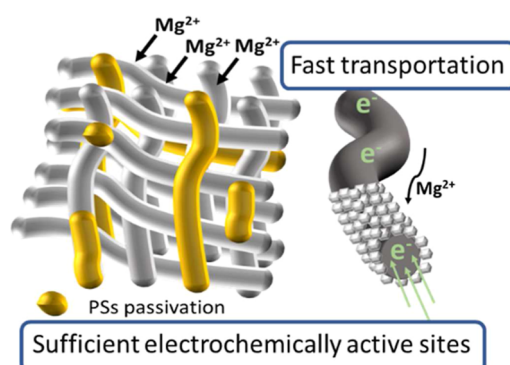


Insights into the Degradation Mechanism of the Magnesium Anode in Magnesium–Chalcogen Batteries: Revealing Principles for Anode Design with a 3D-Structured Magnesium Anode

Liping Wang,^{*} Thomas Diemant, Zhenyou Li, Bosubabu Dasari, and Zhirong Zhao-Karger^{*}

ABSTRACT: Magnesium–chalcogen batteries are promising post lithium battery systems for large-scale energy storage applications in terms of energy density, material sustainability, safety, and cost. However, the soluble reaction intermediates, such as polysulfides or polyselenides, formed during the electrochemical processes can severely passivate the Mg metal anode, limiting the cycle life of the batteries. It is necessary to scrutinize the failure in Mg–chalcogen batteries from an anodic perspective. Herein, the Mg metal anode failure mechanism is thoroughly examined, revealing that it is induced by an inhomogeneous Mg deposition promoted by soluble intermediates from chalcogen cathodes. To further confirm the mechanism and solve this anode failure problem, a multifunctional 3D current collector is used to decrease the local current density and regulate the Mg deposition behavior. The present findings are anticipated to provide guidance for anode design, enhance the lifespan of Mg–chalcogen batteries, and facilitate the development of other magnesium metal batteries.

KEYWORDS: 3D magnesium anode, inhomogeneous Mg deposition, anode passivation, polysulfides shuttle, magnesium–chalcogen batteries



1. INTRODUCTION

Rechargeable magnesium batteries (RMBs) have shown great potential as a cost-effective, safe, and environmentally friendly technology for electrochemical energy storage and conversion. Magnesium metal has a low reduction potential [-2.36 V vs standard hydrogen electrode] and high theoretical capacities (3832 mA h cm^{-3} , 2205 mA h g^{-1}). The natural abundance of Mg was determined to be the eighth and the third in Earth's crust and sea water, respectively, indicating promising availability and low cost for large-scale applications. Besides, in contrast to lithium, magnesium is less susceptible to dendrite formation during deposition and may be a good choice for a safe metal anode.^{1–7} When coupled with a sustainable chalcogen cathode, such as sulfur (S) or selenium (Se), Mg–chalcogen batteries possess a higher theoretical volumetric capacity than Li–chalcogen batteries, making them a promising candidate for emerging energy storage markets.^{8–10}

In comparison with the progress made in the fields of electrolytes and cathodes, there has been less research work concentrated on the Mg anode. The Mg metal foil is considered to be used both as an electrode and a current collector, which is thought advantageous for a battery system. Though this concept is attractive, there are still formidable challenges in practice. First, magnesium offers slower reaction kinetics compared to lithium due to the divalent magnesium ion with higher charge density (120 C mm^{-3} for Mg^{2+} vs 52 C mm^{-3} for Li^+).^{11,12}

Second, with a hexagonal structure, Mg has a limited ductility, making it difficult to cost-effectively form the desired thin foil as an anode for RMBs.^{13,14} Additionally, the unavoidable interactions between Mg metal and organic electrolyte solutions have been found to play a crucial role in the electrochemical performance of RMBs.^{15,16} It is well known that lithium-ion batteries are able to form solid electrolyte interfaces via reactions with the electrolyte, which allow the transport of lithium ions between the anode and the electrolyte without substantial degradation.¹⁷ In contrast, magnesium strongly tends to form insulating passivation layers^{18–21} or surface adlayers composed of some species in the electrolyte. The coverage layers on the Mg surface may increase interfacial resistance and kinetic barriers for Mg^{2+} transfer, leading to high overpotential and low Coulombic efficiency for Mg plating and stripping.²² The problem is getting even worse when using chalcogen cathodes, such as in Mg–S and Mg–Se batteries. After the dissolution of magnesium polysulfides/polyselenides (Mg-PSs) into the electrolyte, they

