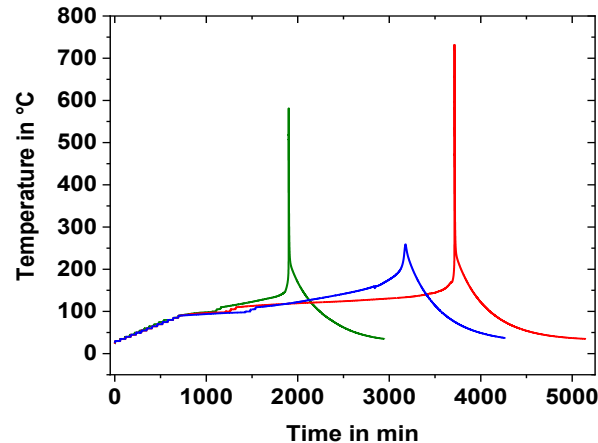


How Calorimetry can help in Battery Research - Thermal characterization and safety tests in battery calorimeters

C. Ziebert, N. Uhlmann, N. Löffelholz, P. Finster, M. Yasseri, I.U. Mohsin, M. Rohde, H.J. Seifert

KIT, Institute for Applied Materials – Applied Materials Physics



Short institute presentation

Karlsruhe Institute of Technology (KIT)

1/10/2009 - Foundation of KIT

Merger of the [University of Karlsruhe \(TH\)](#) and the [Research Center Karlsruhe GmbH](#)



Campus South

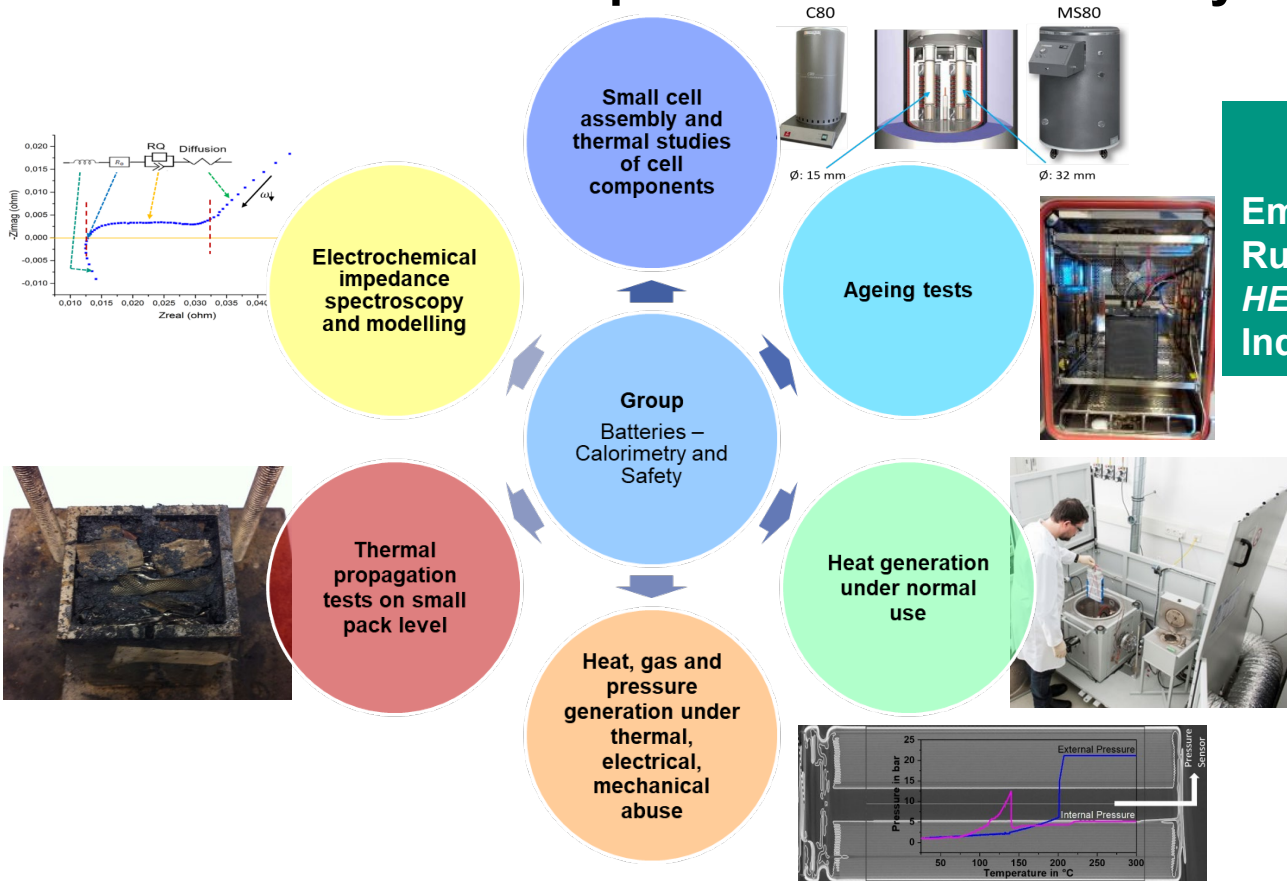
Data 2021

Employees:	9.783
Students:	22.275
Professors:	385
Budget:	1 billion euros
Patents:	51
Spin-offs:	37



Campus North

The Group Batteries – Calorimetry and Safety



Data 2022

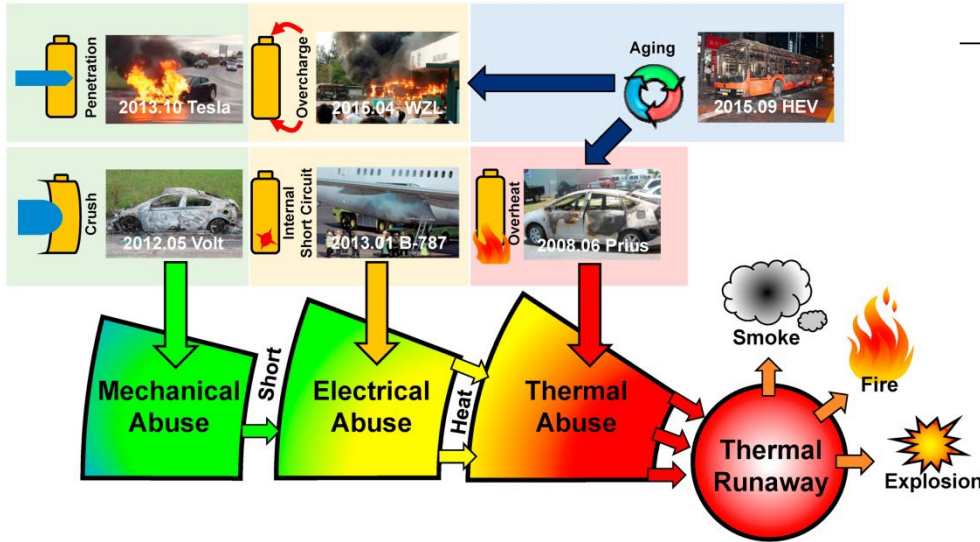
Employees:	15
Running LIB projects:	4
<i>HELIOS, POLiS, BatgasMod, AnaLiBa</i>	
Industry cooperation:	8



Dr. Carlos Ziebert
 Group leader Batteries – Calorimetry and Safety”

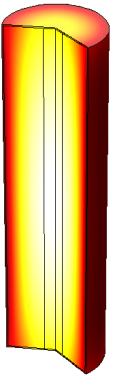
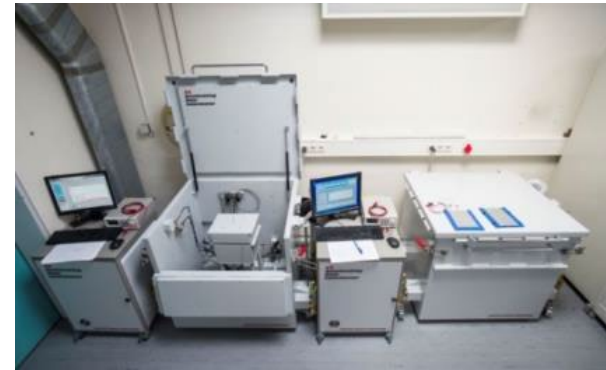
E-Mail: Carlos.Ziebert@kit.edu

