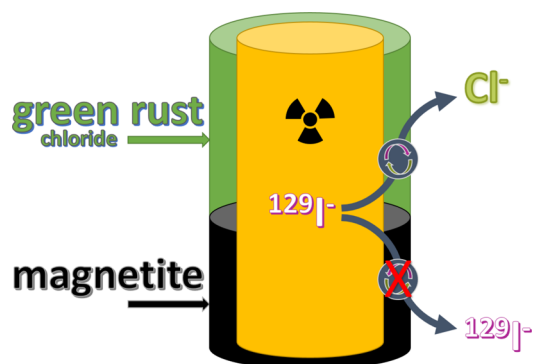


Retention of Iodide by Chloride Green Rust and Magnetite

Tim Platte,* Nicolas Finck,* Frank Heberling, Robert Polly, Tim Prüssmann, Kathy Dardenne, and Horst Geckeis

ABSTRACT: Green rust (GR), a layered double hydroxide (LDH) containing Fe, and magnetite can be found in natural and engineered environments. The ability of chloride GR (GR-Cl) and magnetite to retain iodide as a function of various parameters was investigated. Sorption equilibrium is achieved within 1 day of contact time between iodide and preformed GR-Cl in suspension. pH_m variations (7.5–8.5) have no significant influence, but the iodide sorption decreases with increasing ionic strength set by NaCl. Sorption isotherms of iodide suggest that the uptake operates via ionic exchange (IC), which is supported by geochemical modeling. The short-range binding environment of iodide associated with GR is comparable to that of hydrated aqueous iodide ions in solution and is not affected by pH_m or ionic strength. This finding hints at an electrostatic interaction with the Fe octahedral sheet, consistent with weak binding of charge balancing anions within an LDH interlayer. The presence of sulfate anions in significant amounts inhibits the iodide uptake due to recrystallization to a different crystal structure. Finally, the transformation of iodide-bearing GR-Cl into magnetite and ferrous hydroxide resulted in a quantitative release of iodide into the aqueous phase, suggesting that neither transformation product has an affinity for this anionic species.

KEYWORDS: Chloride green rust, Iodide, X-ray diffraction, X-ray absorption spectroscopy, nuclear waste disposal, magnetite, sorption



INTRODUCTION

Geological disposal is considered as the internationally preferred option to dispose of radioactive waste. In such repositories, the waste matrix is intended to be encapsulated in metallic containers and surrounded by engineered barriers. Canisters may start corroding when in contact with groundwater, resulting in the formation of Fe(II)-bearing phases such as green rust (GR) compounds,^{1–3} which are known to be transient compounds between metallic iron and final, thermodynamically more stable corrosion products. GR is the Fe endmember of the layered double hydroxide (LDH) family and bears a permanent positive layer charge that is balanced by anions and water molecules in the interlayer. The general structural formula of GR can be written as $[\text{Fe}(\text{II})_{1-x}\text{Fe}(\text{III})_x(\text{OH})_2]^{x+} [(x/n)\text{A}^{n-}, m\text{H}_2\text{O}]^{x-}$, with x representing the fraction of ferric iron and A representing the intercalated anions.⁴ Depending on the nature of the intercalated anions, GR can crystallize either with a rhombohedral (e.g., chloride or carbonate green rust) or a hexagonal (e.g., sulfate green rust) unit cell. Because of the abundance of chloride ions in various groundwaters, chloride-containing GR (GR-Cl) should be considered as one possible phase occurring upon iron corrosion in suboxic and anoxic environments. These phases are especially expected in scenarios assuming corroding steel containers in a deep geological repository (DGR) in rock salt formations.^{5–8}

Depending on the anionic composition of the groundwater, carbonate- and sulfate-containing GR are also likely to be present.^{9,10}

Anionic species intercalated within LDHs can be exchanged for negatively charged species present in the contacting solution. This mechanism gives these layered minerals the ability to bind dissolved anionic pollutants present in groundwaters which may otherwise be only poorly retained by clay minerals.^{11,12} This ability to sorb anionic species can be of great interest, especially in the near-field of a DGR for nuclear waste. For example, nuclear waste contains significant amounts of long-lived ¹²⁹I (half-life of 1.57×10^7 years) which will be partially released as dissolved iodide species as soon as groundwater comes into contact with the waste matrix,¹³ and which is hardly retained by major mineral phases in the near-field (e.g., clay minerals).^{11,12,14–17} However, the mobility of anionic species such as iodide in aqueous environments may be lowered upon interaction with LDHs such as AFm phases in

66 cementitious material¹⁸ and GR. The goal of this study is to
67 investigate the iodide retention by preformed GR-Cl in
68 suspension and to thoroughly characterize the involved uptake
69 mechanism in order to establish a reliable geochemical model
70 for potential iodide retention in the near-field.

71 The preparation of iodide-containing GR (GR-I) and of a
72 complete solid solution between the isostructural iodide and
73 chloride GR endmembers has been reported.^{19,20} However, the
74 concentrations of dissolved iodide used in these studies
75 substantially exceed the amounts expected in the case of
76 canister failure in a DGR. The aim of this study is to investigate
77 the sorption behavior of iodide by preformed GR-Cl at
78 different pH_m , contact times, and ionic strengths using more
79 environmentally relevant iodide concentrations. Additionally,
80 sorption experiments in the presence of sulfate have been
81 performed where the porewater should be closer to real
82 conditions as sulfate is naturally present in groundwaters. We
83 also investigated the fate of iodide during conversion of iodide-
84 bearing GR-Cl samples into magnetite and compared the
85 results to those obtained in uptake experiments by preformed
86 magnetite. Conversion reactions from iodide-bearing GR to
87 the thermodynamically more stable magnetite aim to mimic
88 reactions expected to occur during canister corrosion in a DGR
89 over longer periods of time.

90 ■ MATERIALS AND METHODS

91 **Sample Preparation.** All samples have been prepared
92 using ultrapure water (UPW, 18.2 M Ω -cm, Milli-Q system,
93 Millipore) and reagents of ACS grade or higher. The sources of
94 Fe(II), Fe(III), Cl(-I), SO₄²⁻ and I(-I) were FeCl₂·4H₂O,
95 FeCl₃, NaCl, Na₂SO₄ and NaI, respectively. Unless otherwise
96 indicated, all steps from sample preparation to analysis were
97 performed under anoxic conditions by using an Ar-filled
98 glovebox (<1 ppm of O₂) and airtight transfer vessels and
99 sample holders. The NaOH solution was likewise prepared by
100 dissolving NaOH(s) into degassed UPW in the glovebox. pH
101 values were measured with a glass combination pH electrode
102 (Metrohm LL Solitrode) that was calibrated before each use
103 by commercial pH buffer solutions (pH 4, 7, 10). For samples
104 at high ionic strength, the measured operational “pH” values
105 have been corrected to pH_m according to the literature.²¹
106 Redox potentials (or E_h values) were recorded using a
107 combined platinum electrode (Radiometer Analytical); all
108 reported values are quoted with respect to the standard
109 hydrogen electrode. Suspensions were stirred during E_h and
110 pH_m measurements. With respect to samples at high salinity,
111 molality was used as the unit of concentration ($a_i \neq c_i$). At
112 ionic strengths below 0.1 mol/L, the conversion shows no
113 significant difference (mol/L \approx mol/kg).

