the catalytic properties.<sup>31–36</sup> It was shown that the metal-support interaction can provide stabilization of the metal platinum particles.<sup>31,33</sup> Oxidation of the metal platinum particles with the formation of the oxide structures on the surface leads to deactivation of the catalysts of the ammonia oxidation reaction.<sup>13,19,37</sup> Therefore, stabilization of metallic Pt species might be beneficial for the NH<sub>3</sub>+O<sub>2</sub> catalytic process. As

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potential catalysts for the selective  $\text{NH}_3$  oxidation at low temperature, the Pt/TiO<sub>2</sub> systems should be investigated in detail using the modern physicochemical methods.

Two techniques for the synthesis of Pt/TiO<sub>2</sub> catalysts were applied in this work. Apart from the traditional impregnation technique, pulsed laser ablation in liquids (LAL) was used for the synthesis of the catalysts. The LAL method leads to the formation of the dispersed particles with a defective, distorted structure.<sup>38–41</sup> As the defects of the TiO<sub>2</sub> support might stimulate the metal-support interaction,<sup>42–44</sup> the LAL can be a promising method for the preparation of the Pt/TiO<sub>2</sub> catalysts active in the ammonia oxidation reaction. Previously, it was shown that the composites prepared by LAL are active in CO oxidation reaction,<sup>38,39</sup> low-temperature ammonia oxidation,<sup>45</sup> phenol photodegradation process under visible light.<sup>41</sup>

The supported Pt/TiO<sub>2</sub> catalysts were studied using NAP-XPS and *operando* XAS – powerful complementary tools for the investigation of the catalysts under working conditions. The application of these methods provided insights into the evolution of the surface and bulk Pt particle structure under  $\text{NH}_3+\text{O}_2$  conditions showing that the metal platinum particles do not undergo significant oxidation under the reaction conditions, regardless of the preparation method.

## Experimental

### Samples preparation

Two approaches were used for the synthesis of Pt/TiO<sub>2</sub> samples. The first was the incipient wetness impregnation of the commercial TiO<sub>2</sub> support (AEROXIDE P25, Evonik) with a solution of platinum nitrate Pt(NO<sub>3</sub>)<sub>x</sub> (17.87 wt.%, KZCM). The resulted sample was dried at room temperature (for 16h) with further increase of the temperature to 60°C (heating for 1h) and 120°C (heating for 2h). The dried catalyst was calcined in air at 400°C for 4h. The platinum content in the sample was 2 wt.%. This sample is denoted by Pt/TiO<sub>2</sub>-IMP in the text.

The second method for the synthesis of the catalysts was pulsed laser ablation in liquids. The detailed description of the preparation of the composite catalysts by the LAL is given in <sup>38,39</sup>. Briefly, the Pt and TiO<sub>x</sub> dispersions were obtained separately by ablation of platinum and titanium metal plates in liquids. The ablation of the targets was carried out by focused radiation of a Nd: YAG laser (1064 nm, 7 ns, 150 mJ imp., 20 Hz). Based on the earlier study,<sup>39</sup> an ethanol solution (96.3 vol.%) and distilled water were taken as solvents to obtain platinum and TiO<sub>x</sub> dispersions, respectively. The concentration of the components in the resulting dispersions was determined by the loss of the mass of the corresponding target. The resulting solutions were mixed in such a proportion so as to obtain 2 wt.% of platinum in the catalyst. The Pt and TiO<sub>x</sub> dispersions were mixed using a magnetic stirrer at room temperature and dried in air at 60°C. The air-dried powder was calcined in air at 400°C for 4h. The LAL-prepared sample is denoted in the text by Pt/TiO<sub>2</sub>-LAL.

### Physicochemical characterization

To characterize the structure of the catalysts X-ray diffraction (XRD) and transmission electron microscopy (TEM) were used. The XRD data for the catalysts were obtained on a Bruker D8 instrument (Germany) using Cu  $K\alpha$  radiation in a  $2\theta$  range  $15^\circ < 2\theta < 90^\circ$  (step size 0.05°, 5 s per step). Diffraction intensities were measured with the LynxEye position sensitive detector. For crystalline phase analysis, the ICDD PDF-2 powder database was used. The refinement of the structure and the profile analysis were carried out with the TOPAS software package (Bruker, Germany).<sup>46</sup>

TEM experiments were performed on a JEM-2200FS electron microscope (JEOL Ltd., Japan) at the “VTAN” resource center of Novosibirsk State University, Russia. To collect the high-resolution (HRTEM) and HAADF-STEM images with a spatial resolution of 1 Å an accelerating voltage of 200 kV was applied. TEM data were analyzed using “ImageJ” software<sup>47</sup> to determine the particle size distribution. For TEM experiments samples were deposited on 3 mm copper grids coated with a carbon film by dispersing in ethanol and sputtering the dispersion on the grids.

The specific surface area of the samples ( $S_{\text{BET}}$ ) was determined by the standard Brunauer–Emmett–Teller method using the low-temperature adsorption isotherms of N<sub>2</sub> collected at an ASAP-2400 setup (Micromeritics Instrument. Corp., Norcross, GA, USA).

Analysis of the samples by X-ray photoelectron spectroscopy (XPS) under UHV ( $p \sim 10^{-8}$  mbar) conditions (*ex situ* XPS experiments) was performed using an ES-300 spectrometer (KRATOS Analytical). To record the spectra a non-monochromatic Mg  $K\alpha$  source ( $h\nu = 1253.6$  eV) was employed.

*In situ* XPS data were collected at a near ambient pressure XPS setup (SPECS Surface Nano Analysis, GmbH Germany) at the Charles University (Prague, Czech Republic). A monochromatic Al  $K\alpha$  source ( $h\nu = 1486.6$  eV) was used to collect XPS spectra. The powder catalysts were pressed to pellets and fixed on the sample holder using spot welding of Ta foil stripes. The sample holder contained a K-type thermocouple welded near the sample pellet for temperature control. Heating was performed by the electron bombardment at the back of the sample stage, which was in thermal contact with the sample holder while mounted on the NAP manipulator. XPS analysis of the samples before their exposure to the reaction mixture was performed at room temperature (RT) in Ar flow ( $p(\text{Ar}) \sim 1$  mbar) to prevent the surface charging. The *in situ* experiments were performed by stepwise heating the samples in the  $\text{NH}_3+\text{O}_2$  reaction mixture ( $\text{NH}_3:\text{O}_2$  ratio of 1:40 and total pressure  $p_{\Sigma} \sim 1.4$  mbar) from 50°C to 400°C with simultaneous acquisition of XPS data. XPS spectra were collected after heating the samples to a certain temperature and stabilization in the reaction mixture for 20 min. XPS experiments were complemented with simultaneous analysis of the gas mixture by mass spectrometry (Prisma Pro, Pfeiffer Vacuum, Germany) to follow the change of concentrations of the reagents ( $\text{NH}_3$ ,  $\text{O}_2$ ) and products ( $\text{H}_2\text{O}$ ,  $\text{N}_2\text{O}$ ,  $\text{N}_2$ ,  $\text{NO}_x$ ) with temperature increase.

The spectra energy calibration was done using a Ti2p<sub>3/2</sub> line as an internal standard with a binding energy value  $E_b(\text{Ti}2p_{3/2})=458.6$  eV for TiO<sub>2</sub>. Such a calibration procedure gave  $E_b(\text{C}1s)=284.7$  eV for the residual amorphous carbon present on the surface. The Pt4f/Ti2p ratio was calculated based on the area of the corresponding spectral lines. The Shirley background was subtracted before processing the spectra. Ti2p, O1s, C1s, and N1s spectra were fitted with a combination of the Gaussian and Lorentzian functions. The Pt4f spectra fitting was performed using a combination of the Gaussian and Lorentzian functions for oxidized components, while Doniach–Šunjić function was used to describe the asymmetry of metallic Pt<sup>0</sup> doublet. Also, Pt4f spectra fitting was performed with consideration of the FWHM (full width at half maximum) values of the corresponding Ti2p lines. The XPS-Cal program<sup>38,39</sup> was used for processing the XPS data.

*Ex situ* and *operando* X-ray absorption near edge structure (XANES) spectra at Pt L<sub>3</sub> absorption edge were recorded at the P65 beamline of the PETRA III synchrotron radiation source (DESY, Hamburg, Germany) in transmission mode. Energy of the X-rays was selected using a Si(111) double crystal monochromator and higher harmonics were rejected by a pair of Si mirrors. Beam size was selected by slits as 0.2 (vert.) × 1.0 (hor.) mm<sup>2</sup>. Catalyst samples were measured as 100–200 μm sieved powders packed in quartz capillaries (o.d. = 1.5 mm, 0.02 mm wall thickness) heated by a hot air blower. The catalyst bed length was approx. 5 mm and the X-ray beam was probing part near inlet of the catalyst bed. The gas mixture contained 880 ppm NH<sub>3</sub>, 10 vol.% O<sub>2</sub>, and 10 vol.% N<sub>2</sub> in He with a flow of 70 ml/min. Outlet gas composition was analyzed by an MKS Multigas 2030 FTIR analyzer. The spectra were corrected for the energy shift using a spectrum of Pt foil measured simultaneously and then normalized using the Athena program from the IFFEFIT software package.<sup>48</sup> The average oxidation state of Pt was determined by linear combination analysis (LCA) of the XANES data in Athena<sup>48</sup> with Pt foil and PtO<sub>2</sub> reference spectra in the energy range between 11550 and 11600 eV. For the analysis of extended X-ray absorption fine structure (EXAFS), the spectra were background-subtracted, k<sup>2</sup>-weighted, multiplied by a Hanning window with sill size of 1 Å<sup>-1</sup>, and Fourier-transformed in the k-range 2.5–11.0 Å<sup>-1</sup>. The amplitude reduction factor  $S_0^2=0.74$  was obtained by fitting the Pt foil and the PtO<sub>2</sub> (Alfa Aesar, 99.95%) reference spectra to structural models as reported in the *Inorganic Crystal Structure Database (ICSD, CCs = 64923 and 4415)*. The fits were performed on k<sup>1</sup>, k<sup>2</sup>, and k<sup>3</sup>-weighted using Artemis<sup>48</sup> by a least square method in R-space between 1.0 and 3.0 Å. Coordination numbers, interatomic distances, energy shift ( $\delta E_0$ ) and mean square deviation of interatomic distances ( $\sigma^2$ ) were refined during the fitting. The absolute misfit between theory and experiment was expressed by  $\rho$ .

