#### **ORIGINAL PAPER**



# Chemical composition and technofunctional properties of carrot (*Daucus carota* L.) pomace and potato (*Solanum tuberosum* L.) pulp as affected by thermomechanical treatment

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Received: 13 April 2022 / Revised: 30 May 2022 / Accepted: 5 June 2022  $\circledcirc$  The Author(s) 2022

#### Abstract

Fiber rich by-products derived from primary agri-food production such as carrot pomace and potato pulp are available in large quantities, but their functional properties do not necessarily meet the requirements for use in specific food applications. Thermomechanical treatment (extrusion) of carrot pomace and potato pulp changes both dietary fiber polysaccharide structures and technofunctionality of the materials. Solubility of dietary fiber constituents changes, resulting in higher levels of water- and ethanol-soluble poly-/oligosaccharides. On a structural level, particularly arabinans and galactans as neutral side chains of type I rhamnogalacturonan were degraded under thermomechanical stress. Galacturonic acid portions (preferably from homogalacturonan or rhamnogalacturonan I) and their degree of methylation were also negatively affected. On a functional level, water absorption of potato pulp increased up to three times following extrusion, whereas water absorption of carrot pomace decreased with extrusion processing. The observed, enhanced swelling behavior for extruded carrot pomace was accompanied by higher complex viscosity of the dispersions. Swelling of potato pulp particles increased largely (up to 25 times) following extrusion, resulting in highly viscous pastes. Phytochemicals were retained up to 50%, heat-induced contaminants were formed only to a small extent (up to 8.1 mg 5-hydroxymethylfurfural·kg<sup>-1</sup> dry matter for carrot pomace; up to 71 µg acrylamide·kg<sup>-1</sup> dry matter for potato pulp).

#### **Graphical abstract**



Keywords Food by-products · Dietary fiber · Plant cell wall polysaccharides · Pectin · Extrusion · Viscosity

	Abbreviations			
	BfR	German Federal Institute for Risk		
		Assessment		
	DAD	Diode-array detector		
Mirko Bunzel	Dm	Dry matter		
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Extended author information available on the last page of the article				

ESI	Electro-spray ionization
GC	Gas chromatography
HMF	5-Hydroxymethylfurfural
HPAEC	High-performance anion exchange chro-
	matography with pulsed amperometric
	detection
HPLC	High-performance liquid chromatography
IDF	Insoluble dietary fiber
LMW-SDF	Low-molecular weight soluble dietary fiber
LOD	Limit of detection
LOQ	Limit of quantification
MS	Mass spectrometry
PMAA	Partially methylated alditol acetate
RI	Refractive index
SDF	Soluble dietary fiber
SIM	Selected ion monitoring
SME	Specific mechanical energy
TFA	Trifluoroacetic acid
WAI	Water absorption index
WSI	Water solubility index

### Introduction

Dietary fiber, which is mostly composed of non-digestible polysaccharides and oligosaccharides, is known to be beneficial in human nutrition [1]. Diseases such as diabetes mellitus type II are associated with a low-fiber diet [2]. Contrarily, specific dietary fiber constituents can contribute to a positive regulation of blood glucose and cholesterol levels [3, 4]. In addition, dietary fiber intake is closely related to gut health, among other, by positively affecting gut microbiota composition [5, 6]. Therefore, the European Food Safety Authority (EFSA) generally recommends the daily consumption of 25 g of dietary fiber [7], with other recommendations being even higher (IoM [8], up to 38 g for men under age 50). Consequently, there is a trend to enrich various foods with dietary fiber without compromising food quality. Besides their nutritional properties, dietary fiber constituents may offer functional properties such as water binding or gelation [9–11]. However, both nutritional and technological functions strongly differ, depending on the composition and structural details of the fiber constituents.

Incorporation of food by-products derived from primary agri-food production, which are rich in dietary fiber (mostly plant cell wall polysaccharides, but also associated compounds such as lignin and proanthocyanidins), in products such as bread, pasta, and cookies has been widely studied in the last decades [11]. Most often, the by-products were incorporated without further processing. However, several previous studies have shown that thermal and/or mechanical processing modifies the functional properties of by-products [10]. For example, extrusion was shown to be a suitable process to increase the water solubility of food by-products and increase the water holding capacity or viscosity. As a result, syneresis in food products such as deserts and sausages can be decreased or the texture of bread be improved [10]. We recently demonstrated that the functional properties of, for example, apple and chokeberry pomace are strongly affected by extrusion [10, 12–14]. On a polysaccharide structural level, extrusion of these food by-products mainly degraded arabinans as neutral side chains of rhamnogalacturonan I [12, 13].

Whether or not these findings can easily be transferred to other raw materials remains to be answered. Carrot pomace and potato pulp dietary fiber differs from apple pomace fiber mainly in the composition of pectic polysaccharides. Neutral rhamnogalacturonan I side chains of carrot pomace contain arabinans and galactans in approximately equal proportions [15], whereas pectic side chains of potato pulp are rich in galactans [16]. Additionally, potato pulp often contains large portions of residual starch [16, 17], which may affect functional properties, too. Moreover, these raw materials are characterized by their contents of low-molecular weight phytochemicals, with carotenoids being most important for carrot pomace, and chlorogenic acids for potato pulp [1, 9]. Due to material temperatures > 100  $^{\circ}$ C during extrusion, the retention of these nutritionally valuable, but heat-labile substances may be a concern [18, 19]. In addition to a potential degradation of beneficial compounds, toxic phytochemicals such as glycoalkaloids (in potato pomace) and heat-induced contaminants of toxicological concern, such as 5-hydroxymethylfurfural (HMF) and acrylamide, can be present or formed. Acrylamide formation may be especially relevant for potato pulp due to its high levels of asparagine.

Therefore, the aim of this study was to characterize compositional and structural changes of carrot pomace (from juice production) and potato pulp (from starch production) with emphasis on (dietary fiber) polysaccharides, phytochemicals, and heat-induced contaminants caused by extrusion. Additionally, changes of functional properties of the extruded samples were monitored.

#### **Materials and methods**

#### Material

Potato pulp was obtained from Emsland-Stärke GmbH (Emlichheim, Germany). Carrot pomace was kindly provided by GNT Europe GmbH (Aachen, Germany). The residual moisture contents were  $10.3 \pm 0.2\%$  and  $5.7 \pm 0.1\%$  (g·100 g<sup>-1</sup>), respectively (determined by Karl-Fischer titration; Titroline alfa, Schott Instruments GmbH, Germany). Commercially available carrot chips were purchased online. Untreated and extruded materials were milled for 30 s

(coffee mill M55, Petra Electric, Jettingen-Scheppach, Germany) and sieved to a particle size of 0.14 < x < 0.28 mm. The obtained powder was dried at 25 °C and 8 mbar in a vacuum dryer (VO101, Memmert GmbH+Co. KG, Schwabach, Germany) to constant mass.

#### Chemicals

Thermostable  $\alpha$ -amylase Termamyl 120 L (EC 3.2.1.1, from *Bacillus licheniformis*, >500 U·mg<sup>-1</sup> protein (biuret)), amyloglucosidase (EC 3.2.1.3, from Aspergillus niger, 260  $U \cdot mL^{-1}$ ), and protease Alcalase 2.4 L (EC 3.4.21.62, from Bacillus licheniformis, 2.4 AU·g<sup>-1</sup>; all from Sigma Aldrich, St. Louis, Missouri) were used for preparative dietary fiber isolation. A thermostable  $\alpha$ -amylase (EC 3.2.11, from *Bacillus licheniformis*, 3000 U·mL<sup>-1</sup>) and an amyloglucosidase (EC 3.2.1.3, from Aspergillus niger,  $36000 \text{ U} \cdot \text{g}^{-1}$ ; both from Megazyme, Bray, Ireland) were used in the approaches to analyze dietary fiber analysis and starch. In addition, a protease (EC 3.4.21.14, from *Bacillus* licheniformis, 9 U·mg<sup>-1</sup>; Megazyme, Bray, Ireland) was used in the analytical fiber approach. Driselase (from Basidiomycetes) was from Sigma-Aldrich (St. Louis, Missouri). All chemicals and reagents were of analytical grade and purchased from Carl Roth (Karlsruhe, Germany), Merck (Darmstadt, Germany), Sigma-Aldrich (St. Louis, Missouri), or VWR (Radnor, Pennsylvania).