Motivation: Increase of safety and reliability of LIB



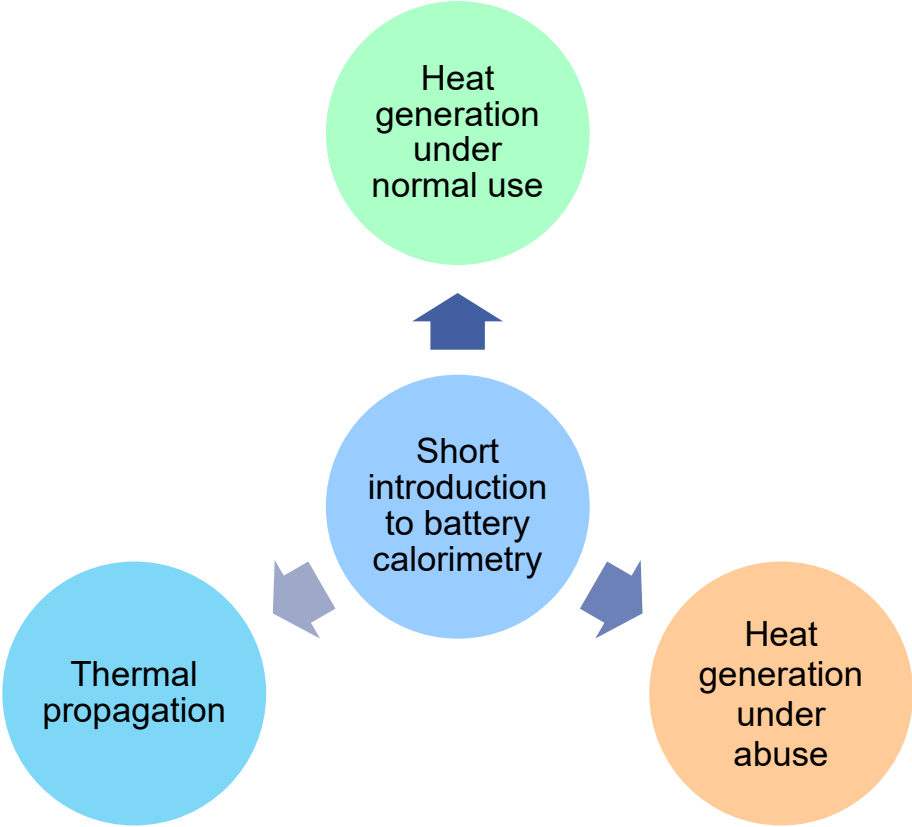
Feng et al., Energy Storage Materials 10 (2018) 246

→ For improving battery management system (BMS) and thermal management system (TMS) electrochemical and thermal behavior of the cells have to be thoroughly studied

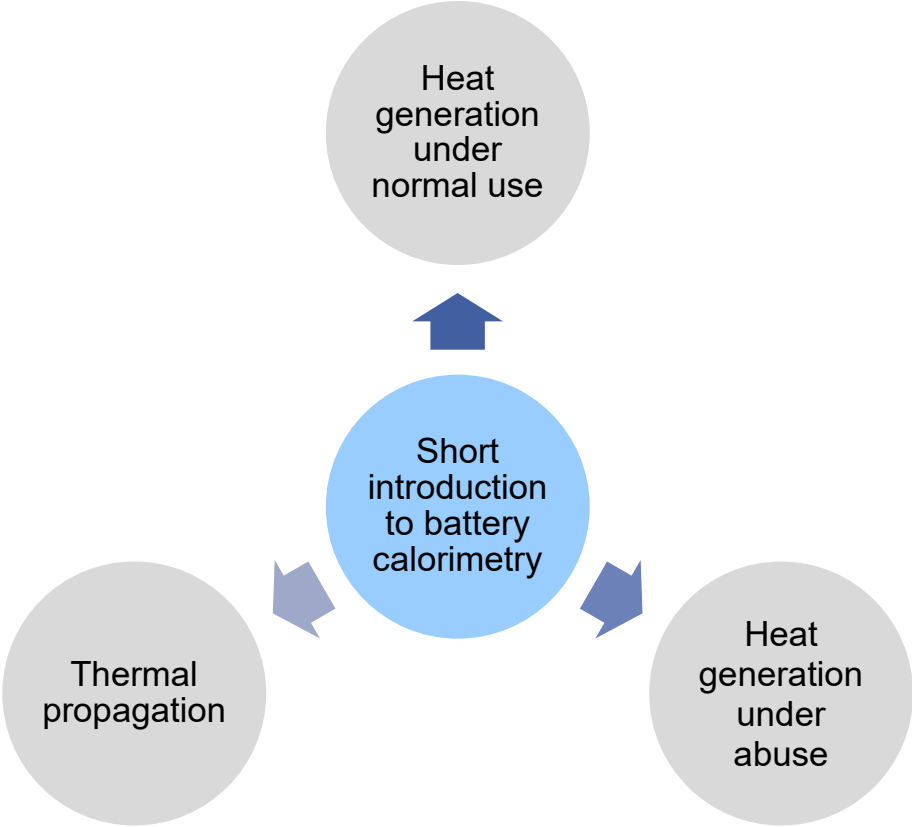


Aim: Improvement of TMS and BMS by determination of quantitative data of thermal properties using calorimeters

Overview



Overview



At IAM-AWP: Europe`s Largest Calorimeter Center



3 EV+ ARC: Ø: 40 cm
h: 44 cm



2 ES-ARC: Ø: 10 cm 2 EV-ARC: Ø: 25 cm
h: 10 cm h: 50 cm

Equipment: 7 Accelerating rate calorimeters (ARC); 2 Tian-Calvet calorimeters; 5 DSC; IR camera; 13 Temperature chambers (23l - 400 l; -40°C to 180°C); 11 Cyclers (210 channels, 0.01-800 A); EIS; 2 GC/MS



How can calorimetry help in battery research?

Research for improving performance parameters

- Higher energy or power density
- Smaller heat release during operation
- Faster charging rates
- Increased cycle life and thermal life

Research for improving safety parameters

- Higher safe operating temperature
- Better resistance to thermal/mechanical/electrical abuse
- Less energy release during decomposition

Differential scanning calorimeters



Tian-Calvet calorimeters



Small ARC

Medium-size ARC



Pressure measurement in ARC



Nail penetration test in ARC



Large-size ARC

Components



1 - 80 mAh



3 - 5 Ah



5- 40 Ah



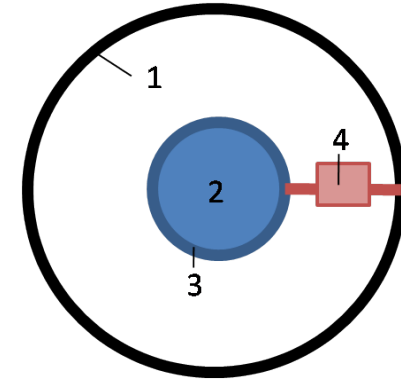
40 - 75 Ah

Cell Size and Capacity

Short introduction to battery calorimetry

Types of calorimeters

- Isoperibolic calorimeter
Measurement of the temperature change $T_s = T(t)$
 $T_c = \text{constant}$, R_{th} is defined
- Isothermal calorimeter (ice calorimeter of Bunsen)
 $T_s = T_c = \text{constant}$, R_{th} is very small
- Adiabatic calorimeter
Variation of the heat supply to the calorimeter
 $T_s = T_c \neq \text{constant}$, $R_{th} = \infty$
- Tian Calvet heat flux calorimeter $T_s - T_c = \text{constant}$



- 1 Calorimeter wall
- 2 Sample
- 3 Container
- 4 Thermal resistance R_{th}

$T_s = \text{Sample temperature}$

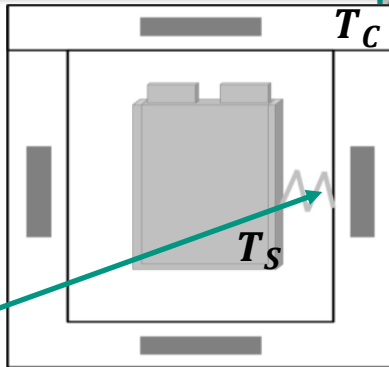
$T_c = \text{Temperature of the calorimeter walls}$

Possible conditions in an ARC

An ARC provides **isoperibolic** and **adiabatic** conditions

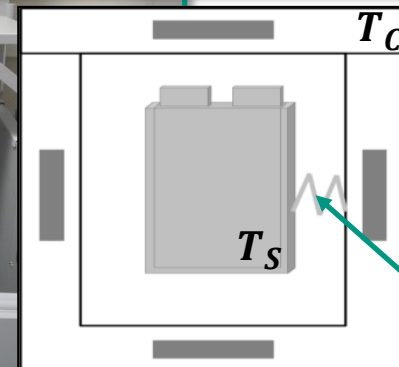
Under isoperibolic conditions the environmental temperature is kept constant.

Under adiabatic conditions the heaters follow immediately any change of the bomb thermocouple thus preventing that the cell can transfer heat to the walls.



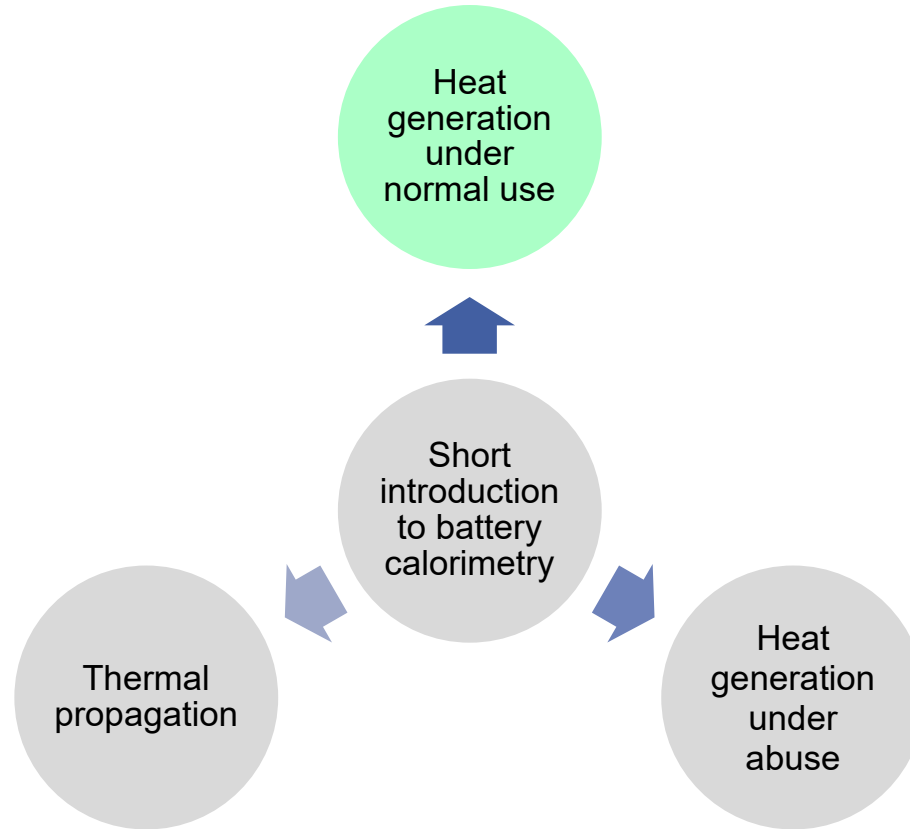
T_C constant

$$T_S(t) = T_{S_0} + \alpha \cdot t$$



$$\begin{aligned} T_C &= T_C(t) \\ &= T_{C_0} + \alpha \cdot t \end{aligned}$$

Overview



Thermal studies of coin cells in a Tian-Calvet calorimeter

Cathode: $\text{Na}_{0.53}\text{MnO}_2$

Anode: Hard carbon

Electrolyte: 1M NaClO_4 [EC:DMC:EMC (vol. 1:1:1) 2% FEC]

