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Synthesis of Ni-Fe-CO₃ layered double hydroxide as Effective Adsorbent to remove Cr(VI) and ARS-dye from aqueous media

Ismail M. Ahmed ^{a,*}, Ahmed I. Abd-Elhamid ^b, Ashraf A. Aly ^c, Stefan Bräse ^{d,e,*}, AbdElAziz A. Nayl ^{a,*}

^a Department of Chemistry, College of Science, Jouf University, Sakaka 72341, Aljouf, Saudi Arabia

^b Composite and Nanostructured Materials Research Department, Advanced Technology and New Materials Research Institute (ATNMRI), City of Scientific Research and Technological Applications (SRTA-City), New Borg Al-Arab, Alexandria 21934, Egypt

^c Chemistry Department, Faculty of Science, Organic Division, Minia University, El-Minia 61519, Egypt

^d Institute of Organic Chemistry (IOC), Karlsruhe Institute of Technology (KIT), Fritz-Haber-Weg 6, 76133 Karlsruhe, Germany

^e Institute of Biological and Chemical Systems – Functional Molecular Systems (IBCS-FMS), Hermann-von-Helmholtz-Platz 1, D-76344 Eggenstein-Leopoldshafen, Germany

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ABSTRACT

Ni²⁺/Fe³⁺LDH, (Ni-Fe-CO₃ LDH) with Ni/Fe molar ratio 3.0 was synthesized by coprecipitation for the remediation of chromium (VI), and Alizarine Red-S (ARS-dye) as anionic species. The investigated adsorbent was characterized by TGA, SEM, XRD, BET and FTIR. The effect of the hydrogen ion concentration of the medium, shaking time, ARS-dye and/or Cr(VI) concentration and adsorbents mass on the process was studied. The results of Ni-Fe-CO₃ LDH fitted well with the pseudo-second-order model. Langmuir isotherm is more favor than the Freundlich isotherm with maximum capacity (Q_{max}) of 69.9 and 6.1 mg/g for ARS-dye and Cr(VI), respectively.

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1. Introduction

Annually, huge quantities of dye-contaminated wastewater are distributed into water bodies from many industrial activities (Khamis et al., 2020). This type of waste has harmful and poisonous effects on living organisms, human organs, and reduces the sunlight needed for aquatic plants to make photosynthesis (Rathinam et al., 2021). On the other hand, a large amount of toxic elements as chromium that results from various industrial applications and discharge into the surrounding environment (Khamis et al., 2020; Gautam et al., 2014). Cr(VI) is harmful as it causes irritation of the skin, eyes and respiratory tract and may lead to lung cancer (Zhang et al., 2019; Hadi et al., 2017). Synthetic dyes cause coloration of the effluent and the degradation of most of them are carcinogenic as anthraquinone – type dyes as Alizarine Red-S. Hence, in the field of wastewater treatment and to safeguard the environment, the removal of organic dyes and Cr(VI) is of utmost importance. Generally, several techniques were applied for the remediation of dyes and Cr(VI) as precipitation, coagulation, aerobic oxidation, solvent extraction, ion exchange, membranes and sorption (Peng et al., 2018; Jargalsaikhan et al., 2021; Genawi et al., 2020; Sheng et al., 2018; Yi et al., 2018, 2014; Chen et al., 2022; Hidalgo et al., 2020; Park et al., 2022). These methods have some limitations, though, in that even the degradable species of dye may be more hazardous. Sorption has an advantage over the abovementioned techniques as it is simple and of low operational cost. Recently more

* Corresponding authors.

E-mail addresses: imibrahim@ju.edu.sa (I.M. Ahmed), ahm_ch_ibr@yahoo.com (A.I. Abd-Elhamid), ashraf.shehata@mu.edu.eg (A.A. Aly), stefan.braese@kit.edu (S. Bräse), aanayel@ju.edu.sa (A.A. Nayl).

attention was paid on layered double hydroxide (LDH) adsorbents, anionic clays that belong to hydroxalite group due to ease of preparation in addition to their higher adsorption capacity towards organic dyes and heavy metals. The LDHs have a general formula $[M_{1-x}^{2+} M_x^{3+} (OH)_2 \cdot 2A^{n-} \cdot x/n \cdot mH_2O]$, where M is metal cation and A^{n-} is the interlayer anion (Ahmed, 2021). LDHs found many applications such as drug delivery, catalysts, gas sensors and adsorbents for the remediation of removal of toxic elements and organic dyes. The performance of LDH anion-exchange can be enhanced by changing the cation in the laminates, temperature, pressure, and solution pH during their preparation that affects the morphology of the obtained LDHs (Yao et al., 2017; Lu et al., 2016; Aguiar et al., 2013; Pahalagedara et al., 2014; Blaisi et al., 2018; Tan et al., 2016; Zhu et al., 2018; Dai et al., 2022; Amin et al., 2022; Jiang et al., 2022; Charafi et al., 2023; Mahieddine and Adnane-Amara, 2023; Li et al., 2016; El-Reesh et al., 2020; Chao et al., 2018; He et al., 2018; Intachai et al., 2022). In spite of their distinctive physicochemical features and the high ion exchange capacity, they have some drawbacks, such as mass loss during anion exchange and their relatively high-water solubility. In this respect, Ni-Fe LDHs have exceptional adsorption properties due to their large surface area and surface charge density. They have also been demonstrated to be effective at removing a number of pollutants from water, including heavy metals, dyes, and organic compounds. They are also considerably more economical than other LDHs. Ni-Fe LDH are a reliable option for water treatment applications since they have been found to have good stability over a variety of environmental conditions, such as pH, temperature, and salinity. In addition to their relatively low solubility product ($pK_{sp} = 60.81$) (El-Reesh et al., 2020). In this study, Ni-Fe- CO_3 LDH, the factors influence the sorption processes as the effect of pH, initial Cr(VI) and ARS-dye concentrations, equilibration time, adsorbent mass and temperature were investigated for the remediation of Cr(VI) and ARS-dye as anionic species. A comparison study was looked into to gauge effectiveness of the prepared Ni-Fe- CO_3 LDHs to remove Cr(VI) and ARS-dye as anionic species with other recently published works.