#### **Extrusions processing**

Extrusion trials were carried out on a laboratory-scale corotating twin-screw extruder (Process 11 Hygenic Twin-Screw Extruder, Thermo Fisher Scientific, Karlsruhe, Germany). The extruder had an  $L \cdot D^{-1}$  ratio of 40 and a die of 2 mm (diameter). The screw configuration was a combination of a kneading zone  $(3 \text{ L} \cdot \text{D}^{-1})$  followed by two reverse elements (for detailed schematic illustration see [20], screw configuration 4). The barrel zone consists of eight sections, which can be heated and cooled separately. The barrel temperatures were adjusted to  $T_{\text{barrel1}} = 40 \text{ °C}, T_{\text{barrel2}} = 60 \text{ °C},$  $T_{\text{barrel3}} = 80 \text{°C}$ , and  $T_{\text{barrel4-8}} = 100 \text{°C}$ . Throughout the experiment, the material  $(0.6 \text{ kg} \cdot \text{h}^{-1}, 0.8 \text{ kg} \cdot \text{h}^{-1}, 0.9 \text{ kg} \cdot \text{h}^{-1})$ was fed in the first section, whereas water was added at the second section by a piston-membrane pump (0.4 kg $\cdot$ h<sup>-1</sup>,  $0.2 \text{ kg} \cdot \text{h}^{-1}$ ). Screw speeds of 200 min<sup>-1</sup>, 600 min<sup>-1</sup>, and  $1000 \text{ min}^{-1}$  were applied.

The material temperature  $T_{\rm M}$  of melt was measured in the die adapter. Specific mechanical energy (SME) was calculated as:

$$SME(Wh \cdot kg^{-1}) = \frac{\frac{n}{n_{max}} \cdot \frac{M_d - M_{d,unload}}{100}}{\dot{m}} \cdot P_{max},$$
(1)

where *n* and  $n_{\text{max}}$  are the actual and maximum screw speed (1000 min<sup>-1</sup>),  $M_{d}$  and  $M_{d,\text{unload}}$  are the actual and idle torque (%),  $\dot{m}$  represents the total mass flow (kg·h<sup>-1</sup>), and P<sub>max</sub> the maximum engine power (1.5 kW).

Samples were collected when the conditions were at steady state. For storage, samples were dried for 30 min at 40  $^{\circ}$ C.

#### **Basic compositional analysis**

Protein contents were analyzed using the Kjeldahl approach with ammonia being detected by an ammonia sensitive electrode (nitrogen conversion factor 6.25) [21]. Ash contents were determined after incineration for 4 h at 500 °C. Starch was analyzed quantitatively following degradation into its glucose monomer units [12]. In brief, after enzymatic hydrolysis using a thermostable  $\alpha$ -amylase and amyloglucosidase, liberated glucose was determined by high-performance anion exchange chromatography with pulsed amperometric detection (HPAEC-PAD; Thermo Fisher Scientific, Waltham, Massachusetts). Starch was calculated as the sum of anhydroglucose. Mono- and disaccharides were determined after aqueous extraction with ultrasonic treatment (four times) using HPAEC-PAD (Thermo Fisher Scientific, Waltham, Massachusetts) as described in detail in [12]. pH was measured with a pH electrode (500 mg of sample in 5 mL of water). To compare data, the pH of recently analyzed apple pomace and its extrudates [12, 13] were also recorded (Table S2).

#### **Dietary fiber analysis**

To determine contents of insoluble dietary fiber (IDF), soluble dietary fiber (SDF), and low-molecular weight soluble dietary fiber (LMW-SDF), a combination of the methods AOAC 985.29 [22] and AOAC 2009.01 [23] was applied. The principle of the method is based on enzymatic digestion of starch and proteins by applying a sequence of thermostable  $\alpha$ -amylase, protease, and amyloglucosidase. SDF and LMW-SDF were differentiated according to their (in)solubility in 80% ethanol. Ethanol-soluble LMW-SDF was obtained from the filtrate after precipitation of SDF and analyzed by size-exclusion chromatography (Hitachi, Merck, Darmstadt, Germany) with refractive index (RI) detection (Knauer, Berlin, Germany) using a TSKgel PWxl guard column (40 mm  $\times$  6.0 mm, particle size 12  $\mu$ m, Tosoh, Tokyo, Japan) and two size-exclusion columns in a row (TSKgel G2500PWxl, 300 mm × 7.8 mm, particle size 13 µm, Tosoh, Tokyo, Japan) [12]. IDF and SDF contents were corrected for residual protein [21] and ash contents.

#### Preparative dietary fiber isolation

Preparative isolation of IDF and SDF was carried out following the principles of AOAC method 985.29 using an enzymatic treatment (thermostable  $\alpha$ -amylase, protease, and amyloglucosidase) as described by Bunzel et al. [24].

#### Molecular weight distribution

SDF was dissolved in 50 mM sodium nitrate ( $2 \text{ g} \cdot \text{L}^{-1}$ ) and treated for 24 h at 40 °C. The supernatant was used for the separation of oligo-/polysaccharides based on their hydrodynamic volumes using HPLC-RI (Hitachi, Merck, Darmstadt, Germany) equipped with a guard column (TosohTSK-gel PWxl 40 mm × 6.0 mm, particle size 12 µm, Tosoh, Tokyo, Japan) and two size-exclusion columns in series (TosohTSK-gel G6000PWxl 300 mm × 7.8 mm, particle size 13 µm; TSKgel G4000PWxl 300 mm × 7.8 mm, particle size 10 µm, Tosoh, Tokyo, Japan). Sodium nitrate was used as eluent at a flow rate of 0.5 mL·min<sup>-1</sup> at 50 °C. Dextrans were used for calibration [13].

#### **Polysaccharide analysis**

#### Monomer composition

The monomer composition of dietary fiber polysaccharides was determined by HPAEC-PAD (Thermo Fisher Scientific, Waltham, Massachusetts) after sulfuric acid hydrolysis (IDF) [25] or methanolysis followed by trifluoroacetic acid (TFA) hydrolysis (SDF) [26]. To determine the monomer composition of the oligosaccharides of LMW-SDF, they were semi-preparatively separated from mono- and disaccharides by HPLC-RI, followed by TFA based hydrolysis of the glyosidic linkages [12].

#### **Methylation analysis**

Methylation analysis of IDF, SDF and LMW-SDF poly-/ oligosaccharides was performed as previously published [27]. In brief, methylation was performed twice with methyl iodide in DMSO/NaOH. Extraction was done using dichloromethane. Methylated poly-/oligosaccharides were hydrolyzed using TFA, reduced with sodium borodeuteride, and acetylated with acetic anhydride using 1-methylimidazole as a catalyst. Identification of the partially methylated alditol acetates (PMAAs) was performed by gas chromatography (GC) and mass spectrometric (MS) detection. PMAAs were semi-quantitatively calculated using GC coupled to a flame ionization detector applying molar response factors [28].

#### Arabinan and galactan profiling

Detailed characterization of neutral rhamnogalacturonan I side chains of SDF and IDF polysaccharides was carried out following partial hydrolysis using *endo*-arabinanase and *endo*-galactanase as described previously [29]. Liberated oligosaccharides were determined semi-quantitatively by HPAEC-PAD (Thermo Fisher Scientific, Waltham, Massachusetts).

#### Degree of (pectin) esterification

Polymer-bound galacturonic acid contents were analyzed spectrophotometrically using the Blumenkrantz procedure [30]. To calculate the degree of esterification of IDF and SDF pectins, quantitative <sup>1</sup>H-NMR spectroscopy was performed [31]. A suspension of 20 mg sample in 1.5 mL of 2 M NaOH (in D<sub>2</sub>O) was ultrasonicated for 2 h. Trimethyl-silylpropanoic acid- $d_4$  (0.5 mg·mL<sup>-1</sup>) was added as internal standard. A standard <sup>1</sup>H-NMR pulse program (zg30) was used on a Bruker Avance 500 MHz instrument (Ettlingen, Germany), 32 scans were acquired with 65,536 data points and an acquisition time of 3.28 s, and a relaxation delay of 35 s were applied. The degree of methylation and acetylation was calculated related to uronic acid contents.

#### Analysis of potential heat-induced contaminants

HMF was determined as previously published [32, 33], applying minor modifications. Sample material (50 mg) was shaken in 900  $\mu$ L of water for 30 min at 800 rpm. Carrez I (150 g·L<sup>-1</sup> K<sub>4</sub>[Fe(CN)<sub>6</sub>]•3H<sub>2</sub>O) and Carrez II (300 g·L<sup>-1</sup> ZnSO<sub>4</sub>•7H<sub>2</sub>O) solutions (50  $\mu$ L each) were successively added, and samples were vortexed and centrifuged. Supernatants were passed through a syringe filter (regenerated cellulose, 0.45  $\mu$ m) and analyzed by HPLC with diode-array detection (DAD; Shimadzu, Kyõto, Japan). A Luna C18(2) (250×4.6 mm, particle size 5  $\mu$ m; Phenomenex, Torrance, California) column was used, and water (A) and acetonitrile were applied as eluents in linear gradients (0 min 95% A, 35 min 75% A, 40 min 0% A, 45 min 0% A, 46 min 95% A, 50 min 95% A). The flow rate was 1 mL·min<sup>-1</sup>. Calibration was performed externally in the range of 5–200  $\mu$ M.