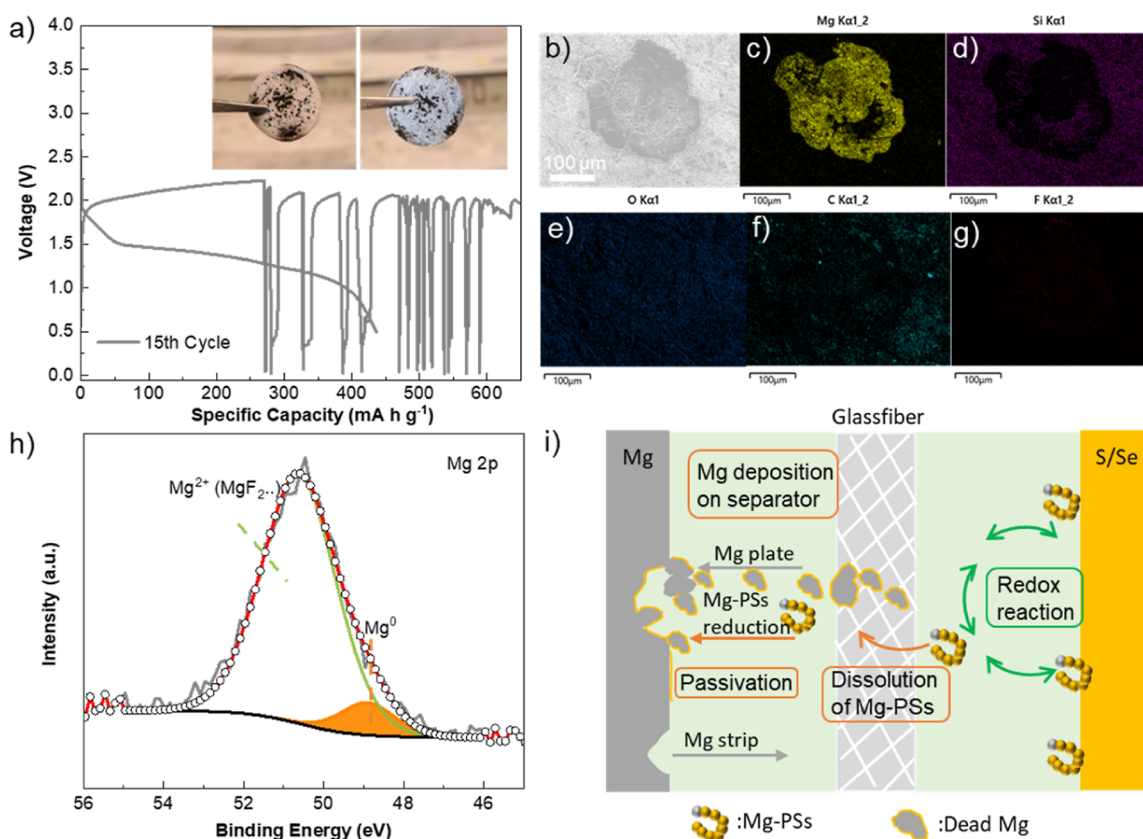


Figure 1. (a) Galvanostatic discharge/charge curve of a Mg–S cell when it failed (inset shows the photographs of the Mg anode (right) and glass fiber separator (left) obtained from this cell after disassembly). (b) SEM image, (c–g) EDX maps, and (h) Mg 2p XPS spectrum of a glass fiber separator after disassembling from a Mg–S cell and washing with the DME solvent. (i) Schematic depiction of the failure mechanism of Mg metal anodes in Mg–S batteries.

may diffuse across the separator to the Mg anode, where they can be further reduced, leading to the acceleration of detrimental passivation on the Mg anode. As a result, Mg–S/Mg–Se systems have mostly reported short cycle lives, especially without a Li mediator or corrosive halogen compounds inside the electrolyte.^{23–30} There are some pioneering works about electrolyte engineering^{31,32} and cathode modification.³³ However, to the best of our knowledge, there is a lack of studies on the dynamic evolution of the Mg metal anode during cycling and its correlation with the degradation or failure of Mg–S/Mg–Se batteries.

Various cathode and separator design strategies have been proposed in order to control the dissolution and diffusion of polysulfide from the cathode to the anode side in Mg–S/Mg–Se batteries.^{34–36} In contrast, less research effort was devoted to the optimization of anode materials for Mg–chalcogen batteries. Sievert et al. dispersed fine Mg particles in carbon and demonstrated the effectiveness of structure design for the improvement of Mg–S batteries. However, finely dispersed magnesium may strongly react with oxygen in air, and passivation may occur when handling the material.³⁷ In fact, the composition and morphology of the electrolyte/anode interface may considerably affect the electrochemical performance of the batteries.^{38,39} To tackle the critical issues in Mg–chalcogen batteries, it is also required to design the structure of the magnesium anode rationally.

Herein, a systematic investigation was carried out to discover the underlying reasons for the Mg–S and Mg–Se batteries' failure. To further confirm the mechanism and circumvent the

obstacles originating from the Mg foil anode, a novel structure of the Mg anode based on a multifunctional 3D current collector was designed. A freestanding active carbon cloth (ACC) acts as the 3D current collector, which provides two advantages: (1) the enlarged surface area of the ACC lowers the local current density, which enables uniform magnesium electrochemical deposition; (2) the interconnected scaffold of the ACC can improve the contact between electrolyte and electrode, fasten Mg^{2+} ion transport, and improve the kinetics of the electrode. Remarkably, these ACC-based anodes can greatly alleviate the early failure of Mg–S/Mg–Se cells. This study highlights the metal anode degradation mechanism in Mg–S/Mg–Se batteries and provides guidelines for a reasonable structural design of metal anodes in magnesium-based batteries.

2. RESULTS AND DISCUSSION

2.1. Failure Mechanism of the Magnesium Anode in Mg–S Batteries. Coin cells comprised of a 0.4 M $\text{Mg}[\text{B}(\text{hfp})_4]_2$ electrolyte,⁴⁰ an activated carbon cloth/sulfur (ACC/S) cathode, and a Mg foil anode were cycled at a current rate of 0.1 C. To reveal the origin of high polarization and fast degradation of Mg–S cells composed of a Mg foil anode and a ACC/S cathode, we first conducted scanning electron microscopy (SEM)–energy dispersive X-ray spectroscopy (EDX) and X-ray photoelectron spectroscopy (XPS) analysis of the Mg foil anode and separator (close to the anode side) by recovering the coin cells after failure (Figure 1). The typical discharge/charge curve when a cell fails is shown in Figure 1a. The failure always occurred during the charge process showing a

