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# Tailored Redox-Active Catholytes Enabling High-Rate and High-Loading All-Solid-State Lithium-Sulfur Batteries

Jingui Yang<sup>1</sup> | Ruizhuo Zhang<sup>1</sup> | Ramon Zimmermanns<sup>2,3</sup> | Mareen Schaller<sup>2</sup> | Sylvio Indris<sup>2,4</sup> | Jaehoon Choi<sup>3,5</sup> | Simon Fleischmann<sup>3,5</sup> | Torsten Brezesinski<sup>1</sup> | Florian Strauss<sup>1</sup> 

<sup>1</sup>Institute of Nanotechnology, Karlsruhe Institute of Technology (KIT), Karlsruhe, Germany | <sup>2</sup>Institute for Applied Materials–Energy Storage Systems, Karlsruhe Institute of Technology (KIT), Karlsruhe, Germany | <sup>3</sup>Helmholtz Institute Ulm (HIU) Electrochemical Energy Storage, Ulm, Germany | <sup>4</sup>Applied Chemistry and Engineering Research Centre of Excellence (ACER CoE), Universite Mohammed VI Polytechnique (UM6P), Ben Guerir, Morocco | <sup>5</sup>Karlsruhe Institute of Technology (KIT), Karlsruhe, Germany

**Correspondence:** Torsten Brezesinski ([torsten.brezesinski@kit.edu](mailto:torsten.brezesinski@kit.edu)) | Florian Strauss ([florian.strauss@kit.edu](mailto:florian.strauss@kit.edu))

**Received:** 10 July 2025 | **Revised:** 23 January 2026 | **Accepted:** 31 January 2026

**Keywords:** catholyte | redox mediation | redox-active electrolyte | solid-state lithium-sulfur battery

## ABSTRACT

All-solid-state lithium-sulfur batteries (ASSLSBs) hold great promise for next-generation electrochemical energy storage due to sulfur's high theoretical specific capacity and low cost. However, sluggish sulfur conversion kinetics and severe volume variations during cycling, as well as poor ionic percolation in composite cathodes, limit their practical viability. To overcome these challenges, we herein introduce solid electrolytes of nominal composition  $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$  (with  $x = 0, 0.2, 0.4$ ), possessing high ionic conductivities of  $\geq 7 \text{ mS cm}^{-1}$  at room temperature. We show that increasing iodine content alters the phase composition and triggers reversible redox activity in these materials. If implemented as catholytes, this enables very fast sulfur conversion kinetics, ultimately leading to ASSLSBs with exceptional performance. The cells achieve 86% sulfur utilization at a rate of  $C/2$  and at  $45^\circ\text{C}$  and offer high-rate capability by delivering  $1175 \text{ mAh g}_{\text{sulfur}}^{-1}$  at  $5\text{C}$  and  $590 \text{ mAh g}_{\text{sulfur}}^{-1}$  at  $15\text{C}$ . Furthermore, the synergistic effects of ionic percolation and redox-activity enable record areal capacities up to  $14 \text{ mAh cm}^{-2}$  with a sulfur loading of  $10 \text{ mg cm}^{-2}$ . Taken together, our findings provide new strategies for designing redox-active catholytes for application in advanced ASSLSBs and further strengthen the redox-mediating role of iodine therein.

## 1 | Introduction

Lithium-sulfur (Li-S) batteries are considered one of the most promising next-generation energy storage systems due to the high abundance and low cost of sulfur, combined with its high theoretical specific capacity ( $1672 \text{ mAh g}^{-1}$ ) and a high theoretical specific energy of approximately  $2600 \text{ Wh kg}^{-1}$  when paired with a lithium metal anode [1–4]. However, the practical implementation of Li-S batteries is still hindered by the insulating nature of both sulfur and lithium sulfide ( $\text{Li}_2\text{S}$ ), the significant volume changes during cycling, and the polysulfide shuttle effect in conventional liquid electrolyte systems, which collec-

tively result in low sulfur utilization, poor Coulomb efficiency, and rapid capacity fading [5–11]. All-solid-state lithium-sulfur batteries (ASSLSBs), utilizing inorganic solid electrolytes (SEs), offer an effective strategy to address several of these issues. By replacing flammable liquid electrolytes with superionic SEs, ASSLSBs can suppress polysulfide dissolution, enhance safety, and mitigate lithium dendrite growth [8, 12]. Nevertheless, sluggish redox kinetics between sulfur and  $\text{Li}_2\text{S}$ , along with (chemo)mechanically-induced degradation caused by significant volume and morphology changes during charge/discharge, remain critical obstacles in achieving high energy and power densities. To overcome these intrinsic challenges, conventional

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approaches have focused on engineering triple-phase boundaries (interfaces) among sulfur, SE, and conductive carbon, enabling ionic and electronic transport pathways and promoting reversible electrochemical  $S_8$ -to- $Li_2S$  conversion [13]. Although these strategies can improve sulfur utilization, they require precise control over microstructure and composition to ensure effective charge percolation throughout thick electrodes [14–16]. In practice, achieving uniform and stable triple-phase interfaces at high sulfur loadings is challenging, and reaction kinetics remain limited by the tortuous transport pathways.

Recently, new strategies based on two-phase reaction mechanisms have been proposed to overcome the three-phase reaction limitation in ASSLSBs. One promising approach is to develop mixed ionic-electronic conductors (MIECs) as catholytes, enabling simultaneous electron and ion transport through a unified, conductive network [17, 18]. This type of architecture reduces transport tortuosity while activating sulfur redox reactions at the interfaces, thereby improving sulfur utilization and reducing dependence on carbon additives. Another intriguing strategy involves the use of redox mediators to facilitate the  $Li_2S_2/Li_2S$  to sulfur conversion. Although redox mediation has been considered effective only in liquid-electrolyte-based systems, where dissolved mediators exhibit fast diffusion [19–22], recent studies demonstrate its feasibility even in ASSLSBs [23, 24]. In particular, Pang's group demonstrated fast conversion kinetics enabled by the  $I^-$  and  $I_2/I_3^-$  redox couples within an amorphous  $Li_2S-B_2S_3-LiI$  SE. The  $I_2/I_3^-$  species are capable of chemically oxidizing  $Li_2S$ , and therefore, enable fast charging, even surpassing that of liquid-electrolyte-based counterparts [24]. However, not all iodine-containing SEs exhibit distinct redox-mediating behavior [25, 26]. Likewise, this effect has not been reported by directly combining iodine with sulfur or  $Li_2S$ , even though a certain degree of performance improvement has been achieved, due to enhancements in electrical conductivity [27–33]. These recent findings indicate that other parameters, such as the chemical environment of iodine and/or microstructure of the composite cathode, may also play a crucial role. Besides, the modest ionic conductivity (around  $1 \text{ mS cm}^{-1}$ ) of these redox-active iodine-containing SEs limits their practical applicability, particularly regarding the implementation in thick, high-sulfur-loading cathodes, where ensuring sufficient ionic percolation presents a major challenge. Therefore, there is still a major need for developing novel SEs that possess both very high ionic conductivities and redox-mediating properties capable of enhancing the  $Li_2S_2/Li_2S$  to sulfur conversion while maintaining fast ion transport throughout the composite cathode.

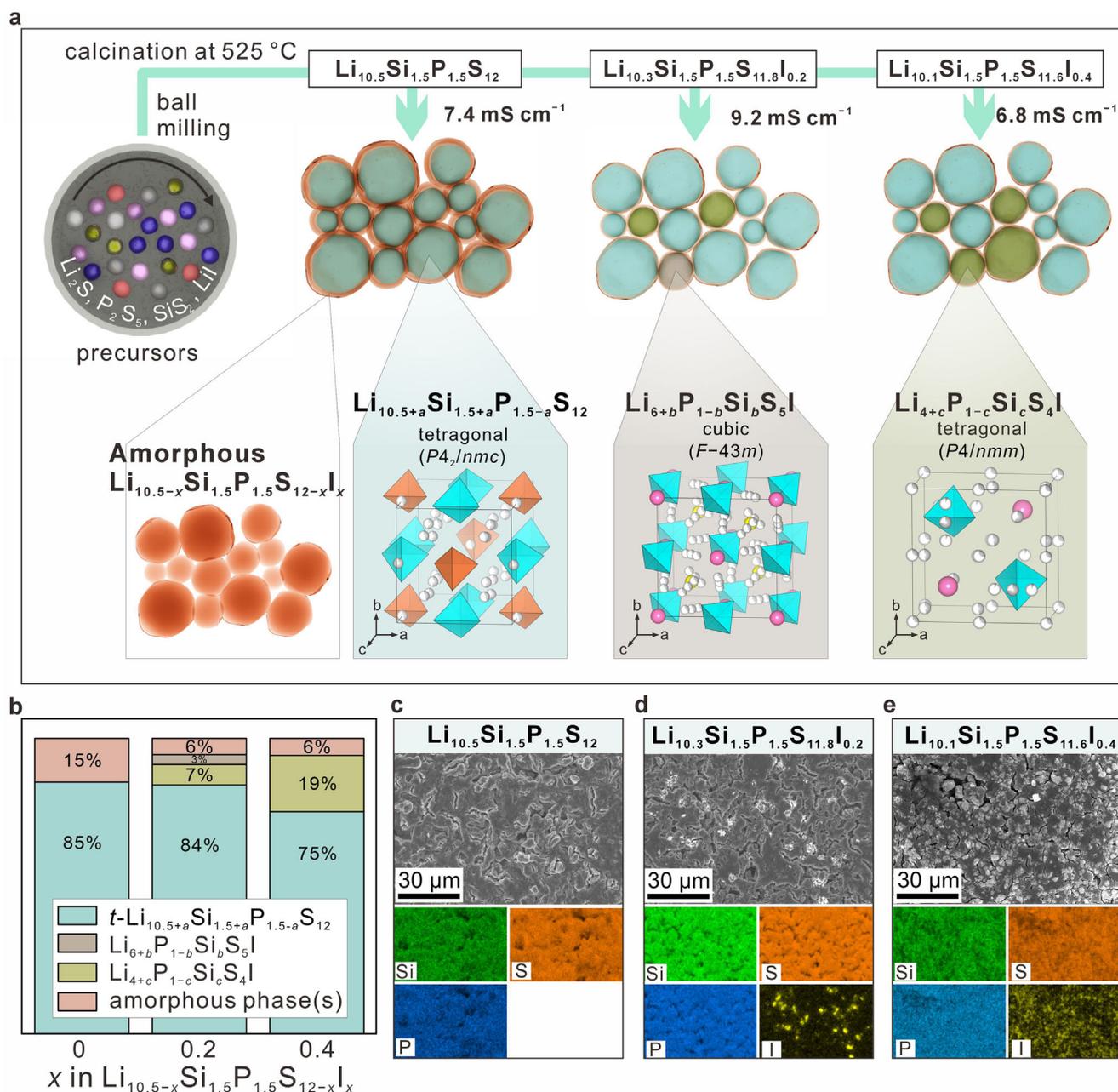
In light of such considerations, we study the effect of lithium iodide substitution on SEs with the nominal composition of  $Li_{10.5-x}Si_{1.5}P_{1.5}S_{12-x}I_x$  (with  $x = 0, 0.2, 0.4$ ). The phase composition and microstructure of the respective samples were carefully examined, and the materials were eventually tested in ASSLSBs. During cathode preparation via mechanical mixing, uniformly distributed, superionic (nanocrystalline) domains form, contributing to high ionic conduction. In addition, an iodine-rich, amorphous phase is created, which not only positively affects conductivity but, above all, exhibits promising redox-mediating properties. This synergistic effect of the iodine-rich, amorphous and superionic, nanocrystalline phases facilitates efficient ion

transport and redox mediation within the catholyte, thereby enabling high energy- and power-density ASSLSBs.

