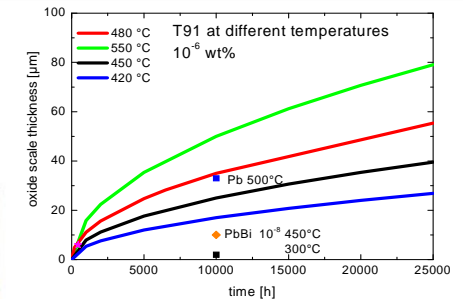
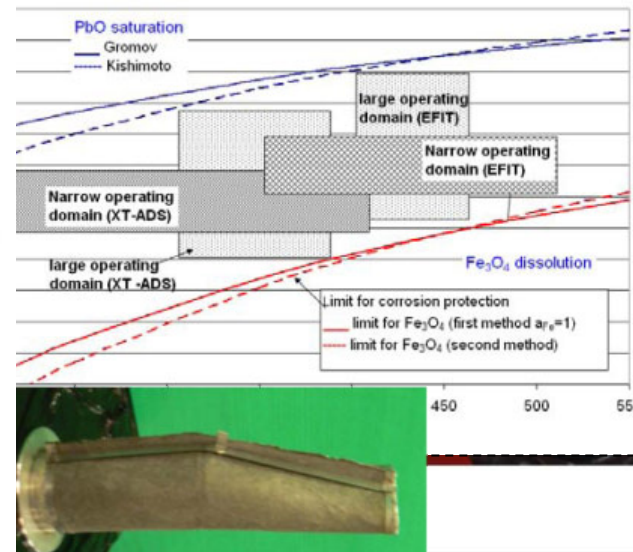
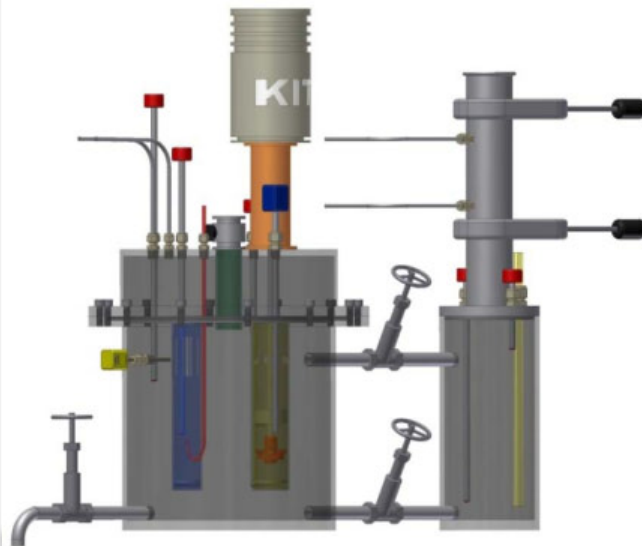


Mini-Pool Reactor

to determine interaction and mass transport of oxygen and other impurities in flowing LBE

Design and Design supporting CFD calculations

C. Bruzzese, A. Weisenburger, A. Class, C. Schroer – KIT



$$w_{T,O,B} = F_B \cdot \rho_{ox} \cdot \delta_B \cdot 4 \cdot \frac{M_o}{M_{Fe_3O_4}}$$

$w_{T,O,B}$ = weight of oxygen (oxidation)