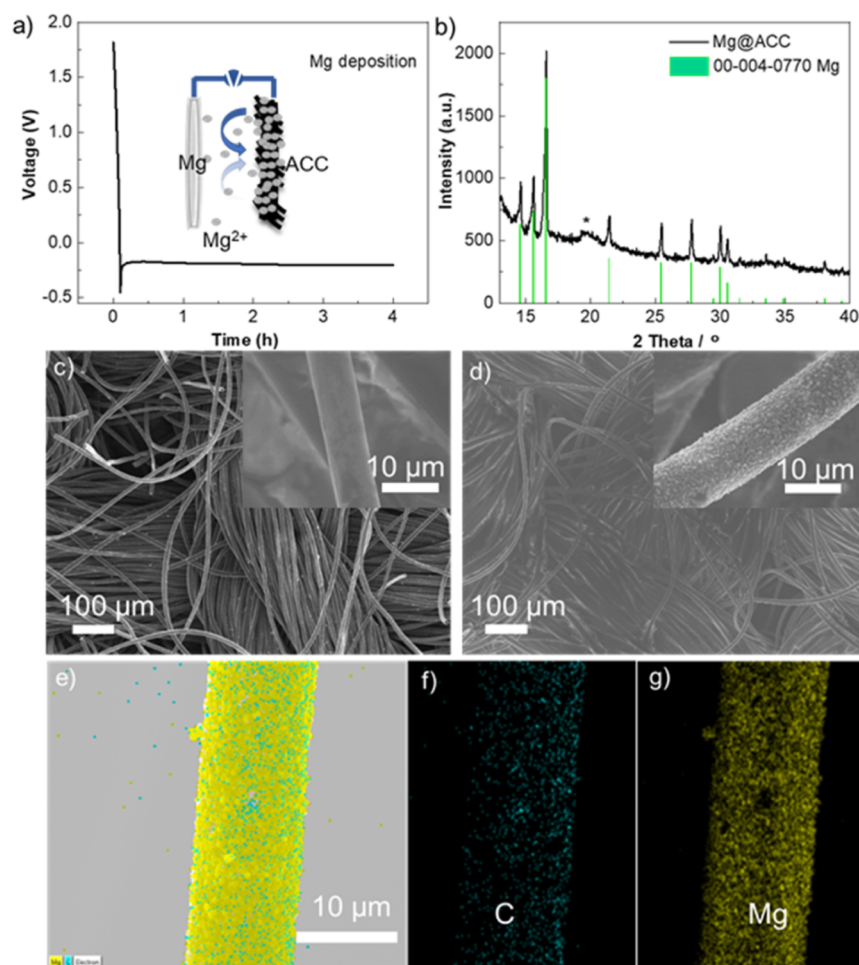


Figure 2. (a) Mg plating profile of a Mg|ACC cell (inset: schematic illustration of Mg deposition on ACC). (b) XRD pattern of Mg@ACC. (c,d) Typical SEM images of (c) ACC and (d) Mg@ACC (Mg: 4 mA h cm⁻²). (e–g) EDX maps of Mg@ACC.

fluctuating curve, which could not reach the upper cutoff voltage anymore. This phenomenon was also observed and reported before.^{9,35,36,41} The photographs in the inset of Figure 1a illustrate the Mg foil and the separator disassembled from the failing cell. Some black spots could be clearly observed on both the anode and separator, where the electrochemical reactions took place. The following analyses were carried out mainly on these black spots. Figures S1–S3 demonstrate the morphology and elemental distribution of the Mg anode (Figures S1 and S2) and separator (Figure S3) without further treatment. As can be seen, the Mg surface was rugged accompanied by caves and pits, which resulted from the Mg stripping process. On the pits, there are many porous, irregularly deposited Mg particles, indicating the nonuniform Mg plating. Furthermore, EDX mapping shows a more intense sulfur signal for the deposits on both anode and separator than for the rest areas, indicating that deposits are more susceptible to form sulfur-containing byproducts or passivation layers than the bulk Mg (Mg substrate). Similar to the separator, the EDX spectrum (Figure S3) indicates that these black deposits are mainly composed of Mg, with some sulfur (S), oxygen (O), carbon (C), and fluorine (F). To further figure out the composition of the black deposits, the separator was rinsed with dimethoxy ethane (DME) in a glovebox to remove the residual electrolyte salt and soluble Mg-PSs (Figure S4). After washing, there were still lots of black spots on the separator, and the color of the DME solvent turned red–brown

(Figure S4b), indicating dissolved Mg-PSs. The top surface and cross-sectional SEM images of the washed separators in Figure S5 illustrate similar structures of these deposits as micrometer-sized islands. The ones circled in red (Figure S5d–f) were observed from cross-sectional SEM images, indicating the penetration of the deposits through the separator. The corresponding cross-sectional EDX maps of the separator are displayed in Figure S6. The distribution of Mg element confirms that the deposits were distributed not only on the surface but also through the separator. In order to elaborate on the composition, the deposits on the DME washed separator were analyzed by XPS. The Mg 2p spectrum (Figure 1h) could be fitted with two peaks at 48.9 and 50.6 eV, which are assigned to metallic Mg⁰ and various Mg²⁺-containing compounds, for example, MgF₂. The results confirm that the black spots on the separator are composed of a freshly deposited Mg core with some byproducts from parasitic reactions on the surface. The corresponding F 1s spectrum (Figure S7a) showed two peaks at 685.5 and 688.6 eV, corresponding to MgF₂ and –CF₃ groups (from the remaining electrolyte), respectively. The O 1s spectrum (Figure S7b) could be fitted with three peaks at 532.7 eV (SiO₂/separator), 531.8 eV (C=O), and 533.3 eV (C–O), which originated from a short period of air-exposure during the ex situ measurements and residuals of the DME solvent used for washing the separator. Interestingly, sulfur was not detectable in the measurements, most probably any S species