Acrylamide contents were analyzed externally by LC–MS/MS according to an accredited method (DIN EN 16618:2015-06).

#### Analysis of low-molecular weight phytochemicals

#### Carotenoids

Carotenoid contents were analyzed according to Abdel-Aal and coworkers (1996) [34]. Sample material (1 g) was

weighed into a brown tube, mixed with 1 mL of Driselase suspension (10 mg·mL<sup>-1</sup>) and 1 mL of water, and allowed to stand overnight under nitrogen. Ethyl acetate (7 mL) was added, and the mixture was left in the dark for 1 h at room temperature after brief vortexing. After vortexing again, the mixture was left in the dark for another 30 min at room temperature. After centrifugation, the supernatant was removed, and extraction was repeated using 3 mL of ethyl acetate and allowing the mixture to stand for 1 h. After centrifugation, the supernatants were combined and made up to 10 mL with ethyl acetate. After filtration (PTFE, 0.45 µm), extracted carotenoids were analyzed by HPLC-DAD (Beckman, Brea, California) on a ProntoSIL C30 column (250×4.6 mm, particle size 5 µm; Bischoff, Leonberg, Germany). Methanol/ methyl tert-butyl ether/water (A, 81/15/4) and methanol/ methyl tert-butyl ether (10/90) each containing 0.1% butylhydroxytoluene were used as eluents. The gradient was as follows: 0 min 100% A, 20 min 40% A, 35 min 40% A, 40 min 100% A, 45 min 100% A. The flow rate was 1.2 mL·min<sup>-1</sup>, the temperature was hold at 30 °C, and the eluent was monitored at 450 nm. Calibration was performed using standard compounds ( $\alpha$ -carotene,  $\beta$ -carotene) dissolved in ethyl acetate with 0.1% butylhydroxytoluene, and concentrations were determined spectrophotometrically at 446 nm ( $\alpha$ -carotene) and 448 nm ( $\beta$ -carotene) after evaporation and dissolving in *n*-hexane [35, 36].

#### Glycoalkaloids

Previously published procedures were modified to analyze glycoalkaloids [37, 38]. Potato pulp sample (37 mg) was mixed with 5% acetic acid, vortexed, shaken for 15 min at room temperature, centrifuged, and the supernatant was collected. The extraction procedure was repeated three times. Combined supernatants were filled up to a volume of 5 mL and filtered (PTFE, 0.45 µm). Quantification was performed by using UHPLC (Shimadzu, Kyõto, Japan) electro spray ionization (ESI) MS (LCMS 2020, Shimadzu, Kyõto, Japan). Samples were loaded onto a Luna Omega Polar C18 column  $(150 \times 2.1 \text{ mm}, \text{ particle size } 1.6 \,\mu\text{m}; \text{Phenomenex},$ Torrance, California) using water (A) and acetonitrile each containing 0.1% formic acid as eluents. The linear gradient was composed as follows: 0.1 min 74% A, 7.0 min 74% A, 8 min 72% A, 9 min 10% A, 12 min 10% A, 13 min 74% A, 15 min 74% A. The flow rate was 0.5 mL·min<sup>-1</sup>, the temperature was held at 40 °C. ESI-MS detection was performed in positive selected ion monitoring (SIM) mode (4.5 kV) at a nebulization gas flow (nitrogen) of  $1.5 \text{ L} \cdot \text{min}^{-1}$ and 20 L·min<sup>-1</sup> drying gas. The interface temperature was set to 350 °C, the desolvation line temperature was 300 °C, and the heating block was operated at 250 °C. Glycoalkaloids were detected by monitoring their  $[M + H]^+$  ions (*m/z* 868.4  $\alpha$ -solanine and *m/z* 852.4  $\alpha$ -chaconine).

#### Chlorogenic acid

Chlorogenic acid (5-caffeoylquinic acid) contents in the potato samples were determined by UHPLC-DAD (Knauer, Berlin, Germany) according to the methods of Ceymann and coworkers (2011) [39] and Malec and coworkers (2014) [40]. Sample (0.5 g) was weighed into a brown tube, and 3.75 mL of methanol containing 5% formic acid was added. After 15 min of ultrasonic treatment (35 kHz) at 30 °C, the sample was vortexed and centrifuged. Immediately before measurement, an aliquot of the supernatant (750 µL) was evaporated, and the dried residue was dissolved in 100 µL of water/acetonitrile (97/3) containing 2% formic acid and analyzed on a Kinetex C 18(2) (150 × 4.6 mm, particle size 2.6 µm; Phenomenex, Torrance, California) column at 40 °C. Eluents to form a linear gradient (flow rate 1 mL $\cdot$ min<sup>-1</sup>) were water (A) and acetonitrile each with 2% formic acid (0 min 97% A, 5 min 97% A, 25 min 92% A, 45 min 74% A, 52 min 40% A, 54 min 0% A, 59 min 0% A, 61 min 97% A, 68 min 97% A). Detection was carried out at 320 nm.

# Water solubility index (WSI) and water absorption index (WAI)

WSI and WAI were determined similar to Anderson et al. [41]. Untreated and extruded materials (0.5 g) were vortexed for 30 s and mixed for 24 h with demineralized water (19.5 g). For WSI determination, tubes were centrifuged (4250×g, 50 min, 25 °C), and for WAI determination, tubes were not centrifuged but rested 1 h for sedimentation before separation of supernatant and precipitate. Supernatant and precipitate were dried at 80 °C, normal pressure for 72 h and weighed. WSI and WAI were calculated according to the following equations:

WSI = 
$$\frac{m_{\text{supernatant,dried}}}{m_{\text{powder}}}$$
, (2)

$$WAI = \frac{m_{\text{preciptate,wet}} - m_{\text{preciptated,dried}}}{m_{\text{preciptated,dried}}}.$$
(3)

#### **Rheological properties**

To prepare dispersions, the ground, sieved, and dried materials (1 g) were mixed with demineralized water (10 g) and stirred on a magnetic mixer (200 min<sup>-1</sup>) for 10 min, sealed with parafilm and rested for 50 min. Rheological properties were analyzed using an Anton Paar Rheometer MC 301 (Graz, Austria) with a parallel plate geometry (50 mm) and a measurement gap of 1.5 mm.

First, samples rested for 90 s in the geometry, afterwards the samples were sheared (oscillatory) at 25 °C with an amplitude of 0.1% and a frequency of 1 Hz (within the linear viscoelastic region). Over a time period of 90 s, ten data points were measured and the average was calculated. The shown complex viscosity  $\eta^*$  is a mean value of nine measurement points.

#### Scanning electron microscopy (SEM)

Extruded, milled, sieved and dried samples were fixed with platinum. A LEO 1530 (Carl Zeiss, Oberkochen, Germany) scanning electron microscope at high vacuum was used to observe the particles. All images were taken at an operating voltage of 3 kV.

#### **Microscopic swelling behavior**

Image processing using a light microscope Eclipse LV100ND (Nikon, Tokyo, Japan) was performed to observe the swelling of particles (0.14 < x < 0.28 mm) in demineralized water for 90 min with a 20-fold magnification. The particle size was evaluated using ImageJ, whereby the particles were circled by hand.

#### Statistics

Quantitative data including data from WAI/WSI determinations and rheological measurements are presented as mean  $\pm$  standard deviation (n = 3). Statistical analyses were performed for quantitative data using OriginPro 2020 9.7.0.188. Differences among samples were tested for statistical significance by using ANOVA, followed by Tukey test ( $\alpha = 0.05$ ). Semiquantitative structural analyses of isolated IDF, SDF, and LMW-SDF (molecular weight distribution, monosaccharide composition, methylation analysis, arabinan and galactan profiling) were performed in duplicate and are given as mean  $\pm$  half range (n=2). Also, experiments to analyze the microscopic swelling behavior were performed in duplicate.

### **Results and discussion**

#### Compositional analysis of the starting material

Protein, ash, starch, free mono- and disaccharide contents (dry matter basis), and pH of the applied carrot pomace and potato pulp samples are shown in Table 1 and Table S1. The high starch content of potato pulp and the larger contents of mono- and disaccharides in carrot pomace as compared to potato pulp are highlighted with respect to data presented below.