114 GR and magnetite samples have been prepared by titrating a
115 stirred solution containing Fe(II) and Fe(III) with a 1 M
116 NaOH solution until pH_m 7.5 (GR, Fe(II)/Fe(III) = 4:1) or
117 9.5 (magnetite, Fe(II)/Fe(III) = 1:2). Although the Fe(II)/
118 Fe(III) ratio in GR-Cl is close to 3,¹⁹ a slightly higher ratio was
119 used to prevent the formation of magnetite and to favor the
120 GR formation.²² After aging for 1 day, the suspension was first
121 washed by centrifuging for 10 min at 3,500 rpm (2,000g) and
122 replacing the supernatant by UPW. For centrifugation only, the
123 sample was taken out of the glovebox in vials sealed with
124 Parafilm. Suspensions were subsequently used in uptake
125 experiments (9 ± 2 g/kg for GR, 6.9 ± 1.5 g/kg for
126 magnetite). For each individual sorption sample the ionic
127 strength was set by adding NaCl powder and the pH_m was

adjusted by using 1 M NaOH or 1 M HCl. Iodide was added 128
and each sample was spiked with ¹²⁵I (100–300 Bq/mL) to 129
quantify the uptake using gamma spectrometry. 130

The effect of several parameters on the iodide sorption by 131
GR was investigated. In all cases, replicates were prepared and 132
sampled after various contact times. Results showed that after 133
1 day there was no significant change in the sorption values. 134
Investigated parameters were the ionic strength set by NaCl 135
and adjusted to 0.2–5 M, the pH_m adjusted within the range 136
7.0–8.5 for GR and 8.0–10.0 for magnetite, and the starting 137
iodide concentration. After 2 weeks of contact time, a fraction 138
of some of the GR sorption samples was converted into 139
magnetite by titrating with 1 M NaOH to pH_m 11.0.²³ This 140
conversion was completed after 10 days. The complete sample 141
list considered in this study can be found in Table S1 in the 142
Supporting Information. 143

For the analysis of the samples, suspensions were ultra- 144
centrifuged for 60 min at 90,000 rpm (Beckman Coulter XL- 145
90K), the concentration of iodide in the supernatant was 146
quantified using a γ -counter (Packard Cobra Auto-Gamma 147
5003), and the concentration of dissolved Fe was quantified by 148
ICP-MS (Thermo Scientific Element XR). The precise 149
quantity of suspended solid phase was determined considering 150
the total mass balance of Fe in the system and results from 151
ICP-MS analysis. These exact values were taken into account 152
to calculate the sorption coefficient R_d as 153

$$R_d \left[\frac{\text{kg}}{\text{g}} \right] = \left(\frac{c_0 - c_L}{c_L} \right) \times \frac{m_j [\text{kg}]}{m [\text{g}]} \quad (1) \quad 154$$

where c_0 is the initial iodide concentration, c_L is the iodide 155
concentration at equilibrium, m_j is the mass of the solvent, and 156
 m is the mass of the solid phase. Since molality was used as the 157
unit of concentration in the manuscript, this is also taken into 158
account in the sorption coefficient R_d by using the mass of 159
water (kg H₂O) instead of its volume (L). 160

Solid Phase Characterization and X-ray Absorption 161
Spectroscopy. For the analysis of GR and magnetite 162
compounds (XRD (X-ray diffraction), SEM-EDX (scanning 163
electron microscopy and energy-dispersive X-ray spectroscopy), 164
and XAS (X-ray absorption spectroscopy)), an aliquot of 165
the sample slurry was centrifuged in the glovebox at 13,000 166
rpm (14,000g) for 15 min. The supernatant was removed and 167
replaced by UPW twice. For XRD analysis the sample was 168
encapsulated in an airtight and low background holder 169
equipped with an O-ring. Diffractograms have been recorded 170
using a D8 ADVANCE diffractometer equipped with a Cu 171
anode and a LynxEye XE-T detector (Bruker AXS). 172
Identification of the crystalline phase was performed by 173
comparison with the PDF-2 database using DIFFRAC.EVA 174
v5.0 (Bruker AXS). For SEM analysis, a small amount of slurry 175
was dried on a sample holder, which was transported to the 176
microscope [Quanta 650 FEG (FEI)] under anoxic conditions 177
and placed into the microscope quickly to minimize air 178
exposure as much as possible. 179

Information on the iodine short-range coordination environ- 180
ment was provided by XAS at the iodine K-edge. X-ray 181
absorption spectra were recorded at room temperature at the 182
ACT station of the CAT-ACT beamline²⁴ at the KIT light 183
source (Karlsruhe Institute of Technology, Germany) with a 184
storage ring energy of 2.5 GeV. Detailed information on 185
sample preparation, experimental setup, and data treatment 186

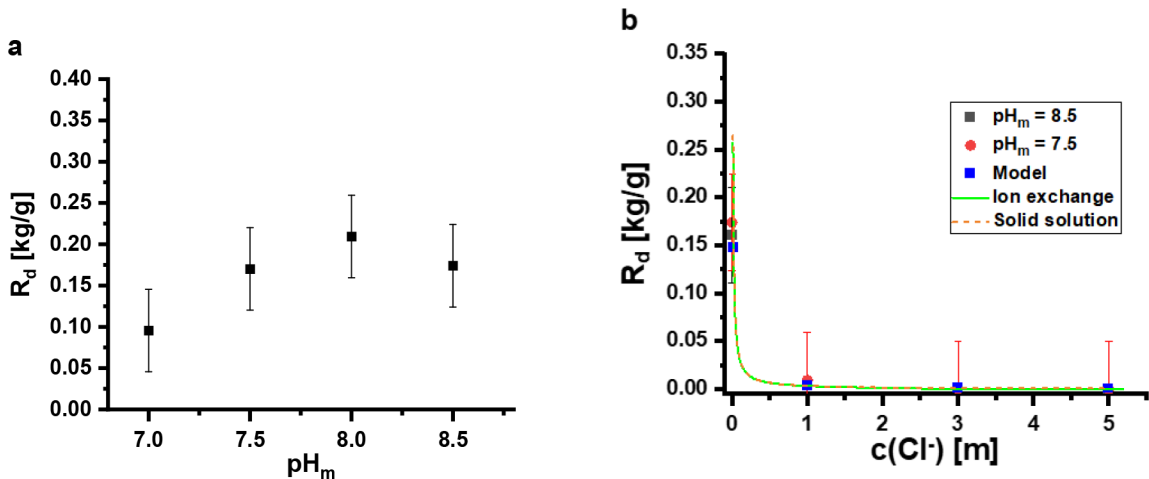
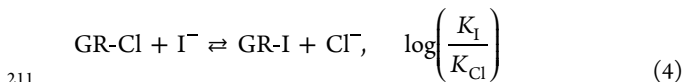
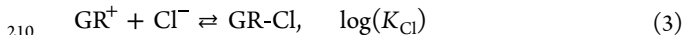
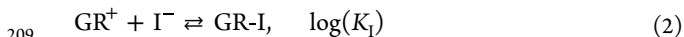


Figure 1. Sorption of iodide by GR-Cl as a function of pH_m (a). Sorption of iodide by GR-Cl at different NaCl concentrations (b). Data correspond to averaged values between 1 and 7 days. Equilibrium was reached within 1 day. Blue squares show the model calculation, at the exact experimental conditions, as they were applied for the adjustment of the ion-exchange parameter. The continuous lines represent generic model calculations at average experimental conditions: $\text{pH}_m = 7.5$, $c(\text{GR}) = 9 \text{ g/kg}$, $c_0(\text{I}^-) = 15 \mu\text{M}$. The experimental data and model agree well at all $c(\text{Cl}^-)$ up to 5 M.

187 following standard procedures can be found in the [Supporting](#)
188 [Information](#).