2. Experimental

All chemicals were used without further purifications, distilled water extracted with a purification system was used Milli-Q direct 8 purifications (Millipore, France).

2.1. Synthesis of Ni-Fe- CO_3 LDH

250 mL of 1.5 M $NiCl_2 \cdot 6H_2O$ and 0.5 M $FeCl_3$ were added drop wise to 50 mL mixture of NaOH (1.0 M) and Na_2CO_3 (2.0 M) with vigorous stirring for 2.0 h and maintaining the pH of 11.0 ± 0.1 . The slurry formed was aged at 80 °C for 5.0 days, centrifuged, washed with distilled water and finally, dried at 80 °C overnight before being used.

2.2. Instrumentation

XRD of LDH was characterized using a Shimadzu XRD-7000 diffractometer. The concentrations of Cr(VI) and/or ARS were investigated by Perkin Elmer UV-Visible Spectrophotometer. FT-IR spectra were performed using (FTIR)IR – Tracer 100, Shimadzu, Japan. The BET was characterized utilizing Quantachrome, NOVA 4200 e series, USA. The morphology of LDH was studied by Thermo Scientific Quattro ESEM, USA. The thermal decomposition behavior was examined by a Shimadzu, TGA 51.

2.3. Sorption of Cr(VI) and ARS-dye onto Ni-Fe- CO_3 LDH

0.025 g of the Ni-Fe- CO_3 LDH was equilibrated with 10.0 mL of and 10.0 mg/L for Cr(VI) or ARS-dye at pH 6.0, unless otherwise was stated. ARS-dye concentration was measured by UV-Vis spectrophotometer at λ_{max} 555.0 nm while Cr(VI) was estimated using 1,5-Diphenylcarbazine method at λ_{max} 545.0 nm (Marzenko, 1986). The removal percent was estimated as follow:

$$R\% = \left(\frac{C_o - C_e}{C_o} \right) \times 100 \quad (1)$$

Where C_o and C_e are the initial and equilibrium concentration, respectively.

3. Results and discussion

3.1. Characterization of Ni-Fe- CO_3 LDH

3.1.1. TGA

TGA is used to evaluate the thermal behavior materials. The Ni-Fe- CO_3 -LDH shows two decomposition steps refer to the surface moisture, interlayer water and hydroxyl groups (12.5%, 25–200 °C). The second (from 200 to 350 °C) is due to partially decarboxylation, mass loss of 15.6% (Cardinale et al., 2022), Fig. 1.

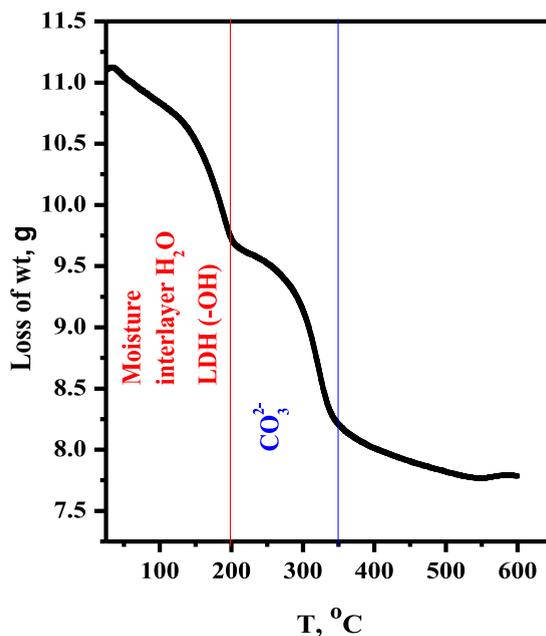


Fig. 1. The thermogravimetric analysis (TGA) of Ni-Fe-CO₃ LDHs.

3.1.2. SEM

The SEM instruments are utilized as an effective technique to detect the morphology of the surface of the Ni-Fe-CO₃ LDH. To understand the efficiency of the sorption technique, SEM images of the surfaces of Ni-Fe-CO₃ LDH was represented in Fig. 2. As shown in Fig. 2, 3D hierarchical micro/nanostructures were formed with various types of textural pores that clearly appeared with increasing the magnifications (Habib et al., 2020). The distinct morphologies are attributed to the presence of Ni²⁺ ions which reduces the surfaces energies difference between the polar- and nonpolar-planes (Habib et al., 2020; Kim et al., 2017). The fabricated Ni-Fe-CO₃-LDH materials illustrated aggregated flakes that create many cavities that can enhance the adsorption processes of anionic species (Qi et al., 2011).

3.1.3. FTIR

FT-IR spectra in Fig. 3, before and after sorption show very characteristic bands for the hydrotalcite-like phases. The pre-adsorption (a) band at 3439 cm⁻¹ that refer to the stretching vibration of hydroxyl group, bending vibration of water appears at 1633 cm⁻¹ while carbonate vibration appears at 1360 cm⁻¹. The three peaks at 400–700 cm⁻¹ that refers to correspond to M–O (M: Ni²⁺, Fe³⁺) appeared in all LDHs samples. While the aromatic ring at ARS loaded LDH appears at 1016 cm⁻¹, the change in the FTIR spectra pre and post sorption confirms the complexation between LDH and both adsorbates (Flavio et al., 2008; Ahmet, 2009; Ayawei et al., 2015; Mališová et al., 2018; Xue et al., 2019).

3.1.4. XRD

XRD of Ni-Fe-CO₃ LDH, Fig. 4, shows different diffraction peaks at $2\theta \approx 11.68, 23.27, 34.99, 36.76, 45.87, 61.5,$ and 65.31° . These peaks can be due to the 003, 006, 009, 012, 015, 110, and 113 diffraction peaks, respectively. The peaks (003), (006) and (009) are assigned to the lamellar material. While the diffraction peaks around 60° and 61.5° which correspond to carbonate anion (Wiyantoko et al., 2015) and by applying in Sherrer equation, the corresponding crystallite (grain) size was found to be 0.47 nm. Indeed, most of these peaks have straightly and symmetrically characteristics, completely proving that considerable purity of Ni-Fe-CO₃-LDH.