As shown in Fig. 1, the potato pulp dietary fiber fraction is largely dominated by IDF (IDF: 54.2 g·100 g<sup>-1</sup> dm; SDF: 9.2 g·100 g<sup>-1</sup> dm, LMW-SDF was not detected; reported on a dry matter (dm) basis and to be discussed in more detail later). As we used a thermostable  $\alpha$ -amylase to determine dietary fiber contents, the contribution of resistant starch to dietary fiber can be excluded. This approach was chosen because we were interested in the fate of non-starch polysaccharides as dietary fiber contents and less in the fate of starch. This is because the contribution of starch to dietary fiber in the final food

**Table 1** Compositional analysis of carrot pomace and potato pulp before and after extrusion  $[g \cdot 100 g^{-1} dry matter, mean \pm standard deviation, n=3, pH: n=1)]$ 

	Carrot pomace				Potato pulp				
$W_{H2O}[\%]$	Untreated	25	43	25	Untreated	46	28 200	28	
SME [Wh•kg <sup>-1</sup> ]		200 175.0	253.8	385.0		186.0	213.5	376.5	
<i>Т</i> <sub>М</sub> [°С]		116.5	116.5	130.0		109.5	118.0	133.5	
Free mono- and	disaccharides	6							
Glucose <sup>a</sup>	$1.7$ $\pm$ 0.2 $^{\rm A}$	$1.6 \pm 0.2^{\text{A}}$	2.1 $\pm$ 0.4 $^{\rm A,B}$	$2.4~\pm~0.1$ $^{\rm B}$	0.02 $\pm$ 0.005 $^{\rm A}$	0.02 $\pm$ 0.01 $^{\rm A}$	0.02 $\pm$ 0.01 $^{\rm A}$	0.01 $\pm$ 0.002 $^{\rm A}$	
Fructose <sup>a</sup>	$1.8\pm0.2$ $^{\rm A}$	$1.9\pm0.3$ $^{\rm A}$	$2.7~\pm~0.6$ $^{\rm A,B}$	3.5 $\pm$ 0.1 $^{\rm B}$	0.09 $\pm$ 0.2 $^{\rm A}$	0.1 $\pm$ 0.03 $^{\rm A,B}$	$0.06\pm0.01^{\rm A,B}$	0.04 $\pm$ 0.01 $^{\rm B}$	
Sucrose <sup>a</sup>	4.4 $\pm$ 0.5 $^{\rm A}$	$4.2\pm0.4$ $^{\rm A}$	4.8 $\pm$ 0.9 $^{\rm A}$	$1.1 \pm 1.0^{\text{ B}}$	<loq< td=""><td><loq< td=""><td><math>0.01 \pm 0.001</math></td><td><loq< td=""></loq<></td></loq<></td></loq<>	<loq< td=""><td><math>0.01 \pm 0.001</math></td><td><loq< td=""></loq<></td></loq<>	$0.01 \pm 0.001$	<loq< td=""></loq<>	
Maltose <sup>a</sup>	0.8 $\pm$ 0.1 $^{\rm A}$	$1.0\pm0.2$ $^{\rm A,B}$	$1.4 \pm 0.4$ <sup>B</sup>	$1.2 \pm 0.2^{A,B}$	0.1 $\pm$ 0.01 $^{\rm A}$	0.1 $\pm$ 0.01 $^{\rm A}$	0.1 $\pm$ 0.002 $^{\rm A}$	$0.2~\pm~0.02$ $^{\rm B}$	
ta	3.95	3.94	3.91	3.93	5.37	5.33	5.30	5.07	

Extrusion conditions vary in overall water content ( $w_{H2O}$ ) and screw speed (*n*) at a barrel temperature of 100 °C resulting in different specific mechanical energies (SME) and material temperatures ( $T_{M}$ )

<LOQ below limit of quantification

<sup>a</sup>Means within a row and a food by-product that are marked with different letters differ significantly (ANOVA, Tukey test,  $\alpha = 0.05$ )



**Fig. 1** Dietary fiber contents (g·100 g<sup>-1</sup> dry matter (dm), mean  $\pm$  standard deviation, n=3) of untreated and extruded carrot pomace and potato pulp samples. The extrusion conditions varied in overall water content (w<sub>H2O</sub>) and screw speed (*n*), the barrel temperature was set to 100 °C resulting in different specific mechanical

products (in which the food by-products are used as ingredients) depends on several parameters, which cannot be mimicked in its entirety here. IDF also dominates in carrot pomace (37.4 g·100 g<sup>-1</sup> dm); however, the SDF content (26.7 g·100 g<sup>-1</sup> dm) is higher than in potato pulp and even some LMW-SDF was detected in the starting material (1.9 g·100 g<sup>-1</sup> dm). Contents of 13–23 g·100 g<sup>-1</sup> dm were previously described for SDF of carrot pomace, too [1, 42, 43].

Finally, it should be noted that the raw materials that were used for the extrusion experiments differed in their water contents (potato pulp: 10.3%; carrot pomace: 5.7%).



# Influence of extrusion parameters on the extent of thermomechanical treatment

As expected, SME increased with increasing screw speed for both materials and decreased with increasing water contents (Fig. 2). For carrot pomace and a water content of 43%, the increase of screw speed from 200 to 1000 min<sup>-1</sup> led to an increase of SME from 73.5 to 253.8 Wh kg<sup>-1</sup>. By reducing the water content to 25%, the SME increased by ~ 100 Wh kg<sup>-1</sup> at each screw speed. For potato pulp, a significant increase in SME with a reduction in water content from 46 to 28% was observed, too. Material temperatures showed similar tendencies for increasing screw speeds and





**Fig. 2** Dependency of the specific mechanical energy input (SME) (**A**) and material temperature  $(T_{\rm M})$  (**B**) on screw speed (*n*) for potato pulp (triangles) and carrot pomace (quadrangles) for various overall water contents (w<sub>H20</sub>) and a barrel temperature ( $T_{\rm B}$ ) of 100 °C; total

feed rate ( $\dot{m}$ ): 1 kg•h<sup>-1</sup>. Extrusion conditions that were chosen to perform an in-depth chemical/functional analysis are marked by black bordered symbols

decreasing water contents. For example, the material temperature of carrot pomace increased at both water contents by 15 °C when the screw speed was increased from 200 to 1000 min<sup>-1</sup>. Generally, under comparable conditions, higher SME values and material temperatures were determined for potato pulp as compared to carrot pomace. Based on the demonstrated variability of SME and material temperatures at different conditions, three samples of each starting material were chosen for a detailed chemical and functional analysis. These samples comprised: carrot pomace: (a) water content ( $w_{H2O}$ ) 25%, screw speed (*n*) 200 min<sup>-1</sup>; (b)  $w_{H2O}$ =25%, *n*=1000 min<sup>-1</sup>; (c)  $w_{H2O}$  43%, *n*=1000 min<sup>-1</sup>; potato pulp: (a)  $w_{H2O}$ =28%, n=200 min<sup>-1</sup>; (b)  $w_{H2O}$ =28%, *n*=600 min<sup>-1</sup>; (c)  $w_{H2O}$ =46%, *n*=600 min<sup>-1</sup> (black bordered symbols, Fig. 2).

# Influence of extrusion on the morphology of particle surfaces

Scanning electron microscope images showed that particles of the starting material of carrot pomace had a rougher surface as compared to the surface of potato pulp particles (Fig. 3). No apparent alterations of the surface of the carrot pomace particles after extrusion processing were observed. Neither an increase in screw speed nor higher water contents modified the surface of carrot pomace particles. In contrast, the surface of the potato extrudate particles became rougher with increasing thermomechanical treatment, which was observed for apple pomace, too [12, 13].

#### Compositional data as affected by extrusion

Compositional data (protein, ash, starch, free monoand disaccharide contents, pH) demonstrated that thermomechanical treatment by extrusion has less of an impact on the parameters analyzed here for both by-products, with the exception of the sugar composition (Table 1; dietary fiber data are discussed in more detail below). The sucrose content of carrot pomace decreased sharply (by 3.3 g·100 g<sup>-1</sup> dm) under maximum stress ( $w_{H20}=25\%$ , n=1000 min<sup>-1</sup>). In contrast, contents of glucose and fructose increased suggesting the hydrolytic cleavage of the glycosidic linkage of sucrose during extrusion. Thus, although reaction of the reducing monosaccharides can be expected during extrusion (e.g., in the Maillard reaction) their contents increase with increasing thermomechanical stress.