189 **Modeling of Sorption Data.** Geochemical modeling was
190 performed using PHREEQC 3 and the thermodynamic
191 database SIT.dat (PHREEQC Interactive v. 3.4.0-12927
192 SIT.dat database).²⁶ Two models were developed in order to
193 analyze possible uptake mechanisms and to describe
194 experimental results quantitatively, an ion-exchange model
195 and a solid solution model. The ion-exchange model uses an
196 affinity parameter for I^- binding relative to Cl^- binding to
197 exchange sites (GR^+), and the latter uses only the GR-I
198 solubility constant as an input parameter for the uptake
199 calculations. The solid solution model is a thermodynamic,
200 more complete description, while the exchange model does not
201 take solid phase stability and solubility into account. To model
202 the ion-exchange reaction, two half-reactions were defined (eqs
203 2 and 3), which sum up to the overall ion-exchange process
204 (eq 4).²⁵ The overall affinity of iodide to exchange for chloride
205 in the GR structure, $\log(k_s)$ as defined by eq 5, was adjusted to
206 obtain an optimal fit between data and model.²⁷ The individual
207 constants for the half-reactions (eqs 2 and 3) are arbitrary (i.e.,
208 one is defined relative to the other):



$$212 \quad \log(k_s) = \log\left(\frac{K_I}{K_{\text{Cl}}}\right) \quad (5)$$

213 As an alternative model, the iodide uptake by GR-Cl has
214 been described as a solid solution between GR-Cl ($\text{Fe(II)}_3\text{Fe-}$
215 $(\text{III})(\text{OH})_8\text{Cl} \cdot n\text{H}_2\text{O}$) and GR-I ($\text{Fe(II)}_3\text{Fe(III)}(\text{OH})_8\text{I} \cdot$
216 $n\text{H}_2\text{O}$).²⁸ For this purpose, the solubility of GR-Cl was
217 recalculated from the reported free energy formation ($\text{dG} =$
218 -2131.75 kJ/mol ²⁹) as $\log K_{\text{Sp}}(\text{GR-Cl}) = -79.70$ (eq 6). The

unknown solubility of GR-I was taken as an adjustable
219 parameter. 220

$$\log(K_{\text{Sp}}(\text{GR-Cl})) = 1.0a(\text{Fe}^{3+}) + 3.0a(\text{Fe}^{2+}) \\ + 8.0a(\text{OH}^-) + 1.0a(\text{Cl}^-) \quad (6) \quad 221$$

222 ■ RESULTS AND DISCUSSION

Characterization of GR and Magnetite. X-ray diffracto- 223
grams of the synthesized GR compounds (Figure S1) evidence 224
the presence of only green rust minerals, and electron 225
micrographs show that samples are made of thin hexagonal 226
platelets (Figure S3). These results compare well with reported 227
findings for GR-Cl samples prepared by precipitation from 228
ferric and ferrous ions or by oxidation of $\text{Fe}(\text{OH})_2$.^{19,23} The 229
synthesized magnetite is made of octahedral crystals of 100– 230
200 nm, and the crystal structure was assessed by XRD analysis 231
(Figures S2 and S4). 232

Iodide Sorption by GR-Cl. The sorption of iodide by GR- 233
Cl is only slightly affected by pH_m variations (Figure 1). 234 f
Results show a constant sorption with an adsorption coefficient 235
 R_d of $0.18 \pm 0.05 \text{ kg/g}$ in the pH_m range of 7.5–8.5, which 236
slightly decreases to $R_d = 0.10 \pm 0.05 \text{ kg/g}$ at $\text{pH}_m = 7$. Since 237
variations are within uncertainties, results evidence that pH_m 238
does not play a significant role on iodide adsorption. Note that 239
GR is stable only in a limited pH range.³⁰ In contrast, the Cl^- 240
concentration has a significant influence on the iodide 241
sorption. R_d decreases from $0.17 \pm 0.05 \text{ kg/g}$ in 0.02 M 242
NaCl to ~ 0 in $\geq 1 \text{ M}$ NaCl (Figure 1) at $\text{pH}_m = 7.5$, and 243
comparable results were also obtained at $\text{pH}_m = 8.5$. This 244
dependency of the iodide sorption on the Cl^- concentration is 245
consistent with sorption studies of iodide on GR-Cl by Min et 246
al.³¹ Results further agree with sorption studies on other LDH 247
phases (i.e., the absence of pH effect on iodide uptake by 248
LDH)³² and conform to expectations, since according to eq 249
(4) the ion-exchange mechanism is independent of the pH_m 250
but strongly dependent on the Cl^- concentration. 251

The next varied parameter was the starting iodide 252
concentration at a constant solid/liquid ratio and at two 253
 pH_m values. The adsorption isotherm and R_d values are shown 254 f2

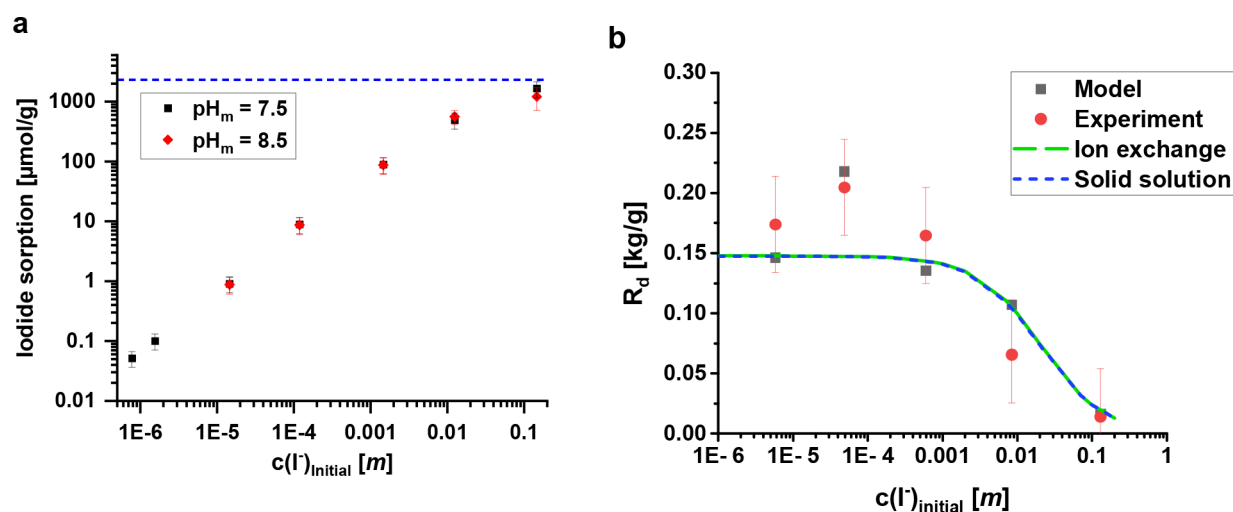


Figure 2. (a) Adsorption isotherms for the sorption of iodide by GR-Cl at different iodide concentrations. $c(\text{GR}) \approx 9 \pm 2 \text{ g/kg}$, $c(\text{Cl}^-) \approx 0.02 \pm 0.01 \text{ M}$. The uncertainty on the iodide concentration is given in Table S2. The maximum amount of anion-exchange sites of GR-Cl is indicated by a blue dashed line in graph (a). (b) R_d values at pH_m 7.5. Black squares show the model calculation, at the exact experimental conditions, as they were applied for the adjustment of the ion-exchange parameter. The continuous lines represent generic model calculations at average experimental conditions: pH_m 7.5, $c(\text{GR}) = 9 \text{ g/kg}$, $c_0(\text{NaCl}) = 0.02 \text{ mM}$.

