

Operational Performance Characterization of Commercial Scale VFB at Various Electrical and Thermal States

Lakshimi Narayanan Palaniswamy¹, Nina Munzke¹, Christian Kupper¹, Bernhard Schwarz¹,
Marc Hiller¹, Frank Säuberlich²

¹Karlsruhe Institute of Technology, ²1st Flow Energy Solutions GmbH

01 Motivation

- With project „BiFlow“ in KIT, a Vanadium Flow Battery (VFB) is used as an electrical as well as thermal storage.
- The VFB could be artificially cooled or heated through a Thermal Coupling Module (TCM) in near future.
- Thermal vs electrical characteristics of the VFB are required in order to optimally control this novel application.

02 Setup and data used for analysis

- VFB is used for self-sufficiency improvement of a student residence in Bruchsal, Germany.
- Operated since April 2022 at max 14 kW and between 12 – 47 °C.
- Runs from 0 – 100 % SOC_{BMS} almost daily.
- Can be operated till 20 kW in near future.

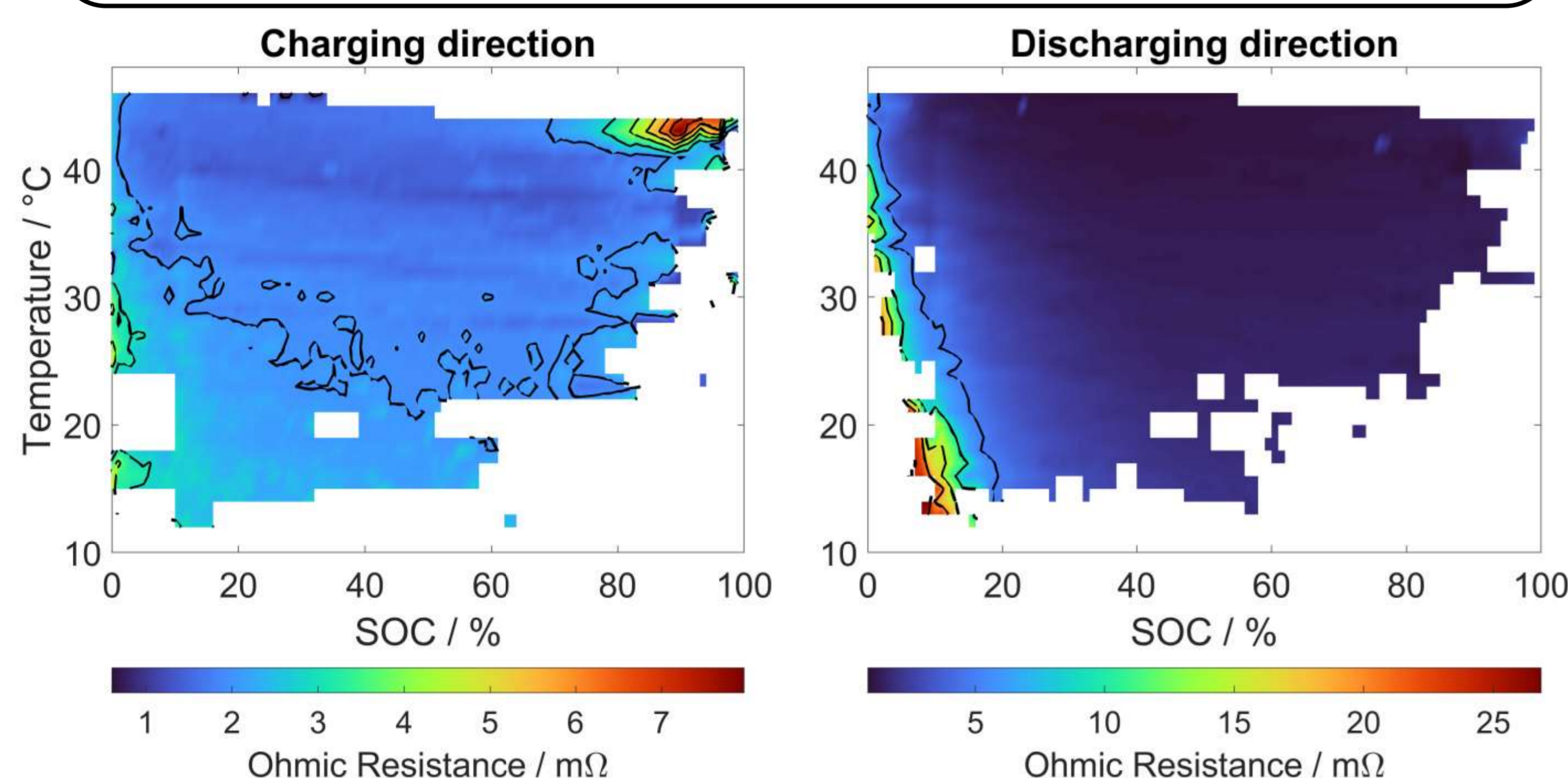
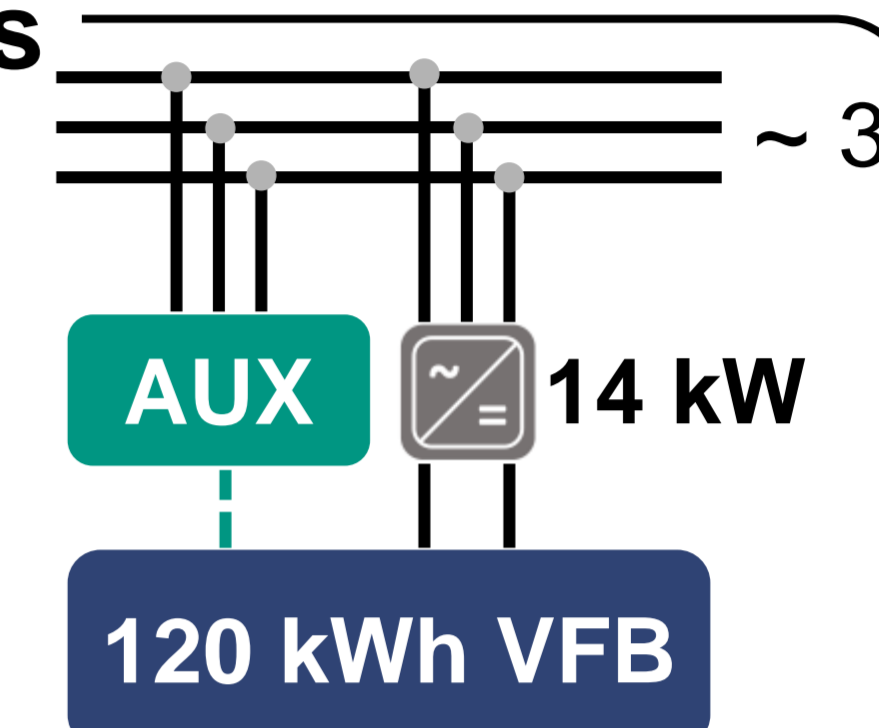