F_B = total surface of cladding

δ_B = thickness of oxide scale

ρ_{ox} = density of oxide scale

$M_o, M_{Fe_3O_4}$ = molecular weight of oxygen and Fe₃O₄

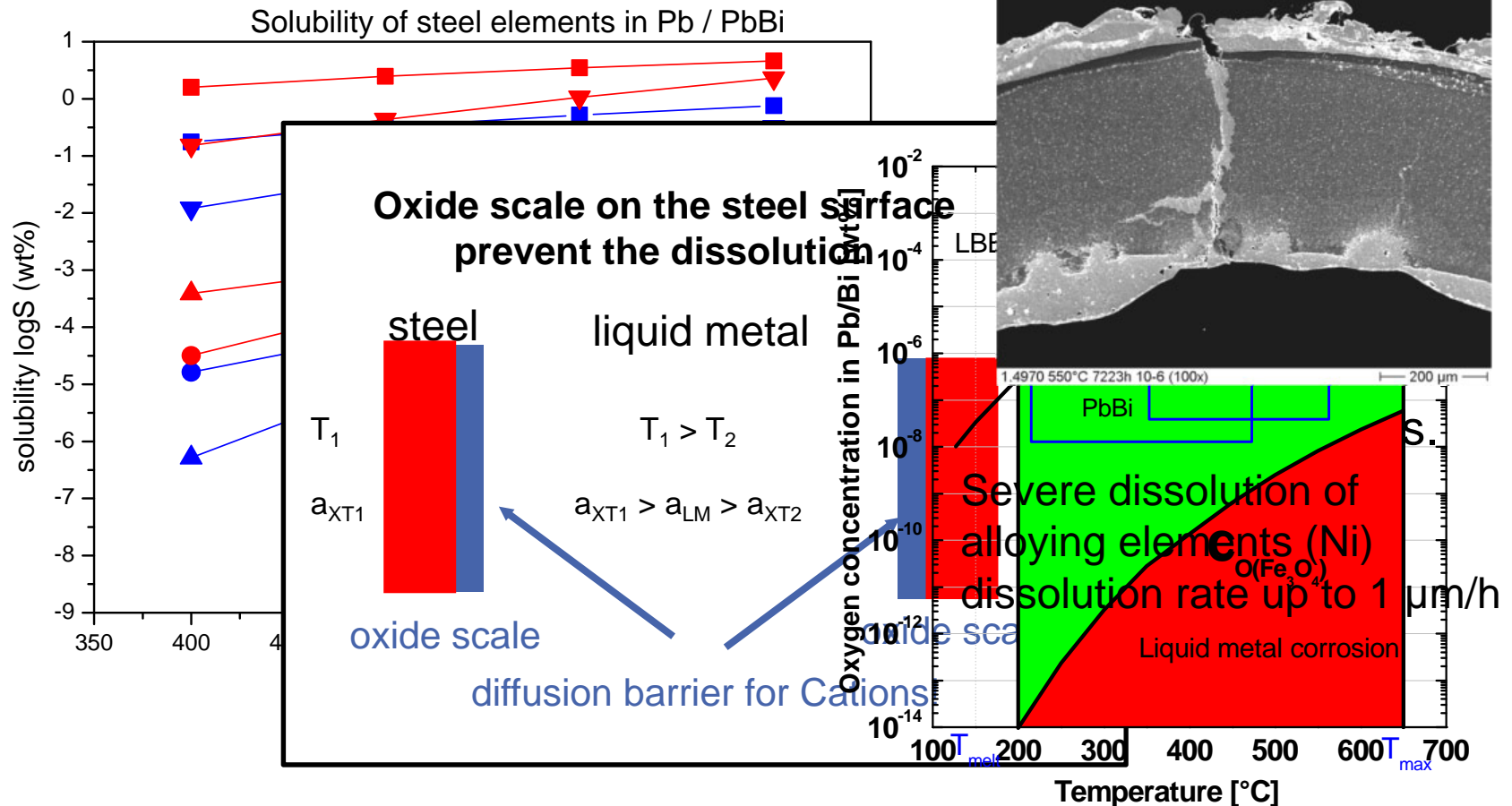
■ Outline

- Introduction
- Questions addressed – Experiments foreseen - Pre-design
- Design oriented CFD
- Summary and next steps

Oxygen – Why relevant for Pb alloy cooled ADS?

- Solubility of metals in liquid Pb PbBi - W, Ta << Fe, Cr < Al < Ni

austenitic steel / 1.4970
oxide scales



Modular Mini-Reactor Pool for

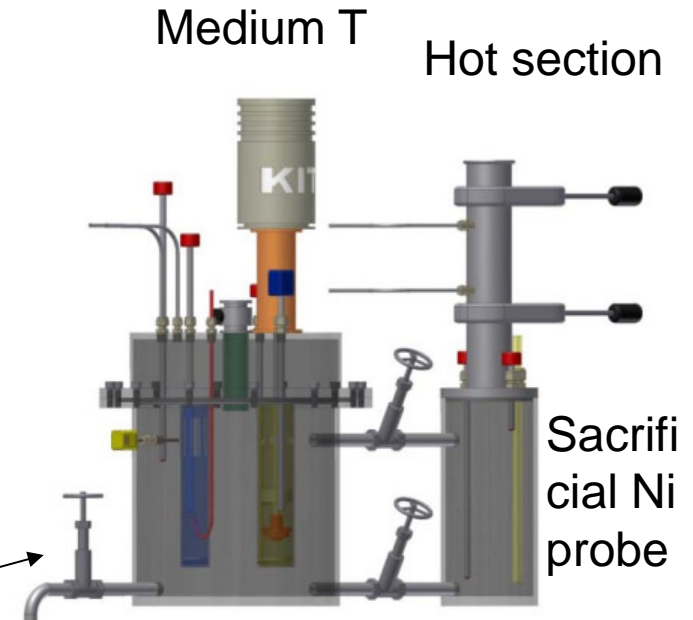
Corrosion, Mass Transport and Filtering

Experimental test cases

- Normal operating conditions: reference cover gas environment
- Cover gas leak & gas/solid entrainment
- HEX-leak (water vapour)
- THEADES crud & filtering
- Sacrificial Nickel probe
- Filter performance

CFD Studies

- Thermohydraulic characterisation
- Mass transport & sources
- Influence of environment gas & solid oxides



Instrumentation:

Oxygen sensors with thermocouples

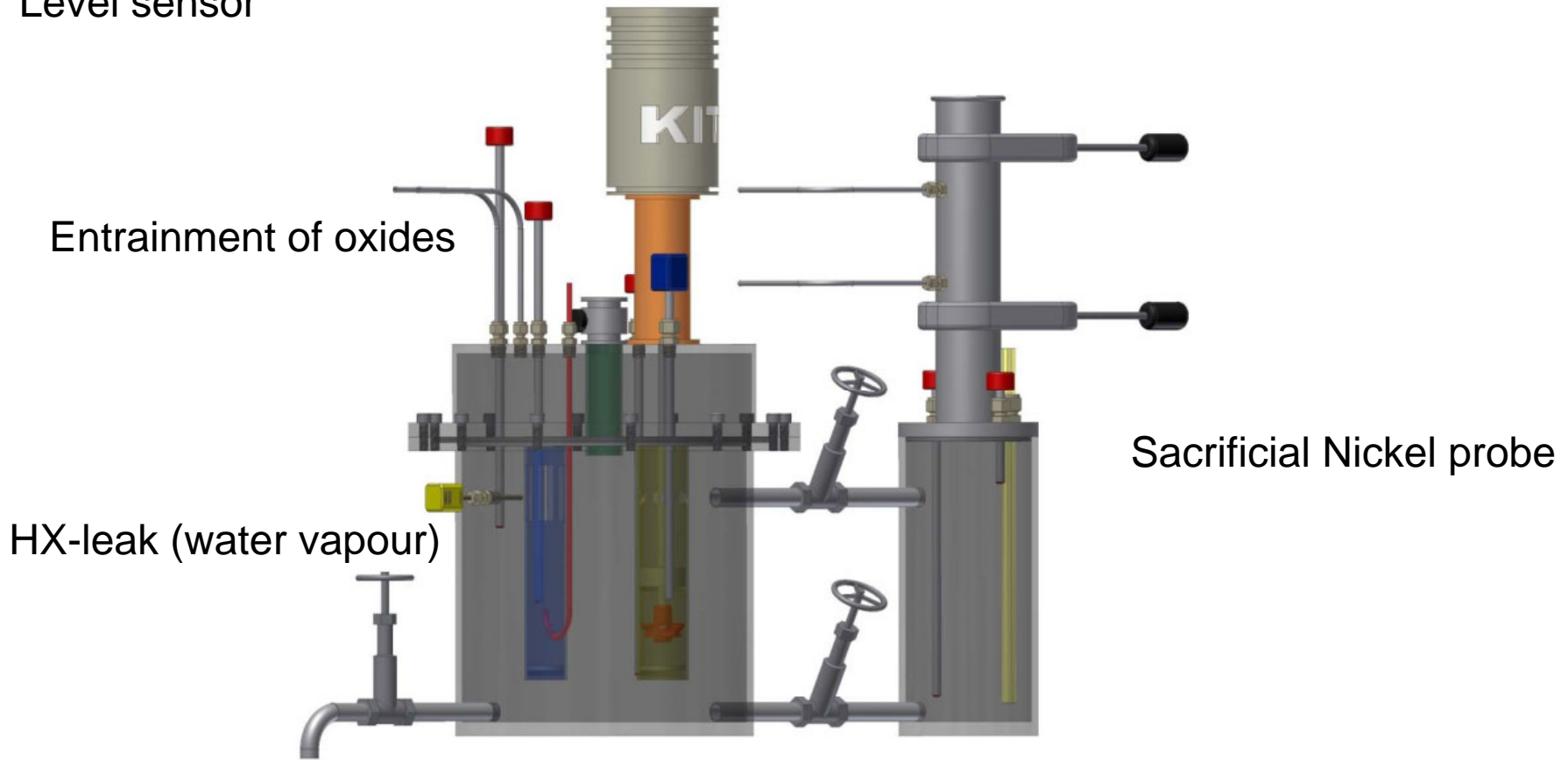
Cold probe

Ultrasound doppler

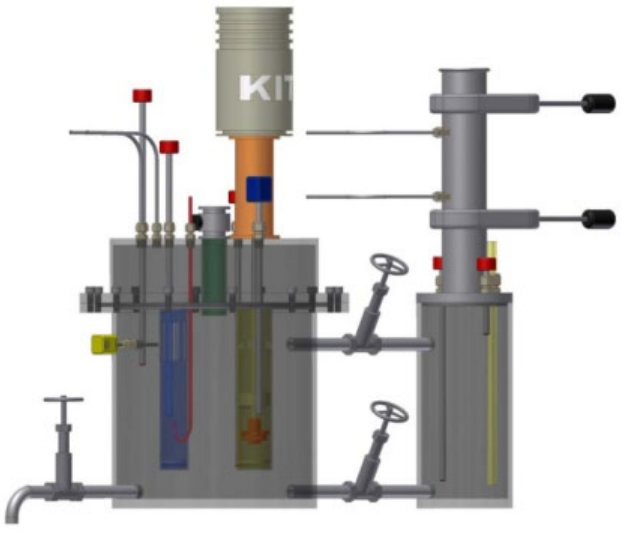
floating gauge - local level (pressure, velocity)

