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CFD Validation of Forced and Natural Convection for the Open Phase of IAEA Benchmark CRP-I31038

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Abstract

The goal of the IAEA Coordinated Research Project "Benchmark of Transition from Forced to Natural Circulation Experiment with Heavy Liquid Metal Loop" (CRP-I31038) is to develop Member State advanced fast reactor analytical capabilities for simulation and design using system, CFD, and subchannel analysis codes. Here, CFD validation employing the commercial CFD code Star CCM + applied to the fuel pin simulator for forced and natural convection cases in the open phase is presented. Experimental data are provided in the benchmark specification provided by ENEA (Italian National Agency for New Technologies, Energy and Sustainable Economic Development) for the NACIE-UP facility (NAtural CIrculation Experiment-UPgrade). Considered is the fuel pin simulator with 19 pins, each consisting of a preheated lower section and heated upper sections, respectively. Three configurations: (i) all pins heated, (ii) inner 7 pins heated and (iii) asymmetric heating, are studied. For each heating configuration data for forced and natural convection are provided. Here, case (i) is studied. Temperatures at three planes are measured near the inlet, in the middle and near the end of the heated section, respectively. In addition, the axial temperature along the wall of one fuel pin simulator (in second row) is measured so that in total 67 thermocouples measure fluid and wall temperatures for validation purposes. The validation confirms that the thermohydraulic inside the fuel pin simulator can be simulated with a good accuracy. Applied is a polyhedral mesh with 2 prism layers, the k-omega SST model with all all-wall treatment and order unity y + values. Moreover, a grid-sensitivity, the importance of conjugate heat transfer inside the fuel pin simulators and the wrapper are studied. The studies indicate that it is possible to implement further simplifications without corrupting the accuracy of the simulation to reduce computational effort.

Keywords CFD · Liquid metal thermal hydraulic · Turbulent flow · Wire-wrapped bundle flow

1 Introduction

Benchmark studies are an essential tool to obtain confidence in simulation capabilities when large thermal loads occur. In particular, for nuclear applications, where failure can be accompanied with hazards to the public, maximum temperatures must be limited, and yet compact solutions

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¹ Karlsruher Institut Für Technologie (KIT), Hermann-Von-Helmholtz-Platz 1, 76344 Eggenstein-Leopoldshafen, Germany must be achieved. The ENEA Brasimone Research Centre (Italy) proposed for a benchmark exercise intended for system-alone, CFD/TH system code coupled simulations and stand-alone CFD simulations based on experimental results obtained from the 2017 campaign performed with the NACIE-UP (NAtural CIrculation Experiment-UPgrade) facility, [1]; Fig. 1 shows the schematic representation of the NACIE-UP facility consists in a rectangular loop. It consists of two vertical pipes with an inner diameter of 62,68mm. The working fluid is lead bismuth eutectic (LBE), a fluid proposed for liquid metal-cooled fast reactors. The experiments allow operation in the regimes of forced and mixed convection by combining a gas-lift pumping and buoyancy.

Inside the loop a fuel pin simulator (FPS) simulating a 19pin fuel bundle is installed. Each pin simulator contains an ohmic heater which can be activated individually, resulting



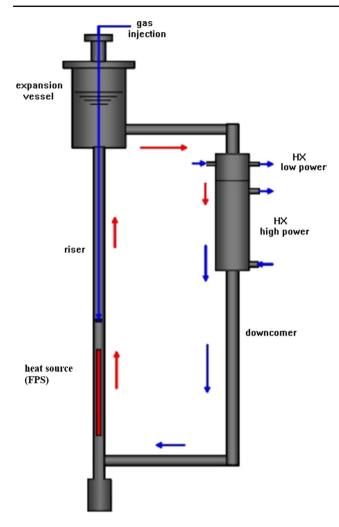


Fig. 1 Schematic representation of the NACIE-UP primary loop [1]

in a maximum total heating power of 250 kW. The 19 wirespaced electrical pins are arranged in a triangular lattice by the hexagonal wrapper. The heated pins are arranged in 3 ranks with a triangular pitch = 8.4 mm and with an active length being 600 mm. The pins have a diameter of 6.55 mm and maximum wall heat flux close to 1 MW/ m². The wire diameter = 1.75 mm. The pitch-to-diameter ratio is 1.2824. The wire pitch is 262 mm. The total length, which includes the non-active length and the electrical connectors, is 2.0 m. The hydraulic diameter is 3.84 mm. The pins are placed on a hexagonal lattice by a suitable wrapper, while spacer grids will be avoided thanks to the adoption of the wire spacer. The primary loop is insulated to ensure well-defined adiabatic experimental conditions.