## Catalytic experiments

The catalytic properties of the Pt/TiO<sub>2</sub> samples were studied in the temperature-programmed reaction of ammonia oxidation (TPR-NH<sub>3</sub>+O<sub>2</sub>). The experiments were performed in a plug flow quartz reactor. 0.145 g of the catalyst was analyzed in the catalytic experiments. Heating of the samples in the NH<sub>3</sub>+O<sub>2</sub> mixture was performed from room temperature to 400°C at a rate of 10°C/min. The reaction mixture containing 0.1 vol.% NH<sub>3</sub>, 4.0 vol.% O<sub>2</sub> (balance He) was fed at a flow of 500 ml/min. Before TPR-NH<sub>3</sub>+O<sub>2</sub> experiments, Pt/TiO<sub>2</sub>-LAL and Pt/TiO<sub>2</sub>-IMP samples were heated in 20%O<sub>2</sub>/He flow at 400°C for 2 h to remove the surface admixtures. A gas-phase FTIR spectrometer (I1801, MIDAC corp., USA) was used to measure concentrations of NH<sub>3</sub>, N<sub>2</sub>O, NO, NO<sub>2</sub>, while O<sub>2</sub> and N<sub>2</sub> concentrations were analyzed using a gas chromatograph (Crystal 2000M, CHROMATEC, Russia). Conversion (in %) of ammonia was calculated as  $X_{\text{NH}_3}=(1-C_{\text{NH}_3}^{\text{out}}/C_{\text{NH}_3}^{\text{in}})\cdot 100$ , where  $C_{\text{NH}_3}^{\text{in}}$  and  $C_{\text{NH}_3}^{\text{out}}$  are the inlet and outlet NH<sub>3</sub> concentrations, respectively. Selectivity (in %) to the reaction products (N<sub>2</sub>, N<sub>2</sub>O, NO, or NO<sub>2</sub>) was calculated as  $S_i=(n_i/\sum n_i)\cdot 100$ , where  $n_i$  – the concentration of the corresponding product.

## Results and discussion

### Structural characterization of Pt/TiO<sub>2</sub> samples

Fig.1 shows the X-ray diffraction patterns for Pt/TiO<sub>2</sub>-LAL (purple line (1)) and Pt/TiO<sub>2</sub>-IMP (green line (2)) samples. For obtained XRD patterns, a full profile Rietveld refinement was performed. The XRD profile Rietveld modeling for the samples are given in ESI file (Fig.S1). The Pt/TiO<sub>2</sub>-LAL sample contains an X-ray amorphous phase as well as the crystalline phases attributed to metallic Pt (ICDD PDF-2 # 04-0802) and anatase structure of TiO<sub>2</sub> (ICDD PDF-2 # 21-1272). The calculated diffraction curve poorly describes the experimental pattern in the region of the anatase reflections (see Fig.S1), which

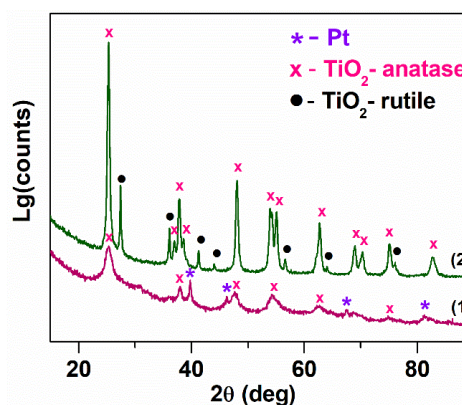
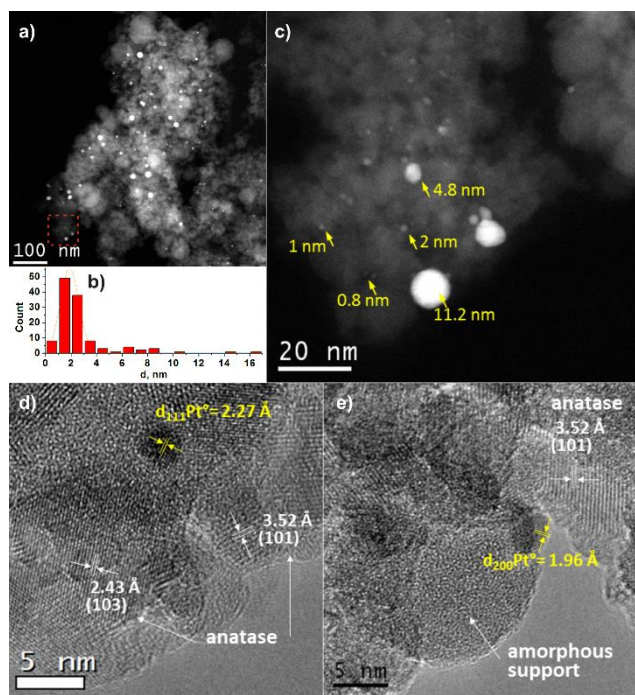


Fig.1. X-ray diffraction patterns for (1) Pt/TiO<sub>2</sub>-LAL, (2) Pt/TiO<sub>2</sub>-IMP.

**Table 1.** Morphology and structural characteristics of the catalysts.

|                          | $S_{BET}$ , m <sup>2</sup> /g | TiO <sub>2</sub> -anatase |          |          |          | TiO <sub>2</sub> -rutile |          |          |          |
|--------------------------|-------------------------------|---------------------------|----------|----------|----------|--------------------------|----------|----------|----------|
|                          |                               | $a$ , Å                   | $c$ , Å  | $D$ , nm | W, wt.%  | $a$ , Å                  | $c$ , Å  | $D$ , nm | W, wt.%  |
| Pt/TiO <sub>2</sub> -LAL | 152                           | 3.804(3)                  | 9.47 (1) | 4.7 (3)  | 100      | -                        | -        | -        | -        |
| Pt/TiO <sub>2</sub> -IMP | 63                            | 3.786(1)                  | 9.508(1) | 18.8 (3) | 84.1 (6) | 4.595(1)                 | 2.960(1) | 29 (2)   | 15.9 (6) |



**Fig.2.** STEM and HRTEM study of the Pt/TiO<sub>2</sub>-LAL sample: (a) HAADF-STEM data, (b) Pt particle size distribution, (c) HAADF-STEM data of the area marked in (a) with red square, (d,e) HRTEM data of selected regions.

suggests that the anatase phase might be defective. The structural characteristics of the TiO<sub>2</sub> phases (lattice parameters ( $a,c$ ), the average crystallite size ( $D$ )) calculated from XRD data are given in Table 1. There is a difference between the values of the TiO<sub>2</sub>-anatase lattice parameters for the Pt/TiO<sub>2</sub>-LAL sample and the data reported for the single crystal anatase

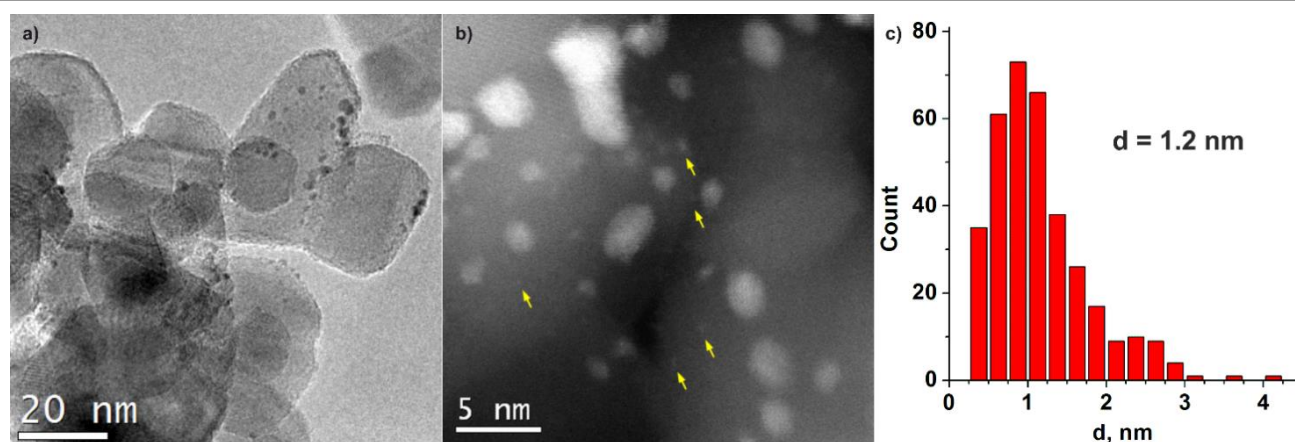
TiO<sub>2</sub> ( $a=3.784$  Å,  $c=9.515$  Å).<sup>49</sup> Ballirano et al.<sup>50</sup> observed the modified lattice parameters ( $a=3.784$  Å,  $c=9.500$  Å) for the nanosized TiO<sub>2</sub>-anatase particles ( $D\sim 21$  nm). For the Pt/TiO<sub>2</sub>-LAL sample, the calculated average crystallite size is  $\sim 5$  nm. Thus, the change of the lattice parameters of the anatase phase might be related to the small size and defective structure of the TiO<sub>2</sub> crystallites. Contribution from the metallic Pt in the Pt/TiO<sub>2</sub>-LAL sample was refined with the introduction of two phases corresponding to large ( $D\sim 25$  nm) and small particles ( $D\sim 2$  nm).