Level sensor

Modular Mini Reactor Pool

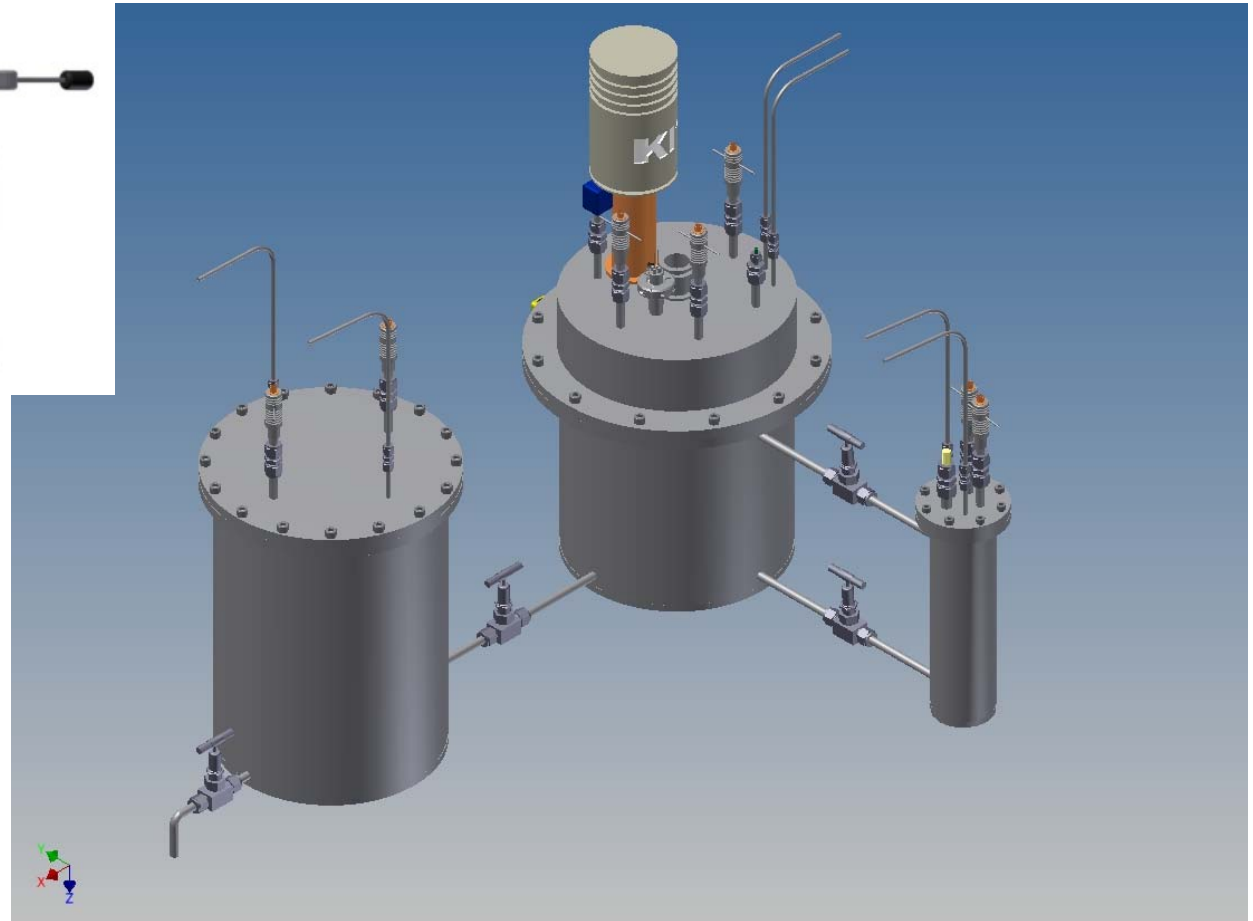


Modular Mini Reactor Pool – 1st design changes



Now - 3 pots:

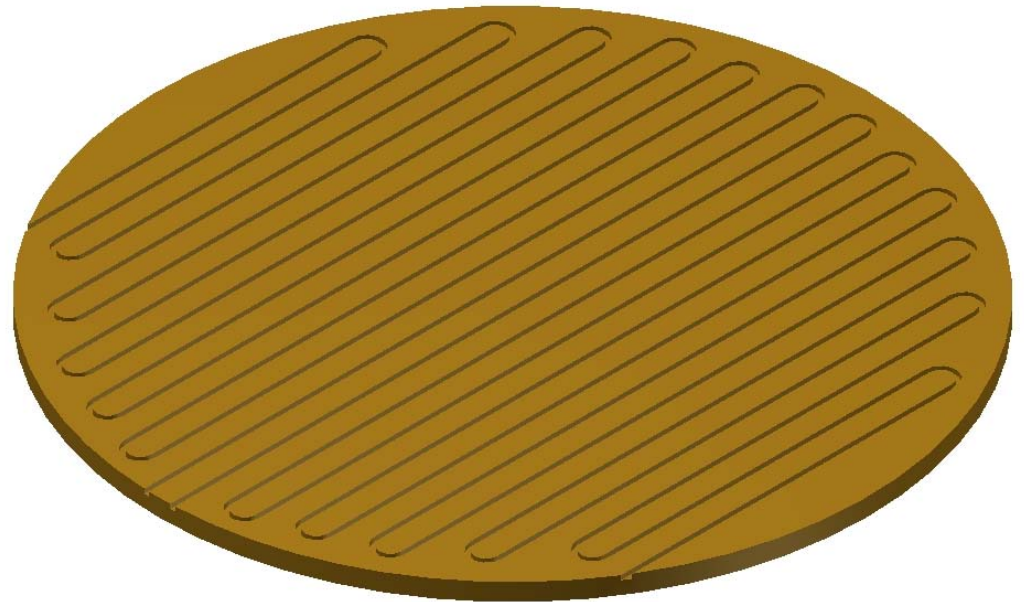
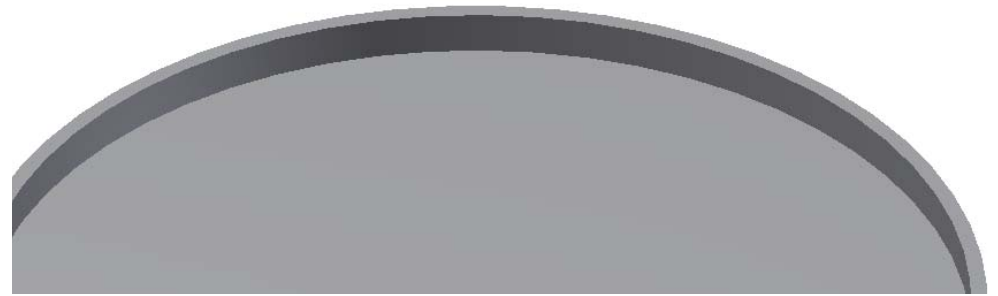
Conditioning
Experimental
Hot - Sacrificial Ni