Charge parameter

(CCCV) Profile at 25°C, CV-Step at 4.0 V ($I < C/20$ or $t > 60\text{min}$)

Discharge parameter

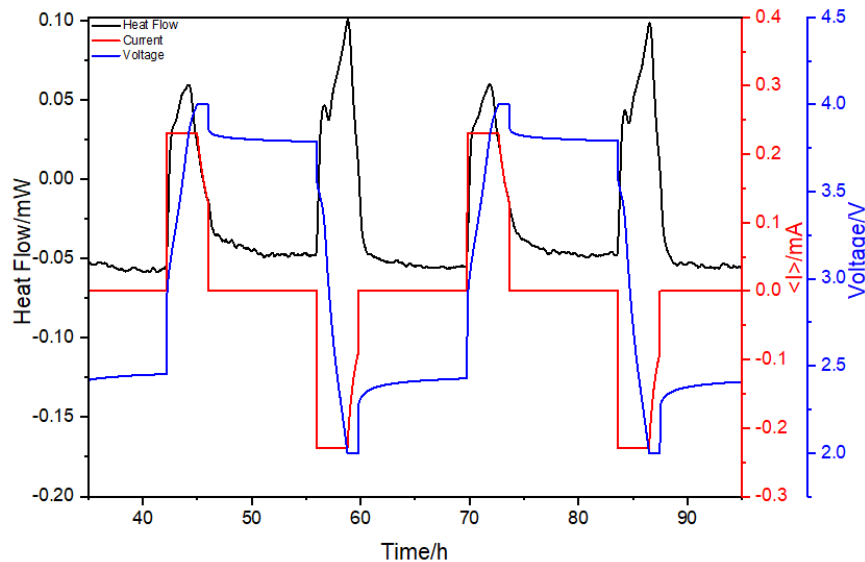
(CCCV) Profile at 25°C, CV-Step at 2.0 V ($I < C/20$ or $t > 60\text{min}$)



MS 80, Setaram
Instrumentation



Vessel \varnothing : 32 mm



Current Flow (1.15 Ah)	Capacity mAh	Heat generation charge (J)	Heat generation discharge (J)
0.2 C	0.82 ± 0.04	1.31 ± 0.03	1.49 ± 0.01

I. Mohsin, C. Ziebert, M. Rohde, H.J. Seifert, *Journal of The Electrochemical Society*, 168 (2021) 050544

Adiabatic Measurements

Worst Case Conditions

→ Cell in a pack surrounded by other cells

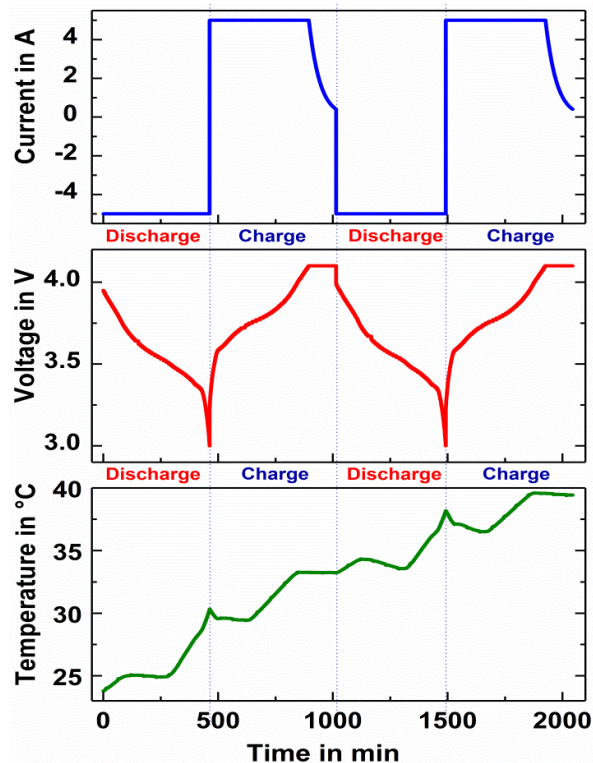
Discharge parameter:

- method: constant current (CC)
- $U_{\min} = 3.0\text{V}$
- $I = 5\text{A} \rightarrow \text{C}/8\text{-rate}$

Charge parameter:

- method: constant current, constant voltage (CCCV)
- $U_{\max} = 4.1\text{V}$
- $I = 5\text{A} \rightarrow \text{C}/8\text{-rate}$
- $I_{\min} = 0.5\text{A}$

→ after each electrochemical cycle the cell temperature increases further



40 Ah pouch cell

$T_{\text{st}} = 23^\circ\text{C}$ (RT)

Isoperibolic measurements

Ideal conditions

→ *Single cell*

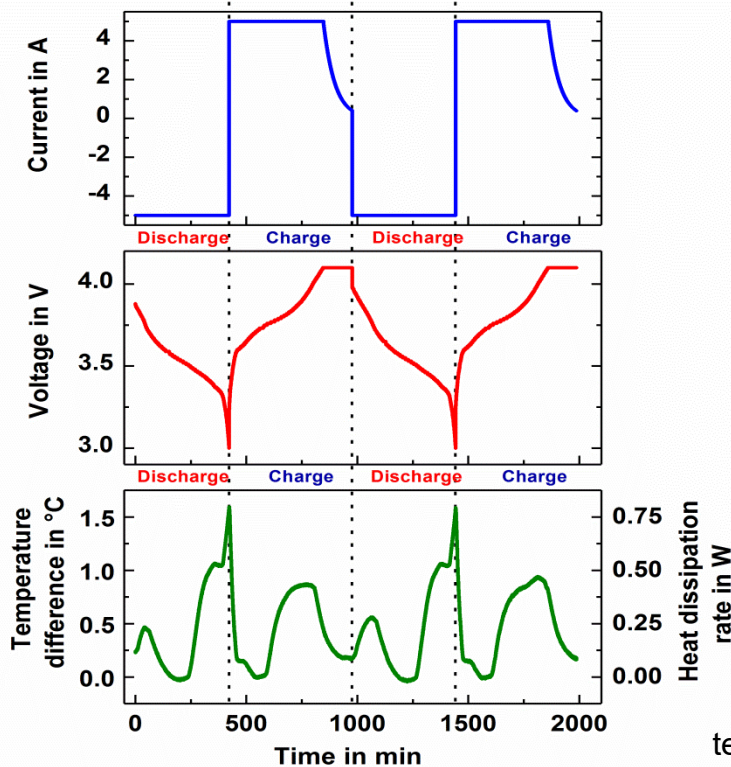
Discharge parameter:

- method: constant current (CC)
- $U_{\min} = 3.0\text{V}$
- $I = 5\text{A} \rightarrow \text{C}/8\text{-rate}$

Charge parameter:

- method: constant current, constant voltage (CCCV)
- $U_{\max} = 4.1\text{V}$
- $I = 5\text{A} \rightarrow \text{C}/8\text{-rate}$
- $I_{\min} = 0.5\text{A}$

→ after one electrochemical cycle the cell temperature reaches its initial value again



40 Ah pouch cell

$$\left(\frac{\delta E}{\delta T}\right) < 0$$

temperature coefficient negative!

Determination of total generated heat

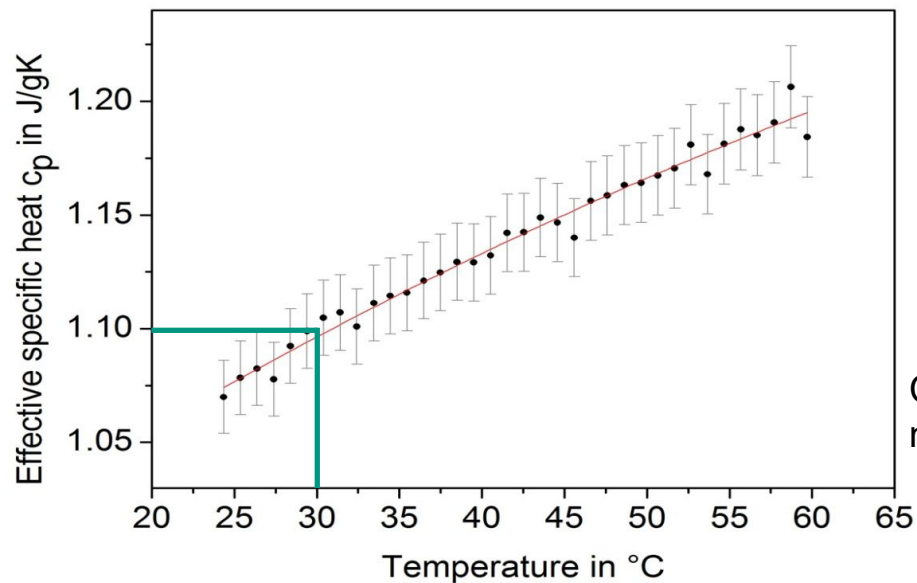
Heat generation of the cell during charging and discharging – Key data for thermal management and safety

Conversion of thermal data (temperature, temperature rate) to heat (Joule) and power (Watt) with the aim of understanding of heat release to determine heat removal requirements for thermal management.