## 2 | Results and Discussion

$Li_{10.5+a}Si_{1.5+a}P_{1.5-a}S_{12}$  SEs crystallizing in the tetragonal  $P4_2/nmc$  space group ( $t-Li_{10.5+a}Si_{1.5+a}P_{1.5-a}S_{12}$ ) have attracted significant interest due to their sustainable elemental composition and superior lithium diffusion coefficient [34]. However, the experimentally reported ionic conductivities of  $t-Li_{10.5+a}Si_{1.5+a}P_{1.5-a}S_{12}$  SEs are significantly lower than theoretical predictions [34, 35]. This discrepancy has been linked to the presence of a major fraction of amorphous side phases, which appear to be detrimental to lithium transport [36, 37]. In this work, we synthetically addressed this issue by modifying the amorphous side phases via iodine substitution in the nominal composition  $Li_{10.5-x}Si_{1.5}P_{1.5}S_{12-x}I_x$  (with  $x = 0, 0.2, 0.4$ ). Figure 1a illustrates the synthesis process, consisting of a high-energy milling step prior to annealing at  $525^\circ\text{C}$ . Stoichiometric amounts of  $Li_2S$ ,  $P_2S_5$ ,  $SiS_2$ , and optionally  $LiI$  were blended and amorphized by ball milling. As can be seen from the corresponding synchrotron X-ray diffraction (SXRD) patterns in Figure S1a, only minor reflections related to  $Li_2S$  remained, indicating a high degree of amorphization upon milling of the precursors. Subsequently, the harvested powder was pressed into pellets and sealed in quartz ampoules under vacuum, followed by heating at  $525^\circ\text{C}$ . As evident from Figure S1b, sharp reflections became visible in the respective SXRD patterns, indicating crystallization. A similar trend was also observed from pair distribution function (PDF) analysis of synchrotron X-ray total scattering data. As shown in Figure S1c, only short-range ordering up to around  $4 \text{ \AA}$  was apparent after the milling step, further expanding to  $> 10 \text{ \AA}$  upon annealing. Features below  $4 \text{ \AA}$  can be assigned mainly to atomic distances within and between neighboring  $[PS_4]^{3-}$  and  $[SiS_4]^{4-}$  tetrahedral building units. The first peak at  $2.09 \text{ \AA}$  is due to the P–S and Si–S bonds, while the second and third peaks at about  $3.4$  and  $3.9 \text{ \AA}$  correspond to the S–S distance within and between the tetrahedra, respectively. Because of the similar size of the two types of tetrahedra, the individual distances for the P–S and Si–S bonds cannot be distinguished from the PDFs. An additional peak around  $4.6 \text{ \AA}$  appeared for the crystalline, iodine-containing samples. Hence, one can assume that it is related to atom pairs involving iodine (I–I, I–S). This peak suggests that iodine is not replacing sulfur in the tetrahedra, since otherwise it would overlap with the prevailing S–S distances.

To qualitatively assess the crystal structure and phase composition of the synthesized  $Li_{10.5-x}Si_{1.5}P_{1.5}S_{12-x}I_x$  SEs, Rietveld analysis was performed on XRD patterns. To this end, the samples were mixed with 20 wt.% of a silicon standard material to determine the fraction of amorphous side phase(s). The diffraction patterns and corresponding Rietveld plots can be found in Figure S2a–c. The calculated lattice parameters of the different crystalline phases, along with previously reported values, are given in Table S1. Overall, the data prove  $t-Li_{10.5}Si_{1.5}P_{1.5}S_{12}$  as the major phase.  $Li_4PS_4I$ - and argyrodite  $Li_6PS_5I$ -type phases, adopting tetragonal and cubic crystal structures, respectively, and amorphous phases were also detected (Figure 1b). Schematic phase compositions of the different samples are presented in Figure 1a. Specifically, for  $Li_{10.5}Si_{1.5}P_{1.5}S_{12}$ , 15 wt.% of amorphous phase(s) was observed,



**FIGURE 1** | Preparation and characterization of  $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$  (with  $x = 0, 0.2, 0.4$ ) SEs. (a) Schematic representation of the synthesis route. The respective ionic conductivities from cold-pressed pellets at room temperature are indicated, and the composition and crystal structure of the individual components, namely,  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$ ,  $\text{Li}_{6+b}\text{P}_{1-b}\text{Si}_b\text{S}_5\text{I}$ , and  $\text{Li}_{4+c}\text{P}_{1-c}\text{Si}_c\text{S}_4\text{I}$ , are mentioned.  $[\text{PS}_4]^{3-}$  and  $[\text{P}_{1-m}\text{Si}_m\text{S}_4]^{(3+m)-}$  polyanions are denoted by brown and cyan tetrahedra, respectively. Lithium, isolated sulfur, and iodine are represented by gray, yellow, and pink balls, respectively. (b) Phase composition of the materials with nominal composition  $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$ . SEM imaging and elemental mapping of (c)  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$ , (d)  $\text{Li}_{10.3}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.8}\text{I}_{0.2}$ , and (e)  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  as sintered pellets.

in addition to  $t\text{-Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$  (85 wt.%). For  $\text{Li}_{10.3}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.8}\text{I}_{0.2}$ , the fraction of the  $t\text{-Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$  phase remained virtually unaltered (84 wt.%), but that of the amorphous phase(s) reduced to 6 wt.%, along with the appearance of 3 and 7 wt.% of  $\text{Li}_6\text{PS}_5\text{I}$ - and  $\text{Li}_4\text{PS}_4\text{I}$ -type phases, respectively. In the case of  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ , the fraction of the  $t\text{-Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$  phase was lowered to 75 wt.%, while 19 wt.% of a  $\text{Li}_4\text{PS}_4\text{I}$ -type phase and 6 wt.% of amorphous phase(s) were found. We further observed that with increasing iodine content in  $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$ , the lattice parameters of the  $t\text{-Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$  phase increase (Table S1). It is hypothesized that there is no iodine introduction

into  $t\text{-Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$ . Rather, the changes in lattice parameters appear to be a result of the increased silicon-to-phosphorus ratio at the 4d site, since  $\text{Si}^{4+}$  has a larger ionic radius than  $\text{P}^{5+}$ , conforming to a more general formula of  $t\text{-Li}_{10.5+a}\text{P}_{1.5-a}\text{Si}_{1.5+a}\text{S}_{12}$  [38]. This kind of  $\text{Si}^{4+}$ -induced lattice expansion has also been reported for the other crystalline side phases, i.e.,  $\text{Li}_{6+b}\text{P}_{1-b}\text{Si}_b\text{S}_5\text{I}$  ( $\text{Li}_6\text{PS}_5\text{I}$ -type) and  $\text{Li}_{4+c}\text{P}_{1-c}\text{Si}_c\text{S}_4\text{I}$  ( $\text{Li}_4\text{PS}_4\text{I}$ -type) [39, 40]. Based on previously reported data, the silicon content was estimated to lie between  $b = 0$  and 0.2 in  $\text{Li}_{6+b}\text{P}_{1-b}\text{Si}_b\text{S}_5\text{I}$  and between  $c = 0$  and 0.3 in  $\text{Li}_{4+c}\text{P}_{1-c}\text{Si}_c\text{S}_4\text{I}$ , both being stoichiometrically lower compared to the precursor material. Hence, we

assume that less  $\text{Si}^{4+}$  incorporation into the two side phases is responsible for the increased silicon-to-phosphorus ratio in the  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  phases.

To gain more insight into the phase distribution on a macroscopic level, scanning electron microscopy (SEM) imaging combined with energy dispersive X-ray (EDX) spectroscopy mapping of the SE pellets was performed. Figure 1c–e shows top-view SEM images and corresponding elemental maps for Si, P, S, and I for the different samples after annealing. As can be seen, unlike iodine, Si, P, and S were uniformly distributed. For  $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$  with  $x = 0.2$  and  $0.4$ , bright particles were visible in the SEM images, specifically located where elemental mapping indicated the presence of iodine. For the sample with  $x = 0.2$ , local high concentrations of iodine further confirmed phase separation into  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$ ,  $\text{Li}_{6+b}\text{P}_{1-b}\text{Si}_b\text{S}_5\text{I}$ , and  $\text{Li}_{4+c}\text{P}_{1-c}\text{Si}_c\text{S}_4\text{I}$ . By contrast, for the sample with  $x = 0.4$ , although the particle size of the I-containing phase(s) remained comparable, the total content approximately doubled (16 vs. 25 wt.%, see Figure 1b), resulting in a higher number density and a more homogeneous dispersion of iodine-rich domains. This, in turn, led to the more uniform appearance in Figure 1e.

The room-temperature ionic conductivity of the  $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$  SEs in the form of cold-pressed pellets was determined by electrochemical impedance spectroscopy (EIS) to be 7.4, 9.2, and 6.8  $\text{mS cm}^{-1}$  for  $x = 0, 0.2, \text{ and } 0.4$ , respectively (Figure S3). Based on these results and literature reports, we conclude that the high ionic conductivity originates from the  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  phase. However, it is clearly reduced by the presence of less conductive amorphous and/or crystalline  $\text{Li}_4\text{PS}_4\text{I}$ -type phases [41, 42].