The X-ray diffraction pattern of the Pt/TiO<sub>2</sub>-IMP sample can be described with a mixture of anatase (ICDD PDF-2 # 21-1272) and rutile (ICDD PDF-2 # 21-1276) phases. The amount of the anatase phase is greater than the rutile phase (see Table 1). The average crystallite sizes of anatase and rutile phases are  $\sim 19$  nm and  $\sim 30$  nm, respectively. The lattice parameters of the TiO<sub>2</sub> phases are similar to those reported for the nanosized TiO<sub>2</sub>.<sup>50</sup> Platinum-containing phases were not detected by the XRD method allowing us to propose the presence of the highly dispersed Pt species in the Pt/TiO<sub>2</sub>-IMP sample.

The smaller size of the TiO<sub>2</sub> crystallites in the Pt/TiO<sub>2</sub>-LAL sample results in a higher value of the surface area ( $S_{BET}$ ) in comparison with the Pt/TiO<sub>2</sub>-IMP sample (see Table 1).

Fig.2 shows TEM data for the Pt/TiO<sub>2</sub>-LAL sample. Most of the TiO<sub>2</sub> particles are 5-10 nm in size, but larger particles from 10 to 200 nm in diameter are also observed. Both the crystalline phase of anatase (Fig.2d) and amorphous TiO<sub>2</sub> particles (Fig.2e) can be identified using HRTEM.

Platinum nanoparticles in the Pt/TiO<sub>2</sub>-LAL sample have a spherical-like shape. Their distribution over the support is



**Fig.3.** TEM study of Pt/TiO<sub>2</sub>-IMP sample: (a) TEM image, (b) HAADF-STEM image (yellow arrows mark the presence of highly dispersed Pt species), (c) Pt particle size distribution.

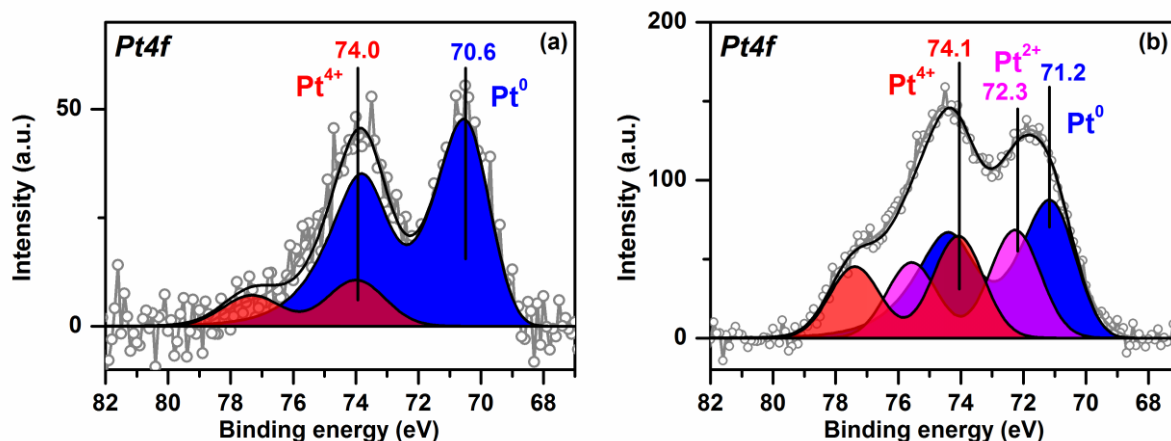


Fig.4. Pt4f XPS spectra for (a) Pt/TiO<sub>2</sub>-LAL, (b) Pt/TiO<sub>2</sub>-IMP samples.

uniform. Most of the platinum particles have a size of 1-3 nm (Fig.2b). However, there are some larger particles with a size of 10-20 nm. The results are in a good agreement with the XRD data.

TEM data for the Pt/TiO<sub>2</sub>-IMP sample are given in Fig.3. The size of the TiO<sub>2</sub> particles varies from 10 to 40 nm. The Pt nanoparticles have a spherical-like shape (Fig.3a). The average size of platinum particles is 1.2 nm (Fig.3c). Also, highly dispersed platinum particles less than 1 nm in size (marked with yellow arrows in Fig.3b) can be well detected due to the high contrast of platinum on the TiO<sub>2</sub> surface in the dark-field images (Z-contrast).

#### XPS analysis of the Pt/TiO<sub>2</sub> samples in UHV

Fig.4 shows the Pt4f X-ray photoelectron (XP) spectra of the Pt/TiO<sub>2</sub> samples fitted to the individual components. The Ti2p and O1s spectra of the samples are given in ESI, Fig.S2. For Pt/TiO<sub>2</sub>-LAL sample the main Pt4f doublet has a  $E_b(\text{Pt}4f_{7/2})$  value 70.6 eV (Fig.4a). The  $E_b(\text{Pt}4f_{7/2})$  value typical for bulk metal Pt<sup>0</sup> surfaces (foils, single-crystals etc.) is usually considered to be 71.0-71.2 eV.<sup>51-53</sup> It cannot be excluded that the interaction of the Pt<sup>0</sup> nanoparticles with the TiO<sub>2</sub> support results in a slight decrease of the observed  $E_b(\text{Pt}4f_{7/2})$  value for the Pt/TiO<sub>2</sub>-LAL sample. Metal-support interaction is known for the supported catalytic systems.<sup>42,44,54-57</sup> It can cause a change in the electronic state of the active component and the support, structure, and morphology of the catalyst. For the Pt-TiO<sub>2</sub> systems, metal-support interaction is most frequently discussed in terms of the charge transfer from TiO<sub>2</sub> to the small Pt particles<sup>32,55,58</sup> with accumulation of the charge at the Pt-TiO<sub>2</sub> interface<sup>55</sup> or encapsulation of the platinum particles by the support.<sup>32,34,54,59</sup> Metal-support interaction is usually observed when samples are heated in a reductive atmosphere. Under these conditions, the reduced, defective TiO<sub>2-δ</sub> structures might be formed facilitating the interaction with Pt particles.<sup>42-44</sup> In our case, the LAL method leads to the formation of defective, amorphous structures of titanium oxide, hence, a metal-support interaction might occur. The accumulation of the charge at the Pt<sup>0</sup>-TiO<sub>2</sub> interface can cause

the inhomogeneous charging of the sample surface, thus resulting the observed negative shift of Pt<sup>0</sup> peaks.

A Pt4f<sub>7/2</sub> peak with a lower intensity at ~74.0 eV (Fig.4a) can be related to oxidized Pt<sup>4+</sup> species.<sup>51,60</sup> It is known that small platinum particles can be easily oxidized with the formation of PtO<sub>x</sub> structures.<sup>61-65</sup> TEM data for the Pt/TiO<sub>2</sub>-LAL sample show the presence of a certain amount of the highly dispersed platinum species. We can propose the highly dispersed Pt species are in Pt<sup>4+</sup> oxidation state.

The Pt4f region for the Pt/TiO<sub>2</sub>-IMP catalyst reveals three platinum states with the  $E_b(\text{Pt}4f_{7/2})$  values of 71.2, 72.3 and 74.1 eV (Fig.4b). The first state might be attributed to the metallic platinum species.<sup>51,53,60</sup> The second and third states of platinum can be related to Pt<sup>2+</sup> and Pt<sup>4+</sup> species, respectively.<sup>51,53,60</sup> The stoichiometry of the PtO<sub>x</sub> species formed by interaction of small platinum particles with oxygen depends on the particle size. According to Wang et. al.,<sup>66</sup> the x value changes from 1 to 2 when particle size decreases below 2 nm. Since we have a distribution of the size of the Pt particles, it can be proposed that the smallest platinum particles oxidize to PtO<sub>2</sub>, while the larger particles give PtO species. The formation of a PtO oxide layer covering the surface of the metal platinum particles is also possible. Thus, the observed Pt<sup>2+</sup> oxidized species can be present as a PtO layer on the surface of Pt<sup>0</sup> particles and/or as oxidized PtO particles. Zhang et al. also observed peaks at 71.2 eV and 72.3 eV for a Pt-TiO<sub>2</sub> film calcined at 400°C.<sup>67</sup> The authors proposed oxidation of Pt<sup>0</sup> sites to Pt<sup>2+</sup> species which substitute Ti<sup>4+</sup> ions in TiO<sub>2</sub> lattice. Hence, the stabilization of the Pt<sup>2+</sup> species due to the interaction with the TiO<sub>2</sub> lattice cannot be ruled out.