To be measured:

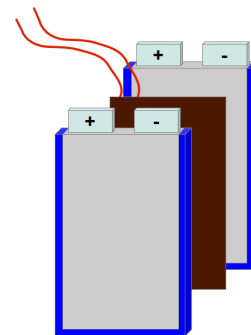
- **Effective specific heat capacity**
- **Heat transfer coefficient**
- **Reversible heat rate and irreversible heat rate**

Effective specific heat capacity c_p



e.g. at 30 °C $c_p = 1.095 \text{ J/g} \cdot \text{K}$

Important input data for simulation



40 Ah pouch cell

Sandwich setup
for pouch cells

Control of the current applied to the heater
mat to ensure a constant heating rate

$$c_p = \frac{\Delta Q}{m \cdot \Delta T_{ad}} = \frac{\int U \cdot I dt}{m \cdot \Delta T_{ad}}$$

m : Mass of the cell

ΔT_{ad} : Temperature difference under
adiabatic conditions

Heat transfer coefficient

Working principle of heat flux sensor (hfs)



gSKIN®-XP
(10mm x 10mm)

Tiny, serially connected semiconductor piles inside the sensor generate a voltage, which is proportional to the heat passing through the surface. The voltage is read out and depending on the sensor's sensitivity the results are converted into the heat flux.

Sensitivity:

$$S_0 = 10.04 \frac{mV \cdot m^2}{W}$$

Room temperature sensitivity

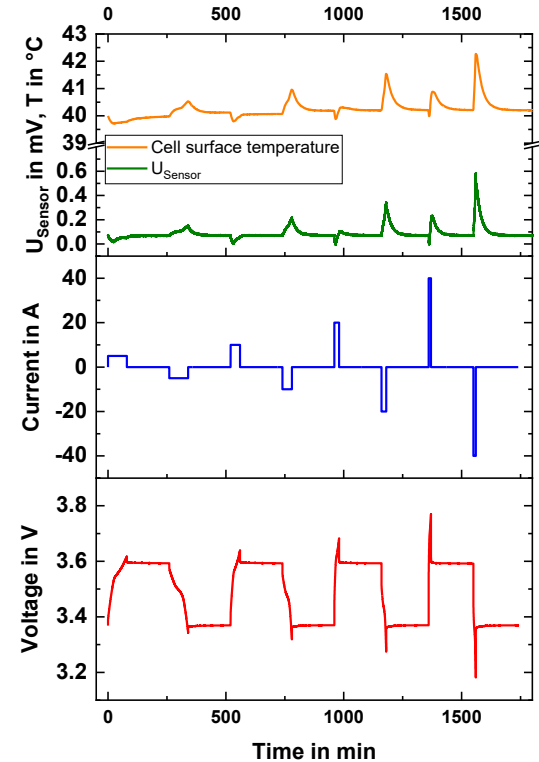
$$\Rightarrow h = \frac{\int \frac{U_{\text{sensor}}}{S(T)} dt}{\int_0^t (T - T_C) dt}$$

<http://shop.greenteg.com/shop/products-rd/gskin-xp/>
<https://www.greenteg.com/faq-heat-flux-sensing/>

$$S(T) = S_0 + (T - 22.5 \text{ } ^\circ\text{C}) \cdot S_C$$

$$S_C = 0.0049 \cdot \frac{mV \cdot m^2}{W \cdot ^\circ\text{C}}$$

Temperature correction factor



Comparison of values for generated heat

1) Adiabatic Measurement

$$\dot{Q}_{gen} = mc_p \frac{dT}{dt}$$

2) Isoperibolic Measurement

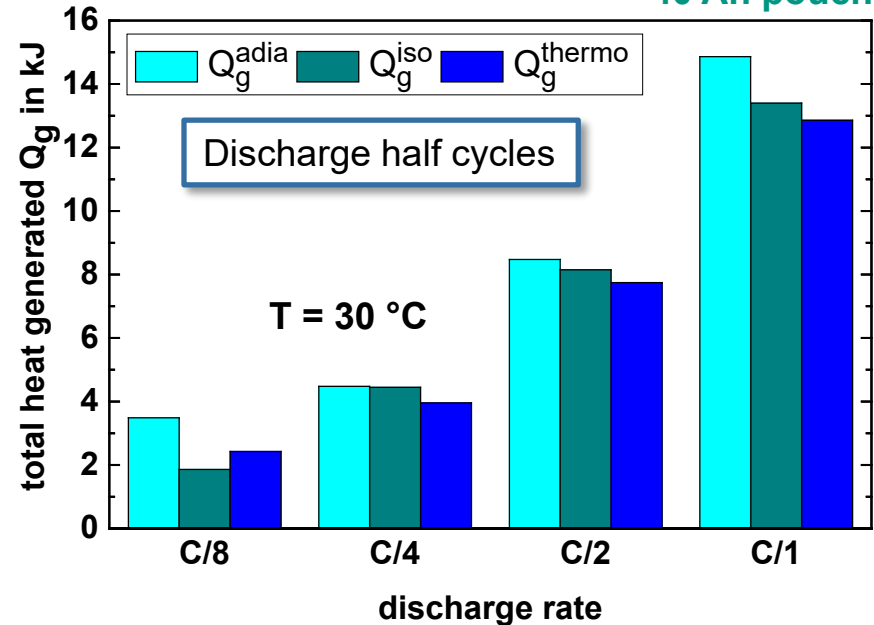
$$\dot{Q}_{gen} = mc_p \frac{dT}{dt} + Ah \cdot (T_S - T_C)$$