# Contents of dietary fiber and its composition as affected by extrusion

In general, a decrease of IDF contents of carrot pomace and potato pulp was observed due to thermomechanical treatment, whereas contents of SDF increased (Fig. 1). This is in line with previous data obtained from extrusion of apple pomace [12, 13, 44] and for heat-treated carrots, where an increased pectin solubility was shown for blanched carrots [45]. Under maximum thermal and mechanical stress  $(w_{H2O} = 25\%, n = 1000 \text{ min}^{-1})$ , carrot pomace contained even more SDF than IDF. An increase of SDF was also evident as a consequence of the extrusion of potato pulp, with the highest extent at maximum SME ( $w_{H2O} = 28\%$ ,  $n = 600 \text{ min}^{-1}$ ). However, for potato pulp, the content of SDF did not consistently increase with increasing SME but other (unknown) factors appear to be a factor, too. LMW-SDF contents did not change significantly for carrot pomace, whereas in case of potato pulp LMW-SDF contents could be detected following treatment at higher screw speed  $(n = 600 \text{ min}^{-1}).$ 



**Fig.3** Scanning electron microscope images of untreated and extruded carrot pomace and potato pulp. The extrusion conditions vary in overall water content ( $w_{H2O}$ ) and screw speed (*n*) at a barrel

temperature of 100  $^\circ\rm C$  resulting in different specific mechanical energies (SME) and material temperatures ( $T_{\rm M}$ )

The results clearly indicate solubilization of dietary fiber during the extrusion processing; however, the extent of solubilization appears to be dependent on the individual extrusion parameters. Extrusion-based solubilization can also be suggested from the molecular weight distribution of the water-soluble material, which, for both by-products, became distinctly broader after extrusion (Fig. 4). However, both increase of SDF and broadening of the molecular weight range may also, at least partially, be explained by the formation of Maillard reaction products. The additional peak at approximately 15 mL (> 670 kDa) for carrot pomace (Fig. 4) may indicate the formation of such products by extrusion, which, however, cannot be confirmed for potato pulp, as a distinct peak at 14 mL was already seen in the untreated sample.

### Composition of dietary fiber non-starch polysaccharides as affected by extrusion

#### Insoluble dietary fiber polysaccharides

The main monosaccharide of the non-starch polysaccharides of the untreated food by-products liberated after acid hydrolysis of IDF is glucose (Fig. 5, Table S3).

This suggested, in conjunction with data from methylation analysis (Table S4, the presence of cellulose, which is composed of  $\beta$ -1,4-glucopyranose units. The portion of the PMAA of 1,4-glucopyranose was determined to be 56.0 mol% for carrot pomace and 50.2 mol% for potato pulp. Glucose as a monomer can also be released from xyloglucans, which consist of  $\beta$ -1,4-linked glucopyranose units largely substituted with xylose at position O-6 [46]. PMAAs of 1,4,6-glucopyranose and terminal xylose units were detected for carrot pomace and potato pulp, suggesting the presence of xyloglucans. Additional hemicelluloses such as xylans and mannans were also identified in both by-products based on the identification of PMAAs resulting from 1,4-xylopyranose (carrot pomace: 5.4 mol% and potato pulp: 1.8 mol%,) and 1,4-mannopyranose (carrot pomace: 5.7 mol%, and potato pulp: 1.8 mol%) units. Overall, water insoluble hemicelluloses tend to be present as minor components only, whereas pectins appear to be the second dominant insoluble polysaccharides next to cellulose in both by-products. Pectins are dominantly composed of homogalacturonan and rhamnogalacturonan I, with the latter bearing oligo-/polymeric arabinan and (arabino)galactan side chains. High portions of pectic monomers such as arabinose (carrot pomace: 9.7 mol% and potato pulp: 10.3 mol%), galactose (carrot pomace: 14.7 mol% and potato pulp: 35.0 mol%,), and galacturonic acid (carrot pomace: 9.0 mol% and potato pulp: 7.9 mol%) were liberated after acidic hydrolysis. The 1,4-linked galacturonic acid units of homogalacturonan are partially substituted with methyl and/or acetyl groups. For carrot pomace IDF, the portion of methyl esterified galacturonic acid (57%) and the degree of acetylation (78%) was higher as compared to potato pulp (35% degree of methylation, 38% degree of acetylation; Table S7). Different from homogalacturonan, the backbone of rhamnogalacturonan I additionally contains alternating 1,2-linked rhamnopyranose units, which can be substituted at position O-4 with aforementioned arabinans and/or (arabino-)galactans. The





**Fig.4** Molecular weight distribution of soluble dietary fiber (SDF) polymers of untreated and extruded carrot pomace and potato pulp as determined by high pressure liquid chromatography with refractive index detection, applying dextrans for calibration (gray lines,

5–670 kDa). The extrusion conditions vary in overall water content ( $w_{H2O}$ ) and screw speed (*n*) at a barrel temperature of 100 °C resulting in different specific mechanical energies (SME) and material temperatures ( $T_{\rm M}$ )

**Fig. 5** Monosaccharide composition (mol%) of insoluble dietary fiber (IDF, n=2), soluble dietary fiber (SDF, n=2), and low-molecular weight soluble dietary fiber (LMW-SDF, n=3) of untreated and extruded carrot pomace and potato pulp. The extrusion conditions vary in overall water content (w<sub>H2O</sub>) and screw speed (n) at a barrel temperature of 100 °C resulting in different specific mechanical energies (SME) and material temperatures ( $T_{\rm M}$ )



17.2

7.8

53.3 52.7

21.7

53.6

21.1

3.6

12.8 13.3 13.2

Untreated

WH20 46%; n 600 min'

186.0 Whike"1; T<sub>12</sub> 109.5 \*

SME

28%; n 200 min'

WHZO SME 213.5 Wh

-kg<sup>-1</sup>; T<sub>M</sub> 118.0 \*



100

mol%

0



ratio of rhamnose to galacturonic acid was 1:4 for both the untreated carrot pomace and the potato pulp, indicating almost similar portions of homogalacturonan and rhamnogalacturonan I. However, IDF pectins of the raw materials differ in their composition of neutral type I rhamnogalacturonan side chains. Potato pulp pectins are rich in galactans as demonstrated by higher galactose (35 mol%) than arabinose (10.3 mol%) contents, being consistent with literature data [16, 17]. Carrot pomace pectins contain more comparable portions of arabinose and galactose and, therefore, less divergent portions of arabinans and galactans as previously reported [15]. Structural details were obtained from methylation analysis. Arabinan side chains consist of 1,5-linked arabinofuranose units that can be substituted at position O-2 and/or position O-3. Almost equal portions of 1,3,5-arabinofuranose (2.4 mol%) and 1,5-arabinofuranose (3.3 mol%) units were determined for carrot pomace IDF (Table S4), indicating highly branched arabinans, with branches being almost exclusively in position O-3. This was confirmed by an arabinan profiling approach [29]. After incubation of carrot pomace IDF with endo-arabinanase, those oligosaccharides that are exclusively linked in position O-3 (total 23.8 mol%) (A-4a, A-6a, A-7b, Fig. S1, Table S5) dominated the liberated, branched oligosaccharides. Only smaller amounts (total 11.1 mol%) of oligosaccharides linked in position O-2 (A-4b, A-7a, Fig. S1, Table S5) were observed. In addition, highly branched oligomers were identified, for example A-7a, which contains neighboring backbone units that are substituted in position O-3 and in both positions O-2and O-3, respectively. In contrast, arabinans of potato pulp pectins appear to be more linear and less branched in position O-3 (2.9 mol% 1,3,5-arabinofuranose vs. 10.6 mol% 1,5-arabinofuranose units), which was confirmed by our arabinan profiling approach (Table S5). Galactans are composed of 1,4-galactopyranose units that can contain terminal and/or internal 1,4-linked arabinopyranose units [47]. Galactan structures of both raw materials appeared to be quite similar. PMAAs resulting from 1,4-linked galactopyranose units were detected in IDF of carrot pomace and potato pulp; however, in the past, we often observed an underestimation of this PMAA. This was clearly evident from the data of potato pulp IDF. In total, the portion of PMAAs resulting from arabinose units was 18.6 mol% versus 15 mol% for PMAAs resulting from galactose units (Table S4), although galactose largely dominates over arabinose in the monomer composition of potato pulp IDF after sulfuric acid hydrolysis (Fig. 5). Incubation of IDF with endo-galactanase (Table S6, Fig. S1) showed that galactans of both raw materials contain internal 1,4-linked arabinopyranose units, which cannot be differentiated from 1,5-linked arabinofuranose units by methylation analysis.

#### Soluble dietary fiber polysaccharides

The monomer composition of potato pulp SDF polysaccharides is dominated by galactose, whereas a more balanced ratio between galacturonic acid, arabinose, and galactose, all of which being pectin monomers, was found for carrot pomace (Fig. 5, Table S3). Structures of SDF pectins of both fiber sources appear to be widely comparable to those of IDF, although a difference exist. For example, a higher galactose (28.6 mol%) to arabinose (24.6 mol%) ratio was found for carrot pomace SDF pectins as compared to carrot pomace IDF pectins (Fig. 5, Table S3).