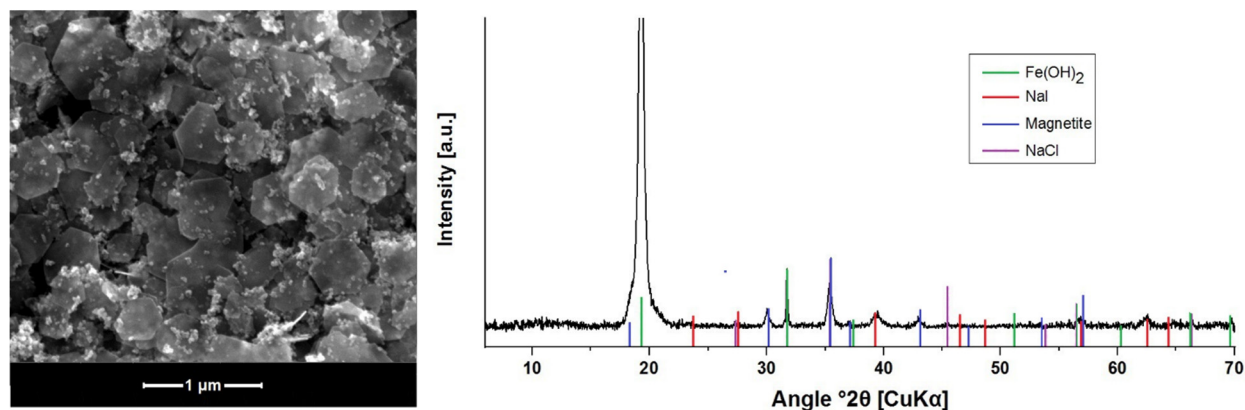


Figure 3. Scanning electron micrograph (left) and X-ray diffractogram (right) of a GR-Cl sorption sample converted into magnetite and $\text{Fe}(\text{OH})_{2(s)}$ by adding NaOH. $\text{pH}_m = 11 \pm 1$, $c(\text{Cl}^-) = 0.02 \pm 0.02 \text{ M}$. On the diffractogram vertical lines show the reference reflections of magnetite,³⁷ $\text{Fe}(\text{OH})_2$,³⁸ NaI,³⁹ and NaCl.³⁹

255 in Figure 2; R_d values are further listed in Table S2. The double
256 logarithmic adsorption isotherm shows a fairly linear increase
257 of adsorption with increasing concentration, in line with
258 anionic exchange as the sole sorption mechanism. At starting
259 iodide concentrations $\geq 0.15 \text{ M}$, the slope of the adsorption
260 isotherms, and thus the R_d values, decreases. Comparable
261 observations have been reported recently by Nedyalkova et
262 al.,³³ who interpreted this behavior as a saturation of the
263 uptake sites. Indeed, data and models indicate iodide
264 concentrations in the solid become high relative to the
265 concentration of available exchange sites at these aqueous
266 concentrations. The change of pH_m only marginally affects the
267 sorption. It was attempted to record an adsorption isotherm at
268 high ionic strength (5 M), but sorption was below the
269 detection limit at these conditions.

270 **Iodide Sorption by Magnetite.** Iodide batch sorption
271 experiments have been performed with magnetite at various
272 pH_m values and ionic strengths (Tables S1 and S4). After 7
273 days of contact time, the iodide sorption was below the limit of
274 analytical uncertainty. Varying the contact time, pH_m , or ionic
275 strength had no effect on the uptake. Separately, magnetite was

also prepared in the presence of iodide (coprecipitation
experiments). Using this approach, no significant iodide uptake
could be detected either. The absence of a significant retention
of iodide may be related to the development of a negative
surface charge on magnetite under the considered pH_m
conditions, which hinders anions from binding the surface.
Furthermore, X-ray diffractograms showed no structural
difference between magnetite synthesized in the absence of
iodide, magnetite prepared in the presence of iodide, and
magnetite after sorption with iodide.

**Transformation of GR-Cl Sorption Samples into
Magnetite.** GR can be transformed into magnetite and
 $\text{Fe}(\text{OH})_{2(s)}$ by increasing the pH_m to >10 . Table S3 shows
precisely which samples have been used for transformation.
Analysis by XRD of transformation samples (Figure 3)
corroborated the presence of ferrous hydroxide and magnetite
besides NaCl and NaI salts, as well as the absence of GR.
Electron micrographs showed that $\text{Fe}(\text{OH})_{2(s)}$ is present as
large hexagonal platelets and magnetite as a fine-grained
material, which agrees with earlier works.^{23,35} The analysis of
the supernatant further revealed that iodide is no longer bound

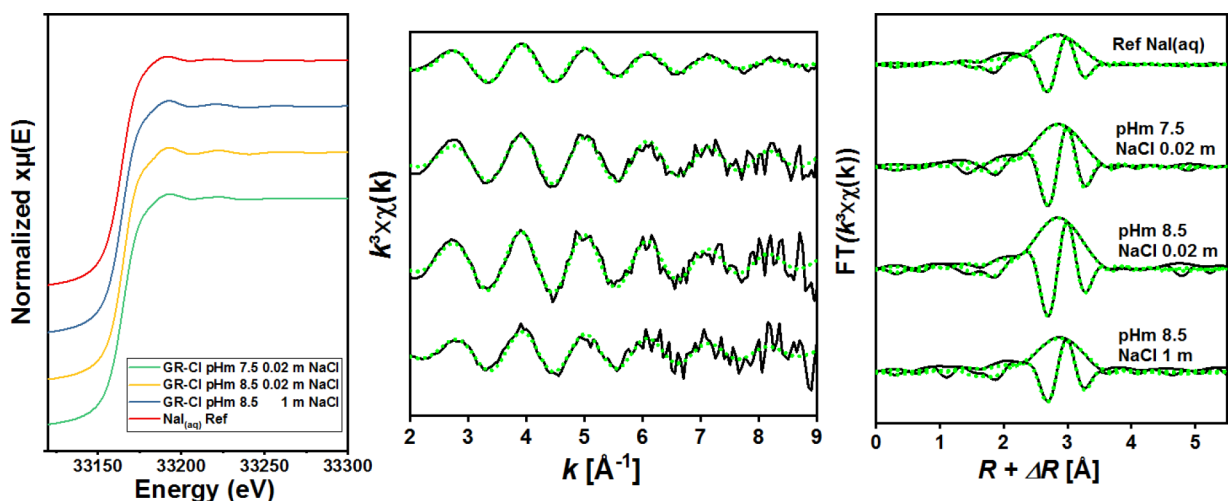


Figure 4. Iodine K-edge XANES of GR samples and the $\text{NaI}_{(\text{aq})}$ reference (left). Experimental (solid black line) and modeled (dashed green line) EXAFS spectra (middle) with the corresponding Fourier transforms (right) of all samples. Fit results are presented in Table 1.

297 to any solid phase, meaning that iodide that was originally
 298 bound to GR has been released into solution during the
 299 transformation. This result implies that neither magnetite nor
 300 $\text{Fe}(\text{OH})_{2(\text{s})}$ are able to sorb iodide. Ferrous hydroxide has a
 301 layered structure; however, in contrast to GR, it does not bear
 302 any permanent layer charge, and its isoelectric point is at pH_m
 303 about 10.³⁶ The absence of iodide retention by this compound
 304 in significant amounts can be related to either the absence of a
 305 permanent layer charge or to the development of a negative
 306 surface charge under the applied pH_m conditions ($\text{pH}_m = 11$).
 307 LDH compounds have two surface sites available for sorption,
 308 the planar sorption sites and the edge sites. The planar sites
 309 bear a permanent positive charge arising from the substitution
 310 of divalent by trivalent cations within the octahedral sheet,
 311 while edge sites consist of amphoteric hydroxyl surface
 312 functional groups (e.g., $\equiv\text{Fe}^{2+}-\text{OH}$ and $\equiv\text{Fe}^{3+}-\text{OH}$ for
 313 GR). Considering reported studies on other LDHs,³³
 314 experimental findings may suggest that iodide anions can
 315 only occupy interlayer sites where they are held through
 316 electrostatic attraction and cannot sorb on edge sites.
 317 Magnetite has a point of zero charge of $\text{pH} = 6.4$.³⁴ At pH
 318 around 10, the surface thus has a negative surface charge,
 319 which could be one origin to the absence of iodide species
 320 retention by magnetite.

321 Iodide Sorption by GR-Cl in the Presence of Sulfate.

322 The influence of the presence of sulfate in the sorption
 323 experiments with GR has also been investigated (see Tables S6
 324 and S7). At low sulfate concentrations (1–32 μM , concen-
 325 trations comparable to that of iodine), no significant influence
 326 on the iodide retention could be evidenced; calculated R_d
 327 values are in the same range (≈ 0.18 kg/g) as that for sorption
 328 without added sulfate (≈ 0.17 kg/g). At higher sulfate
 329 concentrations (35–45 mM, concentrations comparable to
 330 that of chloride) the iodide retention significantly decreased,
 331 and the sorption constant R_d is below the detection limit.