The contribution of the oxidized platinum species to the Pt4f spectrum for Pt/TiO<sub>2</sub>-IMP sample is higher than in the case of the Pt/TiO<sub>2</sub>-LAL sample. Such a result is in a good agreement with the TEM data which show higher amount of the highly dispersed platinum species in the Pt/TiO<sub>2</sub>-IMP sample.

The ratio of the Pt4f and Ti2p line intensities (Pt4f/Ti2p) in the Pt/TiO<sub>2</sub>-LAL is significantly lower (about 3.5 times) than for the Pt/TiO<sub>2</sub>-IMP. This can be explained by the presence in the Pt/TiO<sub>2</sub>-LAL sample a certain amount of the large platinum

particles which results in low intensity of the platinum signal. A partial encapsulation of the platinum particles by a  $\text{TiO}_x$  layer is

also possible. Furthermore, the  $S_{\text{BET}}$  of the  $\text{Pt}/\text{TiO}_2$ -LAL sample is almost 2.5 times higher than the one of the  $\text{Pt}/\text{TiO}_2$ -IMP

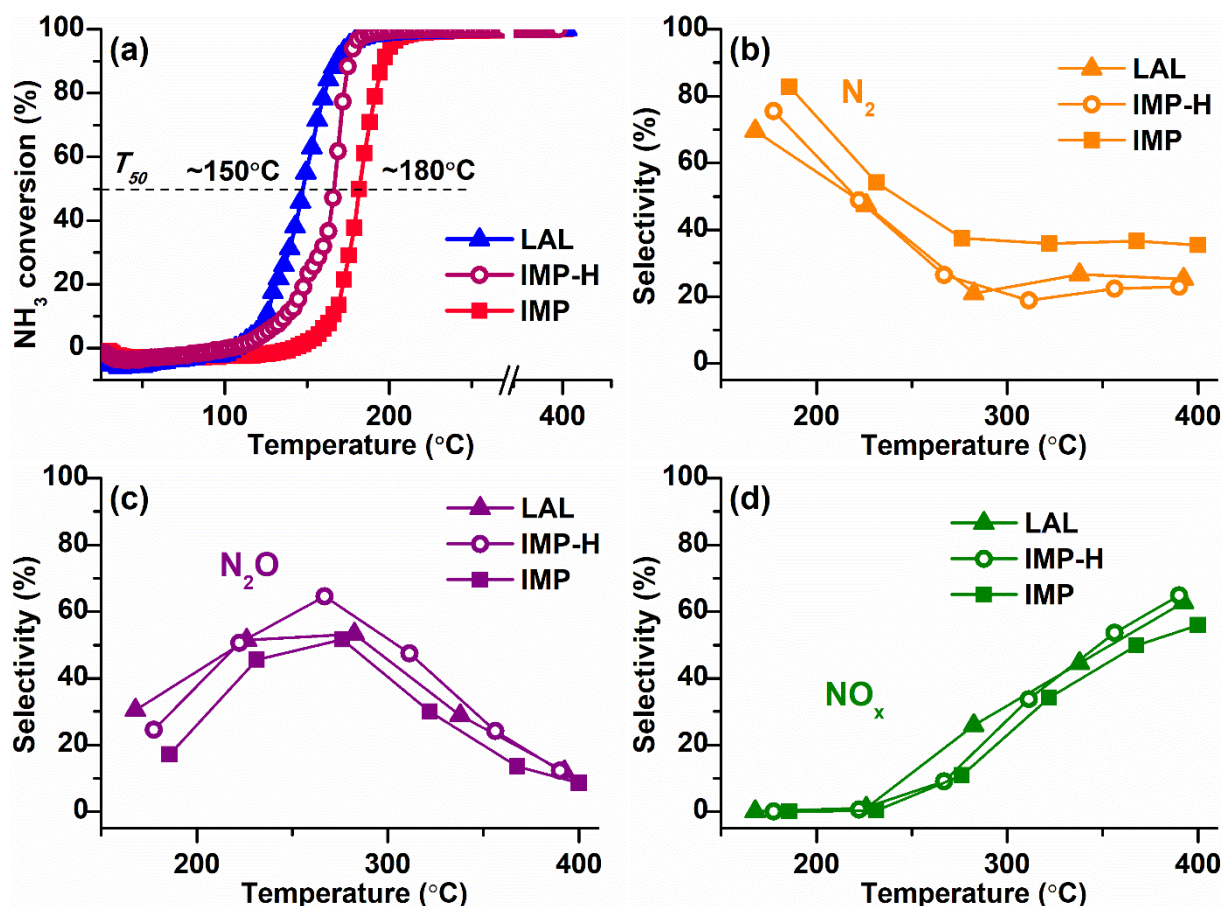


Fig. 5. TPR- $\text{NH}_3+\text{O}_2$  data for  $\text{Pt}/\text{TiO}_2$  catalysts: (a)  $\text{NH}_3$  conversion; products selectivity: (b)  $\text{N}_2$ , (c)  $\text{N}_2\text{O}$ , (d)  $\text{NO}_x$ . Sample  $\text{Pt}/\text{TiO}_2$ -LAL marked as triangles,  $\text{Pt}/\text{TiO}_2$ -IMP as squares, and  $\text{Pt}/\text{TiO}_2$ -IMP-H as circles. The reaction mixture: 0.1 vol.%  $\text{NH}_3$  and 4.0 vol.%  $\text{O}_2$  (balance He).

sample (see Table 1). This can lead to a higher intensity of the titanium signal due to larger surface.

To sum up, the *ex situ* characterization shows that the sample prepared using the LAL technique comprises mostly metallic platinum nanoparticles in contact with  $\text{TiO}_2$ . The  $\text{Pt}/\text{TiO}_2$ -IMP sample shows more dispersed and oxidized platinum particles.

#### Catalytic activity of the $\text{Pt}/\text{TiO}_2$ samples in $\text{NH}_3+\text{O}_2$ reaction

The activity of the samples in ammonia oxidation was studied using the temperature-programmed reaction  $\text{NH}_3+\text{O}_2$  (TPR- $\text{NH}_3+\text{O}_2$ ). Data on the ammonia conversion and the selectivity to the reaction products as function of the temperature are given in Fig.5.

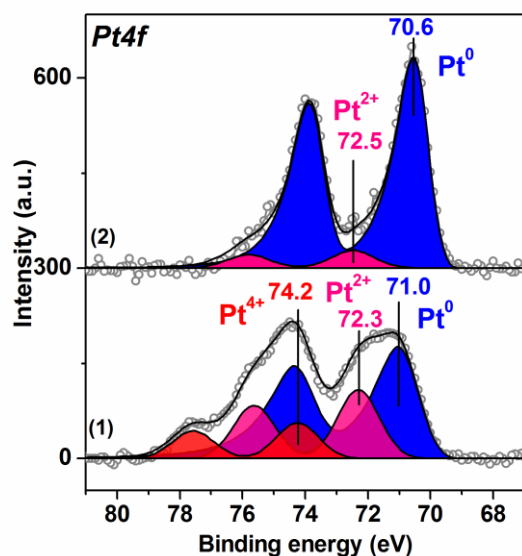
All samples show low-temperature activity reaching 100% conversion of ammonia at  $T < 200^\circ\text{C}$ . Comparison of the  $\text{NH}_3$  conversion curves shows that the  $\text{Pt}/\text{TiO}_2$ -LAL sample is more active at low temperatures. The temperature of the 50% ammonia conversion ( $T_{50}$ ) is  $\sim 150^\circ\text{C}$ , while for the  $\text{Pt}/\text{TiO}_2$ -IMP sample the  $T_{50}$  value is  $\sim 180^\circ\text{C}$ . Metallic platinum is proposed to be more active in the oxidation of ammonia in  $\text{O}_2$  excess.<sup>68,69</sup> Therefore, higher low-temperature activity

observed for the  $\text{Pt}/\text{TiO}_2$ -LAL sample can be attributed to the presence of higher amount of the metallic platinum particles.

To confirm this assumption, the  $\text{Pt}/\text{TiO}_2$ -IMP sample was reduced in 20% $\text{H}_2/\text{He}$  flow at  $250^\circ\text{C}$  for 2 h in a catalytic reactor directly before the catalytic experiments (the reduced sample is denoted by  $\text{Pt}/\text{TiO}_2$ -IMP-H). This procedure should lead to an increase of the amount of the reduced platinum forms, and, accordingly, contribute to the improvement of the low-temperature activity. Indeed, one can see a decrease of  $T_{50}$  value (Fig.5a, the IMP-H curve) for the  $\text{Pt}/\text{TiO}_2$ -IMP-H sample in comparison with the initial  $\text{Pt}/\text{TiO}_2$ -IMP catalyst.

The selectivity to the reaction products is similar for all samples. In the temperature range up to  $250^\circ\text{C}$ , the main products are molecular nitrogen and  $\text{N}_2\text{O}$ . The maximum selectivity of  $\text{N}_2$  is observed in the region of  $\text{NH}_3$  conversion below 100% ( $T < 200^\circ\text{C}$ ). At higher temperature the contribution of nitrogen oxides becomes more significant:  $\text{N}_2\text{O}$  at lower temperatures, and  $\text{NO}$  and  $\text{NO}_2$  oxides at temperatures above  $320$ - $350^\circ\text{C}$ . Such temperature-dependent product distribution is typical for bulk Pt structures<sup>8,10</sup> as well as platinum particles stabilized on oxide supports.<sup>15,69,70</sup>

Thus, although all samples show activity in the  $\text{NH}_3+\text{O}_2$  reaction at  $T < 200^\circ\text{C}$ ,  $\text{NH}_3$  conversion for the Pt/TiO<sub>2</sub>-LAL and Pt/TiO<sub>2</sub>-IMP-H samples is observed at lower temperatures. To follow the evolution of the oxidation/charge state of Pt during the catalytic reaction the samples were analyzed by NAP-XPS.