3.1.5. BET measurement

The surface area information can be deduced from the shape of adsorption isotherm. The adsorption isotherm of Ni-Fe-CO₃-LDH is mainly mesoporous in nature according IUPAC classification and classified as Type III (Sing, 1985). The measured BET surface area of Ni-Fe-CO₃-LDH is 110.70 m²/g and the pore volume and pore size were 0.12 cc/g and 15.45 Å, respectively, Fig. 5.

3.2. Sorption investigations

3.2.1. Effect of pH

pH of the solution affects the nature of the adsorbent and adsorbate. The influence of medium pH was examined in the range 3.0–9.5 on the sorption behavior of Cr(VI) and ARS-dye using Ni-Fe-CO₃ LDH as adsorbent, Fig. 6. It is obvious that

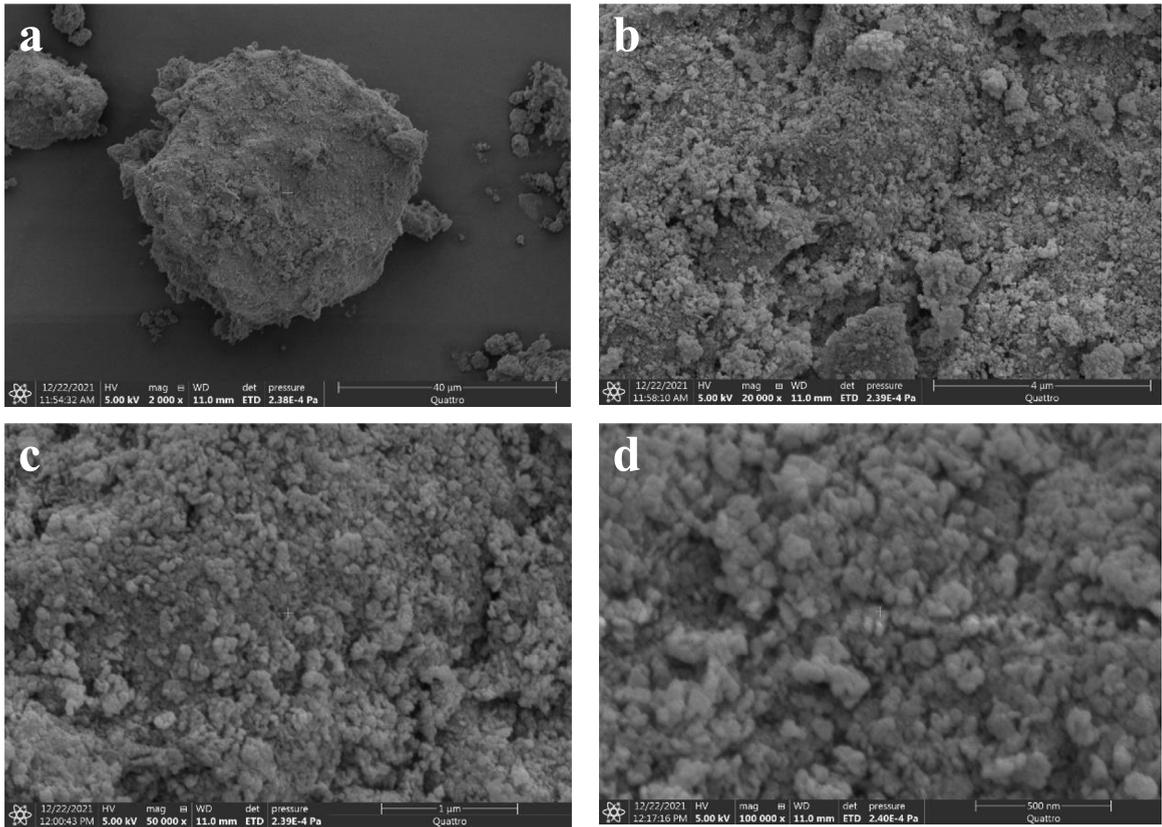


Fig. 2. SEM of Ni-Fe-CO₃ LDH with magnifications of (a) 2000x, (b) 20000x, (c) 50000x and (d) 100000x.

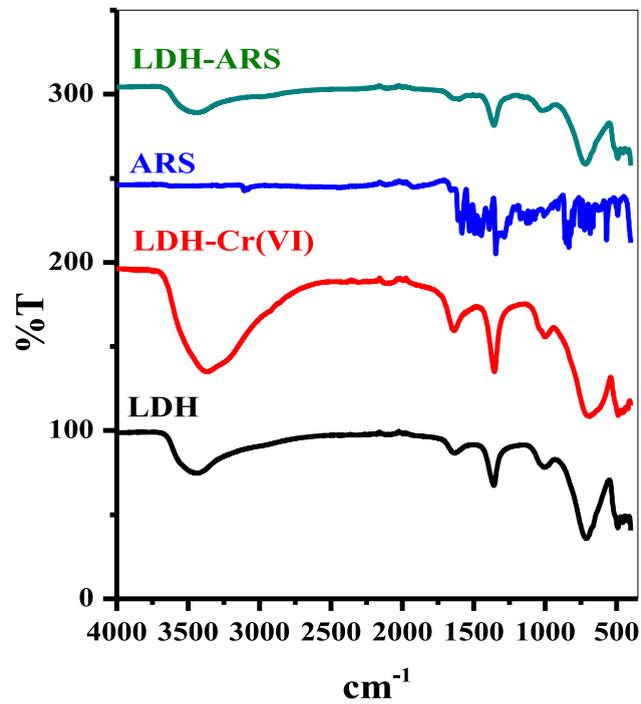


Fig. 3. FTIR of Ni-Fe-CO₃ LDH, Ni-Fe-CO₃ LDH-ARS, ARS and Ni-Fe-CO₃ LDH-Cr(VI).