3) Measurement of irreversible and reversible heat

$$\dot{Q}_{gen} = -I(E_0 - E) - IT \frac{dE_0}{dT}$$

E_0 : Open circuit voltage (OCV), E : cell potential

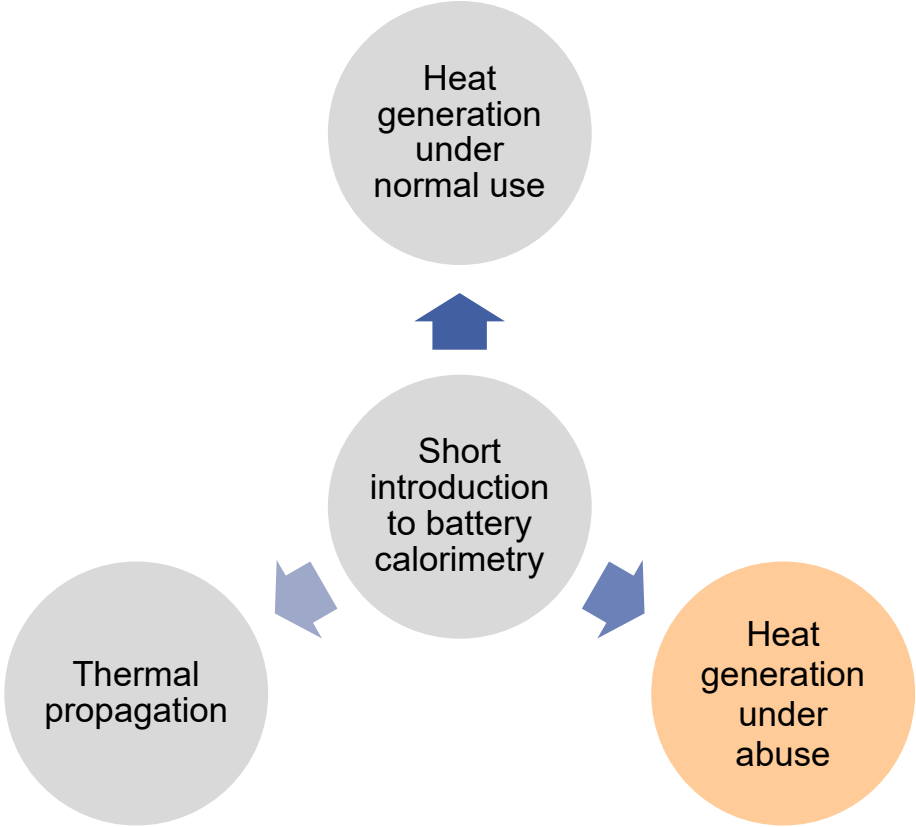
40 Ah pouch cell



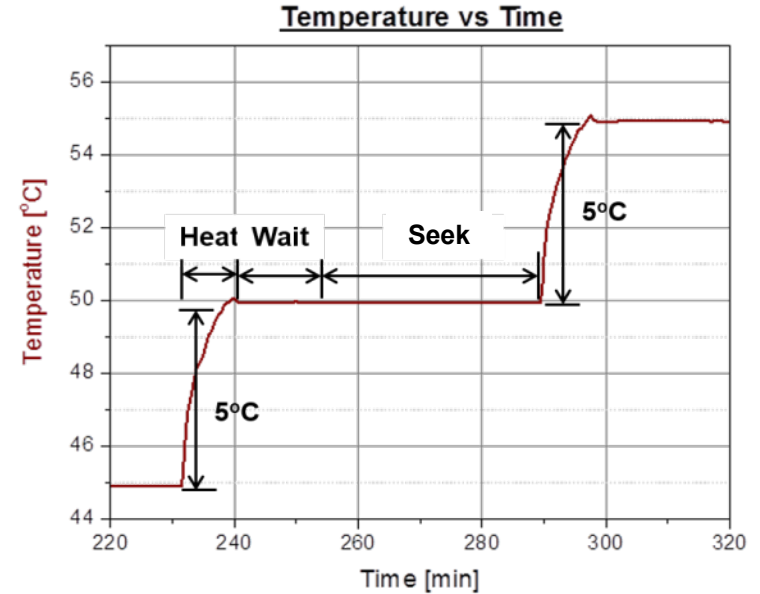
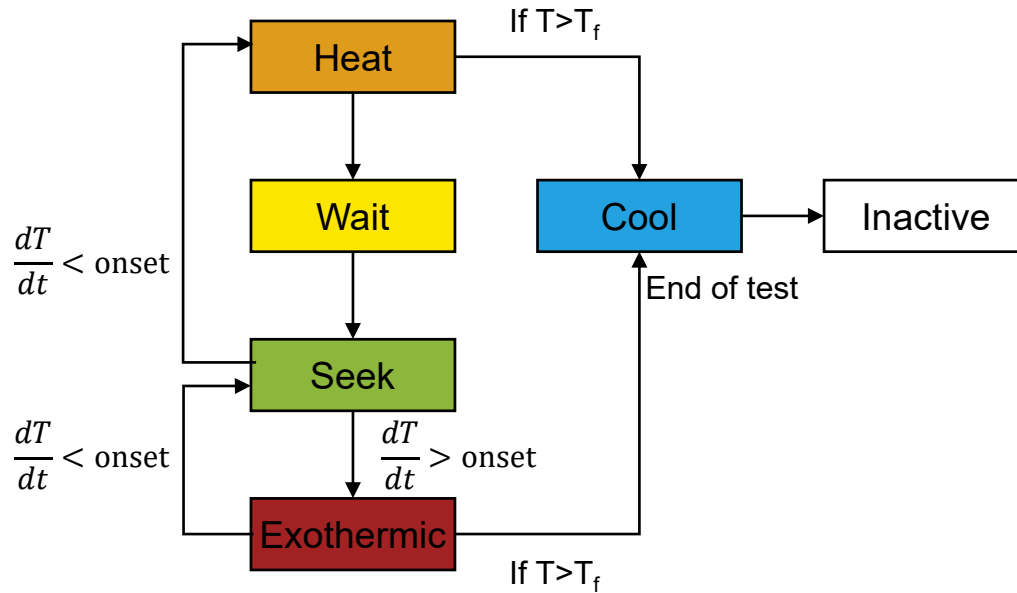
Conclusion: good agreement between the values determined by the different methods

E. Schuster, C. Ziebert, A. Melcher, M. Rohde, H.J. Seifert, J. Power Sources 268 (2015) 580-589

Overview



1) Thermal abuse: Heat-Wait-Seek (HWS) Method in ARC



Example of a Heat-Wait-Seek step

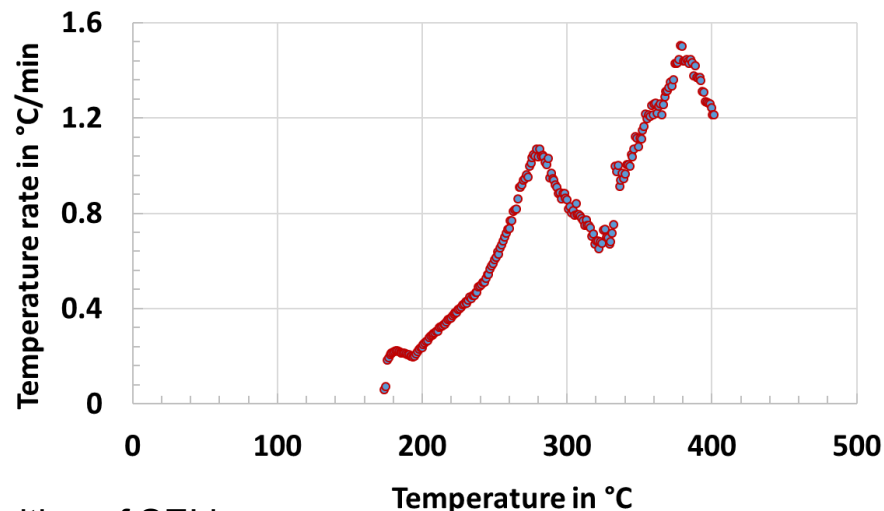
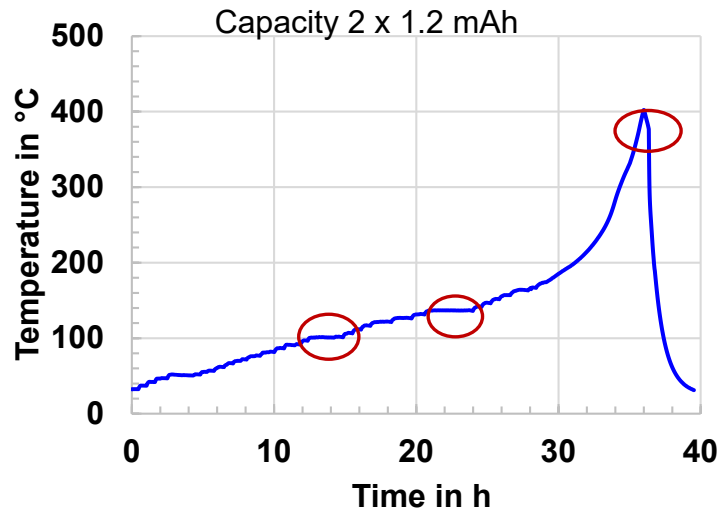
C. Ziebert, A. Melcher, B. Lei, W.J. Zhao, M. Rohde, H.J. Seifert, *Electrochemical-thermal characterization and thermal modeling for batteries*, in: L.M. Rodriguez, N. Omar, Eds., *EMERGING NANOTECHNOLOGIES IN RECHARGABLE ENERGY STORAGE SYSTEMS*, Elsevier Inc. 2017, ISBN 978032342977.

Thermal runaway: Two stacked Na-ion cells

Cathode: $\text{Na}_{0.53}\text{MnO}_2$

Anode: Hard carbon

Electrolyte: 1M NaClO_4 [EC:DMC:EMC (vol. 1:1:1) 2% FEC]



■ >100 °C

decomposition of SEI layer

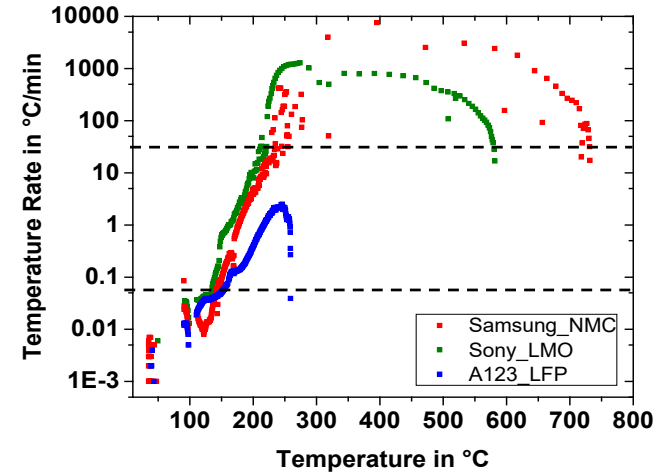
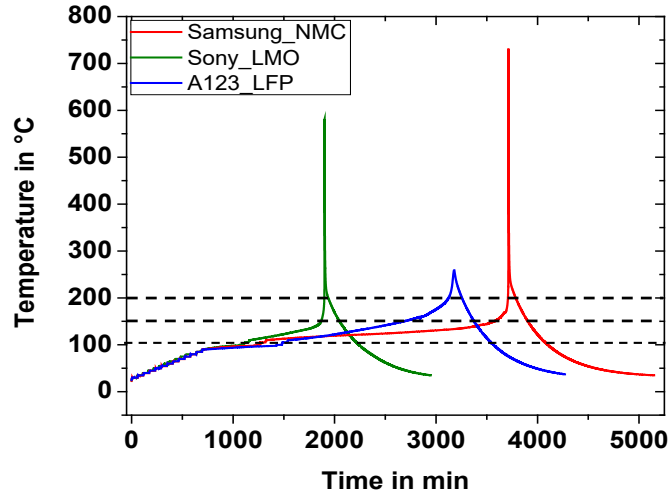
■ >160 °C