Given that promising ionic conductivities were achieved, despite the formation of multiphase materials, the samples were tested as SEs in ASSLSBs. Figure 2a illustrates the general cell configuration, where the materials are employed both as catholyte and as separator, and indium-lithium alloy serves as anode. To manufacture the cathode composite, sulfur was first melt-infiltrated into a carbon host and subsequently blended with additional carbon additive and the SE via high-energy milling. The sulfur content accounted for 30 wt.% of the total cathode composite, as determined by thermogravimetric analysis (TGA) (Figure S4a,b). The first-cycle voltage profiles at a rate of C/2 and at  $45^\circ\text{C}$  are presented in Figure 2b. Cells containing the  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$  SE delivered an initial specific discharge capacity of  $q_{\text{dis}} \approx 1670 \text{ mAh g}_{\text{sulfur}}^{-1}$ . However, upon subsequent charge, only a  $q_{\text{ch}} \approx 670 \text{ mAh g}_{\text{sulfur}}^{-1}$  was achieved (equivalent to about 40% of the discharge capacity), accompanied by a distinct polarization of 1.07 V. Details on the calculation of Coulomb efficiency (CE) can be found in Section S1.

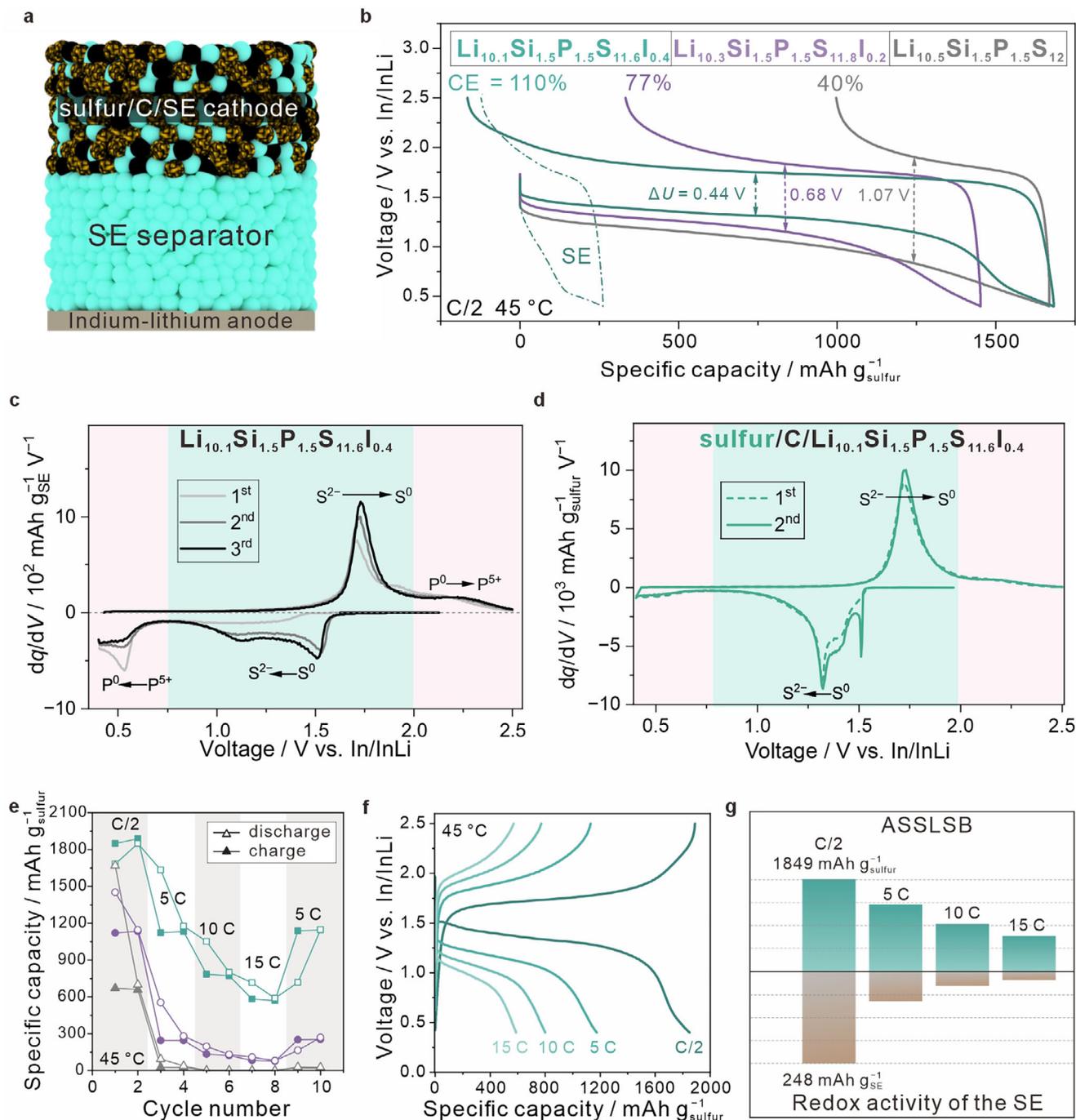
When using  $\text{Li}_{10.3}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.8}\text{I}_{0.2}$  as SE, the voltage difference between charge and discharge was reduced to 0.68 V. While the specific discharge capacity ( $q_{\text{dis}} \approx 1450 \text{ mAh g}_{\text{sulfur}}^{-1}$ ) was lower than that achieved with the  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$ -based cells, about 77% of the capacity could be recovered during charge ( $q_{\text{ch}} \approx 1120 \text{ mAh g}_{\text{sulfur}}^{-1}$ ). Upon incorporating the  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  SE into the ASSLSBs, the voltage hysteresis was further lowered to 0.44 V, and surprisingly, the specific discharge capacity ( $q_{\text{dis}} \approx 1680 \text{ mAh g}_{\text{sulfur}}^{-1}$ ) was found to be somewhat lower than the specific charge

capacity ( $q_{\text{ch}} \approx 1850 \text{ mAh g}_{\text{sulfur}}^{-1}$ ). The actual capacity even exceeded the theoretical one for sulfur, and a kind of overcharging was observed. This suggests that the capacity contribution from the SEs is non-negligible.

Sulfide electrolytes have a narrow thermodynamic stability window; however, studies have shown that certain redox couples, such as  $\text{S}^0/\text{S}^{2-}$  and  $\text{P}^{5+}/\text{P}^0/\text{P}^{3-}$ , are reversible [43–45]. Unfortunately, current research on ASSLSBs often overlooks the capacity contribution of SEs, attributing the full capacity solely to sulfur redox activity. To examine the redox behavior of the  $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$  (with  $x = 0, 0.2, 0.4$ ) SEs, solid-state battery cells with a cathode consisting of 70 wt.% SE and 30 wt.% carbon black were assembled. The cells were cycled between 0.4 and 2.5 V vs. In/InLi at  $0.86 \text{ mA cm}^{-2}$  (corresponding to C/2 for the ASSLSBs), starting from discharge. Results from differential capacity analysis ( $dq/dV$  plots) are presented in Figure 2c and Figure S5a,b. All SEs exhibited similar redox behavior, consistent with previous reports [44, 45]. The peaks in the  $dq/dV$  plots correspond to reversible redox processes, which can be assigned to the  $\text{S}^0/\text{S}^{2-}$  and  $\text{P}^{5+}/\text{P}^0$  couples. Briefly, the initial discharge involves  $\text{P}^{5+}$  reduction below 0.75 V vs. In/InLi and minor sulfur reduction (0.75–1.6 V vs. In/InLi) in the iodine-containing samples, attributed to the presence of trace sulfur and/or polysulfides, most likely stemming from synthesis residuals or the cathode composite preparation. The subsequent charge is dominated by  $\text{S}^{2-}$  oxidation (1.6–2.0 V vs. In/InLi), followed by a minor contribution resulting from  $\text{P}^0$  oxidation to  $\text{P}^{5+}$ . Subsequent cycles show strong currents related to the  $\text{S}^0/\text{S}^{2-}$  redox activity and overlap closely, indicating high reversibility. Notably, the  $\text{S}^0/\text{S}^{2-}$  redox activity increases significantly with iodine content, especially for  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ , which can be attributed to the redox mediation by iodine species.

For the cell with  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  as the active component in the working electrode, the respective voltage profiles at different C-rates are presented in Figure S5c. In the initial cycle at a current density ( $j = 0.86 \text{ mA cm}^{-2}$ ) corresponding to a rate of C/2 in the ASSLSBs, a similar overcharging phenomenon was observed (due to  $\text{S}^{2-}$  oxidation), with the “excess” capacity being highly reversible. As evident from Figure S5c, the material delivered a specific capacity of about  $250 \text{ mAh g}_{\text{SE}}^{-1}$  at  $0.86 \text{ mA cm}^{-2}$ . We assume that, with such a low current density, it exhibits the same electrochemical behavior regardless of whether sulfur is present in the cathode or not. Its contribution to the capacity of the ASSLSB was calculated with reference to the sulfur content in the cathode (Figure 2b). For details on the calculation, see Section S1. After subtracting the contribution from the SE, the efficiency of the ASSLSB was close to 100%, indicating the high reversibility of the sulfur conversion reactions. Aside from that, the capacity contribution from the sulfur amounted to  $\sim 1440 \text{ mAh g}_{\text{sulfur}}^{-1}$ , corresponding to 86% utilization, which is among the highest values reported for ASSLSBs to date [8, 46, 47].

For ASSLSBs, the  $dq/dV$  analysis confirmed that the  $\text{S}^0/\text{S}^{2-}$  redox couple dominates the capacity (Figure 2d; Figure S6a,b). With increasing iodine content, the current related to the  $\text{S}^0/\text{S}^{2-}$  redox activity is strongly increased, while the polarization is markedly reduced. In addition, a new (cathodic) peak appears at about 1.5 V vs. In/InLi in the subsequent cycles. The origin of this peak remains poorly understood and difficult to study in



**FIGURE 2** | Electrochemical performance of ASSLSBs. (a) Schematic illustration of the cell configuration. (b) First-cycle voltage profiles of cells using the Li<sub>10.5-x</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>12-x</sub>I<sub>x</sub> (with  $x = 0, 0.2, 0.4$ ) SEs as catholyte and in the separator. The redox behavior of Li<sub>10.1</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>11.6</sub>I<sub>0.4</sub> within the same voltage window is indicated by the dash-dotted line. Differential capacity curves for the Li<sub>10.1</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>11.6</sub>I<sub>0.4</sub>-based cells (c) without and (d) with sulfur being present in the composite electrode. (e) Rate performance of ASSLSBs using the different SEs. (f) Charge–discharge profiles of a cell with Li<sub>10.1</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>11.6</sub>I<sub>0.4</sub> at different C-rates. (g) Corresponding capacity evolution and estimated contributions from the SE at comparable current densities.

detail. A possible explanation is the formation of polysulfido-type intermediates ( $[\text{PS}_{4+n}]^{3-}$ , with  $n > 0$ ) resulting from reactions between the sulfur and the SE. Such intermediates have been reported in systems prepared by wet-mixing [48].