#### **Dietary fiber oligosaccharides**

LMW-SDF oligosaccharides from untreated carrot pomace were mainly composed of arabinose, followed by glucose and mannose (Fig. 5, Table S3). Arabinose appears to stem from arabino-oligosaccharides, which were mainly linear with a few branches in position O-3 (Table S4). Surprisingly large portions of mannose (17.8 mol%) and glucose (28.0 mol%) were present in the LMW-SDF. Glucose was potentially released from either malto-oligosaccharides or cello-oligosaccharides as degradation products of starch or cellulose, respectively. Although malto-oligosaccharides may theoretically stem from incomplete starch degradation during the dietary fiber isolation, this does not appear to be the most likely option because comparable oligosaccharides were not identified in potato pulp fiber fractions that contained much larger starch contents than carrot pomace. Analysis by <sup>1</sup>H-NMR spectroscopy to investigate the anomeric configuration of the oligomer bound glucose units was not successful because the concentrations were too low for this analytical approach.

### Extrusion-based structural modifications of dietary fiber polysaccharides

Structural modifications during extrusion processing are judged by the interpretation of data from the monomer compositional analysis, methylation analysis, and both arabinan and galactan profiling approaches. Thus, it should always be kept in mind that data are normalized to 100 mol%. As a result, the portions of specific monomers or structural elements may be increased, often being misinterpreted as a synthesis of the structural elements or polymers that contain these monomers during extrusion. However, the certainly more likely explanation is that due to degradation of specific polysaccharides or structural elements increased portions of the remaining/unaltered polysaccharides are calculated.

Carrot pomace IDF polysaccharides contained distinctly lower portions of arabinose and galactose (liberated after sulfuric acid hydrolysis) with increasing thermomechanical



**Fig. 6** Portions of arabinose-related partially methylated alditol acetates (mol%) resulting from methylation analysis of insoluble dietary fiber (IDF; mean  $\pm$  half range, n=2) and soluble dietary fiber (SDF; mean  $\pm$  half range, n=2) from untreated and extruded carrot pomace and potato pulp. The extrusion conditions vary in overall water

content (w<sub>H2O</sub>) and screw speed (*n*) at a barrel temperature of 100 °C resulting in different specific mechanical energies (SME) and material temperatures (T<sub>M</sub>). *t* terminal, *p* pyranose, *f* furanose, *Ara* arabinose

treatment (Fig. 5). As portions of the individual PMAAs did neither drastically nor consistently change, methylation analysis data suggest that arabinans (see Fig. 6) and galactans were degraded mostly independently of their fine structures as an effect of thermomechanical treatment.

Results of our arabinan screening (Table S5) basically agree with this; however, portions of highly substituted structures as represented by compound A-7a decreased with increasing thermomechanical treatment and, thus, appear to be more labile. Potato pulp IDF showed an extrusion-based decrease in the portions of galactose, especially at higher screw speed (600 min<sup>-1</sup>), indicating a degradation of galactans as neutral pectic polysaccharides. These findings are in accordance with our data on apple pomace pectins that also showed decreasing pectin complexity as a consequence of the extrusion processing [12, 13]. Therefore, extrusion processing appears to alter more extensively the side chains of rhamnogalacturonan I (as compared to other dietary fiber polysaccharides), that is, arabinans and galactans, depending on which neutral side-chain dominates the pectin fraction.

Furthermore, changes in the pectin backbone were indicated by a decrease in the portions of galacturonic acid under maximal thermal and mechanical stress (carrot pomace:  $w_{H2O} = 25\%$ ,  $n = 1000 \text{ min}^{-1}$ ; potato pulp:  $w_{H2O} = 28\%$ ,  $n = 600 \text{ min}^{-1}$ ). Also related to galacturonic acid, the ratio of rhamnose to galacturonic acid changed in the maximum stressed samples. For carrot pomace, it decreased from 1:4 in the untreated material to 1:6, suggesting higher portions of homogalacturonan than rhamnogalacturonan I in this extrudate. In contrast, for potato pulp, the rhamnose to galacturonic acid ratio increased from 1:4 in the untreated material to 1:2.5, suggesting a more distinct degradation of homogalacturonan as compared to rhamnogalacturonan I. Finally, the degree of pectin esterification decreased from 57 to 29% for carrot pomace (depending on the extrusion conditions) and from 35 to 12% for potato pulp (with increasing thermomechanical energy input; Table S7). The degree of acetylation remained constant due to extrusion for carrot pomace and decreased with increasing speed ( $n=600 \text{ min}^{-1}$ ) from 38% up to 19% ( $w_{H2O} = 46\%$ ) or 12% ( $w_{H2O} = 28\%$ ) depending on the water content for potato pulp (Table S7).

Possible pectin solubilization was not reflected in the SDF monosaccharide composition of the extrudates (Fig. 5, Table S3). However, because solubilized polysaccharides can a) be sufficiently stable or b) further be degraded, either into LMW-SDF or into degradation products that eluded the analyses performed here, the monomer composition of this fraction is a somewhat hard to judge parameter. But, analyses of glycosidic linkages within the polysaccharides suggest that arabinan structures were further depolymerized, at least when treated under highest stress: the portions of arabinose-related PMAAs decreased in carrot pomace ( $w_{H2O}=25\%$ , n=1000 min<sup>-1</sup>; Fig. 6). Degradation of highly branched arabinan oligomers was also confirmed by the arabinan profiling method (Table S5). In contrast, no hints for extrusion-based arabinan degradation in SDF of potato pulp

were detected (Fig. 6). Also, changes in galactan structures were not observed with the methods used here.

Although extrusion processing resulted in an overall increase of LMW-SDF oligosaccharides in the carrot pomace samples, the monomer composition after extrusion was comparable (Fig. 5, Table S3). Increasing arabinose ratios (54.3 mol% up to roughly 67 mol%) are in line with the described solubilization and further degradation of arabinans. Following maximum thermomechanical treatment, small portions of galactose (3.6 mol%) were liberated after acidic hydrolysis of LMW-SDF, indicating further degradation of solubilized galactan structures during extrusion processing at maximum stress.

In contrast, LMW-SDF was only detected after extrusion of potato pulp at a screw speed of 600 min<sup>-1</sup>, but not at 200 min<sup>-1</sup>. The oligosaccharides that were generated at  $W_{H2O} = 46\%$  and  $n = 600 \text{ min}^{-1}$  contained mainly arabinose, glucose, galactose, and galacturonic acid as monomers (Fig. 5). Methylation analysis suggests the predominant liberation of linear 1,5-linked arabino-oligosaccharides and 1,4-linked galacto-oligosaccharides (Table S4). Again, the origin of 1,4-linked glucose units in this fraction cannot be clarified, although cellulose would be assumed as the most likely source. Increased SME (sample at  $w_{H2O} = 28\%$  and  $n = 600 \text{ min}^{-1}$ ) resulted in the generation of oligosaccharides, in which galacturonic acid was no longer detected. Again, the composition of the liberated LMW-SDF fractions supports our claim that mainly pectins are degraded during extrusion. However, the origin of glucose remains to be clarified in future studies.

#### Technofunctionality as affected by extrusion

Particle surface modifications (in case of potato pulp) and both partial solubilization and further degradation of solubilized polysaccharides were expected to affect the technofunctionality of the food by-products such as hydration properties (WSI/WAI), swelling behavior, and rheological properties.

#### Hydration properties

The comparably low WSI of untreated potato pulp (5.3%)was increased by extrusion processing up to 26.2% depending on SME (Fig. 7A, Fig. S2A) and T<sub>M</sub> (Fig. 7B, Fig. S2B). This may be the result of two factors (a) a high amount of residual starch in the pulp that was modified during extrusion processing (see Table 1) and (b) the solubilization of non-starch polysaccharides as also demonstrated by the increase of SDF and LMW-SDF after extrusion processing (Fig. 1). It has been demonstrated earlier that the WSI of potato starch increases with increasing thermomechanical treatment due to the destruction of starch granules thereby increasing starch solubility [48]. The WSI of untreated carrot pomace was higher (30.6%) as compared to the WSI of untreated potato pulp, which is also reflected by the higher content of SDF and LMW-SDF in the untreated carrot pomace (see Fig. 1). An SME/material temperature dependent increase of WSI was also found for carrot pomace. However, a distinct increase was only seen under the harshest conditions analyzed here. These data reflect well the solubilization of dietary fiber polysaccharides, which is the most important factor for carrot pomace due to negligible starch contents.