exothermic reactions between the electrolyte and the cathode

■ >200 °C

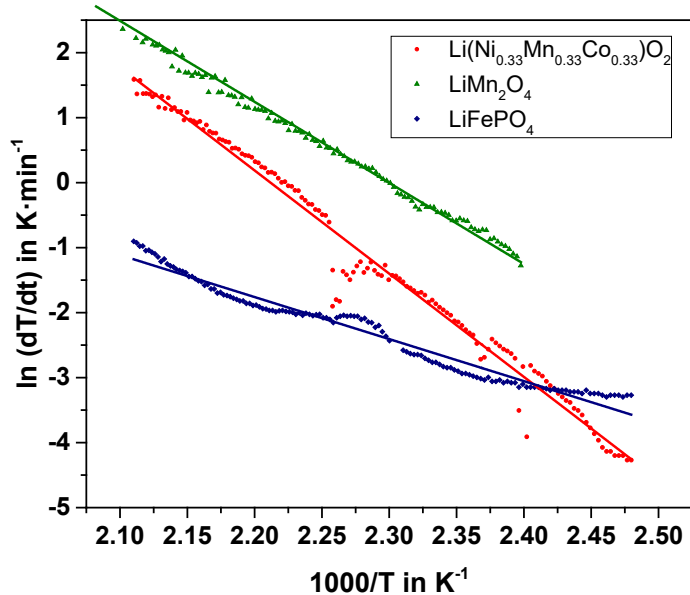
decomposition of the electrolyte

Thermal runaway: 18650 cells with different cathode materials



- $80 < T < 130^{\circ}\text{C}$: low rate reaction, $0.02 - 0.05^{\circ}\text{C}/\text{min}$: exothermic decomposition of the SEI
- $130 < T < 200^{\circ}\text{C}$: medium rate reaction, $0.05 - 25^{\circ}\text{C}/\text{min}$: solvent reaction, exothermic reaction between embedded Li ions and electrolyte \Rightarrow reduction of electrolyte at negative electrode
- $T > 200^{\circ}\text{C}$: high rate reaction, higher than $25^{\circ}\text{C}/\text{min}$: Exothermic reaction between active positive material and electrolyte at positive electrode \Rightarrow rapid generation of oxygen

Activation energies and reaction heats



Cathode Material	LiMn_2O_4 (LMO)	LiFePO_4 (LFP)	$\text{Li}(\text{Ni}_{0.33}\text{Mn}_{0.33}\text{Co}_{0.33})\text{O}_2$ (NMC)
Onset temperature of self-heating in °C	91	90	91
T_{\max} in °C	303	259	731
$(dT/dt)_{\max}$ in °C/min	1429	3	7577
c_p at 60°C SOC100 in J/g·K	0.83	1.19	0.95
E_a in eV	1.07	0.56	1.37
Reaction heat in J/g	180	184	597
Reaction heat in J/g	350-640 [1,2]	260 [2]	600 [2]

[1] R. Spotnitz, J. Franklin, *J. Power Sources*, 113, 81 (2003).

[2] H. F. Xiang, H. Wang, et al., *J. Power Sources*, 191, 575 (2009).

Activation energy: $\ln\left(\frac{dT}{dt}\right) \approx \ln(\Delta T_{ad} \cdot A) - \frac{E_a}{k_b \cdot T}$

E_a : Activation energy, A : pre-exponential factor

k_b : Boltzmann constant = 8.62×10^{-5} eV · K⁻¹

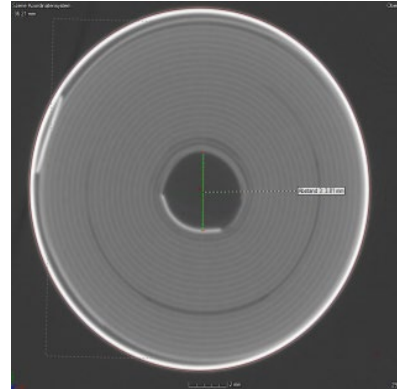
Reaction heat: $\frac{\Delta H}{m} = c_p \cdot \Delta T_{ad}$

Important input data for simulation

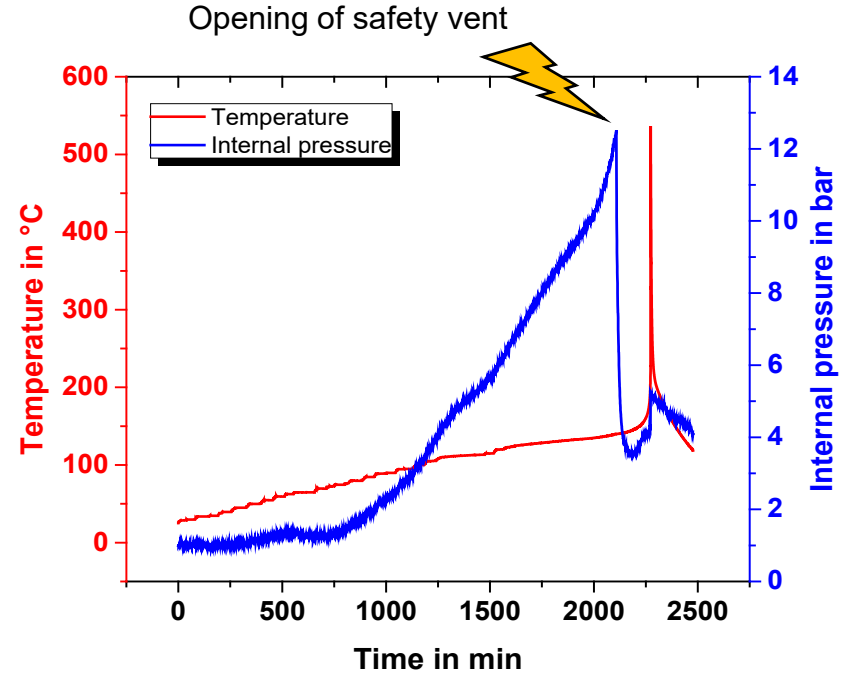
Internal pressure measurements on 18650 cells



Pressure line (\varnothing 1.5 mm)



1.6 Ah 18650 cell



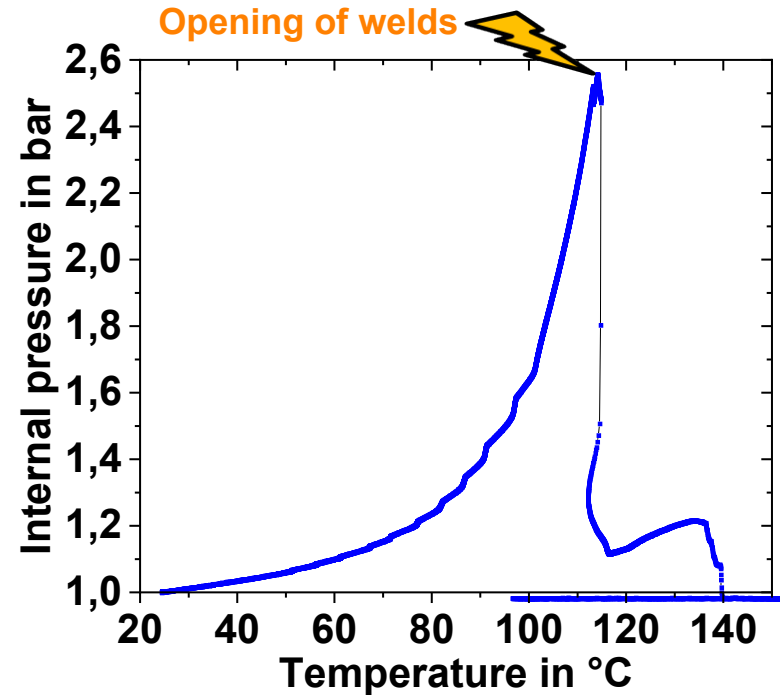
Internal pressure could be used in BMS for early prediction of processes leading to thermal runaway

B. Lei, W. Zhao, C. Ziebert, A. Melcher, M. Rohde, H.J. Seifert, *Batteries* 2017, 3, 14, [doi:10.3390/batteries3020014](https://doi.org/10.3390/batteries3020014).