The rate performance of cells using the different SEs is shown in Figure 2e. Those using the Li<sub>10.5</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>12</sub> SE were only capable of delivering a reversible specific discharge capacity of  $q_{\text{dis}} \approx 660$  mAh g<sub>sulfur</sub><sup>-1</sup> at C/2, due to the major loss in the first charge

cycle. The capacities at rates of 5C, 10C, and 15C were found to be negligible. Cells using Li<sub>10.3</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>11.8</sub>I<sub>0.2</sub> showed some improvements, but the reversible specific discharge capacities at rates  $\geq 5\text{C}$  were still lower than 300 mAh g<sub>sulfur</sub><sup>-1</sup>. Notably, the Li<sub>10.1</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>11.6</sub>I<sub>0.4</sub>-based cells demonstrated superior rate performance, achieving specific discharge capacities of  $q_{\text{dis}} \approx 1850$  mAh g<sub>sulfur</sub><sup>-1</sup> at C/2, 1175 mAh g<sub>sulfur</sub><sup>-1</sup> at 5C, 800 mAh g<sub>sulfur</sub><sup>-1</sup> at 10C, and 590 mAh g<sub>sulfur</sub><sup>-1</sup> at 15C. Representative voltage profiles of an ASSLSB using the Li<sub>10.1</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>11.6</sub>I<sub>0.4</sub> are shown in Figure 2f,

revealing an increase in voltage hysteresis from about 0.44 V at C/2 to 1.15 V at 15C.

For ASSLSBs that are cycled at high C-rates, the calculation suggested above is likely insufficient to quantify and separate the contributions of SE and sulfur to capacity, as increased current densities can lead to inhomogeneous current distribution and different reaction kinetics. However, a semi-quantitative estimate focusing on the evolution of the reversible capacity of  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  with increasing current density remains valid. As shown in Figure 2g, the reversible capacity associated with the SE decreased significantly faster than the total capacity of the ASSLSB. Furthermore, it can be assumed that in the presence of sulfur, the contribution from the SE at high current densities is most likely lower than estimated in Figure 2g. These results clearly show that in ASSLSBs, sulfur continues to account for the largest share of total capacity, and its relative contribution becomes increasingly important with increasing C-rate.

For the cell with  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  as active component in the working electrode, specific capacities of about 100 mAh  $\text{g}_{\text{SE}}^{-1}$  were achieved at  $j = 8.6 \text{ mA cm}^{-2}$  (corresponding to a rate of 5C in the ASSLSBs), without major fading over the first 1500 cycles (Figure S5d). Overall, this underscores the significant involvement of SE in electrochemical redox reactions, which should be taken into account in future studies. In the case of  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ , its high reversibility is particularly advantageous for practical applications, as the SE provides additional capacity beyond that of sulfur, which serves as the actual cathode active material in ASSLSBs.

The sulfur/C/  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  cathode composite milled for different periods of time was also tested in ASSLSBs, with the respective voltage profiles at C/2 shown in Figure 3a. It is obvious that extending the milling time leads to a strong increase in specific discharge capacity from  $q_{\text{dis}} \approx 1160 \text{ mAh g}_{\text{sulfur}}^{-1}$  for 2 h to 1850 mAh  $\text{g}_{\text{sulfur}}^{-1}$  for 10 h and further positively affects rate capability (Figures S7 and S8).

To understand the origin of the fast kinetics in ASSLSBs using the  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ , the cathode was first examined by SXRD and PDF analysis of total scattering data. The SXRD patterns collected from the composite powder ball-milled for 2, 4, and 10 h at 450 rpm are shown in Figure 3b, along with those of the pristine SE and sulfur. Distinct reflections of the  $\text{Li}_{4+c}\text{P}_{1-c}\text{Si}_c\text{S}_4\text{I}$  (minor) and  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  (major) phases were still clearly visible after 2 h of milling. However, those of the  $\text{Li}_{4+c}\text{P}_{1-c}\text{Si}_c\text{S}_4\text{I}$  phase were strongly reduced in intensity compared to the pristine material. As can be seen, if milling of the cathode composite was continued, the intensity of reflections related to the  $\text{Li}_{4+c}\text{P}_{1-c}\text{Si}_c\text{S}_4\text{I}$  phase diminished much faster than that for  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$ . After 10 h of milling, only broad reflections from both  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  and sulfur were still detectable. This result indicates that the  $\text{Li}_{4+c}\text{P}_{1-c}\text{Si}_c\text{S}_4\text{I}$  phase readily amorphizes, which is known to be accompanied by an increase in ionic conductivity by several orders of magnitude [49, 50]. Sulfur and the  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  phase were also partially amorphized, but likely remained in nanocrystalline form after milling. To further substantiate this point,  $^{31}\text{P}$  magic-angle spinning (MAS) nuclear magnetic resonance (NMR) spectroscopy measurements were conducted on both the as-synthesized  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$

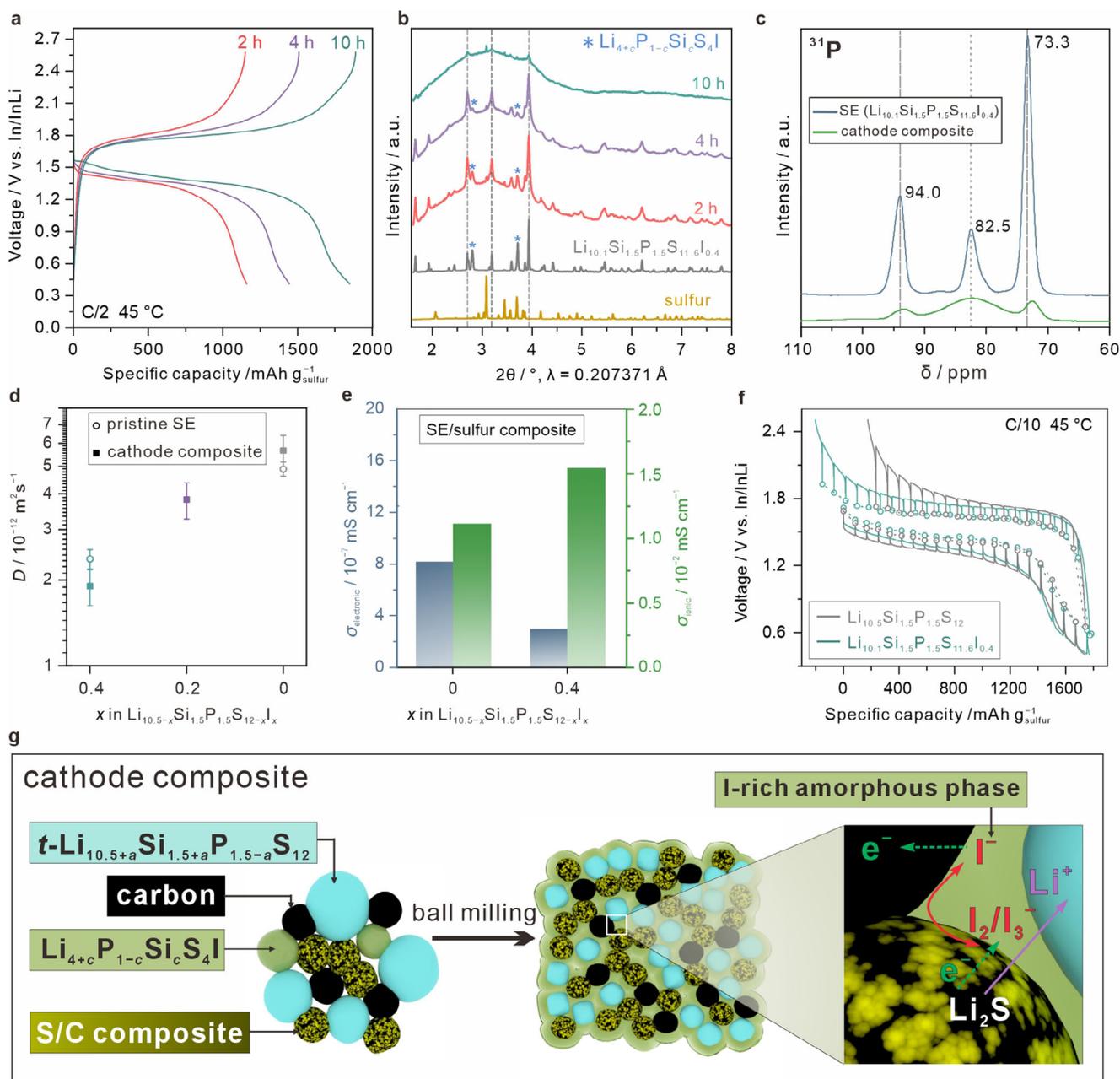
and the corresponding cathode composite. As shown in Figure 3c, the pristine material displays three sharp peaks between 110 and 70 ppm. The  $^{31}\text{P}$  resonances associated with the  $[\text{PS}_4]^{3-}$  tetrahedra in the crystal structure of the  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  phase appear at 94.0 and 73.3 ppm, matching previously reported values (93.8 and 73.1 ppm) and being related to two different crystallographic phosphorus positions [36]. The sharp signal at 82.5 ppm is related to  $[\text{PS}_4]^{3-}$  species within the  $\text{Li}_{4+c}\text{P}_{1-c}\text{Si}_c\text{S}_4\text{I}$  phase, in agreement with the  $^{31}\text{P}$  chemical shift reported for crystalline  $\text{Li}_4\text{PS}_4\text{I}$  [51]. Upon cathode composite preparation (after 10 h of ball milling), all three peaks are broadened, and their relative intensities are reduced. The peaks corresponding to the tetragonal phase show a reduced relative intensity and some minor shift to lower values, but generally their chemical-shift range remains largely unaltered, consistent with partial amorphization and the formation of highly strained, defect-rich, nanocrystalline domains. In contrast, the peak associated with the crystalline  $\text{Li}_4\text{PS}_4\text{I}$ -type phase becomes significantly broader, and the emergence of a wide, diffuse feature agrees with the formation of an amorphous  $\text{Li}_4\text{PS}_4\text{I}$ -derived phase [52].