332 In the presence of sulfate, GR-Cl can transform into sulfate
 333 green rust (GR- SO_4) due to the higher stability of this latter
 334 compound.⁴⁰ Earlier studies showed that for 2.5 g/L GR-Cl
 335 (i.e., ~ 6 mmol/L) and crystallite sizes comparable to that in
 336 the present study (Figure S3), $\sim 90\%$ of the exchange sites are
 337 occupied by SO_4^{2-} for aqueous solutions containing 40 mmol/
 338 L Cl^- and 5 mmol/L SO_4^{2-} ($\text{SO}_4^{2-}/\text{Cl}^- = 1:8$).⁴¹

In experiments at low sulfate concentrations, the amount of
 339 formed GR- SO_4 is likely very low, i.e., the presence of 32
 340 $\mu\text{mol/L}$ sulfate and ~ 20 mM NaCl in uptake experiments with
 341 9 g/kg GR-Cl (i.e., ~ 20 mmol/L GR-Cl) may have resulted in
 342 the transformation of $<1\%$ of GR-Cl into GR- SO_4 .
 343 Experimental sorption data show that this low amount of
 344 GR- SO_4 has no significant effect on iodide uptake.
 345

The uptake of iodide by GR-Cl works very likely because
 346 GR-Cl and GR-I are isostructural and a solid solution can form
 347 between both compounds,¹⁹ i.e., one anion can substitute for
 348 the other within the interlayer, without a pronounced effect on
 349 the Fe-hydroxide layers. Sorption constants obtained for these
 350 experiments (Table S6) are within uncertainties comparable to
 351 the results of the no-sulfate model in Figure 2, supporting this
 352 hypothesis.
 353

Experiments at higher sulfate concentrations, i.e., the SO_4^{2-}
 354 concentration in uptake experiments with 9 g/kg GR-Cl (i.e.,
 355 ~ 20 mmol/L GR-Cl) was higher than that of Cl^- ($\text{SO}_4^{2-}/\text{Cl}^-$
 356 = $\sim 2:1$), imply a nearly quantitative transformation of GR-Cl
 357 to GR- SO_4 . A model describing the GR-Cl conversion to GR-
 358 SO_4 was reported in 2020 by Agnel et al.⁴¹ In the series of
 359 experiments at high SO_4^{2-} concentration, no iodide sorption
 360 could be measured. GR- SO_4 has, thus, a very low affinity for
 361 iodide sorption. GR- SO_4 on the one hand and GR-Cl and GR-I
 362 on the other hand are not isostructural and have different
 363 organizations of the interlayer (hexagonal vs rhombohedral).
 364 Structural changes are likely related to the differences in
 365 geometry, charge, and hydration behavior of the interlayer
 366 anions (spherical and monovalent for Cl^- and I^- compared to
 367 tetrahedral divalent for SO_4^{2-}). These differences are the most
 368 likely explanation for the missing affinity of GR- SO_4 to take up
 369 iodide and point toward the possible description of GR-(Cl, I)
 370 as a solid solution, where solid mixing is always preferred for
 371 isostructural solids.
 372

X-ray Absorption Spectroscopy. Iodine K-edge X-ray
 373 absorption spectra have been recorded for samples prepared
 374 considering various pH_m and ionic strength conditions (Table
 375 S5). In the edge region, XANES spectra are comparable for all
 376 GR samples (Figure 4), implying that variations of pH_m or
 377 ionic strength have no influence on the iodine speciation. The
 378 XANES of all GR samples are also similar to that of the $\text{NaI}_{(\text{aq})}$
 379 reference compound, indicating the same oxidation state and
 380

Table 1. Quantitative EXAFS Analysis of GR Samples and the NaI_(aq) Reference Compound at the Iodine K-edge

Sample	FT range ^a [Å ⁻¹]	Fit range ^b [Å]	Shell	N	d [Å]	σ ² [Å ²]	ΔE ₀ [eV]	R _f
GR-Cl-191	2.9–7.5	2.25–4.1	O	6	3.52(2)	0.015(2)	-1.0	0.014
GR-Cl-192	2.9–7.5	2.25–4.1	O	6	3.52(3)	0.012(2)	-1.1	0.028
GR-Cl-195	2.9–7.5	2.25–4.1	O	6	3.53(2)	0.020(1)	-0.1	0.008
NaI _(aq)	2.9–7.5	2.25–4.1	O	6	3.52(2)	0.022(1)	-1.3	0.004

^aFourier transformed range. ^bR + ΔR interval for the fit. N is the coordination number (fixed), d is the interatomic distance, σ² is the mean square displacement (Debye–Waller term), ΔE₀ is the shift in ionization energy with E₀ threshold energy taken as the maximum of the first derivative, and R_f is the figure of merit of the fit as reported in ref 44. The numbers in parentheses indicate the uncertainty.

381 short-range environment (Figure 4). From the analysis of the
382 XANES, it may be concluded that in all GR samples iodide is
383 surrounded by a hydration shell comparable to that of the
384 aqueous anions and shows only weak interaction with the
385 substrate, unaffected by pH_m, ionic strength, or iodine
386 concentration.

387 The iodine K-edge EXAFS spectra of all GR samples are
388 very similar (Figure 4) and also comparable to that of the
389 NaI_(aq) reference. This agrees with the inspection of the
390 XANES. Fit results indicate that iodine is surrounded by 6 O
391 atoms at d(I–O) = 3.52(2) Å in all samples (Figure 4, Table
392 1). These results agree with the reported crystallographic data
393 of hydrated iodide anions in water^{42,43} and the associated high
394 disorder, as indicated by the relatively large Debye–Waller
395 terms. According to the results, changes of pH_m or ionic
396 strength do not affect the hydration shell made of six water
397 molecules binding iodide via H atoms. Overall, XAS data are
398 consistent with a weak electrostatic interaction with the Fe
399 octahedral sheet, comparable to that reported in earlier studies
400 of iodide uptake by formation of a GR-Cl_{1-x}I_x solid solution.¹⁹

401 **Modeling of Iodide Sorption by GR-Cl.** Two models
402 were developed in order to analyze possible uptake
403 mechanisms and to quantitatively describe experimental
404 results. The first approach is based on an ion-exchange uptake
405 mechanism. Figures 1b and 2b show data used for the model
406 adjustments (model/filled squares), which precisely reflect the
407 experimental conditions. A more generic model line is depicted
408 (c(GR) = 0.025 mol/kg, fixed initial concentrations) to
409 provide a more general view on the sorption behavior
410 predicted by the model. The best agreement between model
411 and experiment was achieved with log(k_s) = log(K_I) – log
412 (K_{Cl}) = 1.07 – 1.00 = 0.07 (eqs 2–5).

