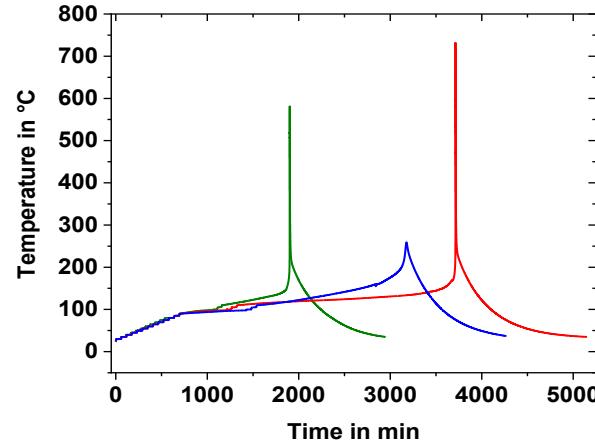


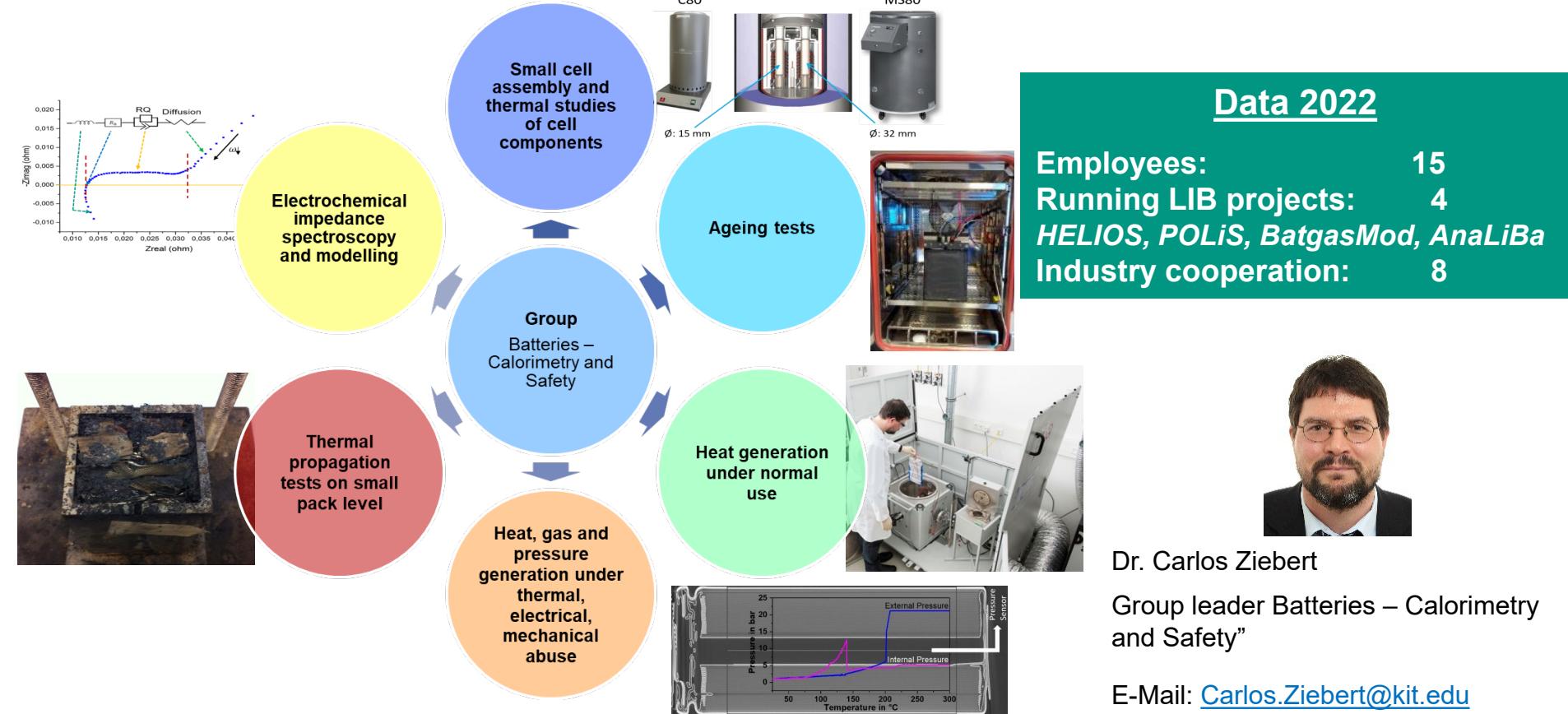
How battery calorimeters can help in advancing thermal management and safety of cells and packs

C. Ziebert, N. Uhlmann, N. Löffelholz, S. Ohneseit, P. Finster, M. Yasseri, M. Rohde, H.J. Seifert

KIT, Institute for Applied Materials – Applied Materials Physics



The Group Batteries – Calorimetry and Safety

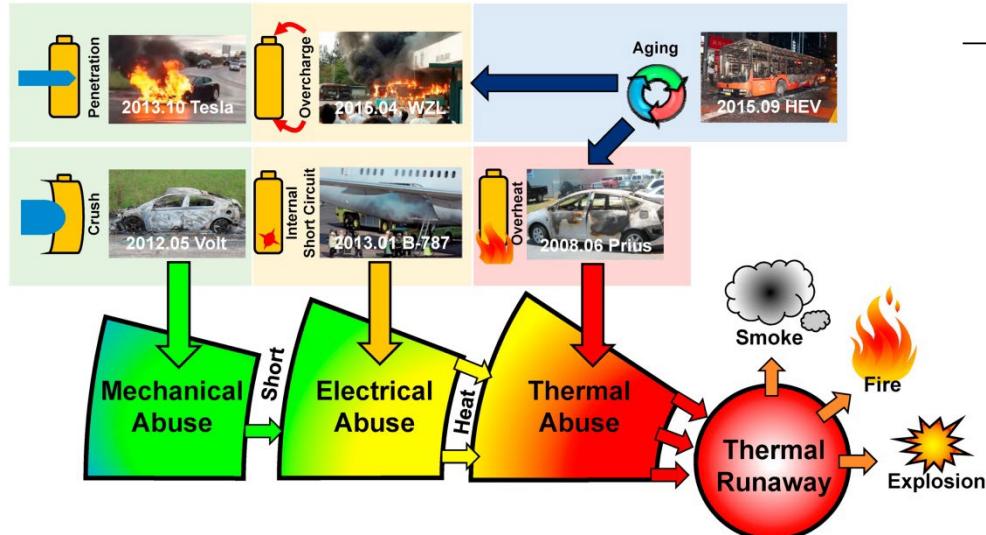


Dr. Carlos Ziebert

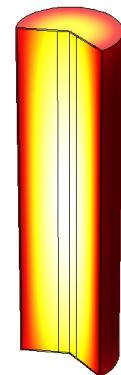
Group leader Batteries – Calorimetry and Safety”

E-Mail: Carlos.Ziebert@kit.edu

Motivation: Increase of safety and reliability of LIB



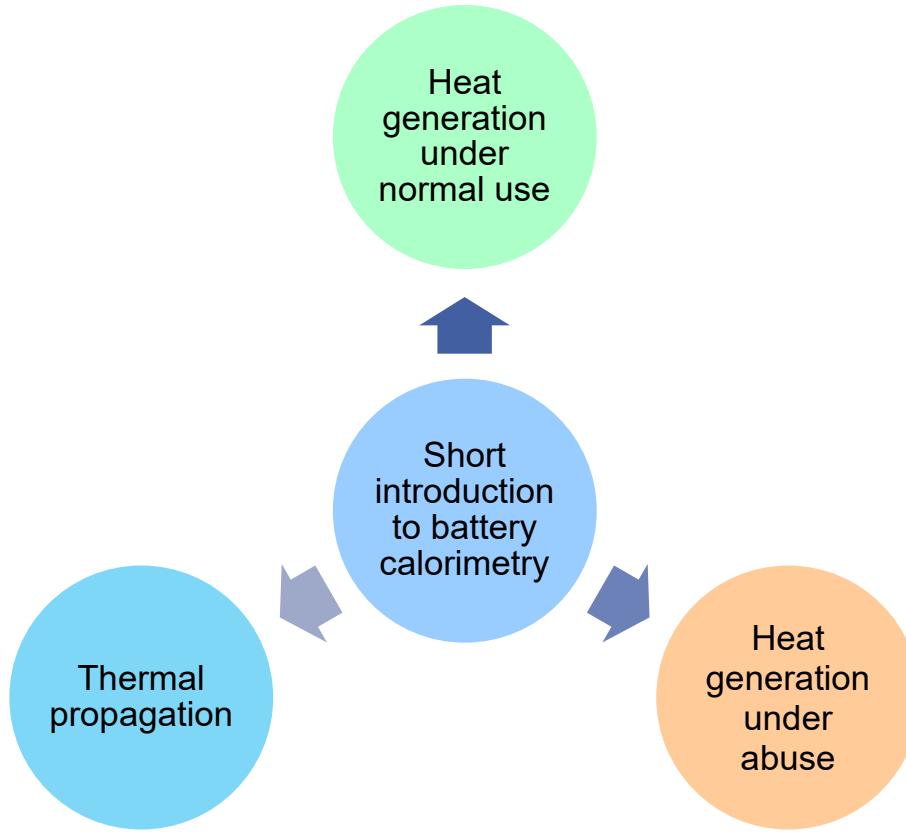
→ For improving battery management system (BMS) and thermal management system (TMS) electrochemical and thermal behavior of the cells have to be thoroughly studied