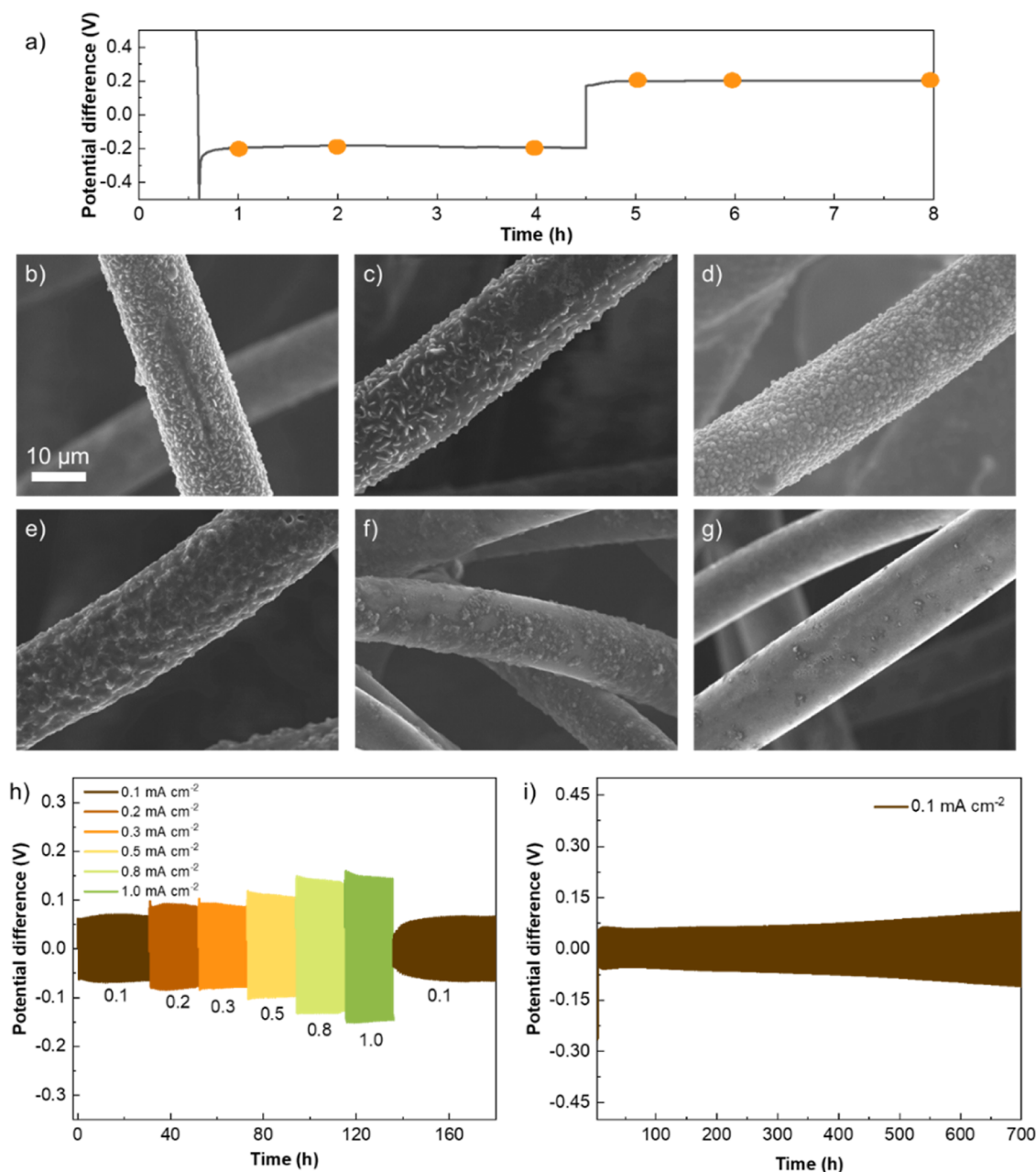


Figure 3. (a) Illustration of the discharge/charge process of the Mg@ACC electrode. Typical SEM images of Mg@ACC after plating Mg metal into ACC for (b) 1, (c) 2, and (d) 4 h and then stripping Mg for (e) 1, (f) 2, and (g) 4 h from Mg@ACC. (h) Mg plating/stripping performance of the Mg| Mg@ACC cell at various current densities (from 0.1 to 1.0 mA cm⁻²) for a plating/stripping time of 0.5 h. (i) Long-term cycling of the Mg|Mg@ACC cell at 0.1 mA cm⁻².

were removed by washing or evaporated in the load lock of the XPS system before the measurement. A direct comparison of the different compositions of the black spots and the rest area of the separator is shown in Figure S8. As expected, the ratio of Mg is much higher in the deposits than in the rest areas, which corresponds to the XPS results.

Taken together, it is rational to postulate that the failure of Mg anodes is highly related to the inhomogeneous nucleation and growth of Mg on the metal foil due to the unavoidable inhomogeneity of the metal electrode surface.^{42–46} In addition, dissolved polysulfide species further accelerate this uneven deposition in Mg–S batteries. As illustrated in Figure 1i, fresh Mg starts to deposit during the charge process. Simultaneously, the dissolved polysulfides accumulate on the surface of the fresh

Mg and may subsequently passivate the Mg or be further reduced by the fresh Mg,⁴⁷ forming Mg-PSs wrapped “dead Mg”. Similar phenomena were reported in batteries with a lithium-metal anode.^{48–51} The high ionic resistance of the polysulfide passivation layer downsizes the nuclei and thus results in a more uneven Mg deposition. This situation severely deteriorates with cycles, where more and more brittle Mg deposits accumulate around the cavities. They are easy to detach from the Mg foil, inducing aggravated local etching and the formation of isolated “dead Mg”. Some of them travel with the electrolyte and penetrates the separator, leading to the failure of the cell. This also explains the phenomenon that the failure always occurs during the charge process, and the fluctuating shape of the charge curve may relate to the unstable “dead Mg”.