413 Figure S5 in Supporting Information shows the comparison
414 between modeled and experimental data for the isotherm at a
415 pH_m of 8.5. No significant difference with data at pH_m 7.5
416 could be found at that higher pH_m, which agrees with the
417 absence of pH dependence on the anionic-exchange
418 mechanism. Figure 1 further shows a high level of agreement
419 between the calculated model values and the experimental data
420 at different ionic strengths, thereby also confirming that high
421 Cl⁻ concentrations impede I⁻ sorption. According to these
422 results, there is no significant preference for one anion over the
423 other (chloride or iodide) for uptake. These results compare
424 well with previously reported solid solution experiments, where
425 the Cl⁻/I⁻ ratio in the GR interlayer was the same as in the
426 contacting aqueous phase.¹⁹ Data from this study further show
427 that the absence of selective uptake of one of these two anions
428 is also valid at higher ionic strength up to 5 mol/kg (Figure 1).
429 This experimental finding is also well captured by the solid
430 solution model. The best fit model used an almost equal
431 solubility constant for both endmembers (log K_{sp}(GR-I) =
432 -79.75; log K_{sp}(GR-Cl) = -79.70) and assumed ideal mixing

within the solid. The slightly lower solubility of GR-I reflects
the slightly higher affinity for iodide incorporation compared
to chloride, which is as well reflected in log(k_s) = 0.07.
Accordingly, the predicted solid solution distribution coefficient
is close to one (D = 1.1),⁴⁵ while experimental R_d values
can be recalculated to solid solution distribution coefficients
ranging from 0.5 to 1.4. The difference in the solubility
products is evident as it reflects the affinity for iodide
incorporation. However, considering the uncertainty of the
solubility constant of GR-Cl (which is not reported in the
literature but is likely quite large), the solubility difference is
most likely not significant. In Figure S6 it is shown that this
simplistic solid solution model matches the experimental data
well and that besides the iodide uptake it also adequately
predicts the total solid content. A generic solid solution model
curve is presented on top of the experimental data in Figures
1b and 2b. It demonstrates the degree of agreement between
the two modeling approaches and the experimental results.
Consequently, it may be concluded that the iodide uptake by
GR-Cl proceeds through an ion-exchange mechanism, which is
equivalent to a solid-mixing process, and that all interlayer
anion-exchange sites are available for iodide uptake by GR.³³

GR-Cl synthesis in the presence of iodide and iodide
retention by preformed GR-Cl results in comparable uptake
and solid phase composition. These results are consistent with
literature observations on other LDH phases that hold the
potential for radioiodine uptake. High iodide uptake could be
achieved by Mg/Al LDHs,⁴⁶ Co–Cr layered hydroxalite⁴⁷ or
high Ca-containing phases such as hydrocalumite, C-S-H, and
portlandite.⁴⁸

Implications for Radioactive Waste Disposal. Steel
corrosion in a DGR can lead to the formation of various Fe
(hydr)oxide phases (e.g., magnetite, ferrous hydroxylchloride,
GR, among others), the nature of which being dependent on
several parameters such as pH, E_h, temperature, or
composition of the contacting porewater.^{5,49,50} For example,
depending on the DGR concept, the Cl⁻ concentration can
vary from low to very high and have a significant impact on
the retention of radionuclides by Fe corrosion products. Among
them, GR-Cl possesses a permanent layer charge, conferring it
the potential to retain anionic species such as iodide. Data
show that the iodide uptake also depends on its concentration
and the chloride concentration present in the porewater.
Indeed, chloride competes with iodide for uptake, and low R_d
values can be expected for iodide when Cl⁻ is present in high
concentrations, though the retention of trace amounts of ¹²⁹I⁻
can still be expected in a DGR near-field. Sulfate and carbonate
are other anions typically present in groundwater. The stability
of GR-SO₄ is higher than that of GR-Cl or GR-I. Furthermore,
Refait et al. report the preferential formation of GR-CO₃ over
GR-SO₄ when carbonate and sulfate anions are present
simultaneously during the preparation of GR.⁵¹ Thus, the

485 affinity of GR for CO_3^{2-} uptake is even higher compared to
486 SO_4^{2-} . Consequently, it must be assumed that carbonate
487 would outcompete iodide on the exchange sites. Overall, the
488 retention or retardation of iodide by GR in a DGR near-field
489 seems limited and highly dependent on the nature and
490 concentration of anionic species present in the porewater.

491 Beside the composition of the porewater, the availability of
492 GR is another parameter affecting the extent of iodide
493 retention. For the given geochemical conditions, the amount
494 of immobilized iodide is linked to the amounts of GR present
495 for uptake. Since the stability of mineral phases depends on the
496 prevailing geochemical conditions and given that near-field
497 conditions will evolve with ongoing canister corrosion,
498 conditions can be expected to evolve from favorable to the
499 formation of GR to favorable to the formation of other more
500 thermodynamically stable phases such as magnetite. For
501 example, a pH increase to alkaline conditions^{52,53} due to,
502 e.g., the interaction of cementitious materials in the DGR or
503 water reduction, would render GR instable, which then
504 converts into magnetite.³⁵ Based on the present study, the
505 conversion of GR to magnetite will result in a release of iodide
506 that was immobilized by GR.

507 This study contributes to elucidate the molecular mecha-
508 nism of iodide uptake by GR-Cl by combining batch
509 experiments, XAS, and geochemical modeling. Good agree-
510 ment between experimental data and models could be achieved
511 using either an ion-exchange or a solid solution model,
512 suggesting that hydrated iodide ions substitute at random for
513 chloride within the interlayer, whether in adsorption or in
514 coprecipitation experiments.

515 ■ ASSOCIATED CONTENT

516 ● Supporting Information

517 The Supporting Information is available free of charge at
518 <https://pubs.acs.org/doi/10.1021/acs.est.3c02041>.

519 Structural characterization of GR and magnetite; list of
520 investigated samples, experimental conditions and
521 results; XAS parameters; and model results (PDF)

522 ■ AUTHOR INFORMATION

523 Corresponding Authors

524 **Nicolas Finck** – *Institute for Nuclear Waste Disposal (INE),*
525 *Karlsruhe Institute of Technology (KIT), 76021 Karlsruhe,*
526 *Germany;* orcid.org/0000-0002-1940-4051; Phone: +49
527 (0) 721-6082-4321; Email: nicolas.finck@kit.edu

528 **Tim Platte** – *Institute for Nuclear Waste Disposal (INE),*
529 *Karlsruhe Institute of Technology (KIT), 76021 Karlsruhe,*
530 *Germany;* orcid.org/0000-0001-8584-2298;
531 Email: tim.platte@kit.edu

532 Authors

533 **Frank Heberling** – *Institute for Nuclear Waste Disposal*
534 *(INE), Karlsruhe Institute of Technology (KIT), 76021*
535 *Karlsruhe, Germany;* orcid.org/0000-0002-2650-2071

536 **Robert Polly** – *Institute for Nuclear Waste Disposal (INE),*
537 *Karlsruhe Institute of Technology (KIT), 76021 Karlsruhe,*
538 *Germany*

539 **Tim Prüssmann** – *Institute for Nuclear Waste Disposal*
540 *(INE), Karlsruhe Institute of Technology (KIT), 76021*
541 *Karlsruhe, Germany;* orcid.org/0000-0002-7903-9199

Kathy Dardenne – *Institute for Nuclear Waste Disposal*
(INE), Karlsruhe Institute of Technology (KIT), 76021
Karlsruhe, Germany 542 543 544

Horst Geckeis – *Institute for Nuclear Waste Disposal (INE),*
Karlsruhe Institute of Technology (KIT), 76021 Karlsruhe,
Germany 545 546 547

Complete contact information is available at: 548
<https://pubs.acs.org/10.1021/acs.est.3c02041> 549