The WAI of untreated potato pulp (8.8 g·g<sup>-1</sup>) was also much lower as compared to untreated carrot pomace (32.4 g·g<sup>-1</sup>) (Fig. 8, Fig. S3). Extrusion processing of potato pulp increased the WAI up to 3 times. However, both increasing SME and increasing material temperature resulted in decreased WAI values, potentially due to destruction of insoluble particles and starch polymers,



**Fig.7** Water solubility index (WSI) of carrot pomace (quadrangles) and potato pulp (triangles) as a function of specific mechanical energy (SME) (**A**) and material temperature ( $T_{\rm M}$ ) (**B**) at various overall water contents (w<sub>H2O</sub>)



**Fig.8** Water absorption index (WAI) of carrot pomace (quadrangles) and potato pulp (triangles) as a function of specific mechanical energy (SME) (**A**) and material temperature ( $T_{\rm M}$ ) (**B**) at various overall water contents ( $w_{\rm H2O}$ )

although a fragmentation of starch was not apparent from the analyzed starch contents (see Table 1). However, it is possible that partial starch fragmentation resulted in oligosaccharides that were still captured in the analytical determination of starch. Different from potato pulp, the WAI values of carrot pomace generally decreased after extrusion processing. The sample that was extruded at a water content of 43% showed a surprisingly low WAI value, which cannot be explained by the solubility and the composition of the dietary fiber polysaccharides (Fig. 1). As the surface morphology of this sample did not differ from the other samples, and an influence of particle size fraction was excluded by the usage of the particle size fraction of 0.14-0.28 µm, the low WAI value of this sample cannot be explained at this time. Another porosity might be an explanation and will be investigated in the following.

#### Swelling behavior

The size of untreated carrot pomace particles increased by ~ 11 times of their initial size when particles were allowed to swell for 90 min (Fig. 9A). A drastic decrease of particle growth was observed for carrot samples that were extruded with a water content of 43% at screw speed of 1000 min<sup>-1</sup>, potentially reflecting the low WAI value of this sample. However, a similar swelling behavior (increase of particle size by ~ 3 time after 90 min) was observed for carrot samples that were extruded with 25% water content at 1000 min<sup>-1</sup> and that had a much higher WAI value than the sample extruded at a water content of 43%. After extrusion processing with 25% water content at screw speed of 200 min<sup>-1</sup> a particle growth of ~ 8 times was observed after 90 min. Thus, although varying in its magnitude, extrusion processing resulted



**Fig. 9** Kinetics of particle size growth in water by microscopic image analysis for carrot pomace (**A**) and potato pulp (**B**). The relative particle size is the ratio between the area occupied by a particle at time  $t(A_1)$  and the area of the particle at the initial time  $(A_0)$ 

in reduced swelling of the particles, which cannot simply be explained by a reduced water absorption of the samples. Again, extrusion processing had an opposite effect on the properties of potato pulp. Whereas the particle size of untreated potato pulp changed only slightly (increase of particle size by  $\sim 2$  times after 90 min) during the swelling experiment, a significant increase in size was observed for extruded potato pulp samples (Fig. 9B). The particle size of samples extruded with 46% water content at screw speed of 600 min<sup>-1</sup> increased by 27.6 compared to particle size of untreated material, tantamount to the maximum swelling of potato pulp particles achieved here. An increase in thermomechanical treatment, or brief in the SME, resulted in reduced swelling capacity, which, however, was still larger as compared to the untreated material. Different from carrot pomace, these findings are in accordance with the results for WAI. The higher the water absorption, the more distinctive the particle growth. The decrease in swelling might be explained by the increase in thermomechanical treatment, which might destruct the insoluble particles as well as starch, and thus a less porous matrix remains and in consequence less water can be absorbed [49].

#### **Rheological properties**

Data for the complex viscosity of aqueous dispersions of carrot pomace are shown in Fig. 10. The complex viscosity of untreated carrot pomace was higher (~606 Pas) as compared to extruded samples, for which a decrease of the complex viscosity was observed depending on conditions applied. Just as seen for WAI and swelling the sample that was extruded at a water content of 43% showed the lowest complex viscosity, too.

Rheological measurements of potato pulp were not feasible due to water release while adjusting the rheometer gap. To compare the rheological behavior, pictures of the water pulp dispersions were taken (Fig. 11). Untreated material formed a liquid-like dispersion showing that it was not able to absorb all added water. In contrast, the sample that was extruded at a water content of 46% formed a very firm, solid-like dispersion (no free water was observed), as well as the sample that was extruded at a comparable SME ( $w_{H2O} = 28\%$ ,  $n = 200 \text{ min}^{-1}$ ). However, increasing SME (by increasing the screw speed to 600 min<sup>-1</sup> at a water content of 28%) resulted in products that produced noticeable softer dispersions. Thus, the sample with the lowest WAI and the



Fig. 10 Complex viscosity as a function of specific mechanical energy (A) and material temperature (B) of carrot pomace



**Fig. 11** Potato pulp dispersions of untreated material (black, top) and different extrusion conditions: 46% overall water content ( $w_{H2O}$ ) at 600 and 1000 min<sup>-1</sup> (*n*) and 28% overall water content at 200 and 600 min<sup>-1</sup>. SME: specific mechanical energies,  $T_M$  material temperatures

lowest tendency to swell also showed the lowest complex viscosity.

# Profiles of selected phytochemicals as affected by extrusion processing

As demonstrated so far, both the profile of dietary fiber and the technofunctional properties of food by-products can be altered using extrusion. However, the food by-products may contain low-molecular weight phytochemicals that were not exhaustively extracted during the first use of the potatoes and carrots, respectively. From a nutritional point of view these phytochemicals can be either beneficial, for example, carotenoids or chlorogenic acid, or detrimental, for example, glycoalkaloids. Thus, knowledge about their fate during extrusion processing is of great interest. Data on phytochemicals of both untreated carrot pomace and potato pulp are presented in Table 2.

Contents of  $\alpha$ - and  $\beta$ -carotenes were reduced by up to roughly 50% during extrusion processing, which is in line with data on  $\beta$ -carotene contents as affected by extrusion published earlier [18, 19]. The SME largely affected the contents of intact carotenoids after extrusion processing. Similarly, contents of chlorogenic acid in in potato pulp decreased by almost up to 50% as a consequence of extrusion processing (Table 2). Just as demonstrated for the carotenoids, increasing SME reduces the amount of intact chlorogenic acids in the potato pulp. (Partial) instability of (poly) phenolic compounds during extrusion has also been detected following thermomechanical treatment of chokeberry pomace [50] and buckwheat [51], respectively.

As expected contents of glycoalkaloids in potato samples were not reduced during extrusion processing (Table 2). Glycoalkaloids are commonly considered quite stable under the influence of heat [52, 53]. In general, glycoalkaloid levels vary depending on factors such as potato variety and storage conditions [37, 54, 55]. Both  $\alpha$ -solanine and  $\alpha$ -chaconine were determined in all samples analyzed here, with  $\alpha$ -chaconine being dominant. This can be explained by the fact that potato pulp contains higher portions of peel components than mesocarp, and that the peel contains higher levels of  $\alpha$ -chaconine [37, 54, 55]. Total contents of glycoalkaloids increased with increasing thermomechanical treatment. Because formation of glycoalkaloids during extrusion can be excluded, it is rather suggested that glycoalkaloids become more accessible for analytical extraction through extrusion processing.

The German Federal Institute for Risk Assessment (BfR) recommended that total glycoalkaloid content in fresh potatoes should not exceed 100 mg·kg<sup>-1</sup> fresh weight, thus avoiding to surpass the no observed adverse effect level of 0.5 mg glycoalkaloids·kg<sup>-1</sup> body weight per day. This value is based on an average consumption of 350 g of potatoes, potato products and dishes per day [56]. However, as extruded potato pulp would be used in lower amounts as a food ingredient and because the values determined here are based on a dry weight basis, a direct comparison of these recommendations with the levels determined here is difficult.

**Table 2** Carotenoid contents of untreated and extruded carrot pomace as well as contents of chlorogenic acid and glycoalkaloids of untreated and extruded potato pulp (mean  $\pm$  standard deviation, n = 3)

	Carrot poma	ace				Potato pulp			
w <sub>H2O</sub> [%] n [min <sup>-1</sup> ] SME [Wh•kg <sup>-1</sup> ]	Untreated	25 200 175.0	43 1000 253.8	25 1000 385.0	w <sub>H20</sub> [%] n [min <sup>-1</sup> ] SME [Wh∙kg <sup>-1</sup> ]	Un- treated	46 600 186.0	28 200 213.5	28 600 376.5
<i>T</i> <sub>M</sub> [°C]		116.5	116.5	130.0	$T_{\rm M}$ [°C]		109.5	118.0	133.5
α-Carotene [mg·100 g <sup>-1</sup> dm] <sup>a</sup>	$2.8 \pm 0.1$ <sup>A</sup>	1.9 ± 0.1 <sup>B</sup>	1.8 ± 0.03 <sup>B,C</sup>	1.5 ± 0.1 <sup>C</sup>	Chlorogenic acid [mg·100 g <sup>_1</sup> dm] <sup>a</sup>	$28.7 \pm 3.2$ <sup>A</sup>	23.8 ± 1.0 <sup>B</sup>	21.9 ± 0.6 <sup>B</sup>	13.3 ± 1.2 <sup>c</sup>
β-Carotene [mg·100 g <sup>-1</sup> dm] <sup>a</sup>	$3.3 \pm 0.1^{\text{A}}$	$2.3 \pm 0.1^{B}$	2.2 ± 0.02 <sup>в</sup>	$^{1.8}_{0.2} \pm ^{\rm C}_{\rm C}$	α-Solanine [mg·kg <sup>−1</sup> ] <sup>a</sup>	$37.9 \pm 1.2^{\circ}$	44.9 ± 1.8 <sup>B</sup>	42.8 ± 0.5 <sup>B</sup>	49.4 $\pm$ 0.6 <sup>A</sup>
Total Carotenoids [mg·100 g <sup>-1</sup> dm] <sup>a</sup>	$6.2 \pm 0.3$ <sup>A</sup>	4.3 ± 0.1 <sup>B</sup>	4.0 ± 0.1 <sup>B</sup>	$^{3.3 \pm}_{0.3 ^{\rm C}}$	α-Chaconine [mg·kg-1]ª	$150.4 \pm 5.4$ <sup>D</sup>	167.3 <u>+</u> 8.8 <sup>B,C</sup>	161.4 ± 2.6 <sup>C,D</sup>	$196.4 \pm 2.1$ <sup>A</sup>
					Total Gly- coalkaloids [mg∙kg <sup>−1</sup> ]ª	$188.2 \pm 6.6$ <sup>D</sup>	212.2 ± 10.5 <sup>B.C</sup>	204.2 <u>+</u> 3.1 <sup>C,D</sup>	$245.9 \pm 2.8$ <sup>A</sup>