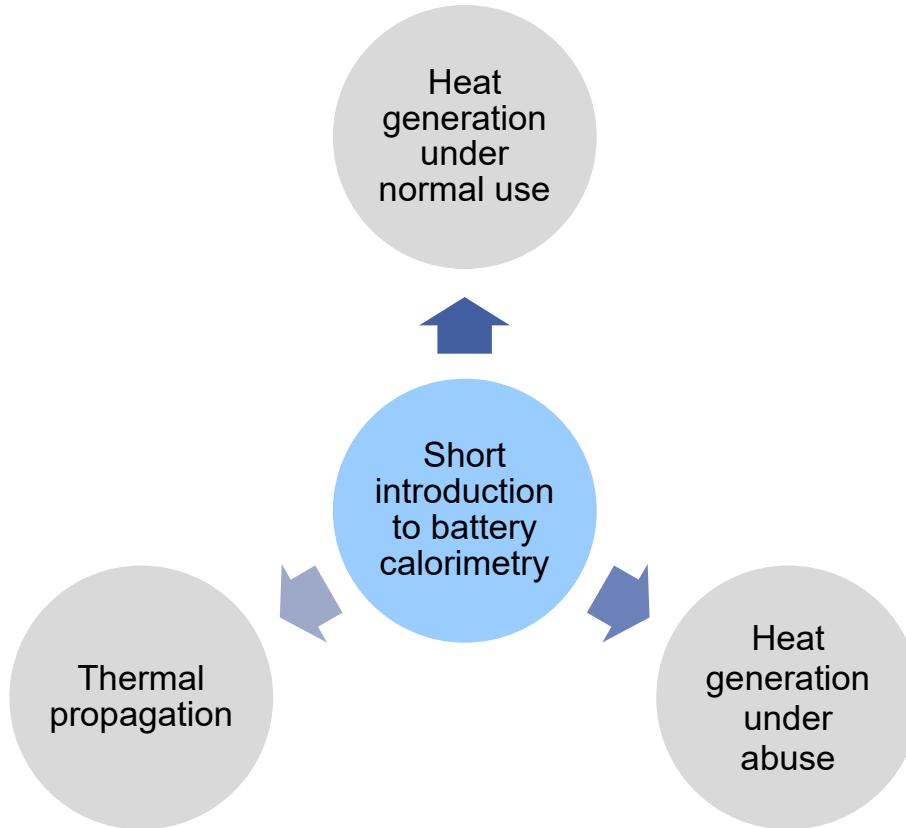
Feng et al., Energy Storage Materials 10 (2018) 246

Aim: Improvement of TMS and BMS by determination of quantitative data of thermal properties using calorimeters

Overview



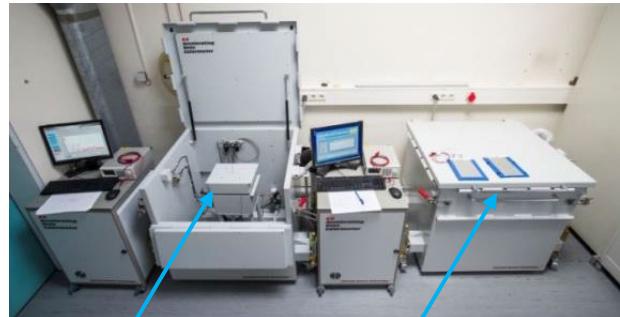
Overview



At IAM-AWP: Europe`s Largest Calorimeter Center



3 EV+ ARC: Ø: 40 cm
h: 44 cm



2 ES-ARC: Ø: 10 cm h: 10 cm 2 EV-ARC: Ø: 25 cm h: 50 cm

Equipment: 7 Accelerating rate calorimeters (ARC); 2 Tian-Calvet calorimeters; 5 DSC; IR camera; 13 Temperature chambers (23l - 400 l; -40°C to 180°C); 11 Cyclers (210 channels, 0.01-800 A); EIS; 2 GC/MS



How can calorimetry help in battery research?

Research for improving performance parameters

- Higher energy or power density
- Smaller heat release during operation
- Faster charging rates
- Increased cycle life and thermal life

Research for improving safety parameters

- Higher safe operating temperature
- Better resistance to thermal/mechanical/electrical abuse
- Less energy release during decomposition

Differential scanning calorimeters



Tian-Calvet calorimeters



Small ARC

Medium-size ARC



Pressure measurement in ARC



Large-size ARC

Nail penetration test in ARC

Components



1 - 80 mAh



3 - 5 Ah



40 - 75 Ah

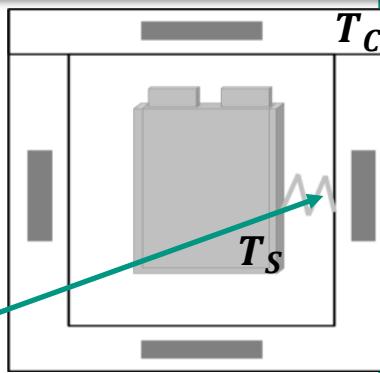
Cell Size and Capacity

Possible conditions in an ARC

An ARC provides **isoperibolic** and **adiabatic** conditions

Under isoperibolic conditions the environmental temperature is kept constant.

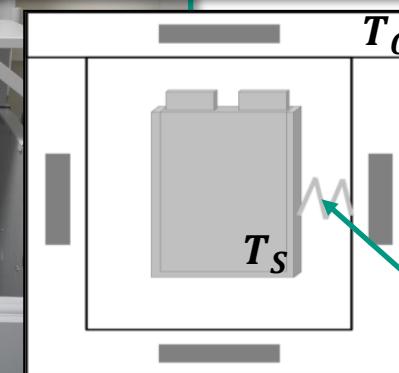
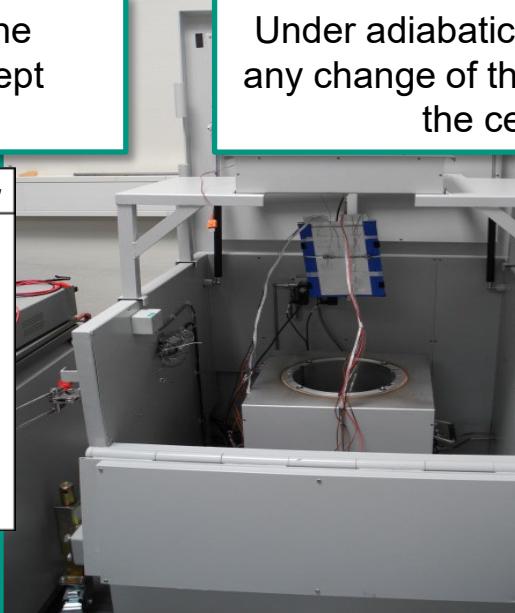
Under adiabatic conditions the heaters follow immediately any change of the bomb thermocouple thus preventing that the cell can transfer heat to the walls.



R_{th} defined

T_c constant

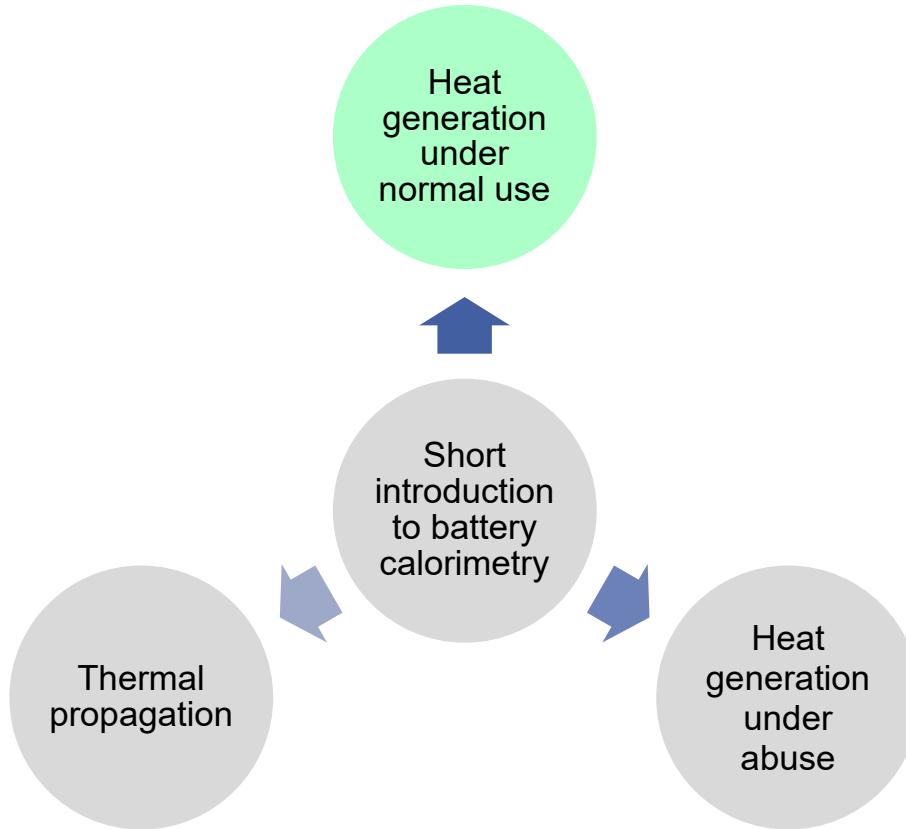
$$T_s(t) = T_{s_0} + \alpha \cdot t$$



$$\begin{aligned}T_c &= T_c(t) \\&= T_{c_0} + \alpha \cdot t\end{aligned}$$

R_{th} very high

Overview



Isoperibolic measurements

Ideal conditions

→ Single cell

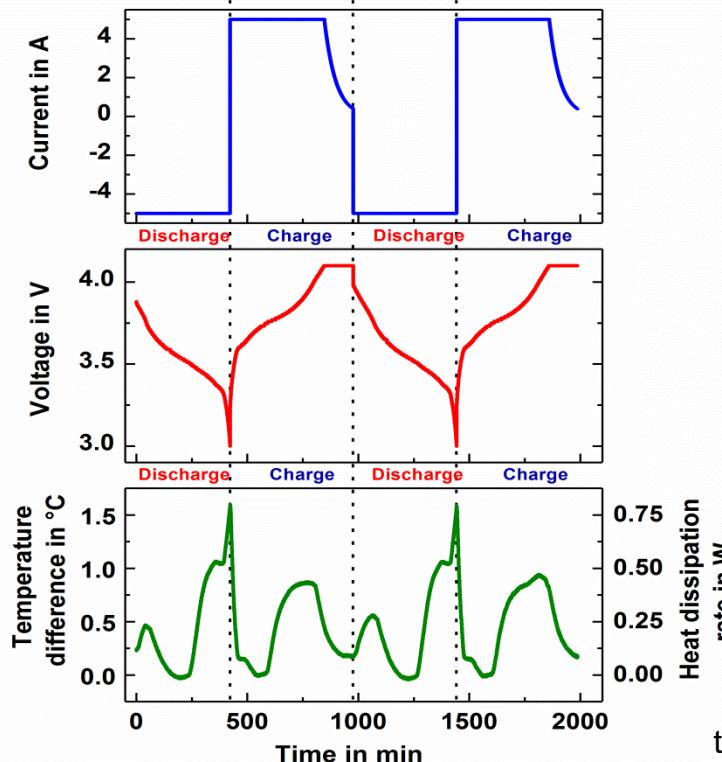
Discharge parameter:

- method: constant current (CC)
- $U_{\min} = 3.0V$
- $I = 5A \rightarrow C/8\text{-rate}$

Charge parameter:

- method: constant current, constant voltage (CCCV)
- $U_{\max} = 4.1V$
- $I = 5A \rightarrow C/8\text{-rate}$
- $I_{\min} = 0.5A$

→ after one electrochemical cycle the cell temperature reaches its initial value again



40 Ah pouch cell

$$\left(\frac{\delta E}{\delta T}\right) < 0$$

temperature coefficient negative!

Adiabatic Measurements

Worst Case Conditions

→ Cell in a pack surrounded by other cells

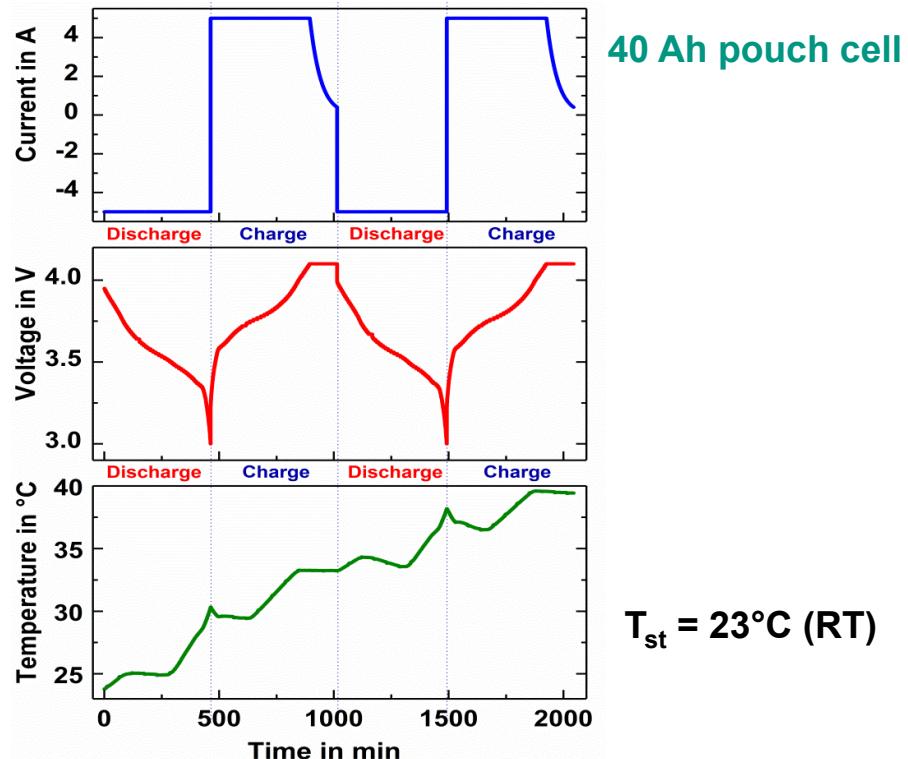
Discharge parameter:

- method: constant current (CC)
- $U_{\min} = 3.0V$
- $I = 5A \rightarrow C/8\text{-rate}$

Charge parameter:

- method: constant current, constant voltage (CCCV)
- $U_{\max} = 4.1V$
- $I = 5A \rightarrow C/8\text{-rate}$
- $I_{\min} = 0.5A$

→ after each electrochemical cycle the cell temperature increases further



Determination of total generated heat

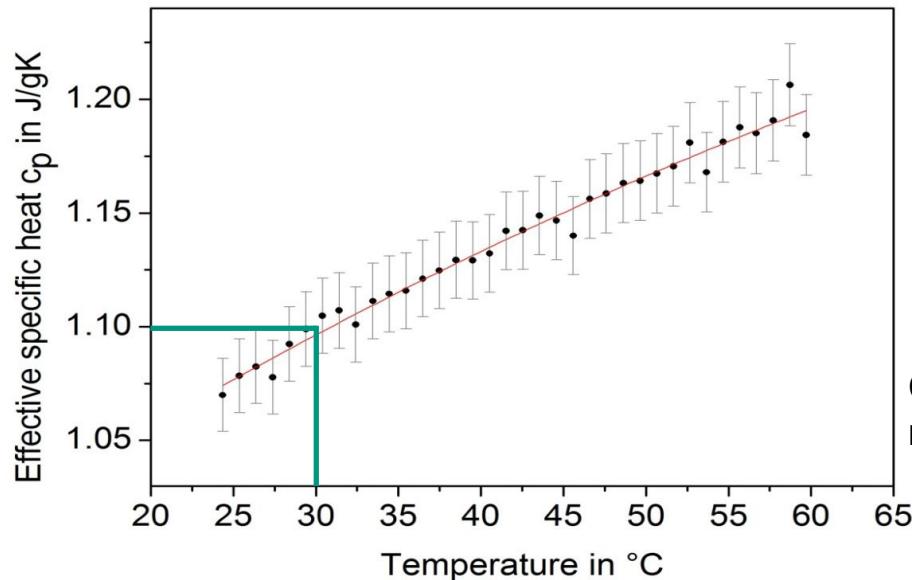
Heat generation of the cell during charging and discharging – Key data for thermal management and safety

Conversion of thermal data (temperature, temperature rate) to heat (Joule) and power (Watt) with the aim of understanding of heat release to determine heat removal requirements for thermal management.

To be measured:

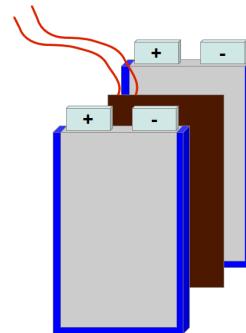
- Effective specific heat capacity
- Heat transfer coefficient
- Reversible heat rate and irreversible heat rate

Effective specific heat capacity c_p



e.g. at 30 °C $c_p = 1.095 \text{ J/g} \cdot \text{K}$

Important input data for simulation



40 Ah pouch cell

Sandwich setup
for pouch cells

Control of the current applied to the heater mat to ensure a constant heating rate

$$c_p = \frac{\Delta Q}{m \cdot \Delta T_{ad}} = \frac{\int U \cdot I dt}{m \cdot \Delta T_{ad}}$$

m: Mass of the cell

ΔT_{ad} : Temperature difference under adiabatic conditions

Heat transfer coefficient

Working principle of heat flux sensor (hfs)



gSKIN®-XP
(10mm x 10mm)

Tiny, serially connected semiconductor piles inside the sensor generate a voltage, which is proportional to the heat passing through the surface. The voltage is read out and depending on the sensor's sensitivity the results are converted into the heat flux .

Sensitivity:

$$S(T) = S_0 + (T - 22.5 \text{ } ^\circ\text{C}) \cdot S_c$$

$$S_0 = 10.04 \frac{\text{mV} \cdot \text{m}^2}{\text{W}}$$

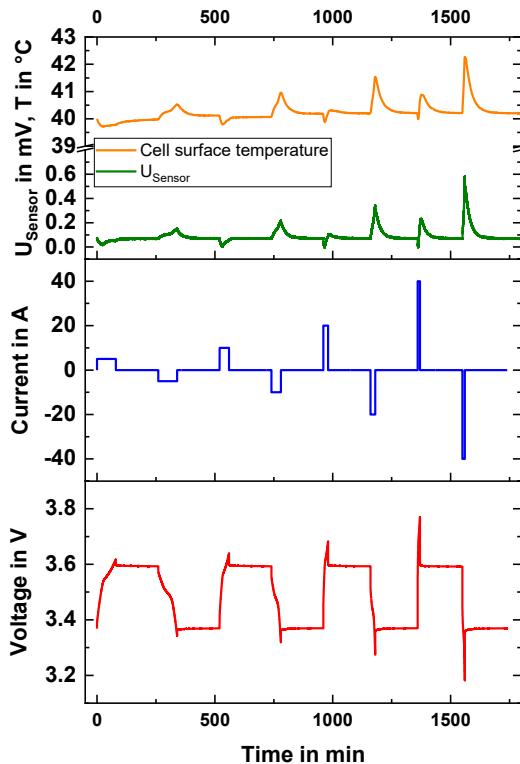
$$S_c = 0.0049 \cdot \frac{\text{mV} \cdot \text{m}^2}{\text{W} \cdot ^\circ\text{C}}$$

Room temperature sensitivity

Temperature correction factor

$$\Rightarrow h = \frac{\int \frac{U_{\text{sensor}}}{S(T)} dt}{\int_0^t (T - T_c) dt}$$

<http://shop.greenteg.com/shop/products-rd/gskin-xp/>
<https://www.greenteg.com/faq-heat-flux-sensing/>