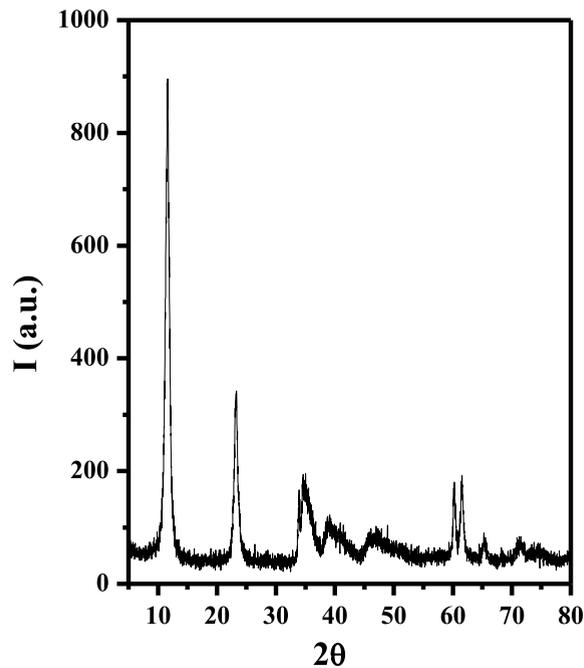


Fig. 4. XRD of Ni-Fe-CO₃ LDH.

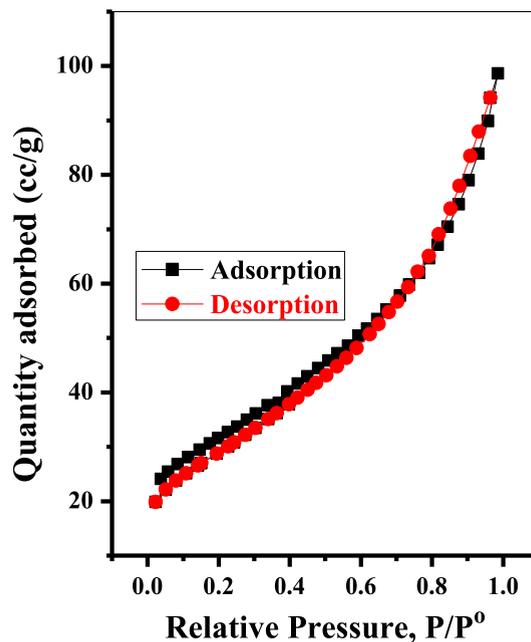


Fig. 5. Nitrogen adsorption/desorption isotherm of Ni-Fe-CO₃ LDH.

the sorption percent of both adsorbents remains constant in range (3.0–8.0) after this pH value the adsorption percent decrease for both adsorbates. In acidic medium the protonated binding sites of the adsorbent interact with $-\text{SO}_3^-$ in the dye through electrostatic attraction and the anionic HCrO_4^- , $\text{Cr}_2\text{O}_7^{2-}$ and HCr_2O_7^- species (Zolgharnein and Rastgardani, 2018; Khan et al., 2017) that favor the interaction with the protonated site. As the pH increases, the surface gains negative charge on the surface of LDH with anionic species (Zhang et al., 2013). The speciation of chromium(VI) can vary depending on the pH, ionic strength, and the presence of other ions or ligands in solution. In this respect, at pH 5.0, Cr(VI) exists primarily in the form of the hydrogen chromate ion $\text{HCrO}_4^- \gtrsim 90\%$ in addition to the minor other oxo species dichromate $\text{Cr}_2\text{O}_7^{2-}$ and

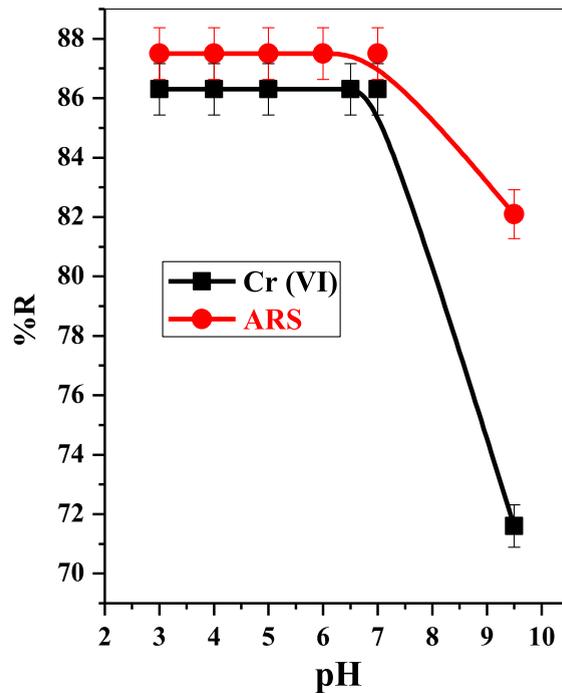
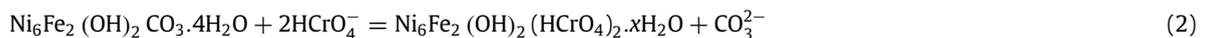


Fig. 6. Effect of pH on the adsorption of Cr(VI) and ARS-dye onto Ni-Fe-CO₃-LDH.

chromate ion CrO₄²⁻ while at pH 1.0 chromic acid is the predominate species (Ahmed, I.M. and Hamed, M.M. and Metwally, S.S, 2020; Volf and Balan, 2013; Ajouyed et al., 2010; Tran, H.N. and Nguyen, D.T. and Le, G.T. and Tomul, F. and Lima, E.C. and Woo, S.H. and Sarmahg, A.K. and Nguyena, H.Q. and Nguyenh, P.T. and Nguyeni, D.D. and Vigneswaran, T.V. and Vo, D.N. and Chao, H.P., 2019). It is worth to mention that the speciation of chromium(VI) is crucial in creating effective treatment strategies to remove chromium(VI) from wastewater or contaminated groundwater. The interaction between Cr(VI) and LDHs occurs through various mechanisms, including adsorption, surface complexation and ion exchange. In adsorption, the Cr(VI) ions are physically adsorbed onto the surface of the LDH through weak van der Waals forces or hydrogen bonding. In surface complexation, the Cr(VI) ions form chemical bonds with the surface functional groups on the LDH particles, such as hydroxyl or carboxyl groups. In ion exchange, the positively charged LDH surface attracts and holds onto the negatively charged Cr(VI) ions, similar to the ion exchange process with ion exchange resins. The ion exchange mechanism representing the possible interaction between the hydrogen chromate anion and the LDHs is given in Eq. (2) while Fig. 7 gives all possible interactions between LDH and CR dye.