Synchrotron X-ray total scattering and PDF analysis (Figure S9) indicated that the long-range ordering ( $>4 \text{ \AA}$ ) is already strongly disturbed after milling for 2 h. Upon further milling, the long-range periodicity is strongly reduced, with only short-range ordering ( $<4 \text{ \AA}$ ) being evident from the PDFs. However, clear assignment of the different peaks to certain bond distances is very challenging, as there is strong overlapping between atomic distances originating from the  $[\text{PS}_4]^{3-}$  and  $[\text{SiS}_4]^{4-}$  tetrahedral building units and the S–S bonds from sulfur.

To further probe the micro- and nanostructure of the cathode containing the  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  SE after 10 h of milling, SEM imaging was performed on cross sections. Sample specimens were prepared via FIB (focused ion beam) cutting under cryogenic conditions to avoid beam damage. As shown in Figure S10a, a clean and flat cross-section was successfully prepared. Although the assignment of different phases is quite challenging, the homogeneity of mixing can be evaluated from high-magnification SEM images. A grainy structure is observed, and numerous bright spots in the nanometer range are found throughout the composite (Figure S10b–f). While some larger spots reach several tens of nanometers, the majority of these spots are too small to be individually resolved, yet they are uniformly distributed across the composite.

Taken together, the observations from SEM imaging and the synchrotron XRD results strongly support the formation of an iodine-rich, amorphous phase and the presence of a nanoscale  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  phase together with sulfur and carbon components within the cathode composite.

To confirm the high ionic conductivity within the composite cathode with respect to the pristine SE,  $^7\text{Li}$  pulsed-field gradient (PFG) NMR ( $^7\text{Li}$  PFG NMR) measurements were performed using a diffusion time of 10 ms (Figure S11). Note that from that latter, a diffusion length of several hundred nanometers to a few micrometers can be estimated. As shown in Figure 3d, all cathodes exhibited high Li-ion diffusivity ( $10^{-12} \text{ m}^2 \text{ s}^{-1}$ ), comparable in magnitude to that of the parent  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  phase. To verify that the high lithium diffusivity primarily originates from



**FIGURE 3** | The origin of fast reaction kinetics in ASSLSBs using  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  as catholyte. (a) Voltage profiles (C/2, 45°C) of cells with cathode composite (sulfur/C/ $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ ) ball-milled for 2, 4, and 10 h and (b) corresponding SXR patterns. (c)  $^{31}\text{P}$  MAS NMR spectra of the pristine  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  and sulfur/C/ $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  cathode composite after 10 h of milling. (d) Room-temperature Li-ion diffusion coefficients for the sulfur/C/ $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$  composites (with  $x = 0, 0.2, 0.4$ ) determined by  $^7\text{Li}$  PFG NMR spectroscopy. Diffusion coefficients of the pristine  $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$  SEs for  $x = 0$  and 0.4 are included for comparison. (e) Electronic and ionic partial conductivities of the  $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$ /sulfur composites (with  $x = 0, 0.4$ ). (f) GITT curves for the initial cycle of cells with  $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$  (with  $x = 0, 0.4$ ). The areal sulfur loading was about  $1 \text{ mg cm}^{-2}$ . (g) Schematic illustrations of the cathode composite and synergistic enhancement of sulfur conversion through improved ionic percolation and effective activation of the SE/ $\text{Li}_2\text{S}$  interface via iodine-mediated redox. The right panel was inspired by literature [24].

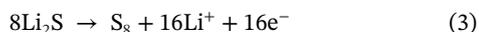
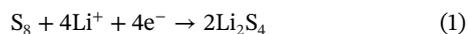
the  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  phase, the diffusion coefficients for the pristine  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  (Figure S12a,b) and  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$  (from previous work [42]) are also plotted in Figure 3d, showing good agreement with the cathode composite data. Subsequently, the ionic and electronic partial conductivities were probed using a series of electrochemical techniques.

SE/sulfur mixtures were fabricated, excluding carbon, to isolate the effect of the SE. Interestingly, a higher density ( $1.96 \text{ g cm}^{-3}$ )

was achieved with the cold-pressed  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ /sulfur composite compared to  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$ /sulfur ( $1.79 \text{ g cm}^{-3}$ ). Given that  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  and  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$  have similar compaction densities ( $1.66$  and  $1.69 \text{ g cm}^{-3}$  when powder material is densified at  $450 \text{ MPa}$ , respectively), the increased densification of the  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ -based composite suggests fewer void spaces, being advantageous for charge percolation. The electronic conductivity was examined by direct current (DC) polarization with ion-blocking electrodes (Figure S13a). Both the

$\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}/\text{sulfur}$  and  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}/\text{sulfur}$  composites revealed rather low electronic conductivities on the order of  $10^{-7}$   $\text{mS cm}^{-1}$  (Figure 3e; Figure S13b). The ionic conductivities were determined via EIS and found to be  $1.62 \times 10^{-2}$   $\text{mS cm}^{-1}$  for  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}/\text{sulfur}$ , compared to  $1.17 \times 10^{-2}$   $\text{mS cm}^{-1}$  for  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}/\text{sulfur}$  (Figure S13c). Since the electronic conductivity is about five orders of magnitude lower than the ionic one, the overall conductivity extracted from EIS can be primarily attributed to ion conduction. Of note, the iodine-rich, amorphous phase has been reported to be softer and more conductive [53, 54]. Therefore, despite the nanocrystalline  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  within the sulfur/C/ $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  composite being slightly less conductive than in the sulfur/C/ $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$  composite, the iodine-rich, amorphous phase enables maintaining a higher overall conductivity in the  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}/\text{sulfur}$  composite, which is beneficial for improving sulfur utilization and rate performance of ASSLSBs.

To examine the equilibrium voltage and overpotential variations in the ASSLSBs depending on the SE used, galvanostatic intermittent titration technique (GITT) analysis was performed (Figure 3f). The hysteresis between the charge and discharge equilibrium voltages indicates asymmetric reaction pathways, consistent with a previous study. The latter has been attributed to a two-step reduction of  $\text{S}_8$  to  $\text{Li}_2\text{S}$  upon discharge (Equations 1 and 2) and a single-step oxidation of  $\text{Li}_2\text{S}$  to  $\text{S}_8$  during charge (Equation 3) according to [55]:



While both the  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$ - and  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ -based cells showed similar equilibrium voltages at various depths of charge/discharge, their overpotentials differed significantly. During discharge, the cells using  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  exhibited lower overpotentials than those with  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$ , likely due to facilitated ion transport. However, at the end of discharge, the overpotentials converged as sulfur became depleted, and both systems ultimately delivered similar discharge capacities. In the subsequent charge cycle, the overpotentials were again significantly lower for the  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ -based cells, becoming more pronounced with increasing state-of-charge (SOC). Having in mind that the lithiation follows a path close to the thermodynamic ground state, whereas the delithiation (Equation 3) is a kinetically dominated process [55], our results clearly demonstrate the beneficial effect of iodine on enhancing the kinetics of the electrochemical  $\text{Li}_2\text{S}$ -to- $\text{S}_8$  conversion. This finding agrees with a recent study reporting on the redox-mediating capability of iodine in a sulfide-based SE, enabling fast solid-solid conversion reactions in ASSLSBs [24]. In particular, we assume that a similar mechanism is at play here, where iodine is being oxidized at the carbon|SE interface, migrates to the SE| $\text{Li}_2\text{S}$  interface, and eventually chemically oxidizes  $\text{Li}_2\text{S}$ . This unique reaction route transforms the SE/ $\text{Li}_2\text{S}$  two-phase boundary into an active interface, thereby increasing the density of reaction sites and improving kinetics, which in turn allows for excellent rate performance of the corresponding ASSLSBs.

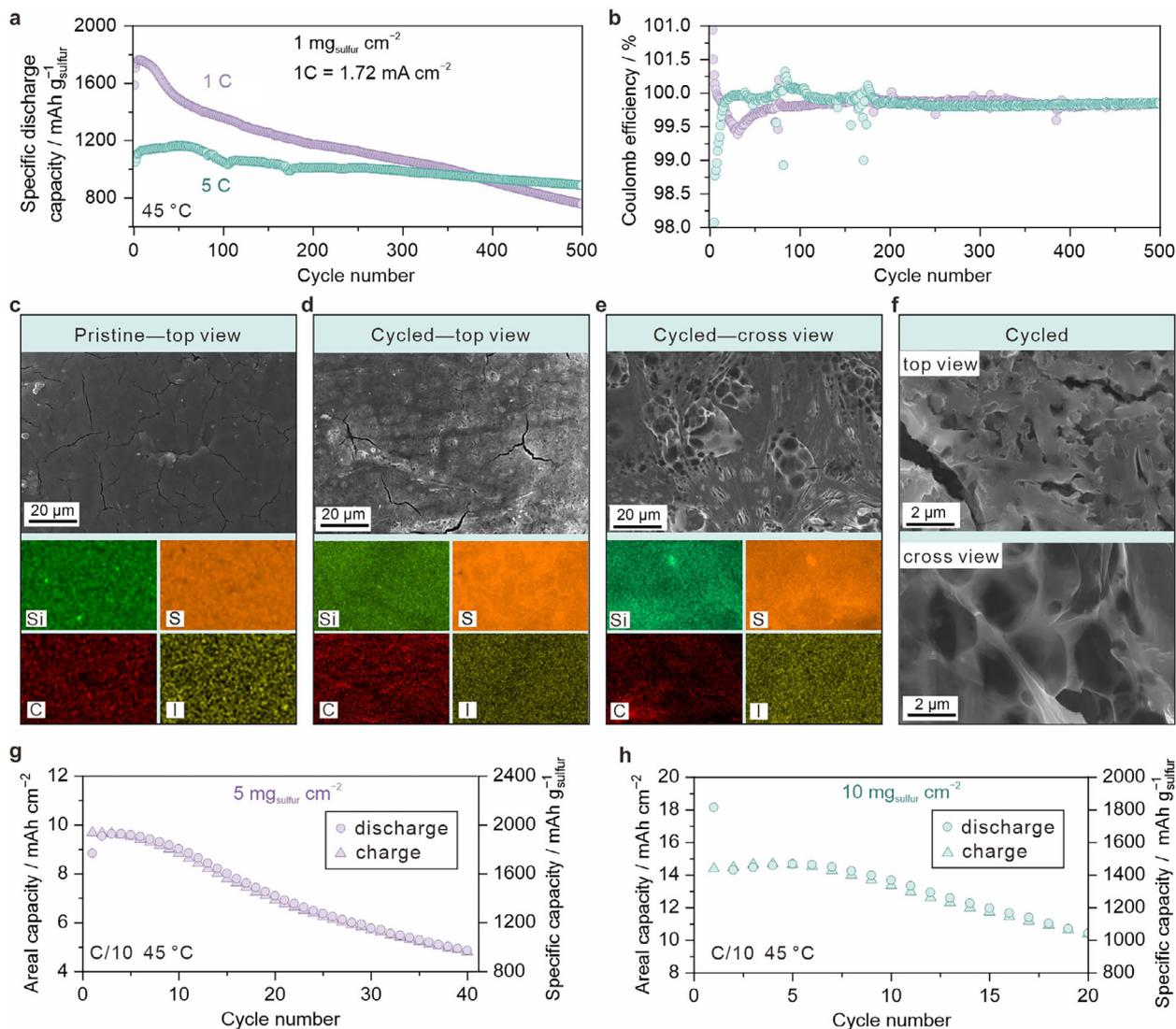
The GITT curves of the second cycle (Figure S14) were very similar to those of the first cycle, except for the better reversibility in both cases and the fact that the iodine-containing cell delivered a higher capacity, resulting from the combined effects of SE redox activity and improved sulfur utilization. Lower polarization and lower overvoltage in the iodine-containing SE at the end of charge confirm the continuing role of iodine redox mediation during cycling.