The extrusion conditions vary in water content ( $w_{H2O}$ ) and screw speed (*n*) at a barrel temperature of 100 °C resulting in different specific mechanical energies (SME) and material temperatures ( $T_{M}$ )

dm dry matter

<sup>a</sup>Means within a row and a by-product that are marked with different letters differ significantly (ANOVA, Tukey test,  $\alpha = 0.05$ )

**Table 3** 5-Hydroxymethylfurfural (HMF; mean  $\pm$  standard deviation, n=3) and acrylamide (n=1) levels of untreated and extruded carrot pomace and potato pulp samples

	Carrot pomac	Potato pulp						
w <sub>H2O</sub> [%]	Untreated	25	43	25	Untreated	46	28	28
$n  [\min^{-1}]$		200	1000	1000		600	200	600
SME [Wh•kg <sup>-1</sup> ]		175.0	253.8	385.0		186.0	213.5	376.5
$T_{\rm M}$ [°C]		116.5	116.5	130.0		109.5	118.0	133.5
HMF [mg·kg <sup>−1</sup> dm] <sup>a</sup>	$4.1 \pm 0.2^{\text{ B}}$	$1.8 \pm 0.1$ <sup>C</sup>	<loq< td=""><td>8.1 <math display="inline">\pm</math> 0.1 <math display="inline">^{\rm A}</math></td><td><lod< td=""><td><lod< td=""><td><lod< td=""><td><lod< td=""></lod<></td></lod<></td></lod<></td></lod<></td></loq<>	8.1 $\pm$ 0.1 $^{\rm A}$	<lod< td=""><td><lod< td=""><td><lod< td=""><td><lod< td=""></lod<></td></lod<></td></lod<></td></lod<>	<lod< td=""><td><lod< td=""><td><lod< td=""></lod<></td></lod<></td></lod<>	<lod< td=""><td><lod< td=""></lod<></td></lod<>	<lod< td=""></lod<>
Acrylamide [µg·kg <sup>-1</sup> dm]	<loq< td=""><td><loq< td=""><td><loq< td=""><td><loq< td=""><td>41</td><td>35</td><td>46</td><td>71</td></loq<></td></loq<></td></loq<></td></loq<>	<loq< td=""><td><loq< td=""><td><loq< td=""><td>41</td><td>35</td><td>46</td><td>71</td></loq<></td></loq<></td></loq<>	<loq< td=""><td><loq< td=""><td>41</td><td>35</td><td>46</td><td>71</td></loq<></td></loq<>	<loq< td=""><td>41</td><td>35</td><td>46</td><td>71</td></loq<>	41	35	46	71

The extrusion conditions vary in water content ( $w_{H2O}$ ) and screw speed (*n*) at a barrel temperature of 100 °C resulting in different specific mechanical energies (SME) and material temperatures ( $T_M$ )

dm dry matter

<sup>a</sup>Means within a row and a food by-product that are marked with different letters differ significantly (ANOVA, Tukey test,  $\alpha = 0.05$ ); <LOQ: below limit of quantification; <LOD: below limit of detection

# Formation of food-borne contaminants during extrusion processing

Although extrusion processing clearly enhances the options to use carrot pomace and potato pulp as ingredients (depending on the extrusion parameters as demonstrated above), excessive formation of food-borne contaminants during extrusion might limit their applicability. HMF, a heatinduced contaminant, which is prone to be formed in samples that are rich in mono- and disaccharides, was already found in untreated carrot pomace ( $4.1 \text{ mg} \cdot \text{kg}^{-1} \text{ dm}$ ), potentially as a result of the drying process of this by-product. With increasing thermomechanical treatment, HMF levels initially decreased, but increased to  $8.1 \text{ mg} \cdot \text{kg}^{-1}$  dm at maximum stress (Table 3).

To the best of our knowledge, there were no studies on HMF in carrot pomace so far. We analyzed commercially available, thermally treated carrot chips to compare with carrot pomace. The analyzed carrot chips contained  $6.6 \pm 1.1$  mg HMF·kg<sup>-1</sup> dm, which is comparable to HMF contents analyzed for carrot pomace samples. Therefore, the potential formation of HMF during extrusion conditions applied in this study does not appear to limit the use of extruded carrot pomace in food products. HMF was neither detected in the untreated potato pulp sample nor in the extrudates, which can be well explained by the low content of free mono- and disaccharides in the pulp.

In contrast to HMF formation, acrylamide formation did not occur in significant amounts during the extrusion of carrot pomace because the analyzed levels were below the limit of quantitation in all samples analyzed in this study (Table 3). However, untreated potato pulp already contained 41  $\mu$ g·kg<sup>-1</sup> dm acrylamide. The acrylamide level decreased slightly to 35  $\mu$ g·kg<sup>-1</sup> dm when a water content of 46% was used during extrusion processing. Increasing thermomechanical stress resulted in an increase up to 71  $\mu$ g·kg<sup>-1</sup> dm. Thus, although quantifiable, the acrylamide formation appears to be comparably low, resulting in acrylamide contents below the benchmark levels in foodstuffs (for example, breakfast cereals:  $300 \ \mu g \cdot kg^{-1}$ ) according to Article 1 in conjunction with annex IV of the Commission regulation (EU) 2017/2158 [57]. Also, it has to be considered that the extrudates are not consumed as a product on their own, but as food ingredients.

In conclusion, extrusion is a promising method to modify the functional properties of carrot and potato based by-products. Technofunctional changes are accompanied by structural changes of dietary fiber polysaccharides. Larger contents of soluble dietary fiber polysaccharides were detected, with pectic polysaccharides being the most susceptible target for structural, extrusion-based modifications. Here, the neutral side chains of rhamnogalacturonan I appear to be mostly affected. Retention of potentially beneficial phytochemicals can be partially achieved; process induced contaminants were formed, but the levels do not to be of major concern. However, extrusion-based functionalization can only be generalized to a limited extent, since it strongly depends on the overall composition of the starting material, with, for example, remaining starch being an important factor. Also, controlling the pH during extrusion may be a useful tool to tune the extrusion-based modifications in a targeted manner; however, details on the role of pH need to be analyzed in future studies.

Supplementary Information The online version contains supplementary material available at https://doi.org/10.1007/s00217-022-04060-5.

Acknowledgements The authors would like to express their thanks to Hannah Gaul, Jan Steffan, and Andrea Butterbrodt for supporting the sample preparation and analyses. Further, the authors thanks ThermoFisher Scientific for providing the extruder Process11 including all the needed equipment as well as GNT Europe GmbH for supplying the carrot pomace.

Author contributions AT: Data curation, investigation, methodology, visualization, writing—original draft, review and editing original draft. VS: Data curation, investigation, methodology, project administration, visualization, writing—original draft. JK: Project administration, methodology, supervision, writing—review and editing. MAE: Conceptualization, funding acquisition, project administration, resources, supervision, writing—review and editing. MB: Conceptualization, funding acquisition, resources, supervision, writing—review and editing. MB: conceptualization, funding acquisition, resources, supervision, writing—review and editing.

**Funding** Open Access funding enabled and organized by Projekt DEAL. The IGF research project (20518 N) of the FEI was supported via AiF within the program for promoting the Industrial Collective Research (IGF) of the German Federal Ministry for Economic Affairs and Climate Action (BMWK), based on a resolution of the German Parliament.

### Declarations

**Conflict of interest** The authors declare that they have no conflict of interest.

Ethical approval This article does not contain any studies with human or animal subjects.

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