Fig 1. Cell level R_{Ohm} map measured during the operation. Resolution: 1 °C by 1 % SOC

04 Auxiliary requirement characterization

- Pumps power requirement = 70 – 90 % of auxiliary load (P_{Aux})
- $P_{Aux} \propto \text{Electrolyte viscosity} \propto \begin{cases} SOC [2] \\ 1/T_{Electrolyte} [2] \end{cases}$
- Additionally, VFB actively regulates the pump speed according to the electrical output requested by the EMS ($P_{EMS,Target}$) \Rightarrow

$$P_{Aux} = f(SOC, Temp, P_{EMS,Target})$$

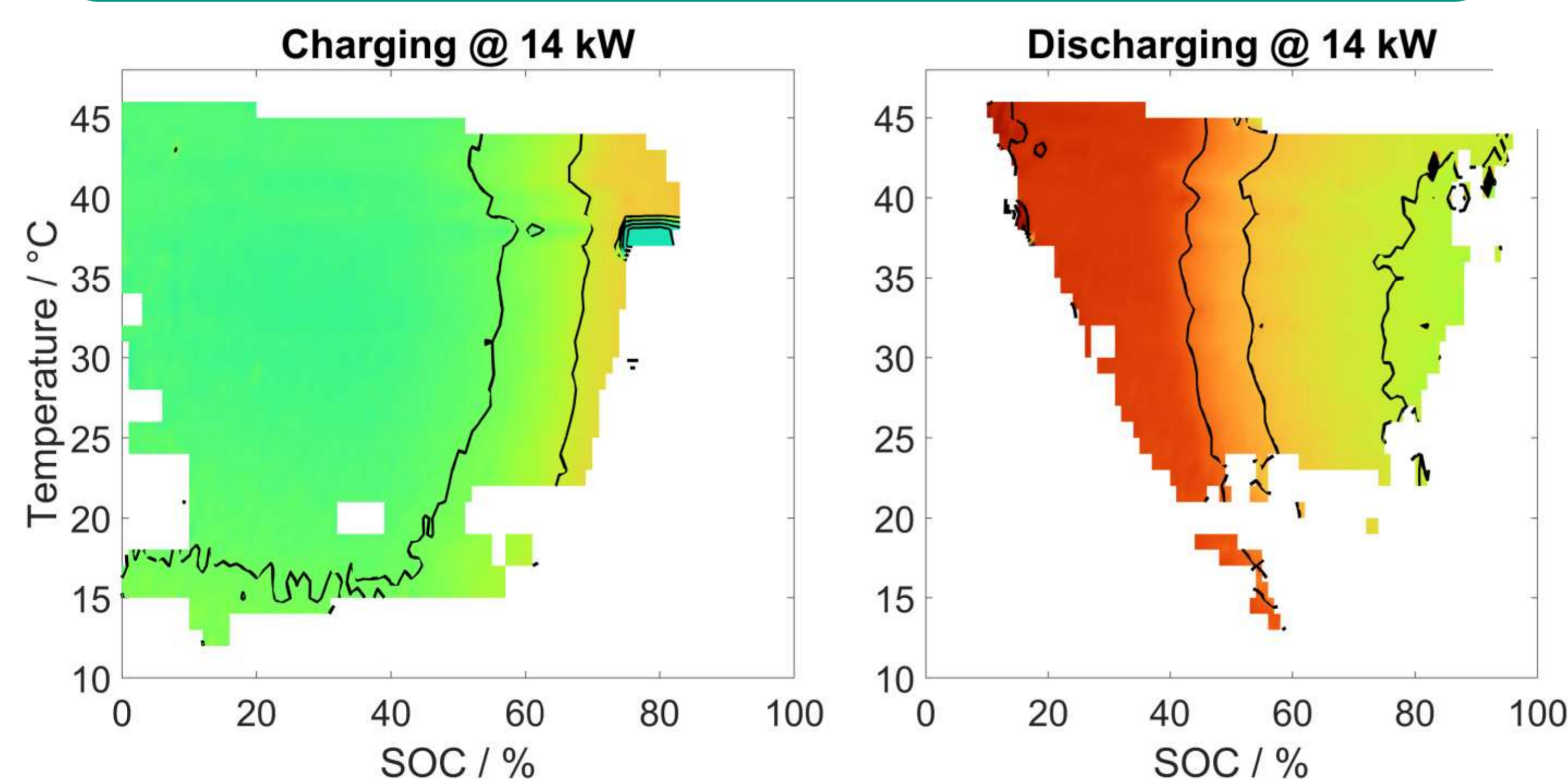


Fig 3. System level efficiency when operated at 14 kW. Resolution: 1 °C by 1 % SOC

03 Cell internal resistance characterization

- Based on 1 year live measurements of stack voltage, current and OCV (from reference cell), internal resistance is estimated as [1]:

$$R_{Ohm} = ((U_{stack}/n_{cell}) - OCV)/I_{stack}$$

	Charging direction						Discharging direction					
Temperature	↑	-	↓	↑	-	↓	↑	-	↓	↑	-	↓
SOC	↑	-	↓	↑	-	↓	↑	-	↓	↑	-	↓
Cell R_{Ohm}	↑	↓	↓	?	↓	?	↓	↓	↓	↓	↓	↓