In the open phase of the benchmark, two symmetric heating configurations are studied. Test ADP10 corresponds to the activation of heating of all pins, while in the case ADP06 only the central and the second inner row are activated. The goal of the open phase is to set up first simulations and choice of suitable models and computational parameters.



In phase two, a complex situation corresponding to asymmetrical heating is to be studied. Researchers do not receive any experimental data during the blind phase. The aim is to demonstrate that computational methods allow predictions once the researchers could validate their implementation for a small number of cases.

Note that each FPS heating configuration is experimentally investigated for a transient. The starting point of operation is a stationary forced convection state which is followed by a pump down-ramping resulting in a stationary natural convection operation. Thus, each of the test cases ADP10, ADP 06 and ADP07 shown schematically in Fig. 2 acquired data for two steady states. In the current study, the case ADP10 for both forced and natural convection is considered. Note that Fig. 2 also indicates the numbering of rods and subchannels. In Fig. 3, details and dimensions of the vertical FPS are shown. The flow enters at the bottom of the test section to flow through an unheated preconditioner section located within the lower half of the vertical arrangement. The heated section follows the preconditioner section beginning at height z = 0 mm, as shown in Fig. 3.

In Fig. 4, positions of the thermocouples in the experimental set-up are depicted. The experiment is equipped with three measurement planes (A, B and C) at heights 38 mm, 300 mm and 562 mm where both wall temperatures (i.e. red dots in the right figure) and subchannel temperatures (i.e. blue dots in the right figure) are collected. In addition, rod 3 is equipped with 10 (plus 3 in the measurement planes) thermocouples to measure the axial surface temperature, TC number from 55 to 67, see Fig. 4. The 13 thermocouples on pin 3 are arranged inline. The temperature data at the thermocouples along with integral operational data serves as the benchmark data. The reader is referred to benchmark specifications in [1] for more details.

2 Benchmark Specification

Table 1 contains the integral operational conditions of the steady-state conditions 1 and 2, corresponding to forced and natural convection, respectively, case ADP10. The table also includes error estimates for the integral parameters. As forced convection is provided by the gas-lift pumping, the LBE mass flow shows an error of up to 11%, and this uncertainty with other ones is relevant for later assessment of prediction capabilities. Moreover, the heating is not fully restricted to the heating section as the fuel pin simulators also show some heating in the preconditioning section. Consequently, the effective heating in the heated section Q_{eff} and the Q_{pre} in the preconditioning will be considered in the simulations. The Q_{tfm} is the power supplied for thermo-flow meter upstream of the test section. Q_{tfm} need not to be considered in the simulation. All simulations should have temperature at the FPS

 Table 1 Integral parameters of

the test ADP10 [1]

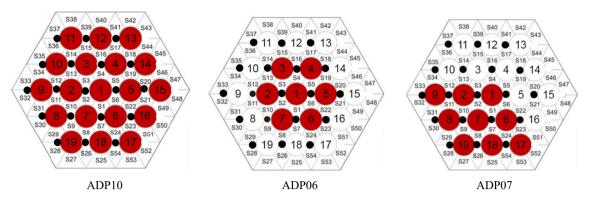


Fig. 2 Bundle cross section, benchmark test cases ADP10, ADP06 and ADP07, active pins (in red) during test

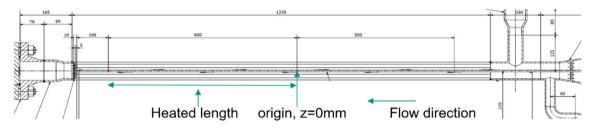


Fig. 3 CAD drawing of the test section and origin of the used coordinate system [1]

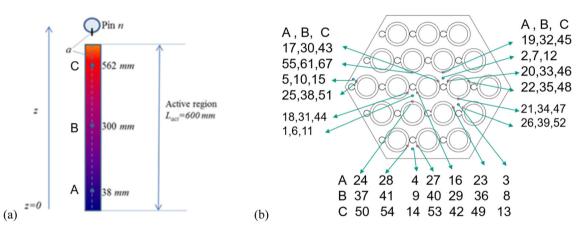


Fig. 4 a Location of planes for TC measurements in the test section (A at 38 mm, B at 300 mm and C at 562 mm), b location and names of thermocouples in measurements planes

Parameter	Steady state 1			Steady state 2		
	Data	σ	σ[%]	Data	σ	σ[%]
$\dot{m}_{ m gas}[m Nl/min]$	10	0.5	5	0	0	0
$\dot{m}_{\rm LBE}[\rm kg/s]$	2.56	0.28	11	1.31	0.14	11
T _{IN,FPS} [°C]	231.3	1.5		219.5	1.5	
$\Delta T_{FPS}[^{\circ}C]$	72.0	0.7	0.9	140.6	0.3	0.2
Q _{nom} [w]	30,000	50	0.2	30,000	44	0.1
Q _{eff} [w]	27,000	1053	3.9	27,000	1010	3.7
Q _{pre} [w]	2236	403	18	2339	217	9.3
Qtfm [w]	1915	3	0.2	1644	4	0.3



inlet ($T_{in,FPS}$) of the value tabulated in Table 1. This temperature is the average temperature at z = 0.0, the start of heating zone.