Comparison of values for generated heat

1) Adiabatic Measurement

$$\dot{Q}_{gen} = mc_p \frac{dT}{dt}$$

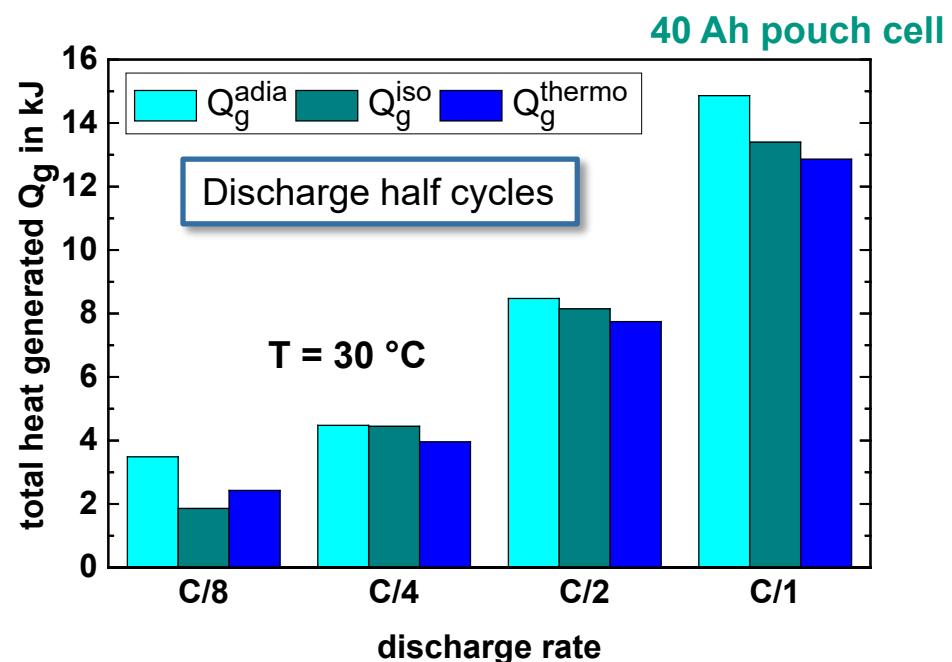
2) Isoperibolic Measurement

$$\dot{Q}_{gen} = mc_p \frac{dT}{dt} + Ah \cdot (T_S - T_C)$$

3) Measurement of irreversible and reversible heat

$$\dot{Q}_{gen} = -I(E_0 - E) - IT \frac{dE_0}{dT}$$

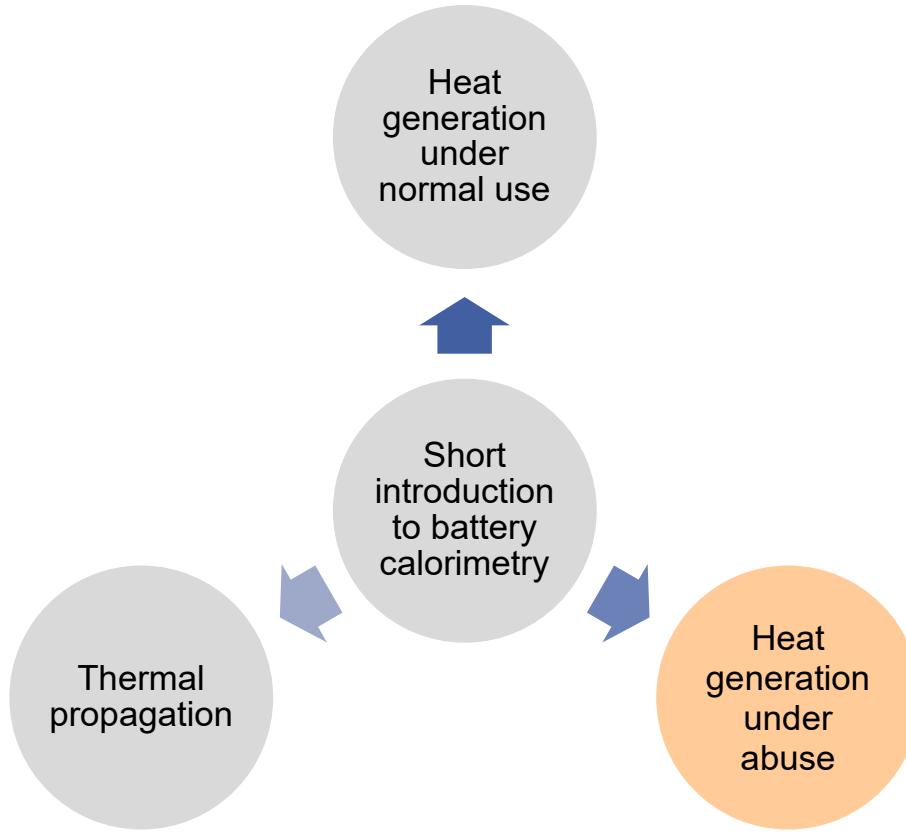
E_0 : Open circuit voltage (OCV), E : cell potential



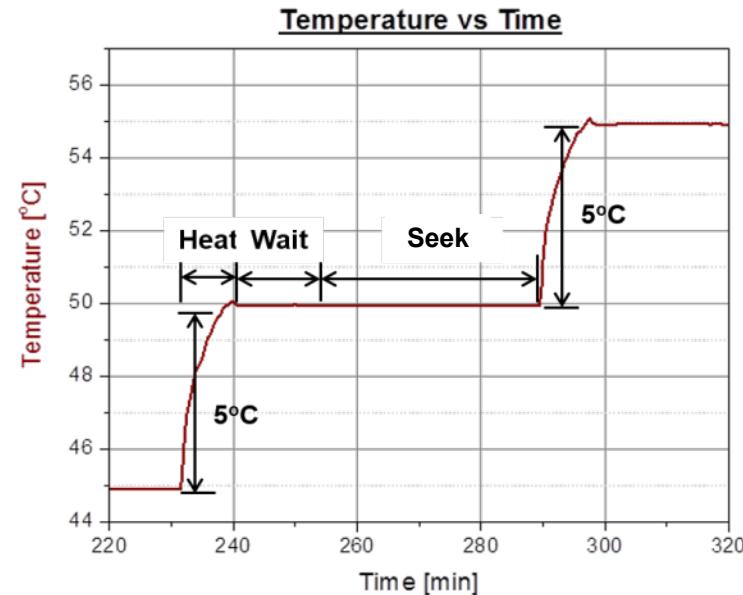
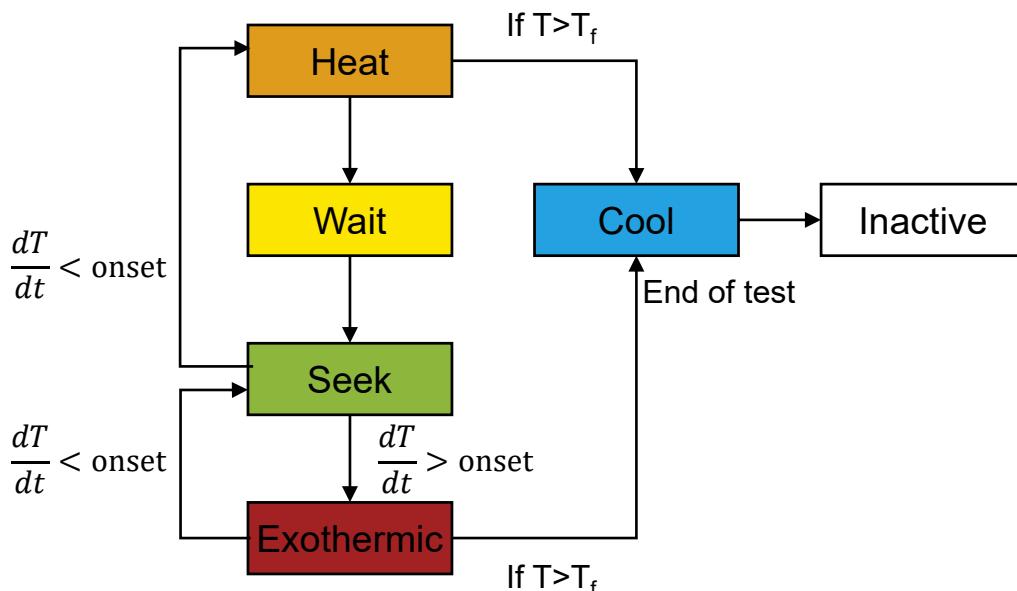
Conclusion: good agreement between the values determined by the different methods

E. Schuster, C. Ziebert, A. Melcher, M. Rohde, H.J. Seifert, J. Power Sources 268 (2015) 580-589

Overview



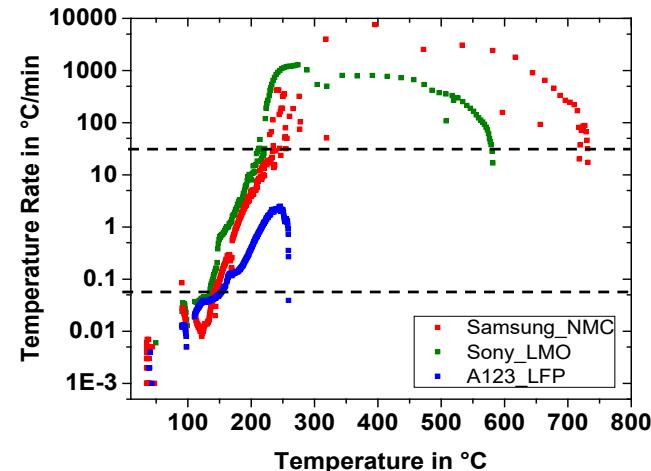
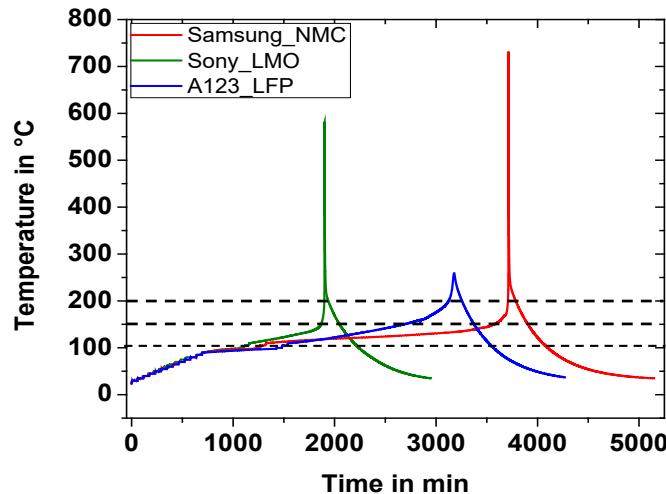
Thermal abuse: Heat-Wait-Seek (HWS) Method in ARC