Internal pressure measurements on pouch cells

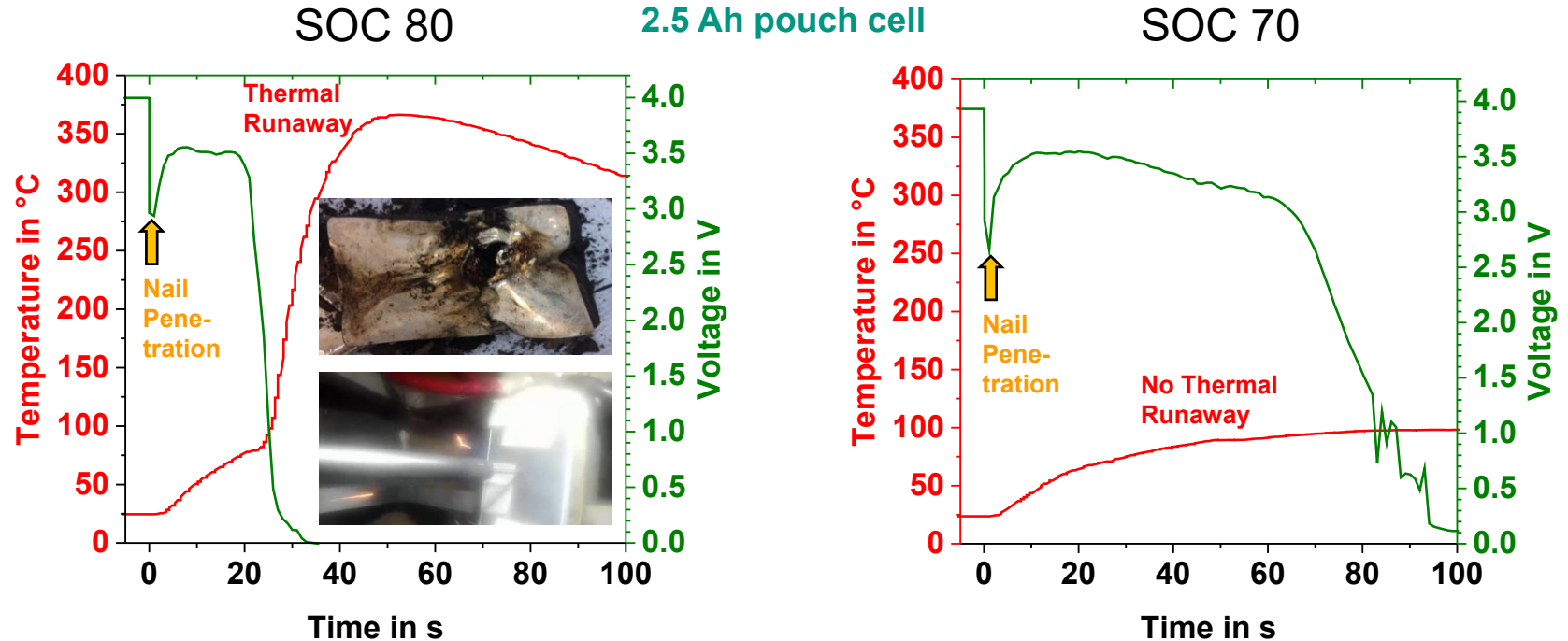


2.5 Ah pouch cell



2) Mechanical abuse: Nail penetration test

Influence of SOC on thermal runaway



2) Mechanical abuse: Nail penetration test

Influence of SOC on thermal runaway

SOC 80

$$T_{\max} = 366.24 \text{ }^{\circ}\text{C}$$

$$T_0 = 24.60 \text{ }^{\circ}\text{C}$$

$$\Delta H = 17.08 \text{ kJ}$$

SOC 70

$$T_{\max} = 98.13 \text{ }^{\circ}\text{C}$$

$$T_0 = 23.65 \text{ }^{\circ}\text{C}$$

$$\Delta H = 3.73 \text{ kJ}$$

Heat of reaction

$$\Delta H = m \cdot c_p \cdot \Delta T$$

$$c_p = 1.0 \text{ J/g K} \quad m = 50.0 \text{ g}$$

Conclusion: ESC as safety measure in case of mechanical abuse/accident

3) Electrical abuse: Overcharge test (red. pressure)

Qualitative result on the bench

Without reduced pressure



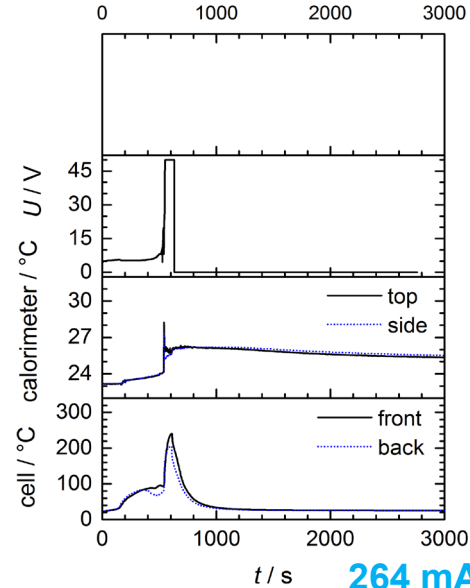
With reduced pressure



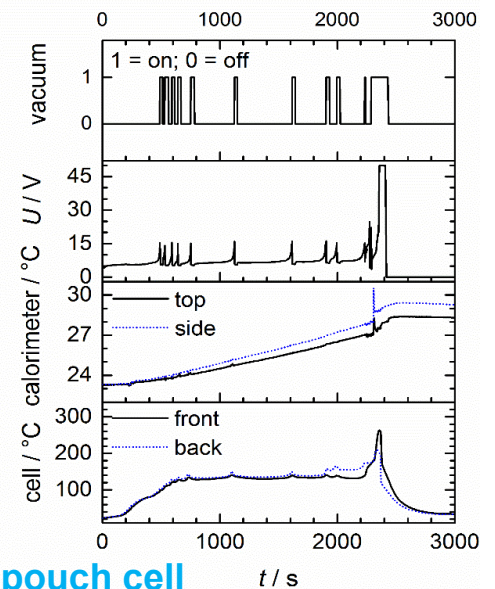
A. Hofmann, N. Uhlmann, C. Ziebert, O. Wiegand, A. Schmidt, Th. Hanemann, *Applied Thermal Engineering*, 124 (2017) 539-544.

Quantitative result in the ARC

Without reduced pressure

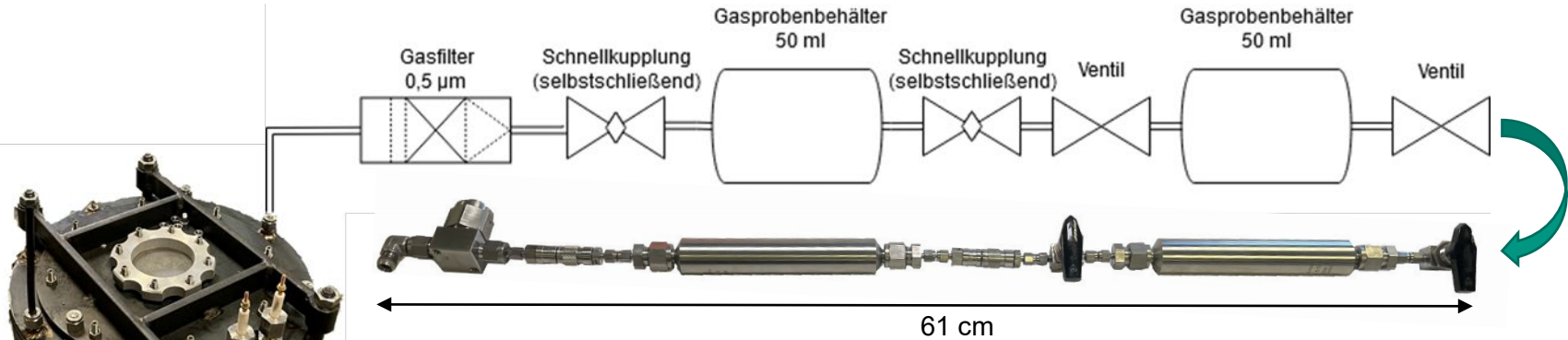


With reduced pressure



Conclusion: Controlled pressure reduction of pouch cells as safety measure for thermal runaway prevention

Gas collection after ARC Abuse-Tests



Large canister (20 l)
for cells with up to 30 Ah (THT)



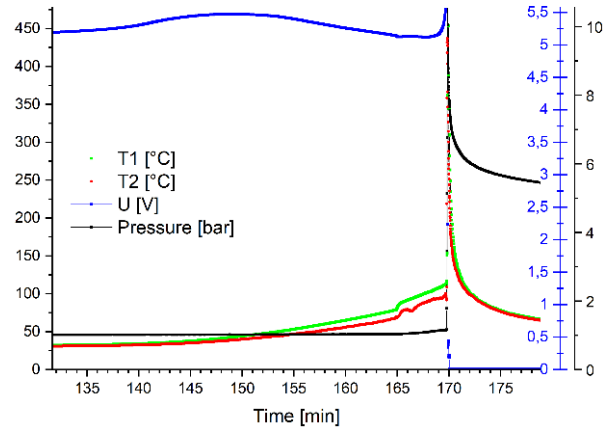
Large canister in EV+ ARC

- Collection option for gases through the Swagelok system
- Measurement of various parameters (two temperatures, pressure in the canister, voltage of the cell)
- Coupling to GC-MS Perkin-Elmer Clarus 690 Arnel 4019