3.2.2. Effect of adsorbent dose

Ni-Fe-CO₃ LDH dose was discussed in the range 5.0–25.0 mg on the sorption percent of Cr(VI) and ARS-dye is plotted in Fig. 8. We noted that, the removal percent increase with the adsorbent dose due to increasing the available sites on LDHs surface.

3.2.3. Effect of contact time

The removal percentage of the two adsorbates onto Ni-Fe-CO₃ LDH was examined in the range (5.0–120 min), as presented in Fig. 9. The removal efficiency of both Cr(VI) and ARS-dye was increased rapidly up to 30 and 25 min. respectively. With increasing contact time, the removal percentage remained constant due to blocking the active sites with the progress of adsorption process (Goharshadi and Moghaddam, 2015).

Two kinetic models were studied to explain the adsorption behaviors. The pseudo first-order kinetics model that presented in Eq. (3)

$$\log(q_e - q_t) = \log q_e - \left(\frac{k_1}{2.303}\right)t \quad (3)$$

The pseudo second order mechanism according to Eq. (4)

$$\left(\frac{t}{q_t}\right) = \left(\frac{1}{k_2 q_e^2}\right) + \left(\frac{1}{q_e}\right)t \quad (4)$$

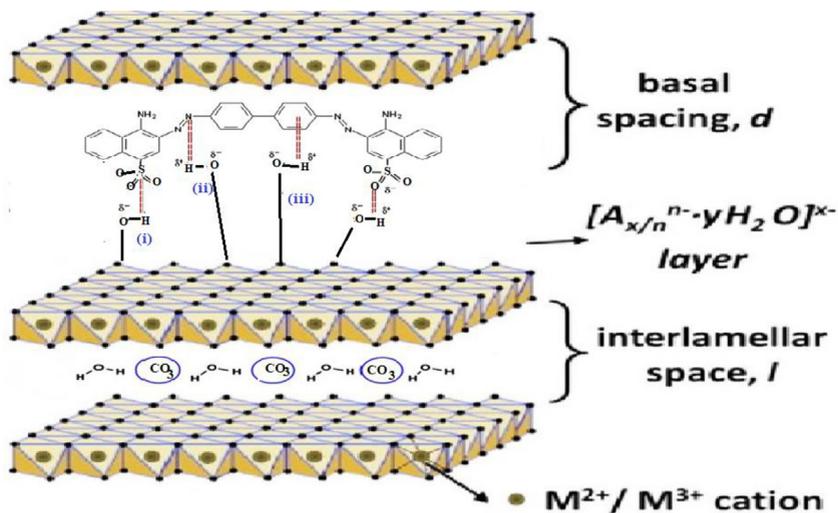


Fig. 7. CR dye-LDH interaction: (i) ionic interaction, (ii) hydrogen bonding between LDH and electronegative residues in the CR, and (iii) H-bonding between LDH and aromatic residue in CR molecule.

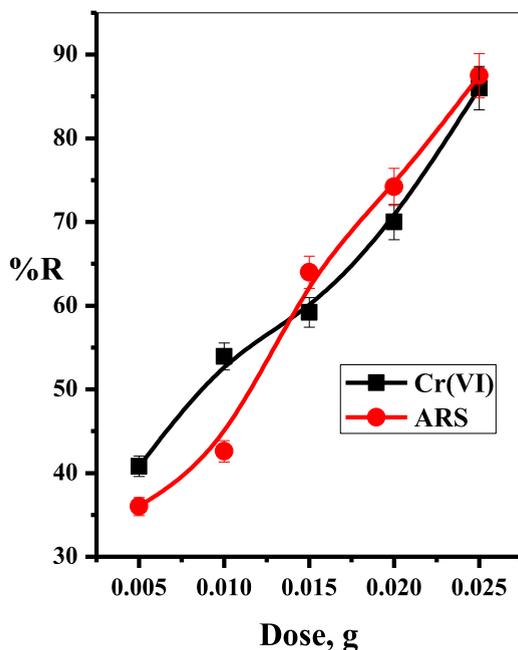


Fig. 8. Effect of adsorbent dose on the adsorption of Cr(VI) and ARS-dye onto Ni-Fe-CO₃-LDH.

where k_1 and k_2 are the rate constants of the pseudo first order and pseudo-second order, respectively, that were estimated from Fig. 10 and summarized in Table 1. The sorption of ARS-dye and Cr(VI) obey the pseudo-second-order model considering that the $q_e(\text{cal})$ values are near to $q_e(\text{exp})$.

3.2.4. Effect of initial concentration

The effect of initial Cr(VI) and ARS-dye concentration on the adsorption was investigated in the range (10–100 mg/L) and (100–400 mg/L), respectively. Fig. 11. It is obviously noted that the sorption of both adsorbate increases with increasing the initial concentration this is due to presence of available adsorbate molecules adsorption process.

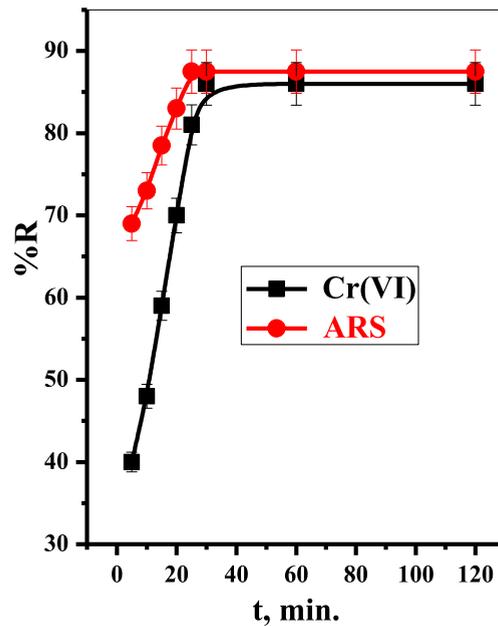


Fig. 9. Effect of contact time on the adsorption of Cr(VI) and ARS-dye onto Ni-Fe-CO₃-LDH.