Example of a Heat-Wait-Seek step

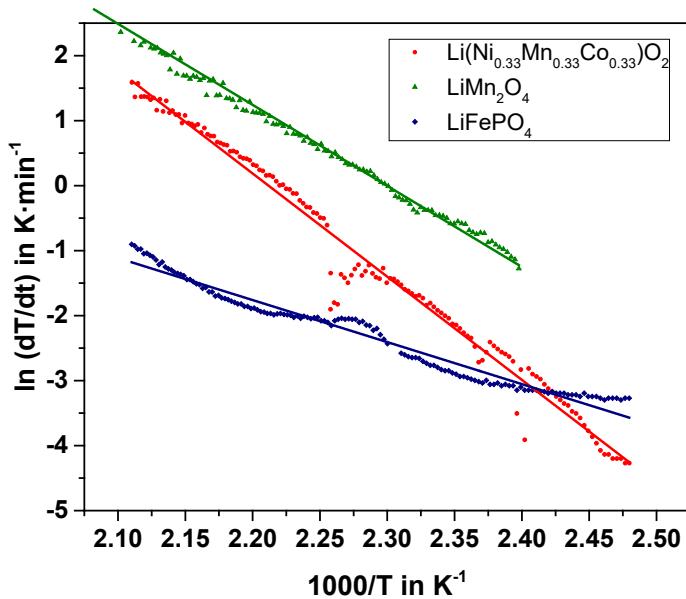
C. Ziebert, A. Melcher, B. Lei, W.J. Zhao, M. Rohde, H.J. Seifert, Electrochemical-thermal characterization and thermal modeling for batteries, in: L.M. Rodriguez, N. Omar, Eds., EMERGING NANOTECHNOLOGIES IN RECHARGEABLE ENERGY STORAGE SYSTEMS, Elsevier Inc. 2017, ISBN 978032342977.

Comparison of 18650 cells with different cathode materials



- $80 < T < 130^\circ\text{C}$: low rate reaction, $0.02 - 0.05 \text{ }^\circ\text{C}/\text{min}$: exothermic decomposition of the SEI
- $130 < T < 200^\circ\text{C}$: medium rate reaction, $0.05 - 25 \text{ }^\circ\text{C}/\text{min}$: solvent reaction, exothermic reaction between embedded Li ions and electrolyte => reduction of electrolyte at negative electrode
- $T > 200^\circ\text{C}$: high rate reaction, higher than $25 \text{ }^\circ\text{C}/\text{min}$: Exothermic reaction between active positive material and electrolyte at positive electrode => rapid generation of oxygen

Activation energies and reaction heats



Activation energy: $\ln\left(\frac{dT}{dt}\right) \approx \ln(\Delta T_{ad} \cdot A) - \frac{E_a}{k_b \cdot T}$

E_a : Activation energy, A : pre-exponential factor

k_b : Boltzmann constant = $8.62\text{e}^{-5} \text{ eV} \cdot \text{K}^{-1}$

Cathode Material	LiMn_2O_4 (LMO)	LiFePO_4 (LFP)	$\text{Li}(\text{Ni}_{0.33}\text{Mn}_{0.33}\text{Co}_{0.33})\text{O}_2$ (NMC)
Onset temperature of self-heating in °C	91	90	91
T_{\max} in °C	303	259	731
$(dT/dt)_{\max}$ in °C/min	1429	3	7577
c_p at 60°C SOC100 in J/g·K	0.83	1.19	0.95
E_a in eV	1.07	0.56	1.37
Reaction heat in J/g	180	184	597
Reaction heat in J/g	350-640 [1,2]	260 [2]	600 [2]

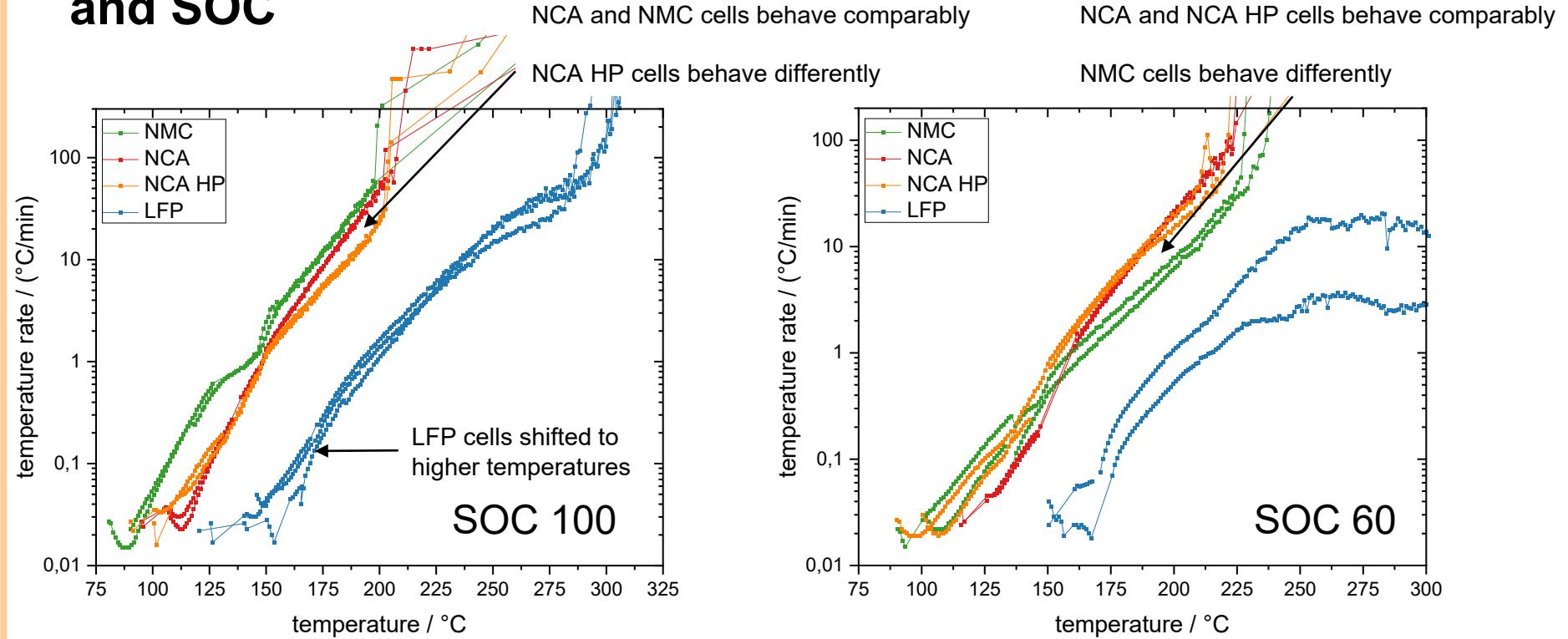
[1] R. Spotnitz, J. Franklin, *J. Power Sources*, 113, 81 (2003).

[2] H. F. Xiang, H. Wang, et al., *J. Power Sources*, 191, 575 (2009).

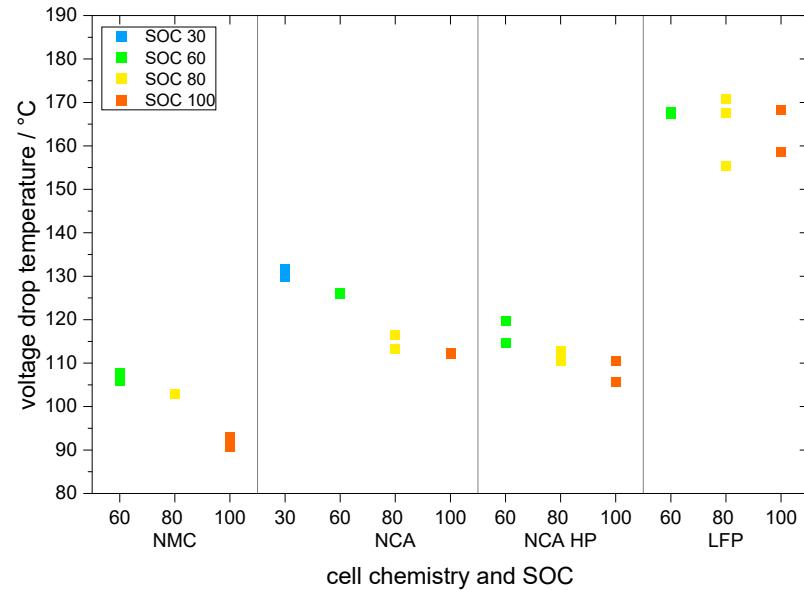
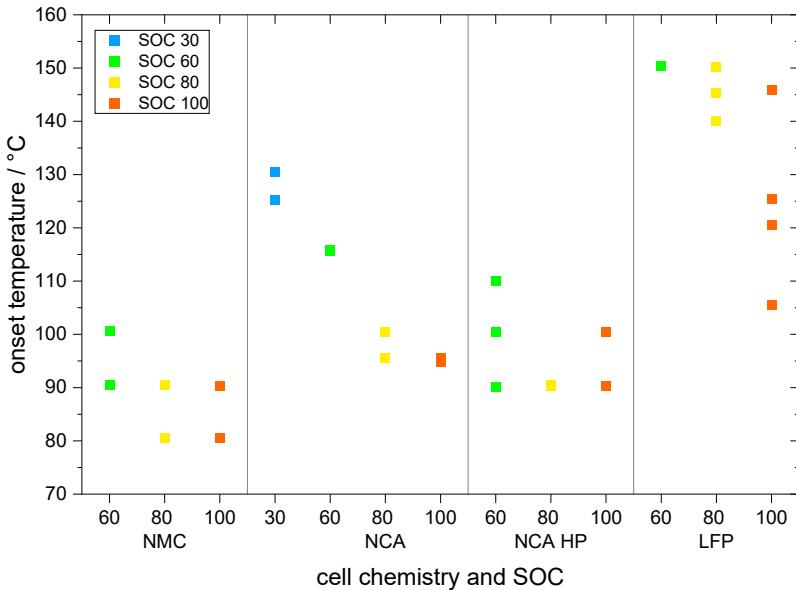
Reaction heat: $\frac{\Delta H}{m} = c_p \cdot \Delta T_{ad}$