Legend = ↑ : High, - : Medium, ↓ : Low, ? : Unknown

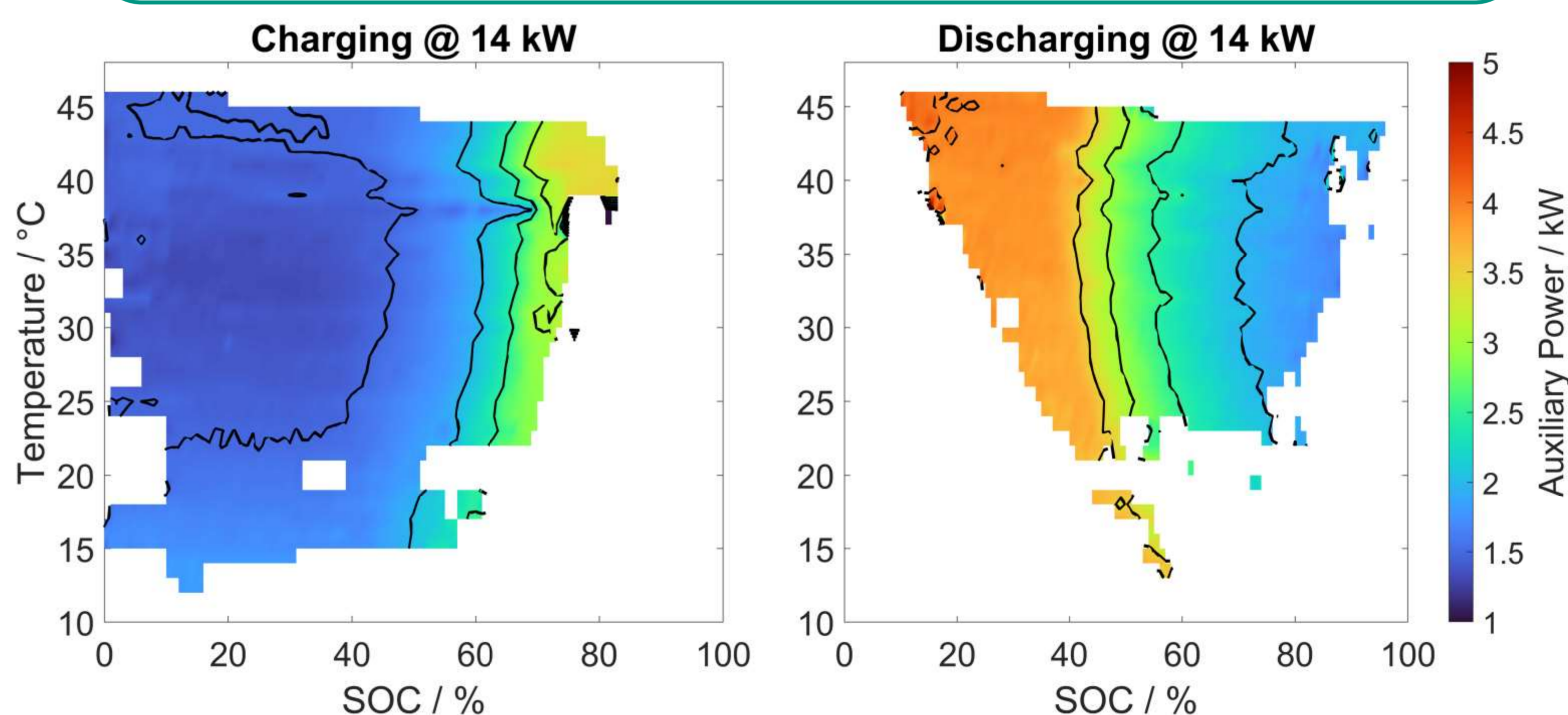


Fig 2. Total Auxiliary power requirement when operated at 14 kW. Resolution: 1 °C by 1 % SOC

05 System to electrolyte efficiency

$$\eta_{sys,charging} = \frac{P_{DC} - P_{R_{Ohm}}}{P_{AC Bus}} \quad \left| \quad \eta_{sys,discharging} = \frac{P_{AC Bus}}{P_{DC} + P_{R_{Ohm}}}$$

where η_{sys} = System efficiency between electrolyte and AC Bus

P_{DC} = Power measured at stacks

$P_{R_{Ohm}}$ = Power losses at the stack

$P_{AC Bus}$ = Power measured at AC Bus (including Aux)

Based on 03 and 04 system level efficiency has to be represented as a three dimensional function

$$\eta_{sys} = f(SOC, Temp, P_{EMS,Target})$$

06 Conclusion and outlook

- Temperature of electrolyte:
 - has a significant impact on the η_{sys}
 - when higher, could improve round-trip efficiency of VFB

Dual usage of VFB as electrical and thermal storage can prove advantageous not only in economical but also in operational perspective.

In future:

- with increased nominal power, η_{sys} would still increase as P_{Aux} would remain same.
- with TCM the unknown temperature regions will be explored further.

References

[1] F. Holger, "Untersuchung von Verlustmechanismen in Vanadium-Flussbatterien", dissertation, Technische Universität München, 2019

[2] X.Li, J. Xiong, A.Tang, Y.Qin, J.Liu, C.Yan, "Investigation of the use of electrolyte viscosity for online state-of-charge monitoring design in vanadium redox flow battery", Applied Energy, vol. 211, pp. 1050-1059, 2018



Contact: Lakshimi Narayanan Palaniswamy, Lakshimi.Palaniswamy@kit.edu

International Flow Battery Forum, 26-29 June 2023

Funding code:
03EI3025A

Supported by:
Federal Ministry
for Economic Affairs
and Climate Action
on the basis of a decision
by the German Bundestag