1st Design Phase

Heating system is designed – all „pots“ are manufactured

6KW total heating power
Temperature up to 650°C



Aim: Support the design - location of sensors and internal

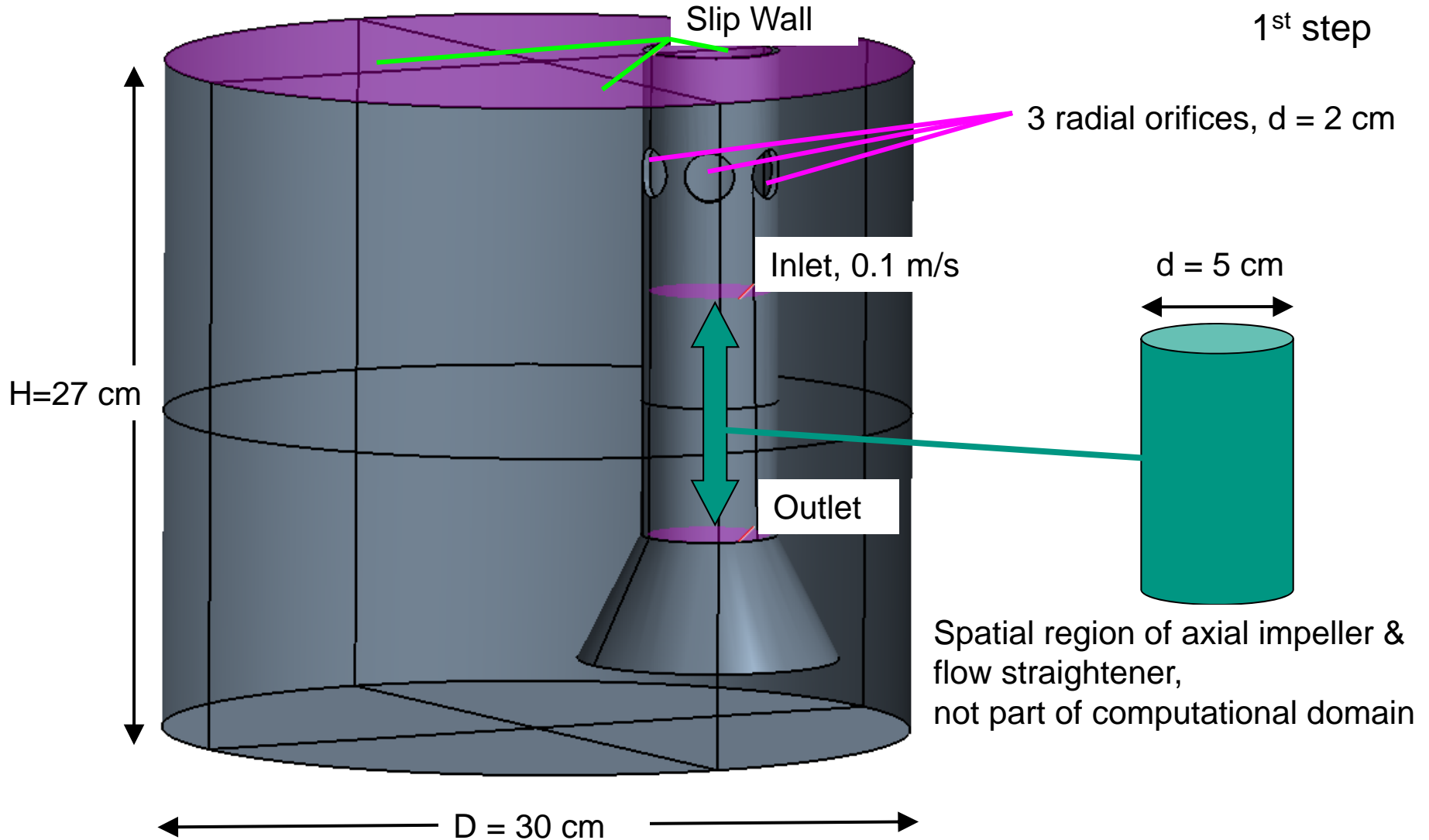
- Evaluation of design based on fluid mechanical aspects
- Identification of main flow patterns & regimes