Table 1
Calculated parameters of the pseudo-first-order and pseudo-second-order kinetic models.

Pollutant	T, °K	q _{eexp} (mg/g)	First-order kinetic parameter			Second-order kinetic parameter		
			K ₁ (min ⁻¹)	q _{ecal} (mg/g)	R ²	K ₂ (g mg ⁻¹ min ⁻¹)	q _{ecal} (mg/g)	R ²
Cr(VI)	298	3.44	0.106	4.06	0.853	0.019	4.50	0.913
	308	3.71	0.107	4.26	0.818	0.023	4.47	0.918
	318	3.92	0.149	3.75	0.917	0.030	4.45	0.967
	328	3.96	0.102	3.12	0.972	0.038	4.41	0.988
ARS-dye	298	35.0	0.094	13.30	0.956	6.96 × 10 ⁻⁴	35.74	0.996
	308	35.6	0.094	11.67	0.960	7.24 × 10 ⁻⁴	35.97	0.998
	318	38.1	0.101	13.00	0.982	5.97 × 10 ⁻⁴	38.79	0.999
	328	39.4	0.089	12.13	0.955	5.86 × 10 ⁻⁴	39.68	0.998

The experimental data were analyzed by Langmuir and Freundlich models. In linear form of Langmuir isotherm is represented according to Eq. (5):

$$\left(\frac{C_e}{q_e}\right) = \left(\frac{1}{Q_{max}b}\right) + \left(\frac{1}{Q_{max}}\right) C_e \tag{5}$$

Where, Q_{max} is the monolayer capacity and b is the binding energy between the adsorbent and the adsorbate. The results are illustrated in Fig. 11 and Table 2. Separation factor or equilibrium parameter R_L can be estimated from Eq. (6).

$$R_L = \frac{1}{1 + bc_0} \tag{6}$$

The adsorption of both systems was found to be favorable, linear, and the adsorption is irreversible (Mane and Vijay Babu, 2013). Q_{max} was found to be 6.1 and 69.93 for Cr(VI) and ARS-dye, respectively while 0 < R_L < 1 that means that the sorption processes are favorable.

The linear equation of Freundlich model is given as:

$$\log q_e = \log K_f + (1/n) \log C_e \tag{7}$$

Where, K_f and n are the adsorption performance and intensity, respectively and can be computed from plotting log q_e against log C_e, Fig. 11; and Table 2. Indeed, Langmuir isotherm is more favors than the Freundlich isotherm for both systems.

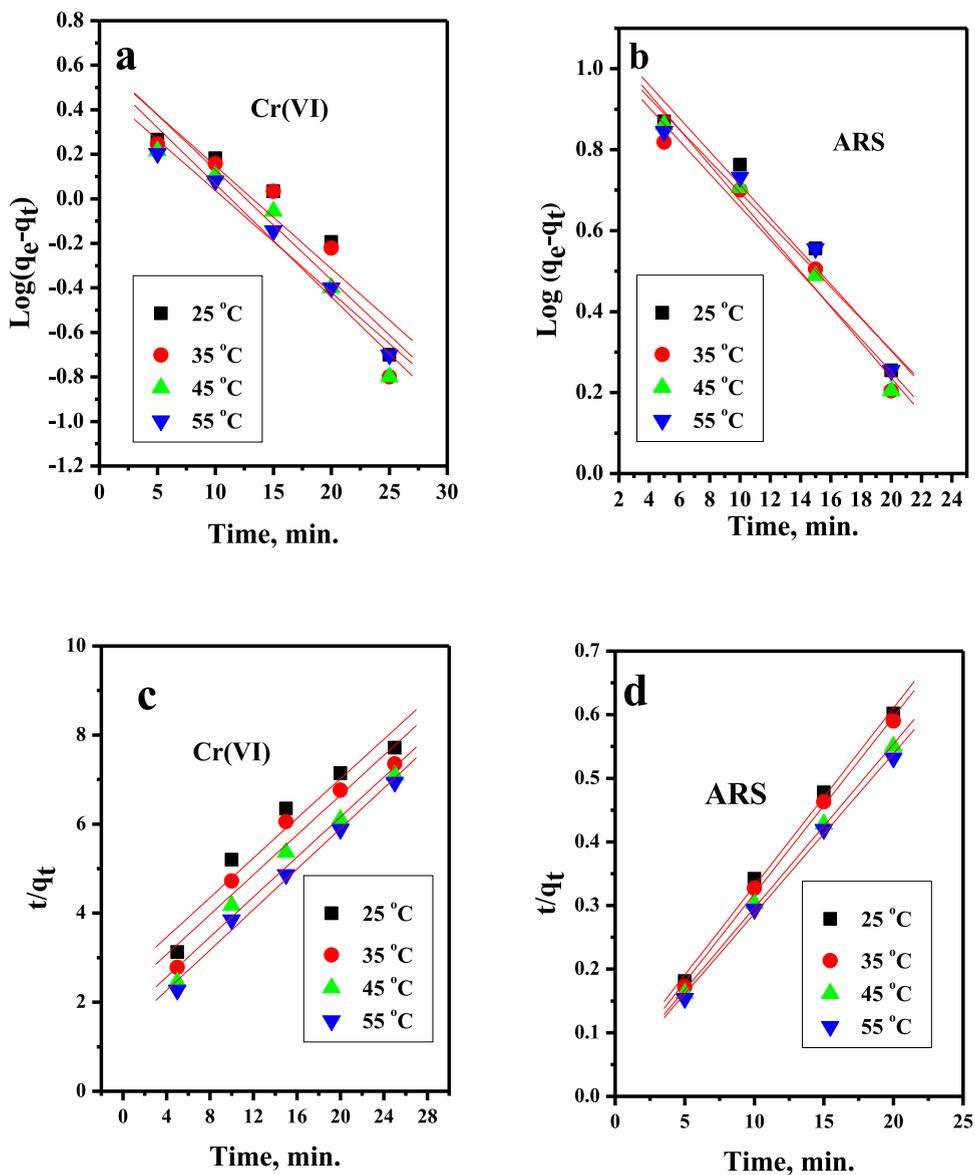


Fig. 10. Pseudo-first-order and pseudo-second-order models for the adsorption of Cr(VI) and ARS-dye onto Ni-Fe-CO₃-LDH.