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553 Notes

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570 ■ REFERENCES

- (1) McGill, I. R.; McEnaney, B.; Smith, D. C. Crystal Structure of 571
Green Rust Formed by Corrosion of Cast Iron. *Nature* **1976**, *259* 572
(5540), 200–201. 573
- (2) Stampfl, P. P. Ein Basisches Eisen-II-III-Karbonat in Rost. 574
Corros. Sci. **1969**, *9* (3), 185–187. 575
- (3) Butler, G.; Beynon, J. G. The Corrosion of Mild Steel in Boiling 576
Salt Solutions. *Corros. Sci.* **1967**, *7* (7), 385–404. 577
- (4) Usman, M.; Byrne, J. M.; Chaudhary, A.; Orsetti, S.; Hanna, K.; 578
Ruby, C.; Kappler, A.; Haderlein, S. B. Magnetite and Green Rust: 579
Synthesis, Properties, and Environmental Applications of Mixed- 580
Valent Iron Minerals. *Chem. Rev.* **2018**, *118* (7), 3251–3304. 581
- (5) Refait, P.; Abdelmoula, M.; Génin, J.-M. R. Mechanisms of 582
Formation and Structure of Green Rust One in Aqueous Corrosion of 583
Iron in the Presence of Chloride Ions. *Corros. Sci.* **1998**, *40* (9), 584
1547–1560. 585
- (6) King, F. Container Materials for the Storage and Disposal of 586
Nuclear Waste. *CORROSION* **2013**, *69* (10), 986–1011. 587
- (7) King, F.; Hall, D. S.; Keech, P. G. Nature of the Near-Field 588
Environment in a Deep Geological Repository and the Implications 589
for the Corrosion Behaviour of the Container. *Corros. Eng. Sci.* 590
Technol. **2017**, *52* (sup1), 25–30. 591
- (8) Lucchini, J.-F.; Borkowski, M.; Richmann, M. K.; Ballard, S.; 592
Reed, D. T. Solubility of Nd³⁺ and UO₂²⁺ in WIPP Brine as 593
Oxidation-State Invariant Analogs for Plutonium. *J. Alloys Compd.* 594
2007, *444–445*, 506–511. 595
- (9) Abdelmoula, M.; Trolard, F.; Bourrié, G.; Génin, J. M. R. 596
Evidence for the Fe(II)-Fe(III) Green Rust “Fougerite †” Mineral 597
Occurrence in a Hydromorphic Soil and Its Transformation with 598
Depth. *Hyperfine Interact.* **1998**, *112* (1–4), 235–238. 599
- (10) Trolard, F.; Génin, J.-M.; Abdelmoula, M.; Bourrié, G.; 600
Humbert, B.; Herbillon, A. Identification of a Green Rust Mineral in a 601
Reductomorphic Soil by Mössbauer and Raman Spectroscopies. 602
Geochim. Cosmochim. Acta **1997**, *61* (5), 1107–1111. 603