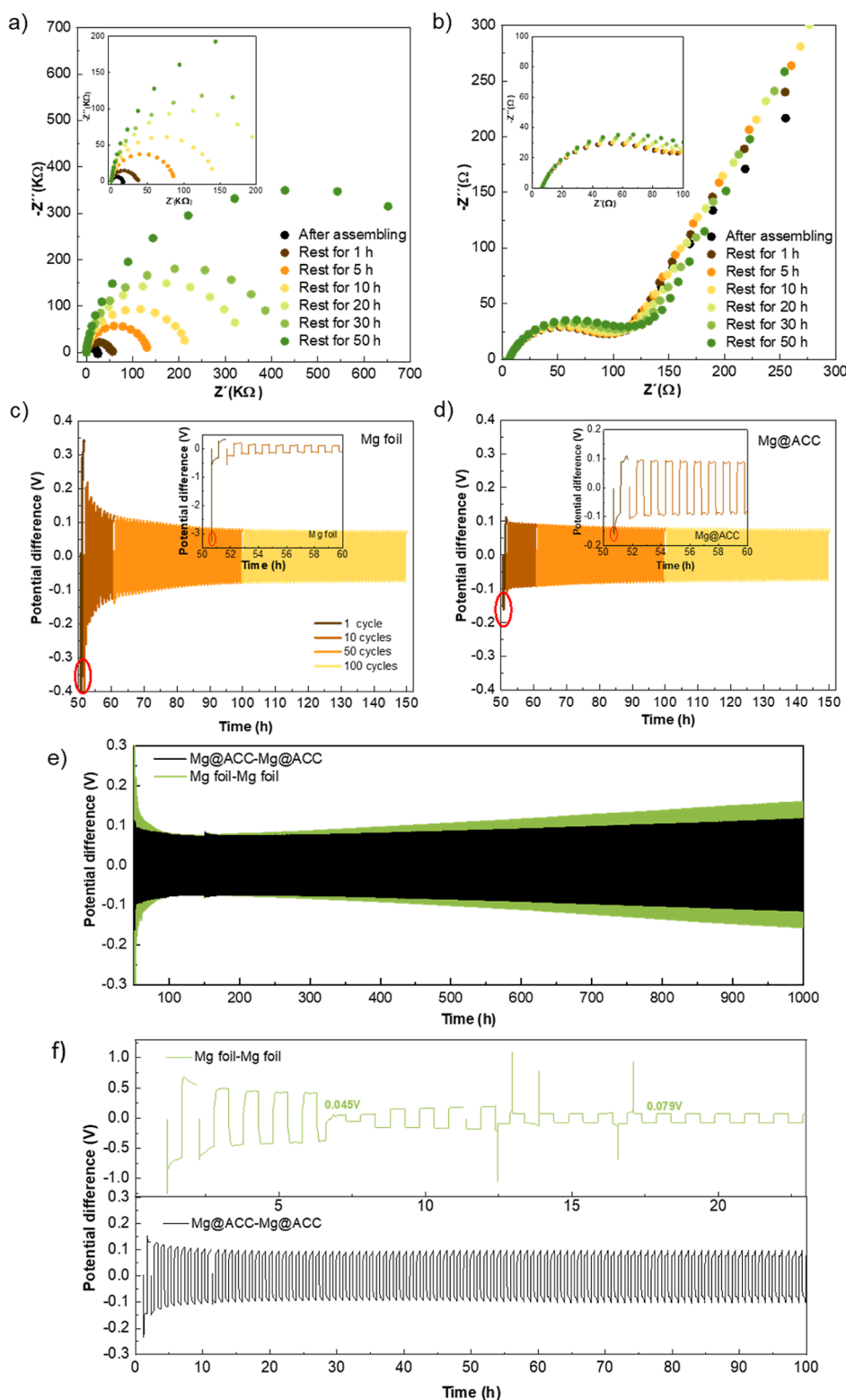


Figure 4. Nyquist plots of (a) Mg foil/Mg foil and (b) Mg@ACC/Mg@ACC cells in the frequency range of 1 MHz to 20 mHz with different rest times at OCV. Mg plating/stripping performance of symmetric (c) Mg foil/Mg foil and (d) Mg@ACC/Mg@ACC cells at the current density of 0.1 mA cm⁻². Insets: enlarged profiles of the first 10 cycles. Galvanostatic plating/stripping profiles in Mg@ACC/Mg@ACC and Mg/Mg symmetrical cells at 0.1 mA cm⁻² with (e) blank electrolyte and (f) electrolyte dissolved with polysulfides.

Based on the abovementioned results and analysis, we conclude that it is necessary to find a way to allow a uniform Mg deposition in order to ensure the performance of the Mg anode for Mg-S/Mg-Se batteries. Many researchers have

reported that 3D current collectors can provide large surface areas, thus decreasing the local current density and regulating the Li metal deposition.^{52,53} Inspired by their works, ACC has been employed as a multifunctional 3D current collector for the

magnesium metal layer gradually grew on the carbon fibers (Figure 3c,d). Upon stripping, magnesium was oxidized again and started to lose electrons and dissolve back into the electrolyte (Figure 3e,f). After being fully charged, the framework of the ACC remained intact (Figure 3g), suggesting its good structural stability. Taken together, these results show that the plating/stripping process of magnesium on the ACC is highly reversible, which guarantees the stable cycling performance of the electrode. To demonstrate the electrochemical behavior of a Mg@ACC electrode, symmetric Mg|Mg@ACC cells were tested at various current densities. As shown in Figure 3h, the overpotentials increased slightly with growing current densities and became stable within a few cycles. Even at the relatively high current density of 1.0 mA cm^{-2} , the cell maintained a low polarization of about 0.12 V. A long-term cyclability test with a current of 0.1 mA cm^{-2} is displayed in Figure 3i. The cell allowed stable operation for more than 700 cycles while maintaining a low polarization below 0.15 V. Long-term cycling performance at a higher current density of 0.5 mA cm^{-2} was also investigated; the results are presented in Figure S10. The cell still shows excellent cyclic stability with an overpotential below 0.15 V after 400 cycles. All these results demonstrate that highly reversible plating/stripping of Mg can be realized successfully with small overpotentials by using a Mg@ACC electrode.

To gain more information about the differences in the electrode/electrolyte interfaces between the Mg foil anode and Mg@ACC, electrochemical impedance spectra (EIS) were acquired for symmetric Mg foil|Mg foil and Mg@ACC|Mg@ACC cells after various rest times at open-circuit voltage (OCV). Figure 4a displays the Nyquist plots measured with a Mg foil|Mg foil symmetric cell. The impedance was measured to be 24 k Ω after assembly and kept increasing incrementally with the rest time. After 50 h, the resistance reached 787 k Ω (i.e., more than 30 times the initial value). This result is in agreement with the previous literatures.^{15,40} The increasing resistance of the Mg electrode may be related to the formation of an adsorption layer from the solvent, which accounts for the difference in the initial voltage spike (-3.24 V) in Figure 4c. For the Mg@ACC|Mg@ACC cell, the impedance was observed to stabilize at approximately 100 Ω with various storage times at OCV (Figure 4b), roughly three orders of magnitude lower than for the Mg foil|Mg foil cell. Correspondingly, the initial voltage spike with Mg@ACC was much reduced to -0.16 V , as shown in Figure 4d. Both the low interfacial resistance and small initial voltage spike point to fast charge transfer on the interface of a Mg@ACC electrode. The galvanostatic intermittent titration technique was also used to further confirm the low polarization of the cell with Mg@ACC, as shown in Figure S11. Besides, the long-term cycling stability of symmetric cells was further tested (Figure 4e, enlarged profiles shown in Figure S12). Compared with bare Mg foil (green), the Mg@ACC (black) symmetric cells displayed a lower voltage polarization and improved plating/stripping stability up to 1000 cycles, revealing the excellent reversible Mg stripping/plating behavior. To evaluate the performance of the two kinds of the Mg electrode with the dissolved magnesium polysulfide, an additional 40 μL magnesium polysulfide solution was added inside the cells. The polysulfide solution (Figure S13) was prepared according to a reported procedure.⁴⁰ With the polysulfide-containing electrolyte (Figure 4f), the cell with the Mg foil anode (green) shows a high overpotential at the beginning and decreases significantly to 0.045 V after 7 h. After that, the voltage curve displays a rectangular shape, which

corresponds to a soft short-circuit behavior.⁴⁴ While the cell with Mg@ACC (black) displays a stable stripping/plating with a voltage hysteresis around 0.09 V after 100 cycles, which demonstrates the high tolerance to polysulfides.