Important input data for simulation

Comparison of 21700 cells with different cathode materials and SOC

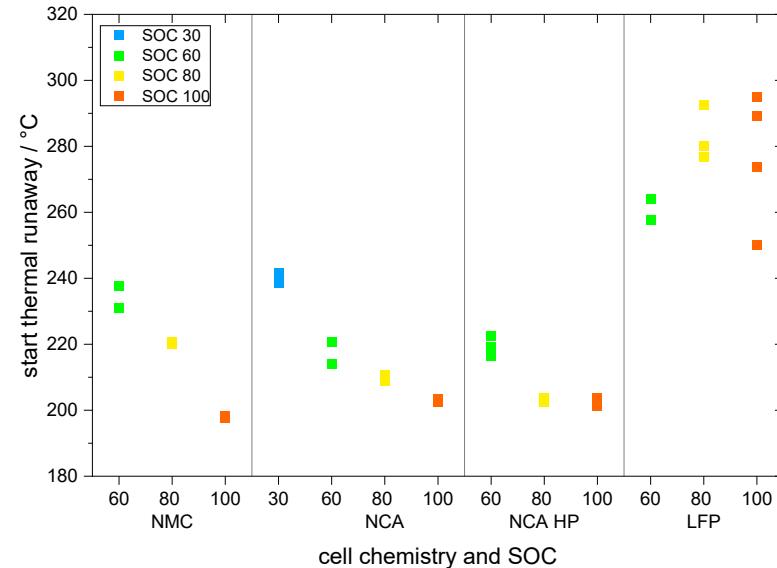
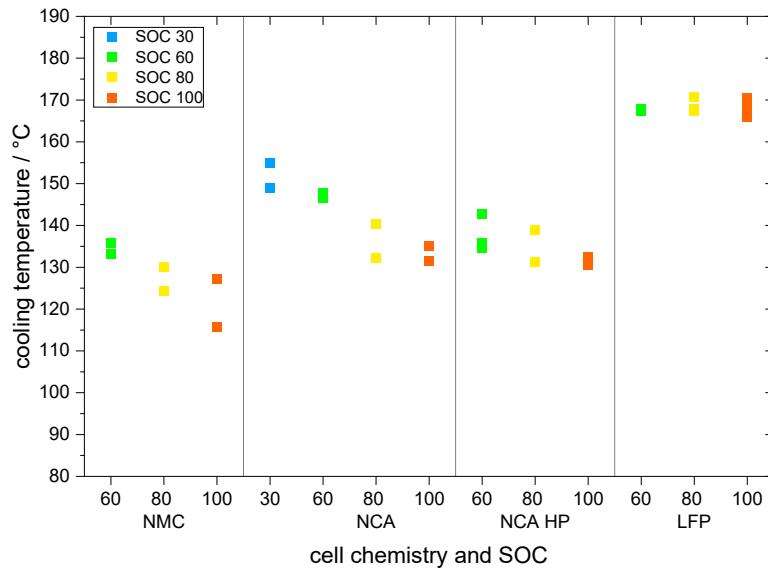


Onset and CID triggering temperature



- NCA and NMC (on the right also NCA HP): **higher SOC results in lower temperature**
- NMC: **lower temperature than NCA, NCA HP and LFP cells**
- LFP: **significantly higher temperatures, no clear SOC influence**
=> data has higher variation, therefore more experiments have been conducted

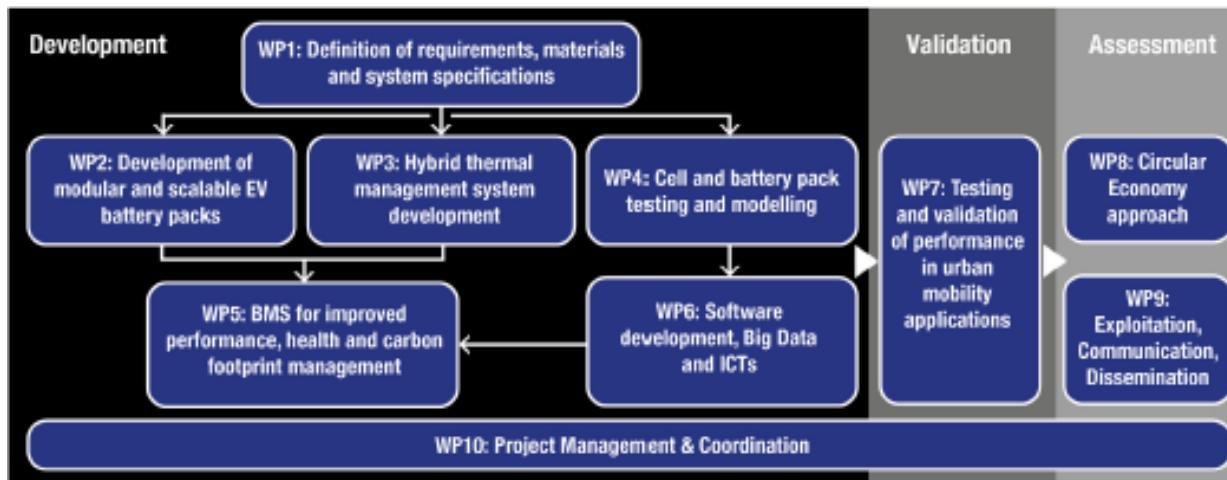
Venting and start of thermal runaway / highest rate (LFP) temperature



- NMC, NCA, NCA HP: **clear influence of SOC, temperatures close to each other**
- NMC: **slightly earlier than NCA cells (for cooling)**
- LFP: **significantly higher temperatures, influence of SOC unclear**
but step between CID triggering and venting is much smaller as well as the self heat rates => harder to detect

HELIOS (High-pErformance moduLar packs for sustainable urban electrOmobility Services)

The HELIOS project aims at developing and integrating innovative materials, designs, technologies and processes to create a **new concept of smart, modular and scalable battery pack for a wide range of electric vehicles used in urban electromobility services**, from mid-size full-electric vehicles to electric buses, **with improved performance, energy density, safety and Levelized Cost of Storage (LCoS)**.

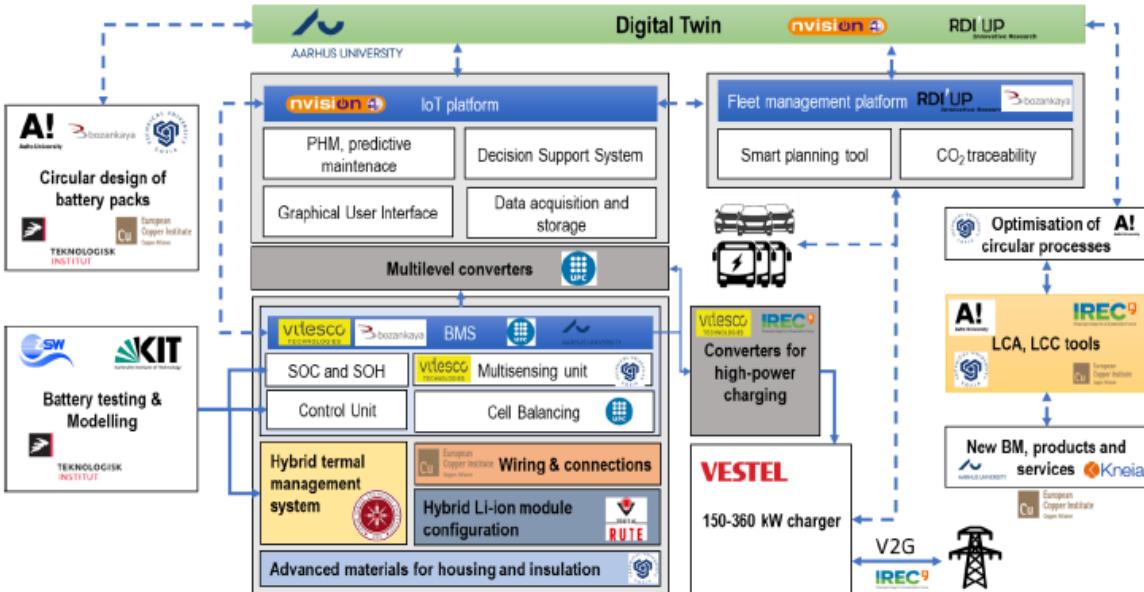


Start date:	01-01-2021
Funding source:	EC
Funding:	appr. 10 million Euro
Partners:	18 from 8 countries