**Fig. 6.** Curve-fitted *in situ* Pt4f XP spectra of (1) Pt/TiO<sub>2</sub>-IMP and (2) Pt/TiO<sub>2</sub>-IMP-H samples acquired in Ar ( $p(\text{Ar}) \sim 1$  mbar, RT).

#### NAP-XPS study of the Pt/TiO<sub>2</sub> samples

Fig. 6 presents the Pt4f spectra fitted into the individual components for the Pt/TiO<sub>2</sub>-IMP and the Pt/TiO<sub>2</sub>-IMP-H samples collected at a NAP-XPS setup before exposure to the reaction mixture. The Pt/TiO<sub>2</sub>-IMP-H sample was in this case prepared directly in the chamber of the NAP-XPS setup by reduction of the Pt/TiO<sub>2</sub>-IMP in H<sub>2</sub> flow at 350°C for 2 h ( $p(\text{H}_2) \sim 1$  mbar). Ti2p and O1s spectra for Pt/TiO<sub>2</sub>-IMP and Pt/TiO<sub>2</sub>-IMP-H samples are given in ESI, Fig.S3.

Similar to the *ex situ* XPS data, the *in situ* Pt4f spectrum of the Pt/TiO<sub>2</sub>-IMP sample shows three doublets with maxima of the Pt4f<sub>7/2</sub> peaks at binding energies ( $E_b(\text{Pt}4f_{7/2})$ ) = 71.0 eV, 72.3 eV, and 74.2 eV. These doublets can be related to the Pt<sup>0</sup>, Pt<sup>2+</sup> and Pt<sup>4+</sup> platinum species, respectively.<sup>51,53,60</sup>

Treatment of the Pt/TiO<sub>2</sub>-IMP sample in H<sub>2</sub> flow results in reduction of Pt<sup>2+</sup> and Pt<sup>4+</sup> species. The Pt4f spectrum of the Pt/TiO<sub>2</sub>-IMP-H sample (Fig. 6 curve (2)) shows the main peak of the reduced Pt species at 70.6 eV. Heating of Pt/TiO<sub>2</sub> in a reductive atmosphere is known to promote the metal-support interaction.<sup>42–44</sup> We do not observe a noticeable change in the Pt4f/Ti2p intensity ratio upon sample heating in H<sub>2</sub>, which suggests that the encapsulation of the platinum particles by the titania does not take place. Nevertheless, the charge transfer from between the support and the platinum particles might take place influencing the  $E_b(\text{Pt}4f_{7/2})$  value. It can be assumed that the reductive treatment results in the formation of the defects on the surface of titania, which promotes the Pt-TiO<sub>2</sub> interaction. Unfortunately, due to the morphology of the supported powder catalysts and the rather low concentration of the active component, we could not detect any noticeable

changes in the Ti2p spectra which might give information on the possible appearance of Ti<sup>3+</sup> species due to metal-support interaction (see ESI, Fig.S3).

The state of platinum in the Pt/TiO<sub>2</sub>-IMP-H sample is similar to the Pt/TiO<sub>2</sub>-LAL catalyst (see Fig. 4a). Pt4f spectra for both catalysts show the main Pt state with the  $E_b(\text{Pt}4f_{7/2}) \sim 70.6$  eV, indicating a similar nature of active sites in these catalysts, namely: Pt<sup>0</sup> species in contact with TiO<sub>2</sub> surface. This is also confirmed by similar catalytic properties of these samples.

The Pt/TiO<sub>2</sub>-IMP and Pt/TiO<sub>2</sub>-IMP-H samples were heated in the  $\text{NH}_3+\text{O}_2$  mixture with simultaneous collection of the NAP-XPS data. The change of the concentrations of the reagents and products with the increase of the reaction temperature was monitored with a mass-spectrometer. MS-data are given in ESI (Fig.S4). Both samples under given reaction conditions showed similar MS results. Conversion of  $\text{NH}_3$  was observed at  $T > 175^\circ\text{C}$ . At temperature below 225°C, the main products were N<sub>2</sub> and N<sub>2</sub>O, while at  $T \sim 225^\circ\text{C}$  partial pressure of NO increased and became predominant at 400°C. These results are in a good agreement with data of the catalytic experiments performed in a plug flow reactor (see Fig. 5).

Fig. 7 shows the evolution of the Pt4f XP spectra collected *in situ* during heating the Pt/TiO<sub>2</sub>-IMP (Fig. 7a) and Pt/TiO<sub>2</sub>-IMP-H (Fig. 7b) samples in the  $\text{NH}_3+\text{O}_2$  mixture. Treatment of the Pt/TiO<sub>2</sub>-IMP sample in the reaction mixture results in a slight increase of the  $E_b(\text{Pt}4f_{7/2})$  value of the peak related to Pt<sup>0</sup> species. The conductivity of the sample surface might slightly change during the reaction due to the removal or accumulation of O-containing surface groups. Thus, the shift of the Pt<sup>0</sup> peaks can be caused by the variation of the charge over the sample surface.

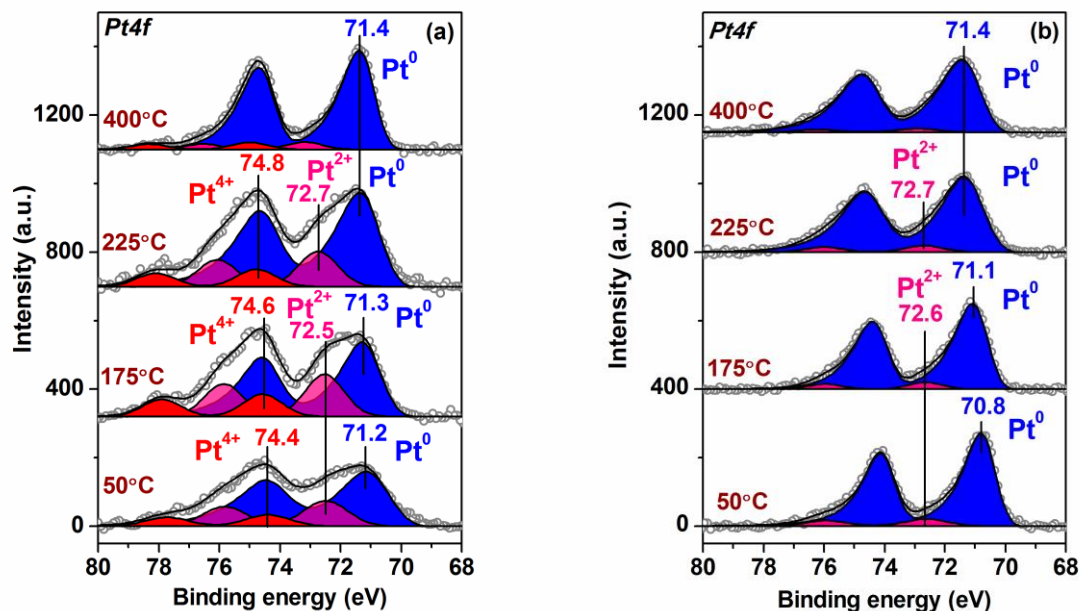
Also, interaction of the platinum particles with oxygen can be the reason for the slight increase of the  $E_b(\text{Pt}4f_{7/2})$  value. Different oxygen species can be formed on the Pt surface: adsorbed oxygen,<sup>8,10,66,71</sup> subsurface oxygen<sup>72</sup> or platinum oxide-like structures.<sup>73–76</sup> The conditions under which various surface oxide structures occur were studied in detail for Pt single-crystals,<sup>73–75,77–79</sup> foils, and nanoparticles.<sup>60,72,80–83</sup>

For surface and bulk platinum oxides, the binding energy of the Pt4f<sub>7/2</sub> peak is usually considered to be more than 72.0 eV.<sup>73–76</sup> Since we do not observe a strong shift of the Pt4f line (the binding energy does not exceed 71.4 eV), the formation of fully oxidized PtO<sub>x</sub> layers or bulk oxides seems unlikely. Smirnov et al.<sup>72,80</sup> showed that dissolution of oxygen in platinum leads to an increase in the  $E_b$  value of the platinum line, while its metal nature is preserved. However, they also observed quite significant shifts of the Pt4f line ( $\sim 1$  eV) for small Pt particles ( $d \sim 1\text{--}2.5$  nm).<sup>80</sup>

Gland et al.<sup>7</sup> observed adsorption of oxygen atoms on edge sites of the stepped Pt single-crystal surface under ammonia oxidation reaction. Gunter et al.<sup>10</sup> detected in their study by *in situ* XPS of ammonia oxidation over a Pt(533) surface the formation of a 1D platinum oxide phase. Imbihl et al.<sup>11</sup> also showed that OH<sub>ad</sub> as well as O<sub>ad</sub> species should be considered during ammonia oxidation. Based on this, we can propose that the  $E_b(\text{Pt}4f_{7/2})$  shift observed in our work might be caused by is

the formation of adsorbed oxygen species ( $O_{ad}$  and/or  $OH_{ad}$ ) on the  $Pt^0$  surface or at the  $Pt^0$ - $TiO_2$  boundary. Unfortunately, analysis of the  $O1s$  spectra of the samples (see ESI, Fig.S5) does not allow to reliably detect signals related to the oxygen species adsorbed on the platinum surface due to low concentration of Pt in the samples, high intensity of the titania

oxygen, and variety of the oxygen-containing species adsorbed on the sample surface. The increase of the  $E_b(Pt4f_{7/2})$  value of the peaks related to the oxidized  $Pt^{2+}$  and  $Pt^{4+}$  species can be explained by the formation of the  $Pt(OH)_x$  structures<sup>51,84</sup> due to



**Fig.7.** Curve-fitted *in situ* Pt4f XP spectra of (a) Pt/TiO<sub>2</sub>-IMP and (b) Pt/TiO<sub>2</sub>-IMP-H samples acquired during heating of the samples in the NH<sub>3</sub>+O<sub>2</sub> mixture. (NH<sub>3</sub>:O<sub>2</sub> ratio of 1:40, total pressure  $p_{\Sigma} \sim 1.4$  mbar).