Table 2

Calculated equilibrium constants for adsorption of Cr(VI) and ARS-dye onto Ni-Fe-CO₃ LDH.

Pollutant	Langmuir isotherm model				Freundlich isotherm model		
	q_e (mg/g)	b (l/mg)	R_L	R^2	$1/n$	K_f (mg/g)	R^2
Cr(VI)	6.10	0.36	0.217	0.996	0.206	20.04	0.950
ARS-dye	69.93	0.036	0.217	0.974	0.178	3.45	0.964

3.2.5. Effect of temperature

The influence of temperature on the removal of Cr(VI) and ARS-dye onto Ni-Fe-CO₃-LDH adsorbent was investigated in the range 298–328 °K, Fig. 12. The sorption increases with temperature, and this may refer to increasing in the rate of diffusion into the internal pores of the adsorbent particle from the external boundary layer (Weber, 1972; Jain and Sikarwar, 2008).

The thermodynamic parameters can be estimated from the following equations (Eqs. (8) and (9)):

$$\ln K_D = \frac{\Delta S^\circ}{R} - \frac{\Delta H^\circ}{RT} \tag{8}$$

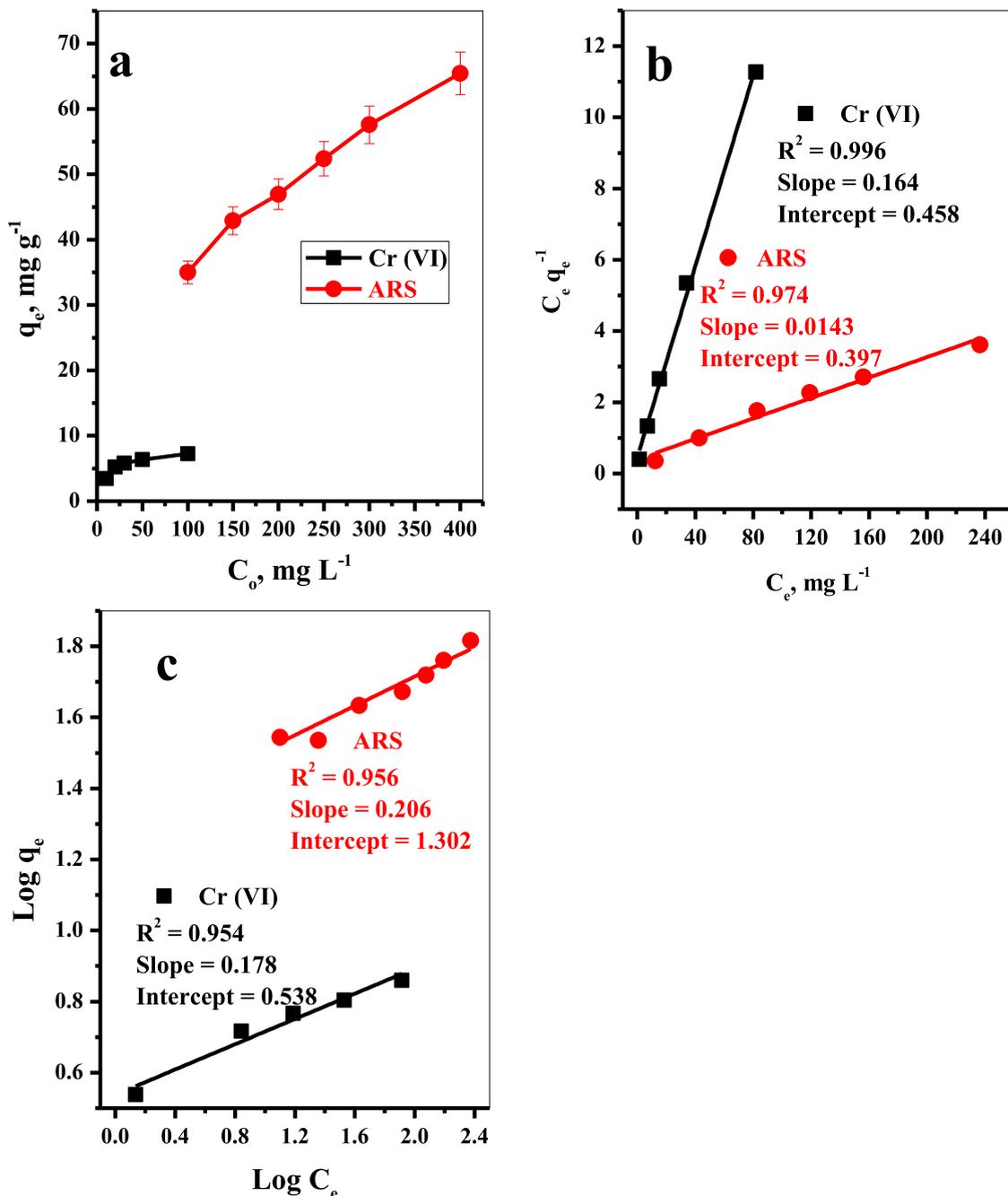


Fig. 11. (a) Effect of initial concentration of Cr(VI) and ARS-dye onto Ni-Fe-CO₃-LDH, (b) Freundlich's adsorption isotherm, and (c) Langmuir's adsorption isotherm.

$$\Delta G^\circ = \Delta H^\circ - T \Delta S^\circ \tag{9}$$

The positive value of ΔH° (30.25 and 17.78 kJ/mol) indicates the endothermic character of the process. The value of ΔH° indicates physisorption where van der Waals interaction, hydrophobic interaction and electrostatic attraction. The positive ΔS° value suggests an increase in the randomness of the system and the negative value of ΔG° indicates that the adsorption is spontaneous and favored at higher temperature and indicating the process is physical process as the ΔG° values ranging from -20 to 0 KJ/mol (Li et al., 2010) also, ΔH° , ΔS° and ΔG° were also given in Table 3.