In [1], the details of the geometric set-up of the fuel pins and recommended physical properties of materials are presented. These data are taken from the OECD handbook [2]. Note that the fuel pin simulators are composed of multiple layers. The outer stainless teal cladding (AISI316L with physical properties in [3]) is followed by an electrical insulating bohrium nitride layer [4]. Inside this heat conducting BNi layer are three more layers corresponding to an Inconel600 (very thin layer, properties for steel are used for Inconel) pipe and an inner copper rod separated by another BNi layer, properties are found in [4]. Time-resolved experimental data of all thermocouples are provided in separate excel files not included in the benchmark specification.

3 Numerical Model and Results

For the simulation of the benchmark defined above, the previous experience gained at KIT is employed, see [5-8]. In these validation cases, experiments for liquid-metal-cooled rod bundles are considered. Figure 5 shows the used computational domain. It depicts the extent of the fluid domain and the domains for simulation of heater and wrapper. An adiabatic condition is applied, thus neglecting heat losses to the environment. Two trials for the simulation of the heater have been undertaken. In the first run, a heat flux is imposed on the inner side of the cladding. This represents a simplified model for a short heater, i.e. excluding preheating in the preconditioning zone. In the second trial, full details of the heater layers are simulated as shown in Fig. 5 (right). The fluid domain includes the full preconditioning section. Solid structures representing the rods in the preheat zone are excluded. Conjugate heat transfer to the rods and wrapper is accounted for. The mesh for the short heater case is composed of 49 M (Million) fluid cells and 13 M solid cells (mesh I). The mesh for the long heater case uses 96 M fluid cells and 29 M solid cells for the heater and wrapper (mesh II). See Fig. 6 for cross sections of the used meshes. In this study, the flow conditions correspond to the two steadystate phases of ADP10 presented in Table 1 are used. The Star CCM + CFD code is used. The SST turbulence model with all y + wall treatment is selected. Material properties according to the benchmark specifications are used, see upper sections. The gravity effect was accounted for in all the calculations. Temperature-dependent physical properties are applied. The inlet condition was set according to Table 1. For the short heater case, the preheating was not considered. Consequently, at the inlet of the computational domain the temperature of the FPS inlet temperature according to Table 1

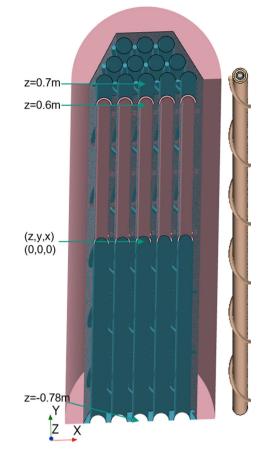


Fig. 5 Computational domain with short, simplified heater (left) and detailed simulated long heater (right)

was set. For the longer heater case, the preheating is considered. Accordingly, the inlet temperature was set such that FPS inlet temperature becomes equal to the specified value in Table 1. For the forced convection case, short and long heater tests with their corresponding meshes were tested. For the natural convection case only mesh II and the long heater are considered. Figure 7 shows the resulting Y + values for the steady-state case 1 using mesh II. Near similar Y + values are preserved for the simulation with mesh I by adjusting the cell size near the walls. The assigned values are suitable for SST and the used wall function treatment.

Figure 8a shows temperature contours at the heater fluid interface in the heated region (z = 0.0 to 0.0.6 m) for ADP10 case steady state1 and mesh II. The temperature field exhibits a strong temperature gradient in all special directions. Note that the FPS inlet temperature is non-uniform due to the preheating. Thus, near the wrapper wall lower temperatures than average are obtained. The average inlet temperature of the heated section is 231.3°C = 503.45 K. The scale in Fig. 8a starts from 499 K which is the lowest local temperature in the selected domain. Figure 8b shows some streamlines originating from a line in the x–y plane (measurement section A, z **Fig. 6** Cross section of meshes used in simulation. Left side is mesh I, and right side is mesh II

Wall Y+ 4.69 2.35 Temperature (K) Temperature (K) > 608 604 554 55 < 499

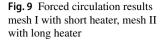
b)