- 604 (11) Kaplan, D. I.; Serne, R. J.; Parker, K. E.; Kutnyakov, I. V. Iodide
605 Sorption to Subsurface Sediments and Illitic Minerals. *Environ. Sci.*
606 *Technol.* **2000**, *34* (3), 399–405.
- 607 (12) SAZARASHI, M.; IKEDA, Y.; SEKI, R.; YOSHIKAWA, H.
608 Adsorption of I⁻ Ions on Minerals for 129 I Waste Management. *J.*
609 *Nucl. Sci. Technol.* **1994**, *31* (6), 620–622.
- 610 (13) Tournassat, C.; Gaucher, E. C.; Fattahi, M.; Grambow, B. On
611 the Mobility and Potential Retention of Iodine in the Callovian-
612 Oxfordian Formation. *Phys. Chem. Earth, Parts A/B/C* **2007**, *32* (8–
613 14), 539–551.
- 614 (14) Balsley, S. D.; Brady, P. V.; Krumhansl, J. L.; Anderson, H. L.
615 Anion Scavengers for Low-Level Radioactive Waste Repository
616 Backfills. *J. Soil Contam.* **1998**, *7* (2), 125–141.
- 617 (15) Muramatsu, Y.; Uchida, S.; Sriyotha, P.; Sriyotha, K. Some
618 Considerations on the Sorption and Desorption Phenomena of Iodide
619 and Iodate on Soil. *Water. Air. Soil Pollut.* **1990**, *49* (1–2), 125–138.
- 620 (16) Ticknor, K. V.; Cho, Y.-H. Interaction of Iodide and Iodate
621 with Granitic Fracture-Filling Minerals. *J. Radioanal. Nucl. Chem.*
622 *Artic.* **1990**, *140* (1), 75–90.
- 623 (17) Fuhrmann, M.; Bajt, S.; Schoonen, M. A. A. Sorption of Iodine
624 on Minerals Investigated by X-Ray Absorption near Edge Structure
625 (XANES) and 125I Tracer Sorption Experiments. *Appl. Geochem.*
626 **1998**, *13* (2), 127–141.
- 627 (18) Aimoz, L.; Kulik, D. A.; Wieland, E.; Curti, E.; Lothenbach, B.;
628 Mäder, U. Thermodynamics of AFm-(I₂, SO₄) Solid Solution and of
629 Its End-Members in Aqueous Media. *Appl. Geochem.* **2012**, *27* (10),
630 2117–2129.
- 631 (19) Platte, T.; Finck, N.; Mangold, S.; Polly, R.; Geckeis, H.
632 Retention of Iodide and Chloride by Formation of a Green Rust Solid
633 Solution GR-Cl 1- x I X: A Multiscale Approach. *Inorg. Chem.* **2021**,
634 *60* (14), 10585–10595.
- 635 (20) Vinš, J.; Šubr, J.; Zapletal, V.; Hanousek, F. Preparation and
636 Properties of Green Rust Type Substances. *Collect. Czechoslov. Chem.*
637 *Commun.* **1987**, *52* (1), 93–102.
- 638 (21) Altmaier, M.; Metz, V.; Neck, V.; Müller, R.; Fanghänel, T.
639 Solid-Liquid Equilibria of Mg(OH)₂(Cr) and Mg₂(OH)₃Cl·
640 4H₂O(Cr) in the System Mg-Na-H-OH-Cl-H₂O at 25°C. *Geochim.*
641 *Cosmochim. Acta* **2003**, *67* (19), 3595–3601.
- 642 (22) Nedel, S.; Dideriksen, K.; Christiansen, B. C.; Bovet, N.; Stipp,
643 S. L. S. Uptake and Release of Cerium During Fe-Oxide Formation
644 and Transformation in Fe(II) Solutions. *Environ. Sci. Technol.* **2010**,
645 *44* (12), 4493–4498.
- 646 (23) Finck, N.; Nedel, S.; Dideriksen, K.; Schlegel, M. L. Trivalent
647 Actinide Uptake by Iron (Hydr)Oxides. *Environ. Sci. Technol.* **2016**,
648 *50* (19), 10428–10436.
- 649 (24) Zimina, A.; Dardenne, K.; Denecke, M. A.; Doronkin, D. E.;
650 Huttel, E.; Lichtenberg, H.; Mangold, S.; Pruessmann, T.; Rothe, J.;
651 Spangenberg, T.; Steininger, R.; Vitova, T.; Geckeis, H.; Grunwaldt,
652 J.-D. CAT-ACT—A New Highly Versatile x-Ray Spectroscopy
653 Beamline for Catalysis and Radionuclide Science at the KIT
654 Synchrotron Light Facility ANKA. *Rev. Sci. Instrum.* **2017**, *88* (11),
655 113113.
- 656 (25) Parkhurst, D. L.; Appelo, C. *Description of Input and Examples*
657 *for PHREEQC Version 3—A Computer Program for Speciation, Batch-*
658 *Reaction, One-Dimensional Transport, and Inverse Geochemical*
659 *Calculations*; U.S. Geological Survey Techniques and Methods; U.S.
660 Geological Survey: 2013.
- 661 (26) Giffaut, E.; Grivé, M.; Blanc, P.; Vieillard, P.; Colàs, E.;
662 Gailhanou, H.; Gaboreau, S.; Marty, N.; Madé, B.; Duro, L. Andra
663 Thermodynamic Database for Performance Assessment: ThermoChi-
664 mie. *Appl. Geochem.* **2014**, *49*, 225–236.
- 665 (27) Heberling, F.; Klaić, T.; Raiteri, P.; Gale, J. D.; Eng, P. J.;
666 Stubbs, J. E.; Gil-Díaz, T.; Begović, T.; Lützenkirchen, J. Structure and
667 Surface Complexation at the Calcite(104)-Water Interface. *Environ.*
668 *Sci. Technol.* **2021**, *55* (18), 12403–12413.
- 669 (28) Prieto, M. Thermodynamics of Solid Solution-Aqueous
670 Solution Systems. *Rev. Mineral. Geochemistry* **2009**, *70* (1), 47–85.
- 671 (29) Chivot, J. *Thermodynamique Des Produits de Corrosion Fonctions*
672 *Thermodynamiques, Diagrammes de Solubilité, Diagrammes E-Ph Des*
Systèmes Fe-H₂O, Fe-CO₂-H₂O, Fe-S-H₂O, Cr-H₂O et Ni-H₂O En
Fonction de La Temperature; Collection Sciences & Techniques; 673
Andra: Châtenay-Malabry, 2004. 674
- (30) Génin, J. M. R.; Bourrié, G.; Trolard, F.; Abdelmoula, M.; 675
Jaffrezic, A.; Refait, P.; Maitre, V.; Humbert, B.; Herbillon, A. 676
Thermodynamic Equilibria in Aqueous Suspensions of Synthetic and 677
Natural Fe(II)-Fe(III) Green Rusts: Occurrences of the Mineral in 678
Hydromorphic Soils. *Environ. Sci. Technol.* **1998**, *32* (8), 1058–1068. 679
- (31) Min, J. H.; Baik, M. H.; Lee, J. K.; Jeong, J. T. Sorption of I and 680
Se onto Green Rusts with Different Interlayer Anions, GR(CO 3 2-) 681
AND GR(Cl⁻). *J. Nucl. Fuel Cycle Waste Technol.* **2013**, *1* (1), 57–63. 682
- (32) Curtius, H.; Kattilparampil, Z. Sorption of Iodine on Mg-Al 683
Layered Double Hydroxide. *Clay Miner.* **2005**, *40* (4), 455–461. 684
- (33) Nedyalkova, L.; Tits, J.; Renaudin, G.; Wieland, E.; Mäder, U.; 685
Lothenbach, B. Mechanisms and Thermodynamic Modelling of 686
Iodide Sorption on AFm Phases. *J. Colloid Interface Sci.* **2022**, *608*, 687
683–691. 688
- (34) Morelová, N.; Finck, N.; Lützenkirchen, J.; Schild, D.; 689
Dardenne, K.; Geckeis, H. Sorption of Americium/Europium onto 690
Magnetite under Saline Conditions: Batch Experiments, Surface 691
Complexation Modelling and X-Ray Absorption Spectroscopy Study. 692
J. Colloid Interface Sci. **2020**, *561*, 708–718. 693
- (35) Jolivet, J.-P.; Tronc, E.; Chanéac, C. Iron Oxides: From 694
Molecular Clusters to Solid. A Nice Example of Chemical Versatility. 695
Comptes Rendus Geosci. **2006**, *338* (6–7), 488–497. 696
- (36) Maćzka, E.; Jartych, E.; Kosmulski, M. Isoelectric Points of 697
Fresh and Aged Fe(OH)₂. *Colloids Surfaces A Physicochem. Eng. Asp.* 698
2014, *441*, 326–330. 699
- (37) Fleet, M. E. The Structure of Magnetite: Symmetry of Cubic 700
Spinel. *J. Solid State Chem.* **1986**, *62* (1), 75–82. 701
- (38) Bernal, J. D. The Oxides and Hydroxides of Iron and Their 702
Structural Inter-Relationships. *Clay Miner.* **1959**, *4* (21), 15–30. 703
- (39) Swanson, H. E.; Tatge, E. *Circular of the Bureau of Standards* 704
No. 539 Vol. 1: Standard X-ray Diffraction Powder Patterns; National 705
Bureau of Standards: 1953; p 43. 706
- (40) Refait, P.; Génin, J. M. R. The Transformation of Chloride- 707
Containing Green Rust One into Sulphated Green Rust Two by 708
Oxidation in Mixed Cl⁻ and SO₄²⁻ Aqueous Media. *Corros. Sci.* **1994**, 709
36 (1), 55–65. 710
- (41) Agnel, M. I.; Grangeon, S.; Fauth, F.; Elkaim, E.; Claret, F.; 711
Roulet, M.; Warmont, F.; Tournassat, C. Mechanistic and 712
Thermodynamic Insights into Anion Exchange by Green Rust. 713
Environ. Sci. Technol. **2020**, *54* (2), 851–861. 714
- (42) Fulton, J. L.; Schenter, G. K.; Baer, M. D.; Mundy, C. J.; Dang, 715
L. X.; Balasubramanian, M. Probing the Hydration Structure of 716
Polarizable Halides: A Multiedge XAFS and Molecular Dynamics 717
Study of the Iodide Anion. *J. Phys. Chem. B* **2010**, *114* (40), 12926– 718
12937. 719
- (43) Maeda, M.; Ohtaki, H. An X-Ray Diffraction Study of a 720
Concentrated Aqueous Sodium Iodide Solution. *Bull. Chem. Soc. Jpn.* 721
1975, *48* (12), 3755–3756. 722
- (44) Finck, N.; Dardenne, K.; Geckeis, H. Am(III) Coprecipitation 723
with and Adsorption on the Smectite Hectorite. *Chem. Geol.* **2015**, 724
409, 12–19. 725
- (45) Heberling, F.; Metz, V.; Böttle, M.; Curti, E.; Geckeis, H. Barite 726
Recrystallization in the Presence of 226Ra and 133Ba. *Geochim.* 727
Cosmochim. Acta **2018**, *232*, 124–139. 728
- (46) Theiss, F. L.; Ayoko, G. A.; Frost, R. L. Sorption of Iodide (I⁻) 729
from Aqueous Solution Using Mg/Al Layered Double Hydroxides. 730
Mater. Sci. Eng., C **2017**, *77*, 1228–1234. 731
- (47) Levitskaia, T. G.; Chatterjee, S.; Arey, B. W.; Campbell, E. L.; 732
Hong, Y.; Kovarik, L.; Peterson, J. M.; Pence, N. K.; Romero, J.; 733
Shutthanandan, V.; Schwenzler, B.; Varga, T. RedOx-Controlled 734
Sorption of Iodine Anions by Hydrotalcite Composites. *RSC Adv.* 735
2016, *6* (79), 76042–76055. 736
- (48) Liu, X.; Asai, A.; Sato, T.; Opiso, E.; Otake, T.; Yoneda, T. 737
Mineral Synthesis in Si-Al-Ca Systems and Their Iodide Sorption 738
Capacity under Alkaline Conditions. *Water, Air, Soil Pollut.* **2013**, *224* 739
(3), 1442. 740
741

742 (49) Schlegel, M. L.; Necib, S.; Dumas, S.; Blanc, C.; Foy, E.;
743 Trcera, N.; Romaine, A. Microstructural Characterization of Carbon
744 Steel Corrosion in Clay Borehole Water under Anoxic and Transient
745 Acidic Conditions. *Corros. Sci.* **2016**, *109*, 126–144.

746 (50) Wang, Z.; Moore, R.; Felmy, A.; Mason, M.; Kukkadapu, R. A
747 Study of the Corrosion Products of Mild Steel in High Ionic Strength
748 Brines. *Waste Manag.* **2001**, *21* (4), 335–341.

749 (51) Refait, P.; Drissi, S. H.; Pytkiewicz, J.; Génin, J.-M. R. The
750 Anionic Species Competition in Iron Aqueous Corrosion: Role of
751 Various Green Rust Compounds. *Corros. Sci.* **1997**, *39* (9), 1699–
752 1710.

753 (52) Chaparro, M. C.; Finck, N.; Metz, V.; Geckeis, H. Reactive
754 Transport Modelling of the Long-Term Interaction between Carbon
755 Steel and MX-80 Bentonite at 25 °C. *Minerals* **2021**, *11* (11), 1272.

756 (53) Bildstein, O.; Trotignon, L.; Perronnet, M.; Jullien, M.
757 Modelling Iron-Clay Interactions in Deep Geological Disposal
758 Conditions. *Phys. Chem. Earth, Parts A/B/C* **2006**, *31* (10–14),
759 618–625.