2.3. Electrochemical Performances of Mg–Chalcogen Batteries. In the next step, the performance of Mg@ACC anodes in Mg–S batteries was investigated using a model ACC/S composite as a cathode material. The ACC/S cathode was fabricated via a commonly used melt-diffusion method, as reported before.¹⁰ The SEM and EDX images of ACC/S in Figure S14 demonstrate the uniform dispersion of sulfur in the porous carbon fibers. Both Mg@ACC and Mg foil anodes were paired with the ACC/S cathode and assembled in coin cells. In comparison to the cell with Mg foil, the Mg@ACC cell showed a lower voltage hysteresis in the first cycle charge–discharge profiles and cyclic voltammetry curves, as shown in Figure 5a,b. The voltage hysteresis can be roughly analyzed by the galvanostatic charge–discharge curves shown in Figure S15. Apart from that, three-electrode cells were also assembled with ACC/S as the working electrode, Mg foil or Mg@ACC as counter electrode (CE), and a Mg ring as reference electrode (RE), respectively. As shown in Figure 5c, considering the working electrode, the main reduction peak of the cell with a Mg@ACC anode emerged at around 1.44 V during the first cathodic scan, while the oxidation peak appeared at around 1.92 V with respect to the Mg_{RE} electrodes. With Mg foil as anode, both the cathodic and anodic signal shifted towards higher voltage polarization (1.31 and 2.03 V, respectively). In parallel, the corresponding voltage versus E_{CE} were recorded, showing an obvious difference between the two cells with different anodes. The reduction peaks overlapped for the cell with the Mg@ACC anode, suggesting a negligible overpotential during the Mg stripping process with Mg@ACC. In contrast, with the bare Mg anode, a detectable overpotential of 0.119 V was noted during discharge. The potential differences were more apparent during cathode oxidation/anode reduction, which is attributed to the higher energy barrier for Mg plating, resulting from the competition between the reduction of sulfur species and Mg^{2+} .^{26,54} The overpotential of the Mg@ACC anode during the charge process was around 0.15 V lower than for the bare Mg anode. The results can be further confirmed by the voltage profiles of counter electrode (E_{CE}) versus reference electrode (E_{RE}), which are presented in Figure 5d. Similarly, the voltage hysteresis during Mg plating is more prominent compared to Mg stripping and the voltage polarization of the Mg@ACC anode is much lower than that of the Mg foil anode. The decreased voltage hysteresis of the Mg@ACC anode coincides with the reduced current density stemming from the high surface area of the carbon framework with extended electrochemically active sites and less insulating passivation.

To monitor the differences in the interfacial conditions, the anode impedance of three-electrode cells with the Mg anode and the Mg@ACC anode was recorded (Figure S16). Similar to prior studies,³⁵ a large resistance of around 4500 Ω was recorded in a fresh cell with a Mg foil anode, which increased vastly to about 6000 Ω after 1 h of rest. For the Mg@ACC anode, an impressive decrease of the resistance to 200 Ω was observed after assembly, and it remained stable after 1 h of rest. It is plausible that the different interfacial resistances are responsible for the different stripping behaviors with the different initial voltage spikes mentioned before in Figure 4c,d. When cycling started, the impedance of the cell with the Mg foil anode dropped to around 500 Ω , which was, however, still much larger