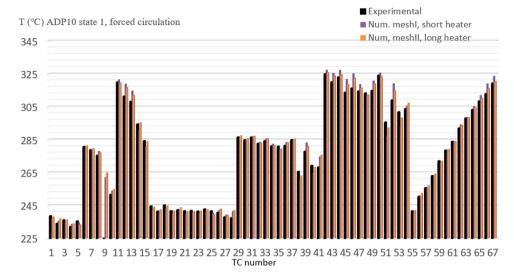
Fig. 7 Y + values, mesh II, ADP10 case steady state 1

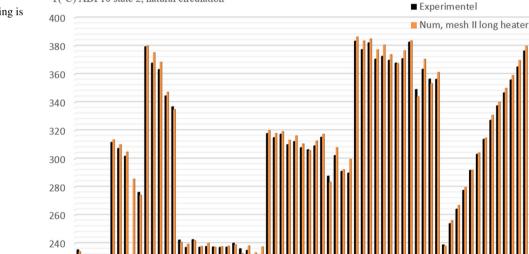
Fig. 8 a Temperature contours at heater fluid interface in the heated region, z = 0.0 to .06 m. ADP10 case steady state 1, mesh II, **b** Streamlines originating from a line in x-y plane just downstream of the start of the heated zone, z = 0.038 m, case ADP10 steady state 1, mesh II

499 x Z Y









T(°C) ADP10 state 2, natural circulation

Fig. 10 Natural circulation results mesh II with preheating is considered, long heater

= 0.038 m). It highlights strong mixing induced by the wirewraps. The streamlines are coloured by the temperature in their positions.

220

1 3 7

5

9

Local temperature comparisons between benchmark experimental results and simulations are presented in Fig. 9 (forced convection) and Fig. 10 (natural convection). In Figs. 9 and 10, the TC numbers employ the numbering indicated in Fig. 4. TC 1-5, 6-10 and 11-15 measuring fluid temperatures in the subchannels are located in measurement planes A, B and C, respectively. Similarly, TC 16-28, 29-41 and 42-54 measuring wall temperatures are installed in the planes A, B and C, respectively. Finally, TC 55-67 represent the wall temperature measurements along pin 3. They are equally distributed with an axial pitch of 43.7 mm starting from z = 38 mm.

Figure 9 shows the numerical results obtain with the different heater models compared to experiential data. The experimental data have been published and discussed in conference and international journal [9–11]. Figure 9 shows the corresponding experimental results for the steady-state case 1. The broken TC number 9 is excluded from the benchmark. The comparison indicates a minimal effect on the numerical results obtained for the short and long cases and even for the more detailed geometry and mesh refinement. Moreover, it proofs a very weak effect when doubling the mesh size. Accordingly, based on the gained experience in the forced convection case, the study of the natural convection case employs mesh II and the long heater geometry. The refined mesh was selected in natural convection simulation for better simulation of the gravitational term, which needs more

11 13 15 17 19 21 23 25 27 29 31 33 35 37 39 41 43 45 47 49 51 53 55 57 59 61 63 65 67

TC number



cells near heated surfaces than for the forced convection. In Fig. 10, results for the natural convection case are compared to the experimental benchmark results. Even though deviations are noticeable at all TCs and between the applied models, the deviations are rated as acceptable. This is in particular the case, considering the experimental uncertainties in Table 1.

In measurement plane A, the relative error appears to be quite large. Note that at this plane the effect of the preconditioning is rather large. Therefore, the actual inlet conditions to the heated section exhibit a large experimental uncertainty. Due to the mixing within the rod bundle, this uncertainty becomes less important along the bundle.

4 Conclusions

In the open phase of the NACIE -UP benchmark, various modelling methodologies were tested. Moreover, less sensitivity of results to further mesh refinement was shown. Considering the good quality of the considered simulations at a relatively low cost, it was recommended to use the finer mesh and more details in the heater model. When looking at the small differences between the simulations and experiments for the more complex modelling strategy, one can still observe slightly better qualitative agreement. This is the main reason, why the more demanding mesh should be employed in the simulations of the blind phase.

Many various hypotheses were tried to explain systematic deviations between simulation and experiments, including asymmetries and heat losses. None of these could be confirmed by a trend in the data, so that it is believed that statistical deviations are dominant and further improvements by more complex models cannot be expected. Accordingly, no further trails for improving the computations than considered in this study were conducted. In regions with high temperatures the uncertainty due to heating power, benchmark specification and modelling (physical parameters, turbulent models) is dominant. In the inlet region with low temperatures, the uncertainty becomes larger as the uncertainty of the boundary conditions becomes more prominent.

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