Besides, in situ EIS measurements were performed to probe the resistance evolution in the ASSLSBs during the first GITT cycle (Figure S15). A contribution in the high-frequency region ( $\sim 10^{-6}$ – $10^{-5}$  Hz) was clearly identified for the cells with  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$ , previously attributed to ionic resistance at the SE grain boundaries [55, 56]. However, this contribution was lacking for the SE pellets (Figure S3). Previous studies suggest that the bulk and grain-boundary resistances of similar superionic conductors are only distinguishable at low temperatures and/or much higher frequencies [36, 57]. Hence, the resistance observed here likely originates from other interfaces present in the cathode. Notably, no such contribution was detected in ASSLSBs using  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ , presumably due to the formation of an iodine-rich interface that is facilitating lithium transport [58]. As expected, the cells using  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  exhibited consistently lower overall impedances throughout cycling, thereby confirming better charge percolation in the case of the iodine-containing SE. Moreover, for  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$ , the bulk and interfacial resistances (intercept with x-axis) were found to steadily increase during the initial cycle, unlike for  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ , where only changes to the diffusive response are apparent from the Nyquist plots.

Distribution of relaxation times (DRT) analysis was further used to examine the electrochemical processes occurring in the middle- and low-frequency regions ( $10^{-5}$ – $10^1$  Hz) (Figure S16). Contributions from charge-transfer resistance at both anode and cathode were observed over a broad range of relaxation times, from  $10^{-3}$  to 1 s, overlapping with one another, thus making it very difficult or even impossible to tell them apart. However, in general, the charge-transfer resistance of ASSLSBs with  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  was lower than that of cells using  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$ , especially during charge. Aside from that, the diffusion-related resistance above 1 s was also lower for  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ , except at the end of charge, where the higher SOC led to an increase.

Based on these results, we hypothesize that  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  exhibits several beneficial effects across multiple aspects. First of all, the in situ formed iodine-rich, amorphous phase has a low Young's modulus, which positively affects densification of the cathode and facilitates charge-transfer kinetics. Combined with the embedded nanocrystalline  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  phase, this greatly enhances ionic percolation. Most importantly, iodine also acts as a redox mediator during charge, increasing reaction sites and improving rate performance (Figure 3g).

The fast kinetics was also confirmed by preparing a cathode composite via simply blending amorphous  $\text{Li}_4\text{PS}_4\text{I}$  (see XRD and EIS data in Figure S17) and  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$  and testing it as catholyte in ASSLSBs. The respective cells were found to deliver a specific discharge capacity of  $q_{\text{dis}} \approx 600$   $\text{mAh g}_{\text{sulfur}}^{-1}$  at 5C



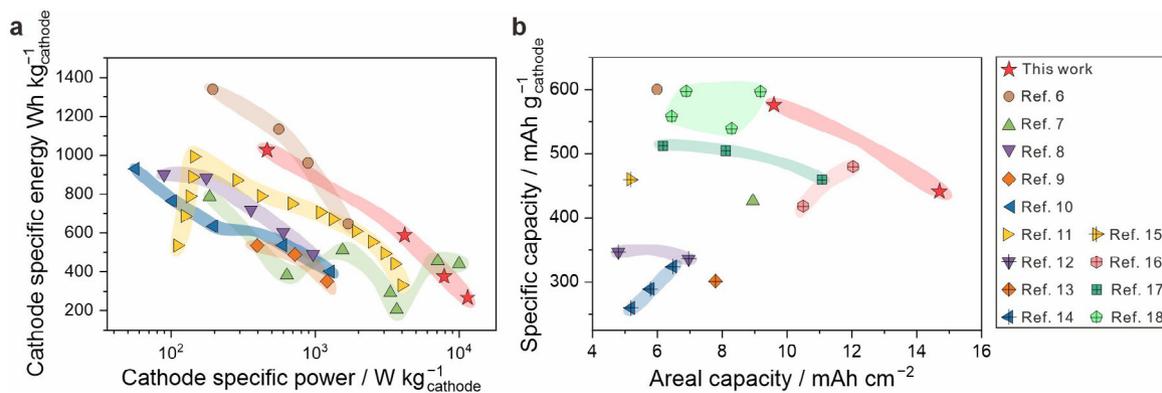
**FIGURE 4** | (a) Long-term cycling performance of  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ -based ASSLSBs at rates of 1C and 5C and (b) corresponding Coulomb efficiencies. (c–e) Top-view and cross-sectional SEM images of the cathode before and after cycling, along with elemental maps for Si, S, C, and I. (f) High-magnification SEM images showing the different pore sizes near the surface and in the bulk. Cycling performance achieved with sulfur loadings of (g)  $5 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$  and (h)  $10 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$ .

(Figure S18), much higher than that achieved with only  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$  (Figure 2e). Overall, these results highlight the effects that the mixing process and presence of amorphous side phases have on battery performance.

The long-term cycling performance of ASSLSBs with about  $1 \text{ mg cm}^{-2}$  sulfur loading was evaluated at rates of 1C and 5C (Figure 4a). After initial activation, specific discharge capacities of  $q_{\text{dis}} \approx 1760 \text{ mAh g}_{\text{sulfur}}^{-1}$  at 1C and  $q_{\text{dis}} \approx 1160 \text{ mAh g}_{\text{sulfur}}^{-1}$  at 5C were achieved, with continuous fading toward  $760 \text{ mAh g}_{\text{sulfur}}^{-1}$  at 1C and  $890 \text{ mAh g}_{\text{sulfur}}^{-1}$  at 5C after 500 cycles. The corresponding CEs are shown in Figure 4b. As can be seen, they exceeded 99.5% already after 20 cycles at 5C and remained well above upon further cycling. If long-term cycling was done at a 1C rate, the initial CE was higher than 100%, due to the significant capacity contribution related to the redox activity of the SE upon charge. During the course of the first 30 cycles, the CE dropped below 99.5%, after which it recovered

and stabilized at values exceeding 99.5% upon further cycling. The faster capacity decay of ASSLSBs cycled at 1C is likely due to more severe (chemo)mechanical degradation caused by greater charge/discharge depths (i.e., higher accumulated capacity) rather than irreversible side reactions, highlighting the need for future strategies, such as including polymer binders within the cathode composite to better maintain electrode integrity [59].

To gain insight into the microstructural and morphological changes of the cathodes upon battery operation, the cells were disassembled after extended cycling (>1000 cycles at 1C), followed by SEM imaging and EDX spectroscopy mapping. The pristine cathodes revealed a dense morphology, with some, mostly minor microcracking and sulfur, carbon, iodine, and silicon being uniformly distributed (Figure 4c). As is evident, no obvious segregation of elements occurred after long-term cycling, with the cathode integrity being largely maintained (Figure 4d). However, cross-sectional SEM imaging demonstrated



**FIGURE 5** | Comparisons between reported (a) high-power and (b) high-loading ( $>3 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$ ) ASSLSBs and our work (red stars). The references on the right-hand side refer to those given in Tables S2 and S3.

that the morphology is changing toward a porous structure with slightly uneven element distribution (Figure 4e). From the higher-magnification SEM images shown in Figure 4f, it can be seen that the pores in the bulk were significantly larger than those in the vicinity of the current collector. This kind of structure is believed to strongly increase charge-transport tortuosity and further cause contact loss, leading to electrochemically inactive (“dead”) material. The origin of pore formation is likely rooted in the severe volumetric and morphological changes during sulfur conversion and possibly also related to the generation of gaseous iodine species [24].

After having proven the excellent rate capability of ASSLSBs employing the  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  SE, high-loading cells were tested. Note that the cathode thickness increased from about  $19 \mu\text{m}$  for  $1 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$  to almost  $95 \mu\text{m}$  for  $5 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$ , and further to around  $190 \mu\text{m}$  for  $10 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$ . An areal capacity of  $9.7 \text{ mAh cm}^{-2}$  was achieved with  $5 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$  at C/10 (Figure 4g), corresponding to a specific discharge capacity of  $q_{\text{dis}} \approx 1940 \text{ mAh g}_{\text{sulfur}}^{-1}$  (including the contribution from the SE). After 40 cycles,  $4.8 \text{ mAh cm}^{-2}$  ( $\sim 970 \text{ mAh g}_{\text{sulfur}}^{-1}$ ) was maintained. When the loading was increased to  $10 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$ , the ASSLSBs were capable of delivering about  $18.1 \text{ mAh cm}^{-2}$  ( $\sim 1810 \text{ mAh g}_{\text{sulfur}}^{-1}$ ). However, the areal charge capacity was found to be “only”  $14.4 \text{ mAh cm}^{-2}$  ( $1440 \text{ mAh g}_{\text{sulfur}}^{-1}$ ) in the initial cycle at C/10 (Figure 4h), likely due to major changes in charge percolation and/or (chemo)mechanical degradation. Nevertheless, a high areal capacity of  $10.4 \text{ mAh cm}^{-2}$  was still maintained after 20 cycles.