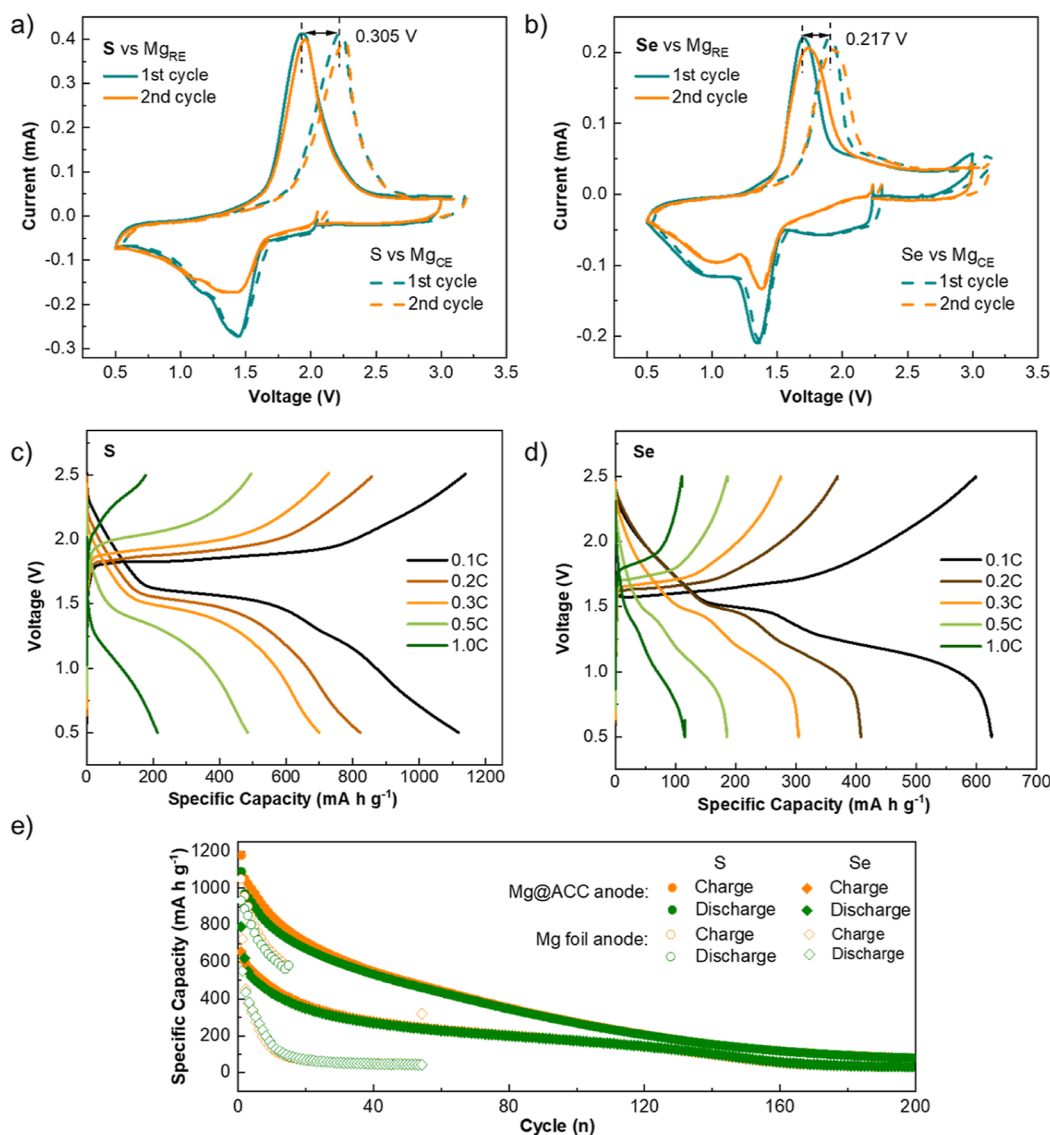


Figure 6. Cyclic voltammetry curves of (a) S|Mg@ACC and (b) Se|Mg@ACC cells with a three-electrode setup for the first two cycles. The scan rate was 0.1 mV s^{-1} . Rate performance of (c) S|Mg@ACC and (d) Se|Mg@ACC cells at current densities of 0.1, 0.2, 0.3, 0.5, and 1 C. (e) Long cycling performance of S|Mg@ACC or Mg foil and Se|Mg@ACC or Mg foil cells at a current density of 0.1 C.

than the cell with the Mg@ACC anode at 300Ω (Figure S16b). The low impedance of the cell with the Mg@ACC anode is associated with fast charge transfer and enhanced kinetics due to its 3D structure. As illustrated in Figure 5e,f, the interconnected carbon matrix in the Mg@ACC anode can provide extended electrochemically active sites with less insulating passivation by PSs, compared with the Mg foil anode.

The cycling stability and rate capability of cells with the Mg@ACC anode were further investigated by extending the chalcogen cathode material to selenium. Similar to sulfur, the selenium cathodes were also prepared by a melt-diffusion method and characterized with SEM-EDX, as shown in Figure S17. Cyclic voltammetry curves of cells with S or Se cathodes versus Mg@ACC anodes in a three-electrode setup are presented in Figure 6a,b. For both Mg-S and Mg-Se cells, the main reduction peak overlapped with respect to the reference electrode and counter electrode during the first two cathodic scans, indicating negligible overpotentials during the Mg stripping process with Mg@ACC. During the cathode oxidation, the potential differences were small, 0.305 V for the

Mg-S and 0.217 V for the Mg-Se cell, which are attributed to the fast charge transfer of the anode as discussed before. The enhanced kinetics were further validated by the rate performances of the Mg-S and Mg-Se cells (Figure 6c,d). The cycling performances of the Mg-S and Mg-Se cells with different anodes (Mg@ACC and Mg foil) were evaluated at 0.1 C (Figure 6e). Moreover, the long-term cycling performances of both Mg-S and Mg-Se cells are shown in Figure S18, up to 800 cycles without an anode failure. However, capacity fading still exists due to the infamous shuttle effect.²⁴ Besides, ACC was reported with a good polysulfide absorption capability,⁵⁵ which may cause the irreversible loss of the active material with some exposure of the carbon fiber surface after long cycling. The excellent rate and cycle life of the cells demonstrates that the 3D conductive carbon framework is beneficial for accelerating charge transfer and homogenizing the metal deposits. Moreover, with its enlarged specific surface area and special structure, it guarantees sufficient numbers of electrochemically active sites, thus avoiding the detrimental passivation of the Mg anode in Mg-S or Mg-Se cells, as illustrated in Figure 5e,f. Finally,

postmortem SEM images of Mg@ACC after cycling are shown in Figure S19. In brief, the morphology and structure of the plated Mg layer were maintained, indicating the good stability and reversibility of the electrode.

3. CONCLUSIONS

In summary, the anode failure mechanism of the Mg–chalcogen battery was investigated, which is highly related to the inhomogeneous nucleation and growth of Mg on the anode surface. During the charge process, there is a competition between sulfur species reduction and Mg^{2+} reduction (or Mg plating) on the anode. The freshly nonuniformly plated Mg reacts continuously with dissolved polysulfides and produces “dead Mg,” which leads to cell failure. Therefore, a special Mg anode with a 3D functional host was designed and further confirmed this conclusion. The soft carbon matrix can regulate a uniform Mg electrodeposition with a reduced nucleation barrier, leading to a much reduced initial overpotential of -0.16 V. In Mg–S/Mg–Se batteries, superior cycle life (up to 800 cycles) and low resistance upon cycling are obtained. This work provides insights into the failure mechanism of magnesium metal anodes and offers an effective pathway of anode structural design toward great breakthroughs in Mg–based batteries.

4. EXPERIMENTAL SECTION

4.1. Electrolyte Synthesis. Commercially available anhydrous dimethoxy ethane (DME, Sigma) was stored over 3 Å molecular sieves in a glove box for at least 24 h prior to use. Hexafluoroisopropanol ($(\text{CF}_3)_2\text{CHOH}$, 99%, Alfa Aesar) was dried over 3 and 4 Å mixed molecular sieves. NaBH_4 (98%, Sigma-Aldrich) and anhydrous MgCl_2 (99%, Sigma-Aldrich) were used as received to produce $\text{Mg}(\text{BH}_4)_2$. The magnesium tetrakis(hexafluoroisopropoxy)borate ($\text{Mg}[\text{B}(\text{hfp})_4]_2$) electrolyte was synthesized in a reaction between $\text{Mg}(\text{BH}_4)_2$ and hexafluoroisopropanol in DME as reported.⁴⁰ The 0.4 M electrolyte solution was prepared by dissolving a proper amount of magnesium salt in DME; the concentration was based on the molecular weight of $\text{Mg}[\text{B}(\text{hfp})_4]_2 \cdot 3\text{DME}$.