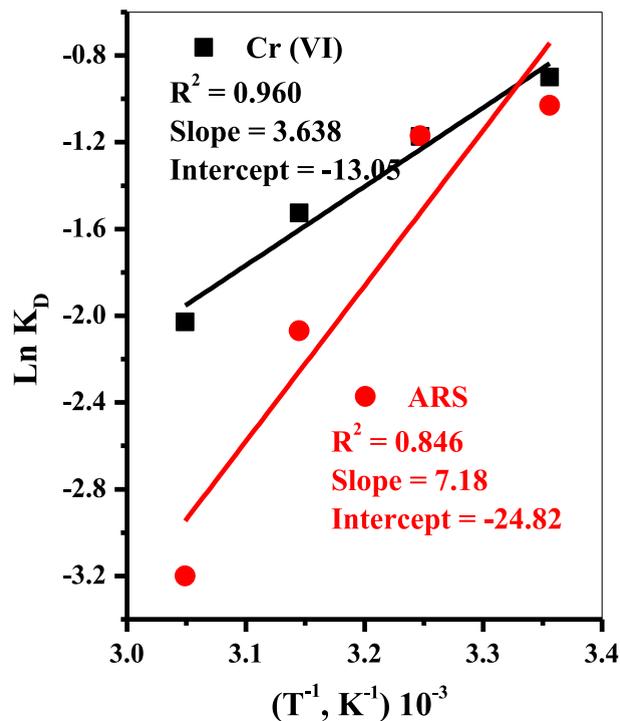


Fig. 12. Effect of temperature on sorption of Cr(VI) and ARS dye onto Ni-Fe-CO₃-LDH.

Table 3

Thermodynamic parameters for sorption of Cr(VI) and ARS dye onto Ni-Fe-CO₃-LDH.

	T, °K	ΔH° (KJ/mol)	ΔS° (J/mol)	ΔG° (KJ/mol)
Cr(VI)	298	30.25	108.46	-2.08
	308			-3.16
	318			-4.27
	328			-5.33
ARS	298	17.78	206.39	-43.72
	308			-45.79
	318			-47.85
	328			-49.92

3.3. Comparison study

Table 4 represented a comparison between the efficiency of Ni-Fe-CO₃-LDH as adsorbents with other adsorbent materials used in the sorption processes of Cr(VI) and ARS-dye (Bhattarai et al., 2022; Ahmed et al., 2020; Alshammari et al., 2021; Nayl et al., 2022; Bagbi et al., 2017; Kumar et al., 2018; Abukhadra et al., 2019; Bhomick et al., 2020; Badran and Khalaf, 2020; Fayazi et al., 2015; Gholivand et al., 2015; Bharath et al., 2022; Machado et al., 2016). The results obtained illustrate that Ni-Fe-CO₃-LDH gives a considerable capacity and efficiency for the Cr(VI) and ARS-dye adsorption.

3.4. Desorption study

Regeneration of spent adsorbent is of great economic importance. In this respect, sodium hydroxide solution of concentration (0.01–0.1 M) showed recovery of Cr(VI) and ARS dye Alizarine ≈ 95% .

4. Conclusion

In this work, Ni-Fe-CO₃ LDHs was investigated for the sorption of Cr(VI) and ARS dye as anionic species in batch systems. Adsorption process fitted pseudo-second order and obey the Langmuir model with monolayer sorption capacity Q_{max} of 6.1 and 69.9 mg/g for Cr(VI) and ARS-dye, respectively. The thermodynamic parameters indicated that the sorption process is endothermic, spontaneous with increasing the randomness of the system. Reuse of the adsorbent was attained using caustic soda solution of concentration (0.01–0.1 M) and the desorption percentages reached ≈ 95%.

Table 4
 Q_{\max} of Ni-Fe-CO₃-LDH compared with recently reported adsorbent materials to remove Cr(VI) and ARS-dye.

Pollutant	Adsorbent	Q_{\max} , mg/g	pH	Ref.
Cr(VI)	Arundo donax Stem biosorbent	76.9	2.0	57
	Fe ₃ O ₄ -coated perlite	8.8	2.0	58
	Fe ₂ O ₃ /HMS composite	10.8	2.0	59
	Magnetite Talc (Fe ₃ O ₄ @Talc) Nanocomposite	13.5	2.0	60
	L-Cysteine magnetite	34.5	2.0	61
	Zirconium oxide-alginate beads	19.0	5.0	62
	Kaolinite nanotubes (KNTs)	91.0	2.0	63
	Ni-Fe-CO₃-LDH	6.1	5.0	This work
ARS	biomass-based activated carbon	91.7	3.0	64
	Maghemite Fe ₂ O ₃	23.2	11	65
	Magnetic activated carbon (MAC)/maghemite nano-composite	108.7	2.0	66
	Polypyrrole-coated Fe ₃ O ₄ nanoparticles	116.3	4.5	67
	Modified Avocado Seeds	67.1	2.0	68
	Single carbon nanotubes (SWCNT)	312.5	2.0	69
	Multiwalled carbon nanotubes MWCNT	135.2	2.0	69
	Ni-Fe-CO₃-LDH	69.9	7.0	This work

CRedit authorship contribution statement

Ismail M. Ahmed: Conceptualization, Methodology, Software, Validation, Investigation, Writing – original draft, Project administration, Funding acquisition. **Ahmed I. Abd-Elhamid:** Conceptualization, Methodology, Validation, Formal analysis, Investigation, Writing – original draft, Writing – review & editing. **Ashraf A. Aly:** Software, Writing – original draft, Writing – review & editing. **Stefan Bräse:** Validation, Writing – review & editing. **AbdelAziz A. Nayl:** Conceptualization, Software, Writing – original draft, Writing – review & editing.

Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Data availability

No data was used for the research described in the article.

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Appendix A. Supplementary data

Supplementary material related to this article can be found online at <https://doi.org/10.1016/j.eti.2023.103214>.

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