Gas analysis after 0.5 overcharge test of 14 Ah prismatic cell

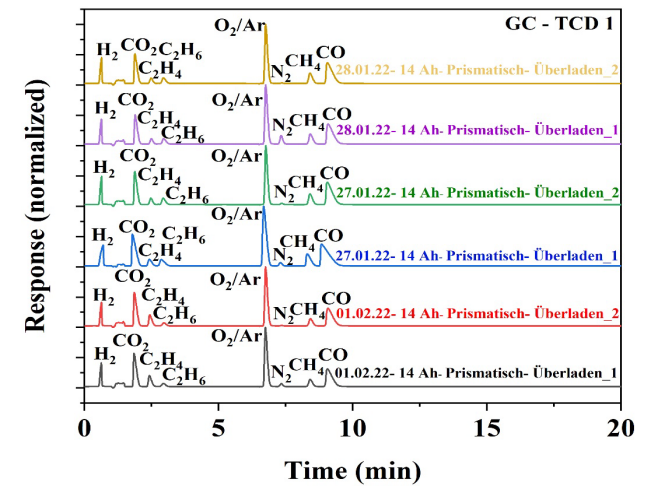


14 Ah prismatic cell

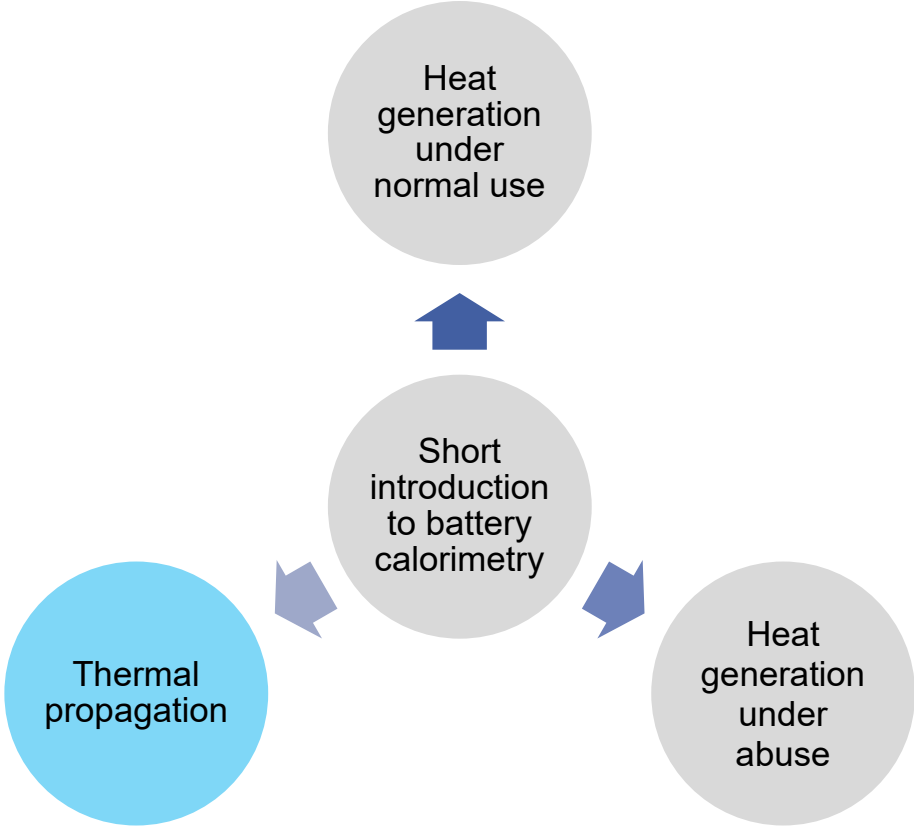


GC-MS Perkin-Elmer Clarus 690 Arnel 4019

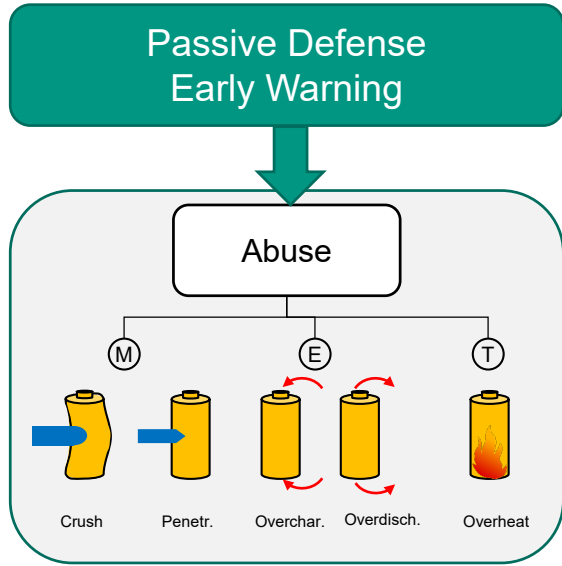
- Cell shows venting after 165 min and goes into thermal runaway after 170 min
- Data determined:
 - Maximum temperature: 534 °C
 - Maximum pressure: 12.5 bar
 - Evolved gas volume: 60 l (at 25 °C, 1013 mbar)



Overview

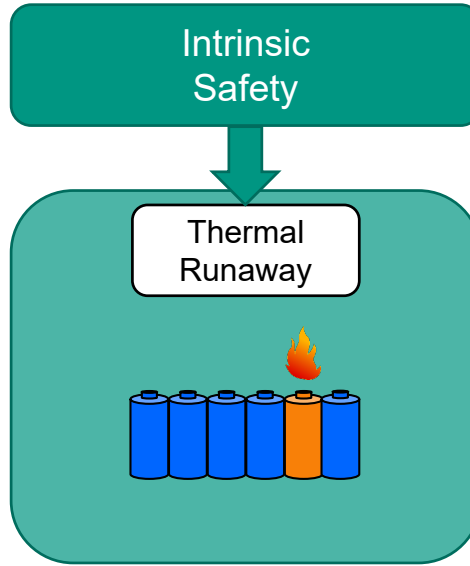


Thermal propagation



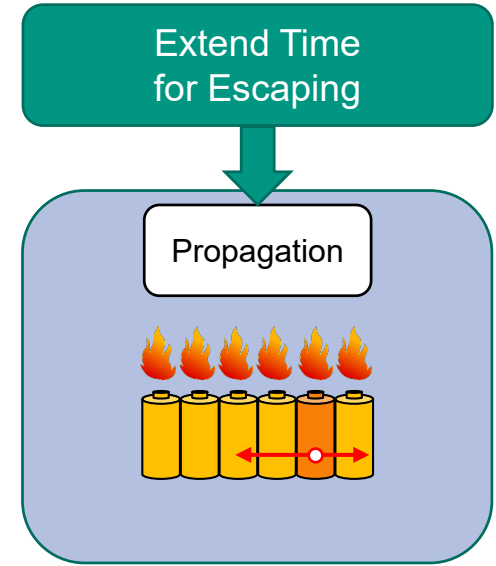
Step 1 – BMS

Detection of mechanical, electric, thermal abuse



Step 2 – Cell

Venting, CID, PTC

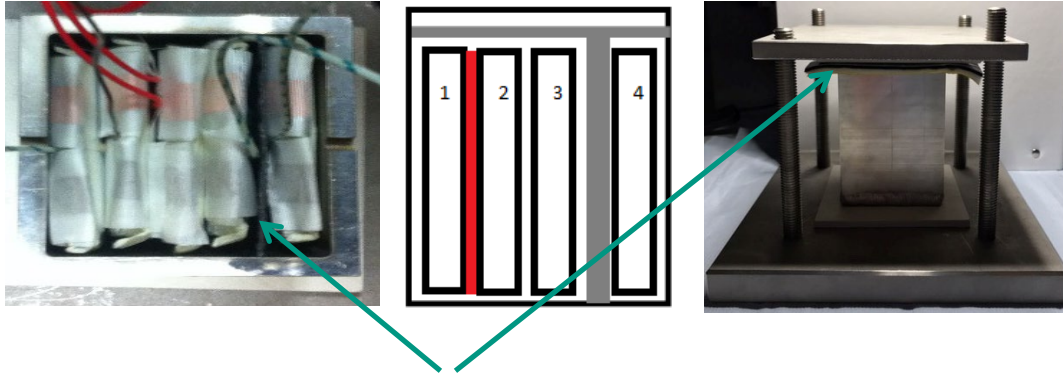


Step 3 – Pack

Passive propagation prevention

Adapted from: Feng et al., Energy Storage Materials 10 (2018) 246

Thermal propagation tests on small pack level

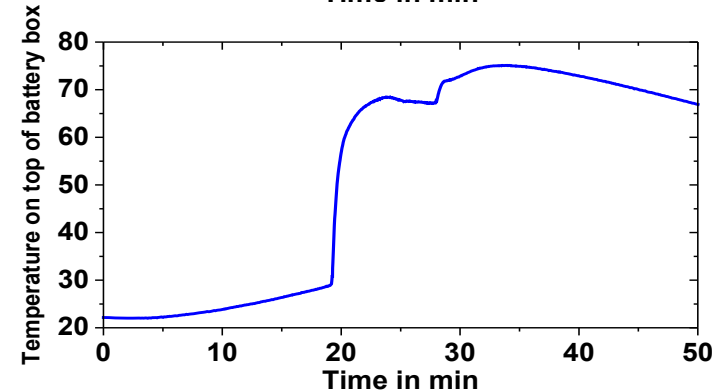
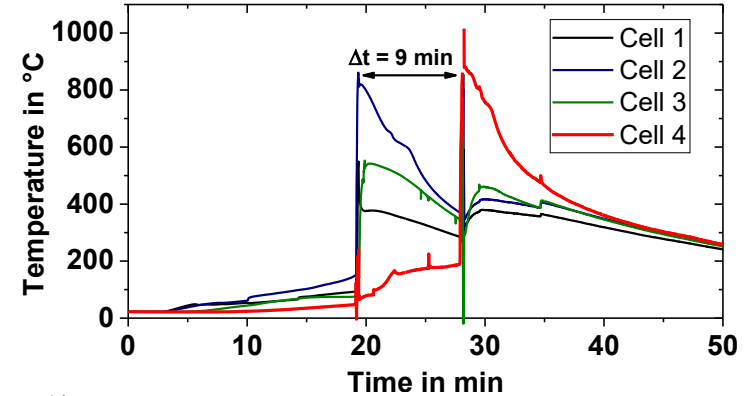


Gray: protective material for cell 4 and lid of battery box
Red: heater mat for thermal runaway initiation

Material qualification for propagation prevention

Optimized Multilayer:

- Extended time for propagation: 9 min
- Improved heat protection: temperature on top of battery box < 80 °C during thermal runaway



Summary: Possible calorimetric measurements

Normal use conditions

- Isoperibolic or adiabatic measurements

- For each:**
- Measurement of temperature curve and temperature distribution during cycling (full cycles, or application-specific load profiles), ageing studies
 - Determination of the generated heat, Separation of heat in reversible and irreversible parts

Abuse conditions

- Thermal abuse: Heat-wait-see test, ramp heating test, thermal propagation test
- Electrical abuse: External short circuit, Overcharge, Deep discharge
- Mechanical abuse: Nail penetration test

- Temperature measurement

- For each:**
- External or internal pressure measurement
 - Gas collection, Post Mortem Analysis, Ageing studies



Important data for BMS, TMS and safety systems

Thank you for your attention!

Contact data

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<https://www.iam.kit.edu/awp/169.php>



We thank

GEFÖRDERT VOM



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und Forschung



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Forschungszentrum Jülich



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German Research Foundation