- Adopted strategy:
 - Force asymmetry of flow field with choice of geometry and boundary conditions (do not rely on existence of large scale symmetry of flow field)
 - Flow field should contain regions with
 - Strongly directed, fast flow → mainly/definite convective transport
 - Stagnant flow, dead water regions → mainly/definite diffusive transport

- CFD-Software: STAR-CCM+ 6 (CD-adapco)

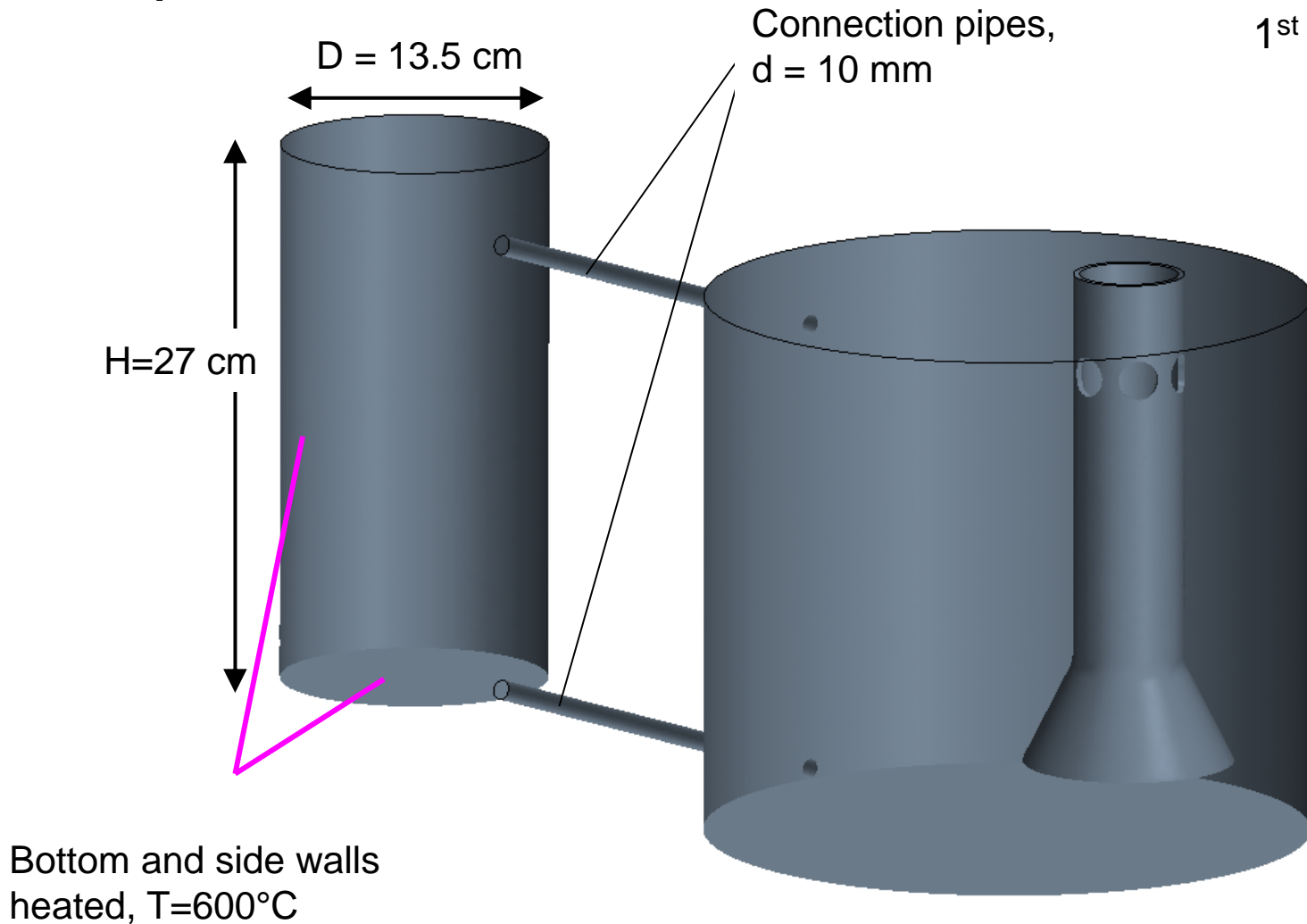
“CFD-Geometry” of main pool/tank, $T=400^{\circ}\text{C}$

1st step



Main pool with auxiliary heated tank (sacrificial Ni at 600°C)

1st step



Numerical Settings

- Finite-Volume Spatial Discretization
- Polyhedral mesh

- Stationary solver
- Segregated flow model, pressure-velocity coupling by SIMPLE method
- Convection scheme: 2nd order upwind

- Fluid: LBE with constant fluid properties at $T=400^{\circ}\text{C}$

- Reynolds-Averaged Navier-Stokes Equations (RANS)
- Incompressible, Buoyancy accounted for by Boussinesq approximation

- Realizable two-layer k-epsilon turbulence model

Results with auxiliary heated tank @ $T=600^{\circ}\text{C}$

- Mean flow velocity in connection pipes approx. 0.14 m/s
- Flow direction according to natural convection loop
- Low flow velocity in heated tank
- Core of large scale vortex in similar position as in simulation without heated tank