4.2. Preparation of the Mg@ACC Anode. A galvanostatic electrodeposition method was used to prepare Mg@ACC anodes, as shown in Figure 2a. Before electrodeposition, the activated carbon cloth (ACC-507-20, Kynol Europa GmbH) and glass fiber membranes [(GF/C) from Whatman] were tailored into proper discs with a diameter of 13 or 16 mm and vacuum dried at 230 °C overnight. CR2032-type coin cells were assembled to deposit magnesium on ACC. The coin cells were composed of a magnesium foil as the counter/reference electrode, a porous glass fiber separator, and a piece of ACC as the working electrode. The cells were operated with an Arbin battery cycling unit at a discharge current density of 1 mA cm^{-2} at 25 °C. The electrodeposition stabilized at around 0.25 V versus Mg^{2+}/Mg in the electrolyte containing 0.4 M $\text{Mg}[\text{B}(\text{hfp})_4]_2 \cdot 3\text{DME}$ and was stopped after 4 h.

4.3. Preparation of Magnesium Polysulfide Solution. 2.053 g (64.0 mmol) of sulfur powder and 0.194 g (8.0 mmol) of Mg crumbs scratched from Mg foil were added to a glass vial and mixed with 30 mL of tetraglyme in a glove box. The suspension was then stirred at 60 °C for 3 days. Finally, the suspension was filtered, and the reddish polysulfide solution (shown in Figure S13) was used for symmetric cell testing.

4.4. Preparation of ACC/S and ACC/Se Cathodes and the Mg Anode. The preparation of the ACC/S composite follows previously published protocols.^{10,56} The ACC was first punched into circular discs with a diameter of 10 mm and dried under vacuum at 230 °C overnight. Elemental sulfur (99.98%, Sigma-Aldrich) was homogeneously dispersed on the ACC discs. The obtained discs were transferred into a glass tube with a diameter of 1 cm. The glass tube was then sealed under vacuum and heated to 160 °C for 16 h. Sulfur loading was determined by subtracting the mass of blank ACC from the loaded

ACC. This amount corresponded to a sulfur loading of $0.7\text{--}0.9 \text{ mg cm}^{-2}$. Similarly, for the ACC/Se composite, instead of sulfur, elemental selenium (99.98%, Sigma-Aldrich) was used at a higher temperature of 260 °C. The selenium loading was around $0.7\text{--}0.9 \text{ mg cm}^{-2}$.

In comparison, magnesium foil (0.1 mm, Gelon Energy Corp) was also used as an anode. Prior to cell assembly, Mg discs were tailored into proper discs with a diameter of 13 mm and scratched carefully on both sides in the glovebox to remove the native oxide layer from their surface.

4.5. Characterization. XRD measurements were conducted on a STOE STADI diffractometer with a $\text{Mo K}\alpha$ X-ray source operated at 50 kV and 40 mA in the range of $10\text{--}40^\circ$. SEM images were obtained using a ZEISS LEO 1530 at 10 kV electron beam with EDX. The SEM samples were prepared on carbon tapes. The chemical state of the surface of the separator(s) was determined by XPS measurements using a Specs XPS system with a Phoibos 150 energy analyzer. The spectra were recorded with monochromatized $\text{Al K}\alpha$ radiation (400 W, 15 kV) at a detection angle of 45° with pass energies of 90 and 30 eV for the survey and detail measurements, respectively. For binding energy calibration, the main C 1s peak of adventitious carbon was set to 284.8 eV. Peak fitting was done with CasaXPS using Shirley-type backgrounds and Gaussian–Lorentzian peak profiles.

4.6. Electrochemical Measurements. The CR2032 coin cells and three-electrode cells (PAT-Cell, EL-CELL) were assembled in an argon-filled glove box (H_2O , $\text{O}_2 < 0.1 \text{ ppm}$). The glass fiber (GF, Whatman, GF/C) membranes were vacuum dried at 230 °C overnight and were as a separator. Symmetric and asymmetric cells were employed to evaluate the cycling stability and cycle lifespan of the anodes. During the electrochemical process, magnesium was continuously plated or stripped at a current density of 0.1 mA cm^{-2} . Electrochemical impedance spectroscopy (EIS) was carried out on an electrochemical workstation (VMP-3 Biologic) from 1 MHz to 20 mHz with a DC voltage amplitude of 10 mV. For Mg–S/Mg–Se coin cells, galvanostatic charge/discharge experiments were performed in a voltage range of 0.5–2.5 V versus Mg/Mg^{2+} and at a current density of 0.1 C (S: 1 C = 1675 mA g^{-1} ; Se: 1 C = 675 mA g^{-1}). Cyclic voltammetry measurements were carried out with a scan rate of 0.1 mV s^{-1} in a voltage range of 0.5–3.0 V versus Mg/Mg^{2+} on a Biologic VMP-3 potentiostat. All electrochemical investigations were conducted at 25 °C.

AUTHOR INFORMATION

Corresponding Authors

Liping Wang – Helmholtz Institute Ulm (HIU)
Electrochemical Energy Storage, Ulm D-89081, Germany;
orcid.org/0000-0002-4113-2208; Email: liping.wang@partner.kit.edu

Zhirong Zhao-Karger – Helmholtz Institute Ulm (HIU)
Electrochemical Energy Storage, Ulm D-89081, Germany;
Institute of Nanotechnology (INT), Karlsruhe Institute of Technology (KIT), Hermann-von-Helmholtz-Platz 1, Eggenstein-Leopoldshafen D-76344, Germany; orcid.org/0000-0002-7233-9818; Email: zhirong.zhao-karger@kit.edu

Authors

Thomas Diemant – Helmholtz Institute Ulm (HIU)
Electrochemical Energy Storage, Ulm D-89081, Germany

Zhenyou Li – Helmholtz Institute Ulm (HIU) Electrochemical Energy Storage, Ulm D-89081, Germany; orcid.org/0000-0001-9624-2124

Bosubabu Dasari – Helmholtz Institute Ulm (HIU) Electrochemical Energy Storage, Ulm D-89081, Germany; orcid.org/0000-0001-8816-2984

Notes

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