HELIOS WP Overview

<https://www.helios-h2020project.eu/project>

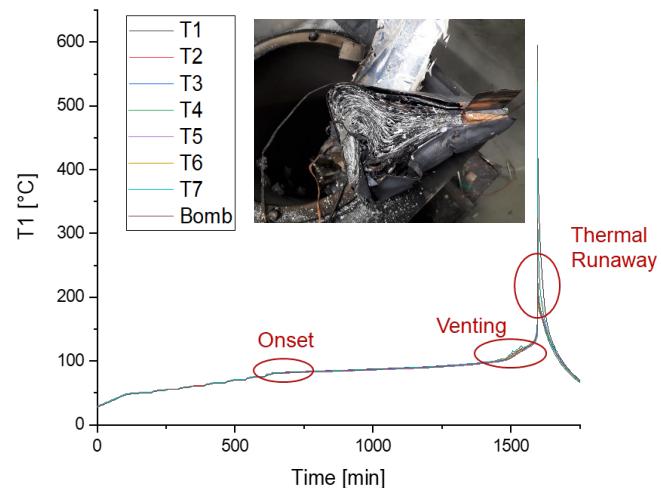
HELIOS (High-pErformance moduLar packs for sustainable urban electrOmobility Services)



HELIOS main building blocks



Sileo S12 e-bus produced by Bozankaya

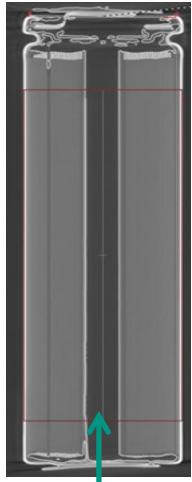


Exemplary safety test on large pouch cell

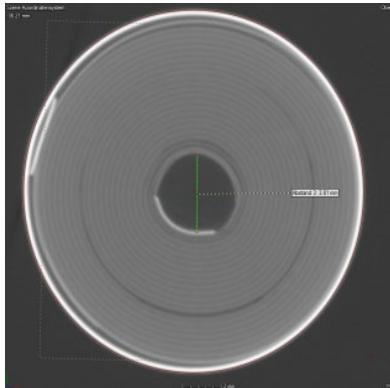


Analiba

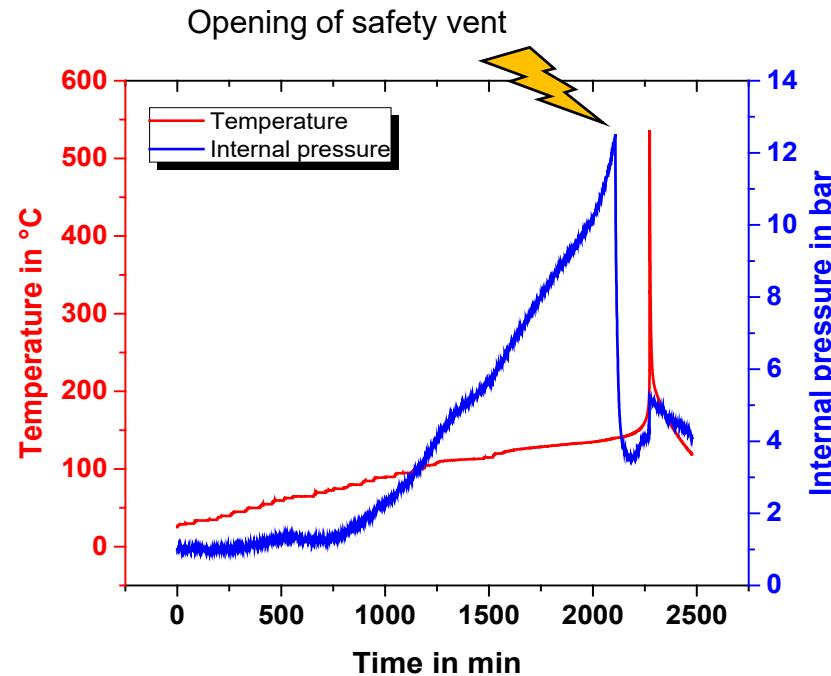
Internal pressure measurements on 18650 cells



Pressure line (\varnothing 1.5 mm)



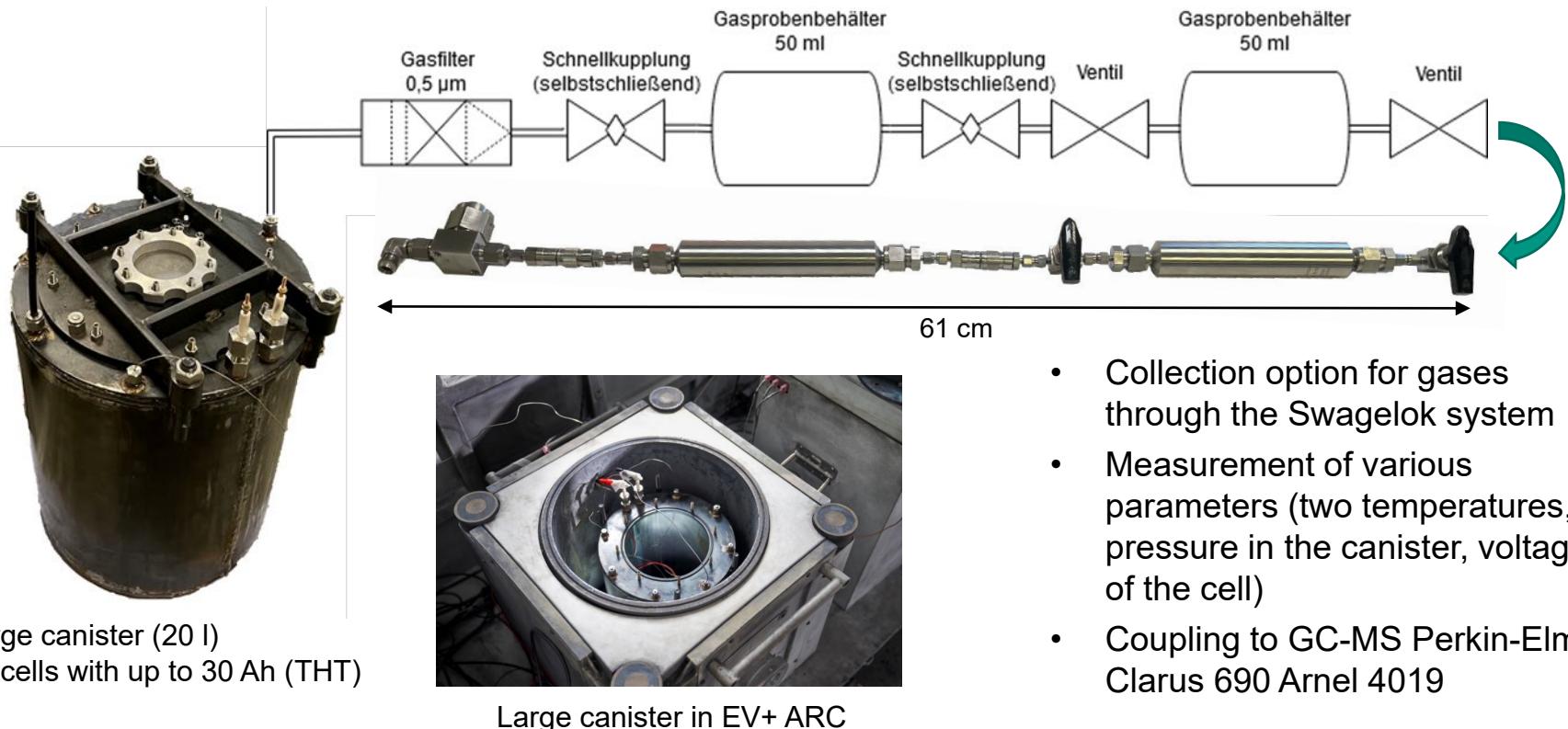
1.6 Ah 18650 cell



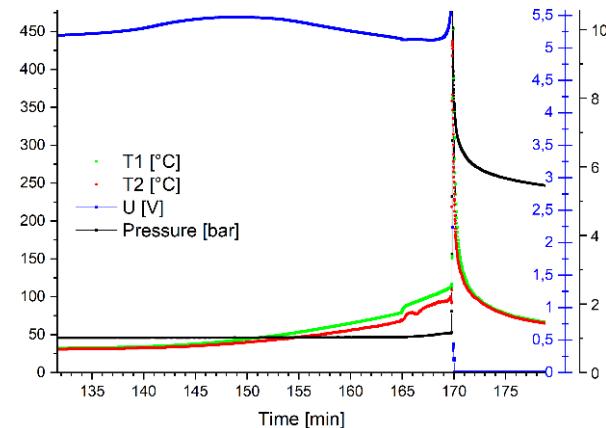
Internal pressure could be used in BMS for early prediction of processes leading to thermal runaway

B. Lei, W. Zhao, C. Ziebert, A. Melcher, M. Rohde, H.J. Seifert, *Batteries* 2017, 3, 14, [doi:10.3390/batteries3020014](https://doi.org/10.3390/batteries3020014).