In order to set the performance of the  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ -based cells in context with reports available in literature, Figure 5a,b summarizes data for other high-rate and high-loading ASSLSBs [14, 24, 27, 31, 32, 46, 48, 58, 60–64]. The reported ASSLSBs often differ with regard to key parameters, such as separator thickness, anode type, sulfur content in the cathode, sulfur loading, and operating temperature. To ensure fair comparison, the total cathode mass was considered in the following calculations, assuming a lithium metal anode in all cases. The original data and details on the calculations can be found in the Tables S2 and S3 and Section S1. In general, the specific energy decreases with increasing output power due to capacity decay and polarization. The ASSLSBs reported in the present work demonstrate one of the best performances (Figure 5a). As can be seen, ref. [6] exhibits a

higher specific energy below  $1 \text{ kW kg}_{\text{cathode}}^{-1}$ , as the sulfur content was 60 wt.% and a low-density catholyte was employed. However, in this particular case, the operating temperature was  $60^\circ\text{C}$ , and the cells showed pronounced fading at high power output.

Realizing high sulfur loadings is challenging but essential for practical applications of ASSLSBs. The goal is to achieve high areal capacities while maintaining high cathode-specific capacities (i.e., high sulfur content and utilization). Figure 5b summarizes reported ASSLSBs with high sulfur loadings ( $>3 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$ ). In general, high operating temperatures ( $\geq 45^\circ\text{C}$ ) and low C-rates (C/50–C/5) appear to be critical for ensuring robust sulfur utilization in high-loading cells, likely due to the unfavorable tortuosity of the transport pathways in thick cathodes. In this regard, our work achieves a record-high areal capacity of about  $14.4 \text{ mAh cm}^{-2}$  with a loading of  $10 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$  at  $45^\circ\text{C}$  and C/10 while maintaining competitive cathode-specific capacities. Furthermore, we calculated an idealized ASSLSB cell model considering a  $30 \mu\text{m}$ -thin SE separator (density:  $2 \text{ g cm}^{-3}$ ) and a Li metal anode (n/p ratio: 1) (Figure S19). In this context, our results suggest that a cell-level energy density of  $600 \text{ Wh kg}^{-1}$  is achievable. At a sulfur loading of  $5 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$ , this configuration delivers  $>600 \text{ Wh kg}^{-1}$  (including the SE contribution). Increasing the loading to  $10 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$  reduces sulfur utilization and slightly lowers the cell-level energy density, but values above  $600 \text{ Wh kg}^{-1}$  are still attainable.

Increasing the sulfur fraction in the cathode composite is critical for practical applications, but the tortuosity of the charge-transport pathways typically increases with increasing sulfur content, leading to reduced sulfur utilization and increased polarization. To examine this effect, we prepared cathode composites with an increased fraction of 37.5 wt.% sulfur using two approaches: (i) keeping the electrolyte fraction constant to maintain ionic transport and redox mediation (sulfur-carbon composite [75 wt.% sulfur]:SE = 1:1 by weight; referred to as cell\_SE), and (ii) keeping the carbon fraction constant to ensure sufficient electronic conductivity (sulfur-carbon composite [75 wt.% sulfur]:Super P:SE = 5:1:4 by weight; referred to as cell\_C). As shown in Figure S20a,b, cell\_SE delivered  $1366 \text{ mAh g}_{\text{sulfur}}^{-1}$  at C/2 and retained  $249 \text{ mAh g}_{\text{sulfur}}^{-1}$  at 15C, whereas cell\_C exhibited severe polarization with  $q_{\text{dis}} < 300 \text{ mAh g}_{\text{sulfur}}^{-1}$  even at C/2. These results demonstrate that ionic rather than electronic transport is the key limitation at higher sulfur

loadings. Notably, cell\_C displayed significantly larger discharge polarization, but similar charge polarization compared to cell\_SE, suggesting that iodine-mediated redox processes remain active, while reduced ionic conductivity hinders the sulfur to  $\text{Li}_2\text{S}$  conversion. Further increasing sulfur content is challenging with our current 75 wt.% sulfur-containing composite, but advanced hosts capable of lowering carbon fraction in the cathode may enable higher sulfur loadings without severely compromising ionic percolation [64].

### 3 | Conclusion

In summary, we have examined the effect of iodine substitution in sulfide-based solid electrolytes with the nominal composition  $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$  (with  $x = 0, 0.2, 0.4$ ). Structural analysis revealed that while iodine is not directly incorporated into the primary  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  phase, for  $x = 0.4$ , it promotes the formation of a secondary, iodine-containing  $\text{Li}_{4+c}\text{P}_{1-c}\text{Si}_c\text{S}_4\text{I}$  phase (19 wt.%) and reduces the fraction of amorphous side phases to about 6 wt.%. Despite the multiphase composition, the ionic conductivity of this composite electrolyte was determined to be  $6.8 \text{ mS cm}^{-1}$  at room temperature. When the electrolyte of nominal composition  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  was incorporated into all-solid-state lithium-sulfur batteries (ASSLSBs), the cells were found to deliver a reversible specific capacity of  $1850 \text{ mAh g}_{\text{sulfur}}^{-1}$  at  $C/2$ . This high capacity is achieved with a substantial contribution from the highly reversible redox of the solid electrolyte itself. Moreover, cells using  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  exhibited an excellent rate capability, retaining  $1175 \text{ mAh g}_{\text{sulfur}}^{-1}$  at  $5C$  and  $590 \text{ mAh g}_{\text{sulfur}}^{-1}$  at  $15C$ , clearly outperforming cells with iodine-free solid electrolyte. Scanning electron microscopy, synchrotron X-ray diffraction, pair distribution function analysis of total scattering data, and NMR spectroscopy revealed the complete amorphization of the  $\text{Li}_{4+c}\text{P}_{1-c}\text{Si}_c\text{S}_4\text{I}$  side phase, accompanied by nanosizing of the  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  main phase during preparation of the cathode composite. Applying a suite of electrochemical characterization techniques confirmed that the iodine-rich amorphous phase not only offers high ionic conductivity, but also actively participates in the redox reactions, thereby enhancing charge-transfer kinetics. This kind of unique interplay between different phases during cathode preparation and battery operation appears to be a key feature. The positive effect of the superionic solid electrolyte was further proven by testing of ASSLSBs, achieving a record-high areal capacity of  $14.4 \text{ mAh cm}^{-2}$  with a mass loading of  $10 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$  at a rate of  $C/10$ . Based on these high-loading cathodes, a cell-level specific energy over  $600 \text{ Wh kg}^{-1}$  can theoretically be achieved when paired with an ultrathin separator and a stable lithium metal anode. Overall, our work provides valuable insights into the rational design of redox-active solid electrolytes for next-generation electrochemical energy storage, paving the way for high-energy and high-power ASSLSBs with superior stability.

## 4 | Experimental Section

### 4.1 | Synthesis

The precursors for synthesis, including  $\text{Li}_2\text{S}$  (99.99%, Sigma-Aldrich),  $\text{P}_2\text{S}_5$  (99%, Sigma-Aldrich),  $\text{SiS}_2$  (99.99%, Goodfellow),

$\text{LiI}$  (99.999%, Sigma-Aldrich), and  $\text{S}_8$  (Sigma-Aldrich, 99.998%), were used as received. Super P and Ketjenblack (EC-600JD) carbons were dried under dynamic vacuum ( $10^{-3} \text{ mbar}$ ) at  $300^\circ\text{C}$  for 12 h prior to use. All materials were stored and handled in an Ar-filled glovebox, with  $\text{H}_2\text{O}$  and  $\text{O}_2$  levels maintained below 0.5 ppm. The  $\text{Li}_{10.5-x}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12-x}\text{I}_x$  (with  $x = 0, 0.2, \text{ and } 0.4$ ) SEs were synthesized via high-energy ball milling and subsequent annealing. A stoichiometric precursor mixture of around 1.5 g was placed in an 80 mL zirconia jar, along with 10 zirconia balls of 10 mm in diameter. The mixture was milled at 450 rpm for a total of 12 h using 24 cycles of 30 min milling and 10 min resting. After milling, the powders were pressed into pellets at 450 MPa, vacuum-sealed in quartz ampoules ( $10^{-3} \text{ mbar}$ ), and annealed at  $525^\circ\text{C}$  for 90 h to produce  $\text{Li}_{10.5}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{12}$  and 8 h for both  $\text{Li}_{10.3}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.8}\text{I}_{0.2}$  and  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ . The heating rate was set to  $5^\circ\text{C min}^{-1}$ , followed by natural cooling. For the mechanochemical synthesis of glass-ceramic  $\text{Li}_4\text{PS}_4\text{I}$  SE, a stoichiometric precursor mixture consisting of  $\text{Li}_2\text{S}$ ,  $\text{P}_2\text{S}_5$ , and  $\text{LiI}$  was ball-milled following the procedure described above.

### 4.2 | Laboratory X-Ray Diffraction (XRD)

Powder samples were sealed in borosilicate capillaries (0.68 mm inner diameter, 0.01 mm wall thickness; Hilgenberg) under an Ar atmosphere. XRD data were collected using a STOE Stadi-P diffractometer with a DECTRIS MYTHEN 1K strip detector in Debye-Scherrer geometry (Mo- $K\alpha$  radiation,  $\lambda = 0.70926 \text{ \AA}$ ). To quantify the amorphous fraction present in the SEs, 20 wt.% Si (640F; NIST) was added as an internal standard reference material. Rietveld refinement was performed using the FullProf Suite (version 2023) software.

### 4.3 | Synchrotron X-Ray Diffraction (SXRD), Total Scattering, and Pair Distribution Function (PDF) Analysis

Synchrotron XRD and total scattering data were collected at room temperature at beamline P02.1, PETRA III at Deutsches Elektronen-Synchrotron (DESY) in Hamburg, Germany, using a wavelength of  $\lambda = 0.207371 \text{ \AA}$ . The total exposure time for SXRD and total scattering measurements was set to 2700 s, divided into 9 cycles of 300 s, with a 60 s rest period after each cycle to mitigate beam-induced damage. The PDFgetX3 software was applied to calculate the  $G(r)$  from the experimental total scattering data [65]. The latter data were first corrected for sample container contribution and Compton scattering, and then the normalized structure functions  $[S(Q)]$  were obtained. Finally, the  $S(Q)$  was Fourier-transformed to yield  $G(r)$  with  $Q_{\text{max}} = 16 \text{ \AA}^{-1}$  and  $r_{\text{poly}} = 1.2 \text{ \AA}$ .