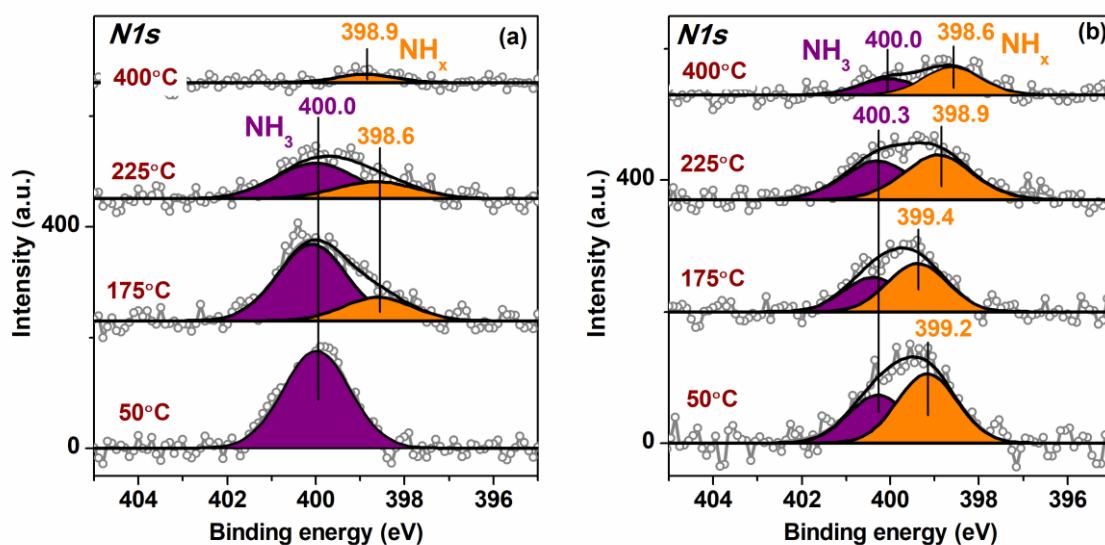
the interaction with the reaction products and intermediates ( $H_2O$ ,  $OH_{ads}$ ). Also, a slight variation of the Pt4f line width during sample treatment in  $NH_3+O_2$  mixture can be observed. The broadening of the Pt4f spectra was caused by the non-uniform charging of the particles surface during the *in situ* NAP-XPS experiments. See ESI for the details.

In case of the Pt/TiO<sub>2</sub>-IMP-H sample the shift of the  $Pt4f_{7/2}$  peak corresponding to the reduced Pt species is more noticeable. Some authors have shown that the encapsulation of the platinum particles by a support with the formation of  $TiO_x$  suboxide layer on the surface of the platinum particles can lead to a positive shift of  $E_b(Pt4f_{7/2})$ .<sup>85,86</sup> The encapsulation of the platinum particles by  $TiO_{2-6}$  when heated in oxygen containing atmosphere is usually observed at rather high temperatures ( $T > 400^\circ C$ ).<sup>67,81</sup> In our work lower temperatures

were used, and the Pt4f/Ti2p intensity ratio changed insignificantly during heating of the sample in the reaction medium. Based on this, we believe that the encapsulation of the platinum particles by  $TiO_x$  suboxide should be excluded. Moreover, encapsulated  $Pt^0$  particles are usually considered catalytically inactive,<sup>44</sup> while we did not observe decrease of the  $NH_3$  conversion during heating. Similar to the Pt/TiO<sub>2</sub>-IMP sample, we can assume that the shift of the Pt4f line can be either associated with the slight change of the surface conductivity during the reaction or with the formation of adsorbed oxygen species ( $O_{ad}$  and/or  $OH_{ad}$ ) on the  $Pt^0$  surface or within the  $Pt^0$ - $TiO_2$  boundary.

Thus, the NAP-XPS data do not show the formation of strongly oxidized platinum species ( $PtO_x$  layers or  $PtO/PtO_2$





**Fig.8.** Curve-fitted *in situ* N1s XP spectra of (a) Pt/TiO<sub>2</sub>-IMP and (b) Pt/TiO<sub>2</sub>-IMP-H samples acquired during heating of the samples in the NH<sub>3</sub>+O<sub>2</sub> mixture (NH<sub>3</sub>:O<sub>2</sub> ratio of 1:40, total pressure p<sub>T</sub>~1.4 mbar).

oxides) during NH<sub>3</sub> oxidation. The obtained data are in a good agreement with the results of the *in situ* study of the interaction of the bulk platinum surface with NH<sub>3</sub>+O<sub>2</sub> reaction mixture,<sup>10</sup> pointing to similarity of the active sites.

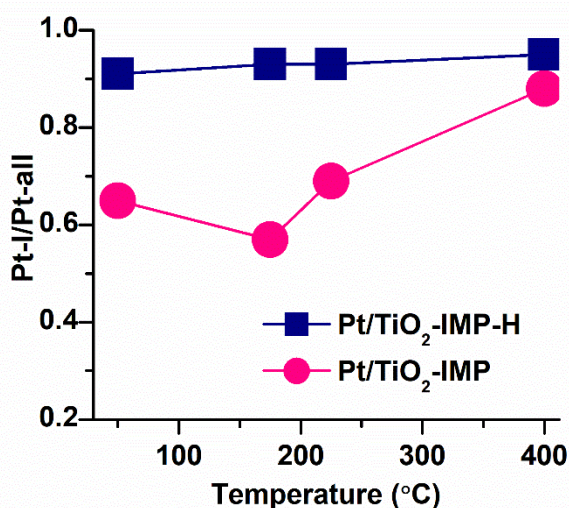
Fig.8 presents *in situ* N1s spectra fitted to the individual components collected for the Pt/TiO<sub>2</sub>-IMP (Fig.8a) and the Pt/TiO<sub>2</sub>-IMP-H (Fig.8b) samples heated in the NH<sub>3</sub>+O<sub>2</sub> mixture at different temperatures. The N1s spectra of the Pt/TiO<sub>2</sub>-IMP sample treated in the NH<sub>3</sub>+O<sub>2</sub> mixture at 50°C show the main peak with E<sub>b</sub>(N1s)~400.0 eV. Such E<sub>b</sub> value was observed after treatment of the TiO<sub>2</sub> support in NH<sub>3</sub> flow at 600°C.<sup>87</sup> The authors assign this N1s peak to Ti-O-N bond. Since we use much lower temperatures, doping of the TiO<sub>2</sub> surface under such conditions is unlikely. NH<sub>3</sub> species adsorbed on the surface of metallic Pt are also characterized by E<sub>b</sub>(N1s)~400.0 eV.<sup>8,10,88</sup> Adsorption of NH<sub>3</sub> on the TiO<sub>2</sub> support surface should also take place. The increase of the temperature results in the appearance of the peak at 398.6-398.9 eV corresponding to adsorbed NH<sub>x</sub> (x=1,2) forms.<sup>8,88</sup> The appearance of such forms indicates dehydrogenation of the NH<sub>3</sub> species, which is a first step of the NH<sub>3</sub> oxidation reaction.<sup>11,89</sup>

It should be noted that for the sample heated in the NH<sub>3</sub>+Ar mixture the N1s spectra also show the peak of the adsorbed NH<sub>3</sub> species (E<sub>b</sub>(N1s)~399.9-400.2 eV), as well as a peak with E<sub>b</sub>(N1s)~398.2-398.4 eV, corresponding to the NH<sub>x,ad</sub> (x=1,2) species (see ESI, Fig.S6). However, the impact of the adsorbed NH<sub>x</sub> on the overall N1s spectrum at all temperatures is low. This result is in a good agreement with the literature data. It is known that the presence of oxygen species adsorbed on the surface of Pt<sup>0</sup> enhances dissociation of NH<sub>3</sub>.<sup>8,89</sup>

At temperatures above 225°C the amount of the adsorbed NH<sub>3</sub> and NH<sub>x</sub> decreases (Fig. 8). In the same temperature range, the selectivity of the reaction changes towards the

formation of NO<sub>x</sub> (Fig.S4). Desorption of NH<sub>x,ad</sub> provides free sites for the oxygen adsorption thus causing a shift of the selectivity towards NO<sub>x</sub> formation.<sup>8</sup> For the reduced Pt/TiO<sub>2</sub>-IMP-H sample, the formation of the adsorbed NH<sub>x</sub> is observed already at 50°C, and the contribution of these species to the overall N1s spectra is higher compared to the Pt/TiO<sub>2</sub>-IMP sample in the entire temperature range. This may be related to the large number of platinum metal species that provide sites for adsorption of ammonia and oxygen. The predominant presence of the dehydrogenated NH<sub>x,ad</sub> species rather than NH<sub>3,ad</sub> on the surface was reported for bulk metal Pt treated in NH<sub>3</sub>+O<sub>2</sub> mixture.<sup>10,90</sup> Note that no NO<sub>ad</sub> species were detected on the samples surface in a good agreement with literature data.<sup>10</sup> The NO desorption is considered to be much faster process than NO formation. It cannot be excluded that at the partial pressure used in NAP-XPS experiments the amount of the NO<sub>x</sub> species adsorbed on the surface is not sufficient for the detection.