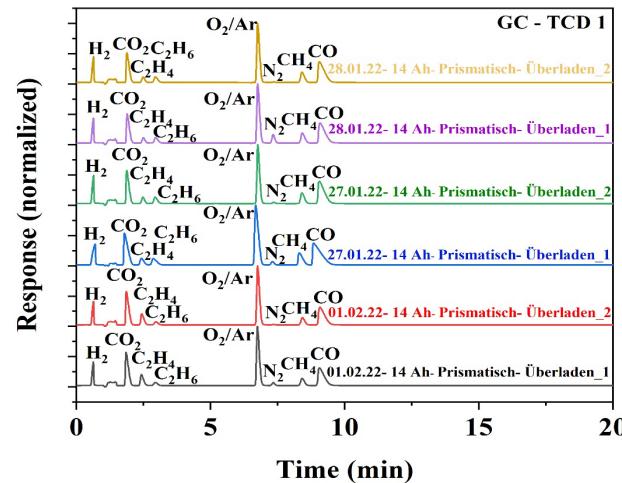
Gas collection after ARC Abuse-Tests



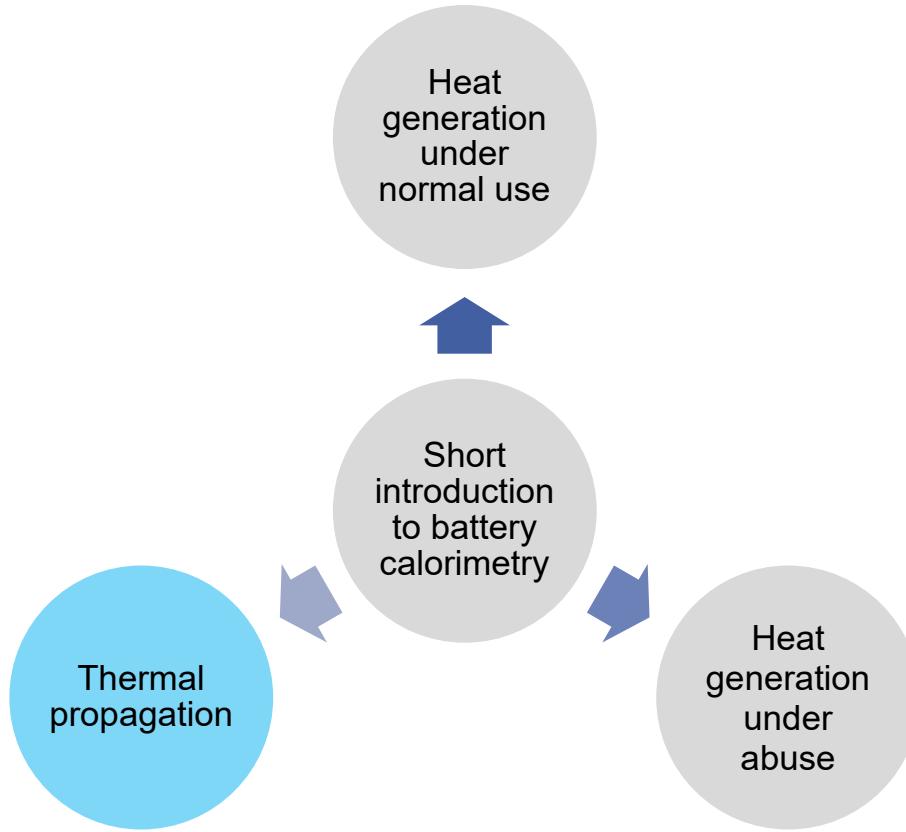
Gas analysis after 0.5 overcharge test of 14 Ah prismatic cell



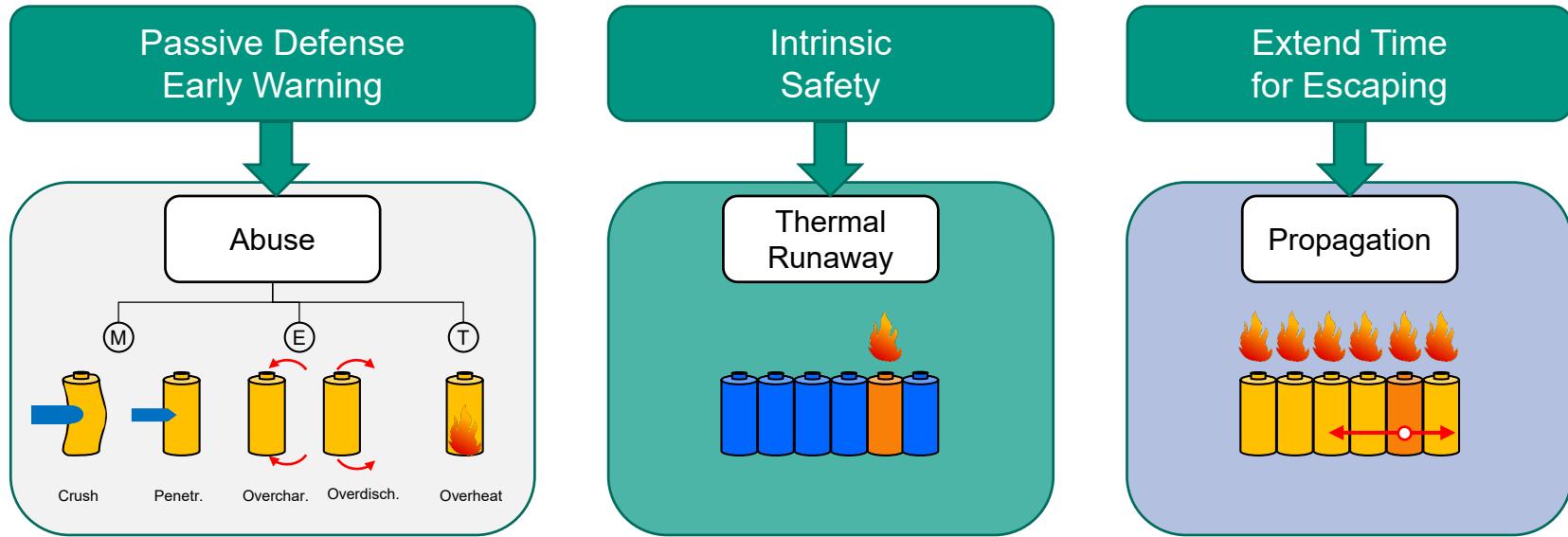
- Cell shows venting after 165 min and goes into thermal runaway after 170 min
- Data determined:
 - Maximum temperature: 534 °C
 - Maximum pressure: 12.5 bar
 - Evolved gas volume: 60 l (at 25 °C, 1013 mbar)



Overview

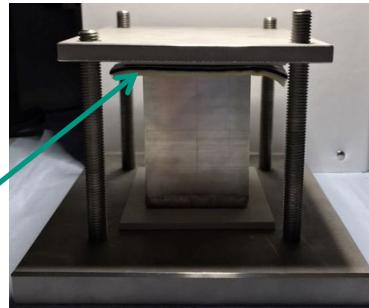
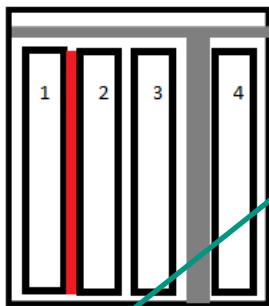
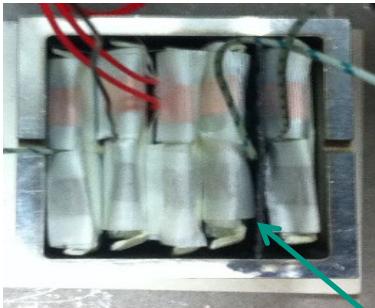


Thermal propagation



Adapted from: Feng et al., Energy Storage Materials 10 (2018) 246

Thermal propagation tests on small pack level

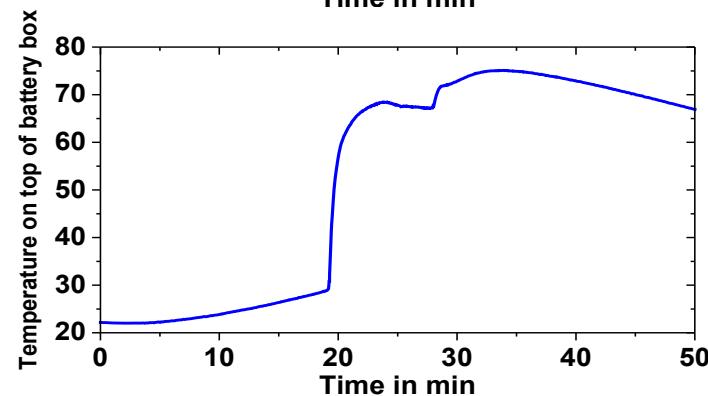
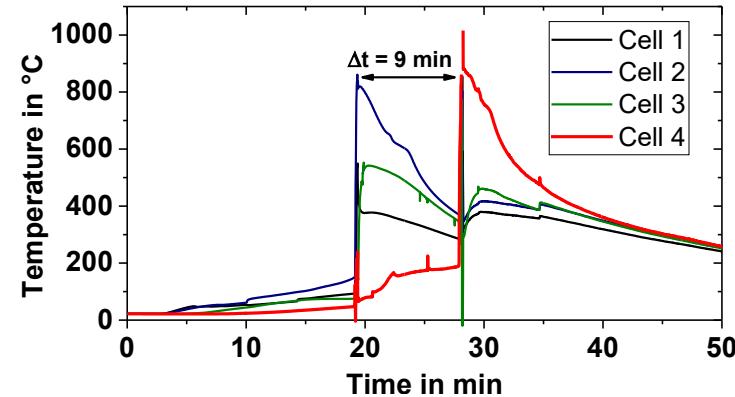


Gray: protective material for cell 4 and lid of battery box
Red: heater mat for thermal runaway initiation

Material qualification for propagation prevention

Optimized Multilayer:

- Extended time for propagation: 9 min
- Improved heat protection: temperature on top of battery box < 80 °C during thermal runaway



Summary: Possible calorimetric measurements

Normal use conditions

- Isoperibolic or adiabatic measurements
 - Measurement of temperature curve and temperature distribution during cycling (full cycles, or application-specific load profiles), ageing studies
 - Determination of the generated heat, Separation of heat in reversible and irreversible parts

Abuse conditions

- Thermal abuse: Heat-wait-seek test, ramp heating test, thermal propagation test
 - Electrical abuse: External short circuit, Overcharge, Deep discharge
 - Mechanical abuse: Nail penetration test
 - Temperature measurement
- For each:**
- External or internal pressure measurement
 - Gas collection and analysis, Post Mortem Analysis, Ageing studies



Important data for BMS, TMS and safety systems

Acknowledgement

Thank you for your attention!

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<https://www.iam.kit.edu/awp/169.php>

We thank

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und Forschung



HELMHOLTZ
ASSOCIATION



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Forschungsgemeinschaft
German Research Foundation



Forschungszentrum Jülich



VDI|VDE|IT **IKC+Ba**

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