### 4.4 | $^{31}\text{P}$ Magic-Angle Spinning (MAS) Nuclear Magnetic Resonance (NMR) Spectroscopy

$^{31}\text{P}$  MAS NMR measurements were performed with a Bruker Avance spectrometer at a magnetic field of 11.7 T, corresponding to a resonance frequency of 202.5 MHz. Spinning was done in 2.5 mm rotors at 25 kHz. Samples were packed into the

rotors in an Ar-filled glovebox. Spectra were acquired with a rotor-synchronized Hahn-echo pulse sequence with a  $\pi/2$  pulse duration of 1.9  $\mu\text{s}$  and a recycle delay of 30 s. Spectra were referenced to  $\text{H}_3\text{PO}_4$  (85%) at 0 ppm.

#### 4.5 | $^7\text{Li}$ Pulsed-Field Gradient (PFG) NMR Spectroscopy

The  $^7\text{Li}$  PFG NMR measurements were performed on a Bruker Avance spectrometer at a magnetic field of 7.05 T. The maximal gradient strength of the diffusion probe is 30 T/m. The samples were stored in an Ar-filled glovebox and measured in sealed 5 mm borosilicate glass tubes. For the PFG experiments, a stimulated-echo pulse sequence was used [66]. Sulfur/C/Li<sub>10.1</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>11.6</sub>I<sub>0.4</sub>, sulfur/C/Li<sub>10.3</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>11.8</sub>I<sub>0.2</sub>, and sulfur/C/Li<sub>10.5</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>12</sub> were measured with a diffusion time of 10 ms and a gradient duration of 1.5 ms. Pristine Li<sub>10.1</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>11.6</sub>I<sub>0.4</sub> was measured with a diffusion time of 60 ms using a gradient duration of 3.5 ms. Li<sub>10.1</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>11.6</sub>I<sub>0.4</sub> exhibited two distinct lithium diffusion coefficients with slow exchange, attributed to the  $t\text{-Li}_{10.5+a}\text{Si}_{1.5+a}\text{P}_{1.5-a}\text{S}_{12}$  and  $\text{Li}_{4+c}\text{P}_{1-c}\text{Si}_c\text{S}_4\text{I}$  phases. The corresponding diffusion coefficients were extracted using a two-component fitting model, as demonstrated in previous work [42].

#### 4.6 | Electrochemical Impedance Spectroscopy (EIS)

Powder samples were loaded into a PEEK sleeve of inner diameter 10 mm and sandwiched between stainless steel rods. The cells were pressed at 3.5 t for 3 min, and EIS measurements were conducted from 0.1 Hz to 7 MHz with a 20 mV voltage amplitude and at a stack pressure of 250 MPa using a BioLogic SP-200 potentiostat.

#### 4.7 | Direct Current (DC) Polarization Measurements

To this end, SE and S<sub>8</sub> in a 5:3 weight ratio were blended in an 80 mL zirconia jar with 10 zirconia balls (10 mm diameter) at 450 rpm for 10 h, with cycles of 30 min milling and 10 min resting. 80 mg of the mixture was then loaded into a PEEK sleeve (10 mm diameter) and sandwiched between stainless steel rods. The cell was pressed at 3.5 t for 3 min, and the as-made pellet was subjected to DC polarization at 0.3, 0.6, 0.9, and 1.2 V at 25°C and under a stack pressure of 250 MPa. Each voltage was applied for 6 h to ensure a stable current response, from which both resistance and conductivity were calculated.

#### 4.8 | Thermogravimetric Analysis (TGA)

TGA measurements were performed using a NETZSCH TG 209F1 Libra instrument under a continuous argon flow of 20 mL min<sup>-1</sup>. The latter served both as a protective and purging gas. Appropriate amounts of composite materials were placed in an Al<sub>2</sub>O<sub>3</sub> crucible and heated from room temperature to 550°C at a rate of 5°C min<sup>-1</sup>.

#### 4.9 | Galvanostatic Intermittent Titration Technique (GITT), In Situ EIS, and Distribution of Relaxation Times (DRT) Analysis

The ASSLSBs were cycled at a rate of C/10 and at 45°C in the voltage window of 0.4–2.5 V vs. In/InLi with alternating periods of 30 min applied current and 35 min open-circuit voltage (OCV) relaxation. In situ EIS data were collected during each relaxation period. DRT analysis was performed using the MATLAB GUI toolbox developed by Ciucci's group [67]. Inductive data were excluded, second-order regularization derivative fitting parameters were used with a regularization parameter of 0.0001, and a radial basis function (RBF) with a full width at half maximum of 0.5 was applied. The sample size was set to 10000.

#### 4.10 | Cryogenic Focused Ion Beam (FIB) Cutting, Scanning Electron Microscopy (SEM), and Energy Dispersive X-Ray (EDX) Spectroscopy

SEM imaging of the pristine and cycled cathode was performed using a LEO 1530 microscope (Zeiss) equipped with a field emission gun and operated at 10 kV. EDX was performed using an Oxford X-Max N detector (Oxford Instruments) at 20 kV. Cryo-FIB cutting and room-temperature SEM imaging were further used to probe the texture of the pristine cathode composite. Cross-sectional specimens of the pelletized cathode composite were prepared using a Capella FIB system equipped with a gallium ion source under cryogenic conditions. The cathode pellet was mounted on a sample holder with carbon tape inside an Ar-filled glovebox and transferred to the scanning electron microscope (SEM) (Zeiss Crossbeam 340) via a transfer shuttle. The nitrogen-gas-cooled cold stage and the anti-contaminator were stabilized at –140°C and –170°C, respectively, with temperature control and monitoring provided by the cryo FIB-SEM sample preparation system (PP3005-06, Quorum). After insertion, the sample was further cooled and stabilized at –140°C. Then, FIB milling was performed with a 3 nA ion current. Cross-sectional SEM images were acquired at an accelerating voltage of 3 kV at room temperature. Image distortion caused by the 54° FIB cutting angle was corrected using the optical tilt correction feature implemented in the SmartSEM software.

#### 4.11 | Electrode Preparation, Cell Assembly, and Electrochemical Testing

The sulfur-carbon composite was prepared by mixing 3 g of S<sub>8</sub> with 1 g of Ketjenblack in a mortar. The resulting mixture was loaded into an alumina crucible, covered with aluminum foil, and heated at 155°C for 12 h under an Ar atmosphere. For ASSLSBs, the cathode was prepared by blending a 1 g mixture of sulfur-carbon composite, Super P, and SE (4:1:5 weight ratio) in an 80 mL zirconia jar with 10 zirconia balls (10 mm diameter) at 450 rpm for 2, 4, or 10 h (30 min milling cycles with 10 min resting periods). In the case of using the amorphous Li<sub>4</sub>PS<sub>4</sub>I and sintered Li<sub>10.5</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>12</sub> mixture as SE, the cathode was prepared by blending sulfur-carbon composite, Super P, amorphous Li<sub>4</sub>PS<sub>4</sub>I, and sintered Li<sub>10.5</sub>Si<sub>1.5</sub>P<sub>1.5</sub>S<sub>12</sub> (4:1:1:4 weight ratio) following the same procedure as described above for 10 h milling.

In general, a customized cell setup with stainless steel dies and a PEEK sleeve (10 mm diameter) was used for cell assembly. The SE (100 mg) was pressed at 62.5 MPa to form the separator layer. The cathode composite was spread onto the separator and compacted at 440 MPa. For ASSLSBs with a low mass loading ( $\sim 1 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$ ), an In foil (9 mm diameter, 45 mg; GoodFellow) and a Li foil (6 mm diameter, 2 mg; Albemarle Corp.) were placed onto the separator. For high-loading ASSLSBs, two and four alternating layers of In and Li foils were used for 5 and  $10 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$  loadings, respectively. Galvanostatic charge/discharge measurements were performed at  $45^\circ\text{C}$  and under 81 MPa external pressure using a Maccor battery cycler. The cells were cycled between 0.4 and 2.5 V vs. In/InLi (1.02–3.12 V vs.  $\text{Li}^+/\text{Li}$ ) at different C-rates ( $1\text{C} = 1672 \text{ mA g}_{\text{sulfur}}^{-1}$ ) after a 1 h OCV rest period.

For cells with  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$ /carbon cathode, the composite was prepared by blending a 1 g mixture of  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  and Super P (7:3 weight ratio) in an 80 mL zirconia jar with 10 zirconia balls (10 mm diameter) at 450 rpm for 10 h (30 min milling cycles with 10 min resting periods). They were assembled and cycled using the same setup, except that the cathode composite loading was  $3.9 \text{ mg cm}^{-2}$ . This corresponds to a  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  loading equal to the combined mass of  $\text{Li}_{10.1}\text{Si}_{1.5}\text{P}_{1.5}\text{S}_{11.6}\text{I}_{0.4}$  and sulfur in ASSLSBs with  $1 \text{ mg}_{\text{sulfur}} \text{ cm}^{-2}$ . The cells were initially discharged, then charged at 0.86, 8.6, 17.2, and  $25.8 \text{ mA cm}^{-2}$  (equal to the current densities at C/2, 5C, 10C, and 15C for ASSLSBs). Subsequent cycling was carried out at  $8.6 \text{ mA cm}^{-2}$ .

## Acknowledgements

F.S. and J.Y. are grateful to the German Federal Ministry of Research, Technology, and Space (BMFTR) for funding within the project MELLi (03XP0447). We acknowledge DESY (Hamburg, Germany), a member of the Helmholtz Association HGF, for the provision of experimental facilities. Parts of this research were carried out at PETRA III, and we are grateful to Martin Aaskov Karlsen and Volodymyr Baran for assistance in using beamline P02.1. Beamtime was allocated for proposal I-20240376. J.C. and S.F. acknowledge funding from the German Federal Ministry of Research, Technology, and Space (BMFTR) in the NanoMatFutur program (03XP0423) and basic funding from the Helmholtz Association. Open access funding enabled and organized by Projekt DEAL.

## Conflicts of Interest

The authors declare no conflicts of interest.

## Data Availability Statement

The data that support the findings of this study are available from the corresponding authors upon reasonable request.

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## Supporting Information

Additional supporting information can be found online in the Supporting Information section.

**Supporting File:** adma72445-sup-0001-SuppMat.docx.