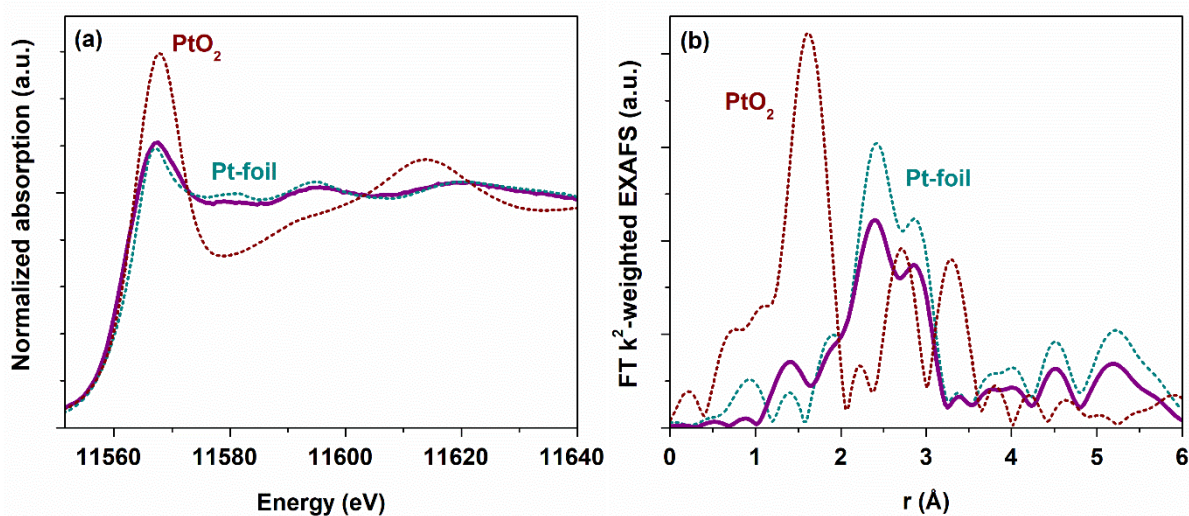
Fig.9 shows variation of the fraction of Pt<sup>0</sup> species for Pt/TiO<sub>2</sub>-IMP and Pt/TiO<sub>2</sub>-IMP-H samples during heating in the NH<sub>3</sub>+O<sub>2</sub> mixture. The fraction of Pt<sup>0</sup> species was calculated as a ratio of the area of the Pt4f peak with E<sub>b</sub>(Pt4f<sub>7/2</sub>)=70.8-71.4 eV



**Fig.9.** Variation of the fraction of the Pt4f peak with  $E_b(\text{Pt}4f_{7/2})=70.8\text{-}71.4$  eV (Pt-I) to the overall Pt4f signal intensity for Pt-TiO<sub>2</sub>-IMP and Pt-TiO<sub>2</sub>-IMP-H samples during NAP-XPS study in the NH<sub>3</sub>+O<sub>2</sub> mixture.

to the overall area of Pt4f spectrum. (Further, “Pt-I” stands for the Pt4f peak with  $E_b(\text{Pt}4f_{7/2})=70.8\text{-}71.4$  eV). For the Pt/TiO<sub>2</sub>-IMP sample, the fraction of the Pt-I peak decreases slightly with an increase of the reaction temperature from 50°C to 175°C, but increases at higher temperatures. The study of the thermal stability of the Pt/TiO<sub>2</sub>-IMP sample (see ESI, Fig.S7) shows that PtO structures are not stable at temperature higher

than 175°C, in a good agreement with literature data.<sup>60,81,82</sup> However, the contribution of the Pt<sup>4+</sup> signal to the Pt4f spectrum remains practically unchanged up to 200°C (Fig.S7). We can propose that in O<sub>2</sub> flow the highly dispersed Pt sites remain in the Pt<sup>4+</sup> state. The higher stability of PtO<sub>x</sub> is known for smaller Pt particles.<sup>62</sup> Also, heating of the Pt/TiO<sub>2</sub>-IMP sample in the reaction mixture from 50 to 225°C results in a slight increase of the Pt4f/Ti2p intensity ratio (from 0.07 to 0.1). The variation of the fraction of the Pt-I peak together with the change in the Pt4f/Ti2p intensity ratio points to the transition of the oxidized PtO to the Pt<sup>0</sup> sites with the adsorbed oxygen species at a temperature range up to 225°C. Such transition might be accompanied by the change of the sample morphology which results in the increase of the Pt4f/Ti2p intensity ratio. Temperature increase to 400°C leads to a significant increase of the fraction of the Pt-I peak as a result of the reduction of PtO and PtO<sub>2</sub> species and increase of the number of Pt<sup>0</sup> sites with the adsorbed oxygen species on the surface. A slight decrease of the Pt4f/Ti2p ratio at this temperature range (from 0.1 to 0.07) might indicate sintering of the platinum particles under treatment in the reaction mixture at higher temperatures. TEM data for the Pt/TiO<sub>2</sub>-IMP sample after the reaction confirms a slight increase of the average size of the platinum particles (See ESI, Fig.S8). For the reduced Pt/TiO<sub>2</sub>-IMP-H sample the fraction of the Pt-I peak remains practically unchanged with the temperature increase. No significant oxidation of the metal Pt<sup>0</sup> is taking place. Only



**Fig.10.** (a) *Ex situ* Pt L<sub>3</sub>-XANES and (b) FT k<sup>2</sup>-weighted EXAFS spectra of Pt/TiO<sub>2</sub>-LAL sample (alongside the data for PtO<sub>2</sub> and metallic Pt reference samples). The EXAFS is Fourier-transformed in the k-range of: 2.5-11.0 Å<sup>-1</sup> and is not corrected for the phase shift.

oxygen species (O<sub>ad</sub> and/or OH<sub>ad</sub>) adsorbed on the Pt<sup>0</sup> surface are formed with the increase of the reaction temperature.

Thus, the NAP-XPS data show that the states of Pt in the analyzed samples upon their treatment in the NH<sub>3</sub>+O<sub>2</sub> mixture at T>225°C are very similar and best described by Pt<sup>0</sup> surface. One can conclude that, despite the difference in the charge states of Pt in the as-prepared samples, the “active” states of the surface observed during the treatment of the samples in the NH<sub>3</sub>+O<sub>2</sub> mixture are similar. The oxidized Pt species initially

present in the Pt/TiO<sub>2</sub>-IMP sample decompose with the temperature increase providing the metallic platinum sites available for oxygen adsorption.

#### XANES/EXAFS study of the Pt/TiO<sub>2</sub> samples

To follow the change of the platinum charge state during the reaction in the bulk, XANES and EXAFS spectroscopy were employed. The experiments were performed for the most active of the studied samples - Pt/TiO<sub>2</sub>-LAL.

XANES and Fourier transformed (FT) extended X-ray absorption fine structure (EXAFS) spectra collected *ex situ* for the Pt/TiO<sub>2</sub>-LAL sample are given in Fig.10. In a good agreement with the data of other methods, the sample contains mostly platinum in the metallic state. The average oxidation state determined by linear combination analysis (LCA) of the XANES data in the energy range between 11550 and 11600 eV is 0.6±0.1. These results are in a good agreement with the XPS data from which the average oxidation state can be estimated as 0.8. Somewhat lower oxidation state observed by XANES may be due to unaccounted number of large Pt NPs (see Fig.2b). FT k<sup>2</sup>-weighted EXAFS spectra (Fig.10b) and the corresponding analysis (Table 2) reveal features very similar to metallic Pt with slightly lower intensity implying rather large (> 2 nm) Pt nanoparticles.<sup>91</sup> No Ti neighbor in the second shell was required to fit the experimental data. (k<sup>2</sup>-weighted EXAFS

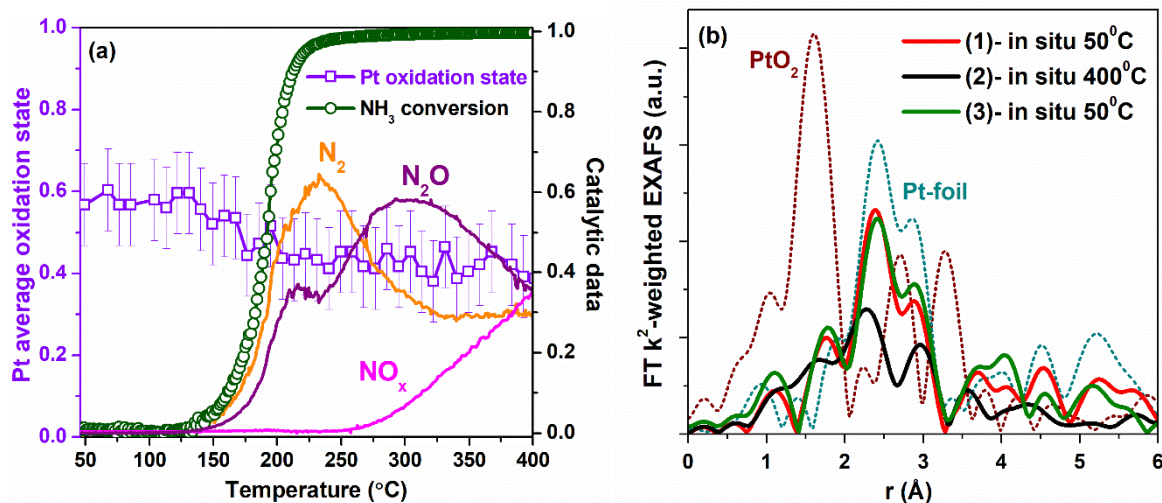
functions and EXAFS fits for all analyzed samples are given in ESI, Fig.S9, and S10). So, EXAFS data do not clearly show the interaction of Pt particles with TiO<sub>2</sub> support (due to very low fraction of Pt atoms at the Pt-TiO<sub>2</sub> interface which would be invisible in the averaged signal). However, the Pt-TiO<sub>2</sub> interaction at the contact of the platinum particles with a TiO<sub>2</sub> surface cannot be ruled out.