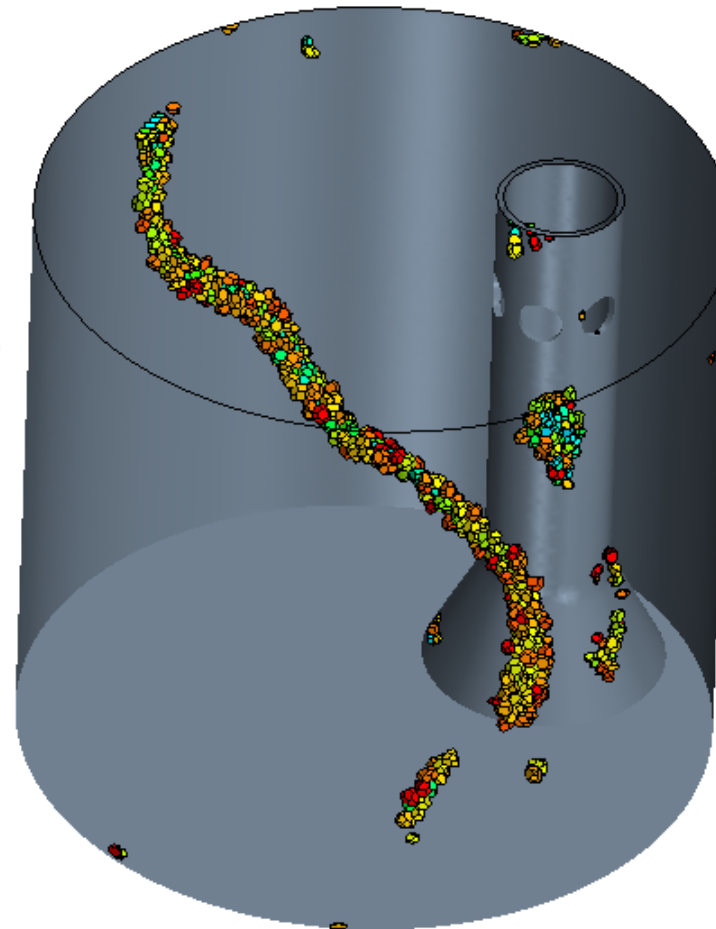
Main Flow Patterns, $T=400^{\circ}\text{C}$: Core of Large-Scale Vortex

1st step

Stable large – scale vortex

Possible position of oxygen sensor (for dead zone)

Stable assymmetric flow pattern



Only cells with velocity magnitude $< 5 \text{ mm/s}$ are shown



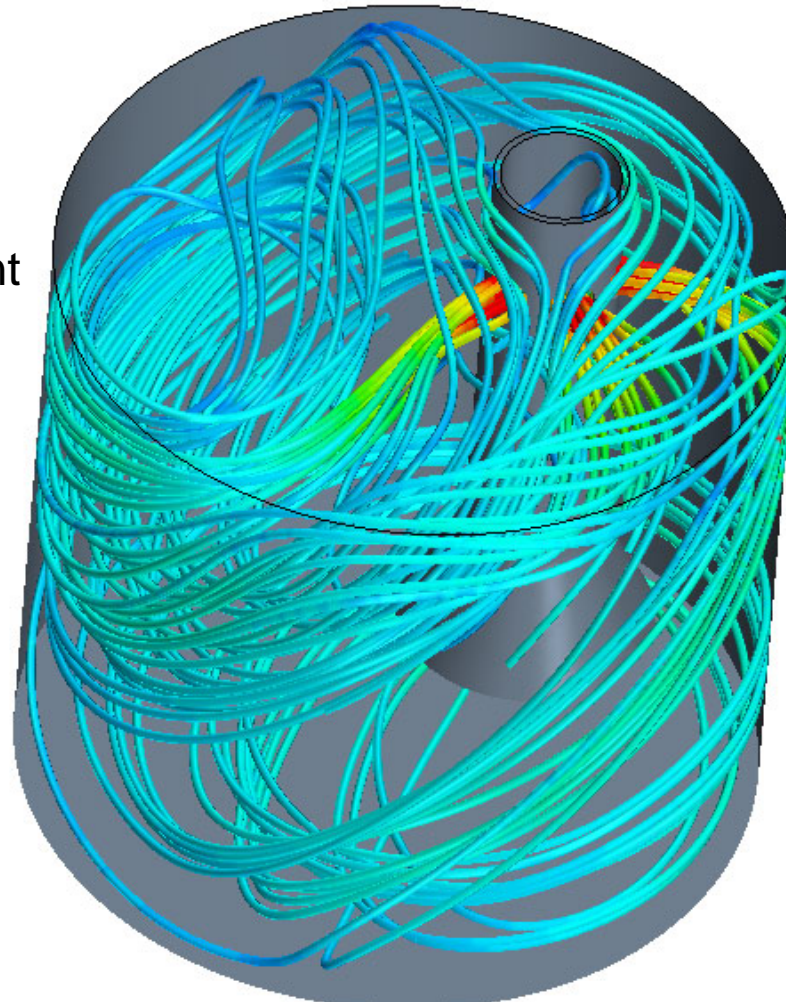
Main Flow Patterns, $T=400^{\circ}\text{C}$: Fast Jets from Orifices

