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Numerical Simulation of Fiber Deposition Behavior in an Air-Liquid Interface Exposure System

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— Fiber geometries and their description –

— Shape factor and drag force -

Particle forces and aerodynamic diameter



For motion **parallel** to the streamlines:

$$\chi^{\parallel} = \frac{4}{3} (\beta^2 - 1) / \left\{ \frac{2\beta^2 - 1}{\sqrt{\beta^2 - 1}} \cdot \ln \left[\beta + \sqrt{\beta^2 - 1} \right] - \beta \right\}$$

For motion **perpendicular** to the streamlines:

 $\chi^{\perp} = \frac{8}{3} (\beta^2 - 1) / \left\{ \frac{2\beta^2 - 3}{\sqrt{\beta^2 - 1}} \cdot \ln\left[\beta + \sqrt{\beta^2 - 1}\right] + \beta \right\}$

For **any** motion: $\chi = \chi^{\parallel} \cos^2(\theta) + \chi^{\perp} \cos^2(\theta)$

Brownian rotation



Effect of ALI geometry on deposition efficiency ω -

Flow inlet: Deposition efficiencies for different heights above membrane (H_{am})



Deposition efficiencies for different exposure system geometries



Effect of fiber orientation on deposition efficiencies



Influence of fiber geometry on deposition efficiency ω

Comparison of deposition efficiencies for spheres and fibers of various aspect ratios