Fig.11a presents a trend of the average oxidation state of platinum in the Pt/TiO<sub>2</sub>-LAL sample during the heating in the NH<sub>3</sub>+O<sub>2</sub> mixture (derived from LCA of *operando* XANES (see Fig.S11)), as well as the change of the NH<sub>3</sub> conversion and the yield of reaction products. According to the *operando* XANES analysis, the oxidation state of platinum does not change significantly during the catalytic reaction.

Fig.11b shows Fourier transformed extended X-ray absorption fine structure (EXAFS) spectra for the Pt/TiO<sub>2</sub>-LAL

**Table 2.** Results of EXAFS fitting of Pt/TiO<sub>2</sub>-LAL spectra to a structural model containing O and Pt nearest neighbors.

| Experiment   | Pt-O      |         | Pt-Pt     |          | DW factor (10 <sup>-3</sup> Å <sup>2</sup> ) | δE <sub>0</sub> (eV) | ρ (%) |
|--|-----------|---------|-----------|----------|--|----------------------|-------|
|  | R (Å)     | CN      | R (Å)     | CN       |  |                      |       |
| <i>ex situ</i>                                     | 1.96±0.03 | 0.9±0.2 | 2.76±0.01 | 9.9±1.4  | 4.7±1.0                                      | 6.2±1.2              | 0.7   |
| <i>in situ</i> (50°C)                              | 2.03±0.05 | 0.9±0.5 | 2.76±0.02 | 11.1±3.3 | 6.2±2.2                                      | 7.8±2.2              | 1.6   |
| <i>in situ</i> (400°C)                             | 1.98±0.04 | 1.5±0.5 | 2.75±0.01 | 12.3±3.1 | 12.1±2.7                                     | 6.1±1.7              | 2.5   |
| <i>in situ</i> (50°C), after heating-cooling cycle | 2.04±0.07 | 1.1±0.8 | 2.76±0.02 | 10.2±4.6 | 5.5±3.2                                      | 8.5±3.7              | 2.9   |



**Fig.11.** (a) NH<sub>3</sub> conversion, N<sub>2</sub>, N<sub>2</sub>O, and NO<sub>x</sub> yields, and Pt average oxidation state profiles obtained from *operando* XANES experiments during heating of Pt/TiO<sub>2</sub>-LAL in the NH<sub>3</sub>+O<sub>2</sub> mixture. (The reaction mixture: 880 ppm NH<sub>3</sub>, 10 vol.% O<sub>2</sub>, and 10 vol.% N<sub>2</sub> in He). (b) FT k<sup>2</sup>-weighted EXAFS spectra of Pt/TiO<sub>2</sub>-LAL sample in NH<sub>3</sub> oxidation feed at (1) 50°C and (2) 400°C, and (3) after cooling down to 50°C. The EXAFS is Fourier-transformed in the k-range of: 2.5-11.0 Å<sup>-1</sup> and is not corrected for the phase shift.

sample at temperature plateaus during NH<sub>3</sub> oxidation (during heating- at 50°C and 400°C, after cooling down in reaction mixture to 50°C). Platinum nanoparticles are rather stable during the experiment. The observed decrease in the backscattering intensity in the spectrum measured at 400°C can be attributed only to the increased disorder due to thermal motion (Debye-Waller factor). Qualitatively, one may notice an increased backscattering on the second Pt shell (3.5

– 4.5 Å) which may indicate sintering of Pt nanoparticles due to thermal cycling. Quantification of this effect by EXAFS is not possible due to limited data quality resulting in no statistically significant changes.

Thus, *in situ/operando* methods applied in our study allowed us to follow the evolution of Pt oxidation states under catalytic conditions. The use of NAP-XPS technique revealed the preservation of metallic Pt species on the surface of TiO<sub>2</sub>

under  $\text{NH}_3+\text{O}_2$  conditions even at high reaction temperatures (Fig.7). To bridge pressure gap between NAP-XPS experiments and realistic catalytic conditions *operando* XANES/EXAFS method was applied. Similar to the results of surface sensitive NAP-XPS, analysis of the average oxidation state of Pt within the bulk of the sample by *operando* XANES/EXAFS does not reveal significant oxidation of the metallic platinum species during the reaction, while the appearance of the oxygen species adsorbed on platinum surface cannot be excluded.

Previously, we performed *operando* XANES study of the Pt/ $\text{Al}_2\text{O}_3$  samples in the  $\text{NH}_3+\text{O}_2$  reaction.<sup>69</sup> In contrast to the Pt/ $\text{TiO}_2$  system, it was shown that during the reaction at least 40% of the platinum surface remains oxidized in the form of the  $\text{PtO}_x$  layer regardless of the charge state of platinum in the initial Pt/ $\text{Al}_2\text{O}_3$  catalysts.<sup>69</sup> We can propose that metal-support interaction in Pt/ $\text{TiO}_2$  samples that is practically absent in case of  $\text{Al}_2\text{O}_3$  support might influence the charge state of platinum and its reducibility.

Comparison of the results collected for Pt/ $\text{TiO}_2$  samples prepared by different preparation techniques allowed us to conclude that for the stabilization of the catalytically active metallic Pt species through the metal-support interaction several approaches can be applied: a) the use of defective  $\text{TiO}_2$  as a support that can be provided by application of the pulsed laser ablation in liquids; or b) the reductive pretreatment of highly dispersed Pt nanoparticles prepared by impregnation. *In situ/operando* methods revealed that, in contrast to Pt/ $\text{Al}_2\text{O}_3$  samples,<sup>69</sup> thus stabilized metallic Pt state remains preserved during the reaction. The obtained results show that Pt/ $\text{TiO}_2$  has a high potential for the catalytic application in ASC system as a catalyst for efficient ammonia oxidation at low temperatures.

## Conclusions

The Pt/ $\text{TiO}_2$  samples with different sizes of Pt particles and oxidation state of platinum were prepared by LAL and impregnation methods and tested as catalysts for the ammonia oxidation reaction. The catalysts containing metallic platinum particles showed activity at a lower temperature ( $T_{50}\sim 150^\circ\text{C}$ ) than the catalysts initially containing oxidized platinum species ( $T_{50}\sim 180^\circ\text{C}$ ). A combination of NAP-XPS and *operando* XAS methods was applied to follow the changes on the surface of the samples and within their bulk during the  $\text{NH}_3+\text{O}_2$  reaction. NAP-XPS experiments allowed to differentiate the oxidation states of Pt on the surfaces and follow their evolution under the reaction conditions, as well as detect the surface intermediates. The results showed that decomposition of the  $\text{PtO}_x$  species with the formation of the metallic sites is required to initiate the  $\text{NH}_3+\text{O}_2$  reaction. Only metallic Pt species were observed during the reaction without the formation of a stable  $\text{PtO}_x$  surface oxide layer. Based on the analysis of N1s spectra the  $\text{NH}_{3\text{ads}}$  and  $\text{NH}_{\text{xads}}$  species were detected on the samples surface during the  $\text{NH}_3+\text{O}_2$  exposure. *Operando* XAS experiments allowed to analyze the sample under more realistic conditions at a higher partial pressure of the reagents. They unraveled that, similar to NAP-XPS results,

the average oxidation state of Pt did not change significantly during the reaction with the metallic platinum being the main Pt state. Combination of *operando* XAS and NAP-XPS methods allowed to address the “pressure” gap problem. Similarity of the NAP-XPS and *operando* XAS results confirms the applicability of the NAP-XPS method for the analysis of the processes taking place on the samples surface during the catalytic reaction.

The NAP-XPS experiments were performed for the first time for the supported Pt catalysts in  $\text{NH}_3+\text{O}_2$  reaction. The obtained results demonstrate a good correlation to the data obtained earlier during *in situ* XPS studies of ammonia oxidation over the model Pt systems (single crystals and foils). Thus, we address the “material” gap problem known for the model catalytic studies and confirm the relevance of the results collected on the model catalytic systems for the analysis of the powder catalysts.

A comparison with the results obtained previously for the Pt/ $\text{Al}_2\text{O}_3$  catalysts suggests that the higher activity of the Pt/ $\text{TiO}_2$  systems at lower temperatures might be associated with the metal-support interaction providing the stabilization of Pt in a metallic state. Thus, Pt/ $\text{TiO}_2$  system should be further studied in details as a potential catalyst for low-temperature  $\text{NH}_3$  oxidation.

## Conflicts of interest

There are no conflicts to declare.

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