1st step

Stable flow jets
 To be used for velocity measurement

oxygen sensors along flow jet

1 in stable dead zone (might be supported by design)



Design-supporting CFD – 2nd step

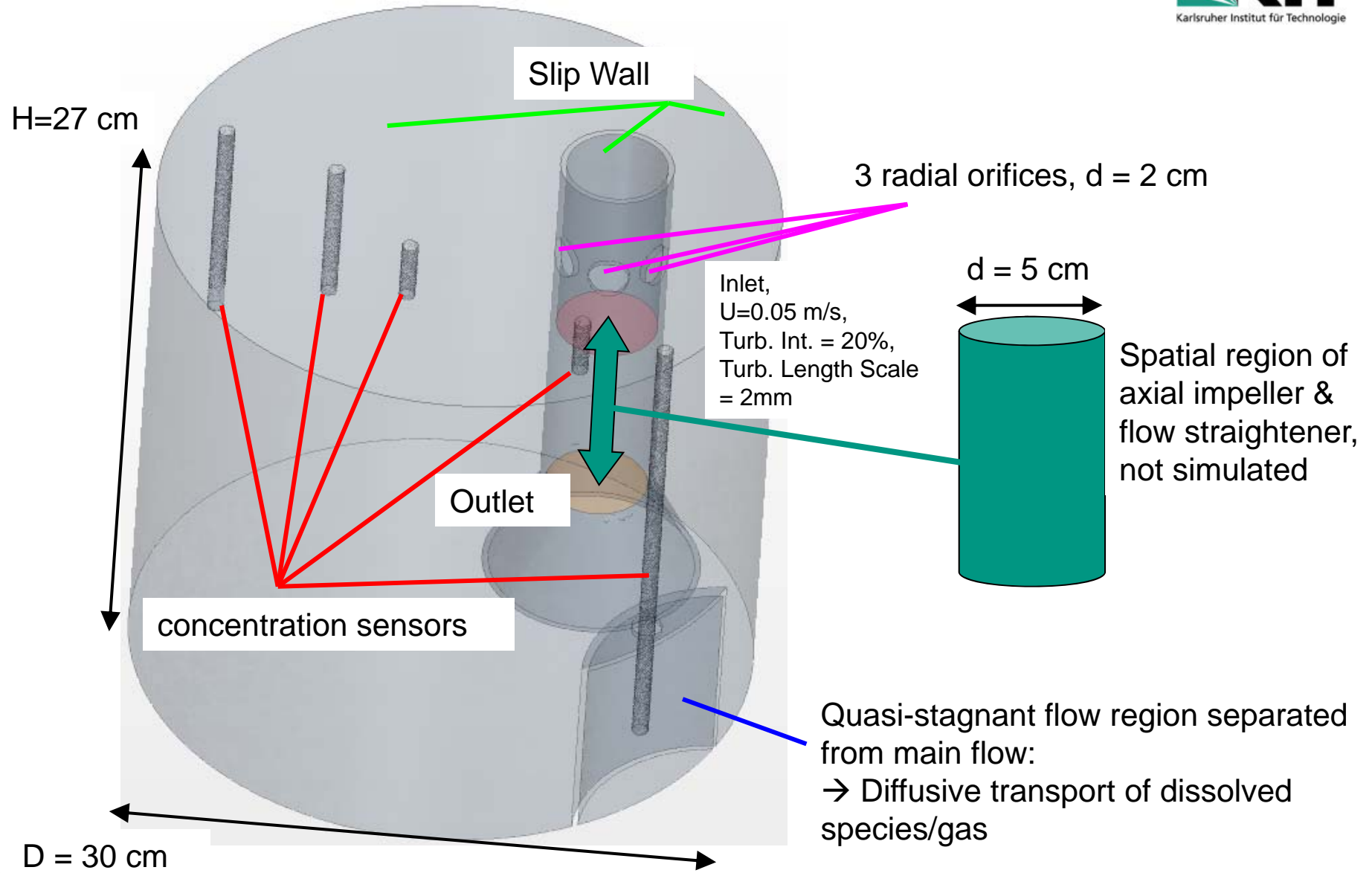
Aim: Support the design by

- Evaluation of design based on fluid mechanical aspects
- Identification of main flow patterns & regimes
- Choice of location of sensors (concentration & velocity) and internals

- Adopted strategies:
 - Force asymmetry of flow field with choice of geometry and boundary conditions (do not rely on existence of a large scale symmetry)
 - Realize properly defined boundary conditions
 - Flow field should contain regions with
 - Strongly directed, fast flow → mainly/definite convective transport
 - Stagnant flow, dead water region → mainly/definite diffusive transport

- CFD-Software: STAR-CCM+ 6 (CD-adapco)

“CFD-Geometry” of main pool/tank, $T=400^{\circ}\text{C}$



Numerical Settings – no changes

- Finite-Volume Spatial Discretization
- Polyhedral mesh

- Stationary solver
- Segregated flow model, pressure-velocity coupling by SIMPLE
- Convection scheme: 2nd order upwind

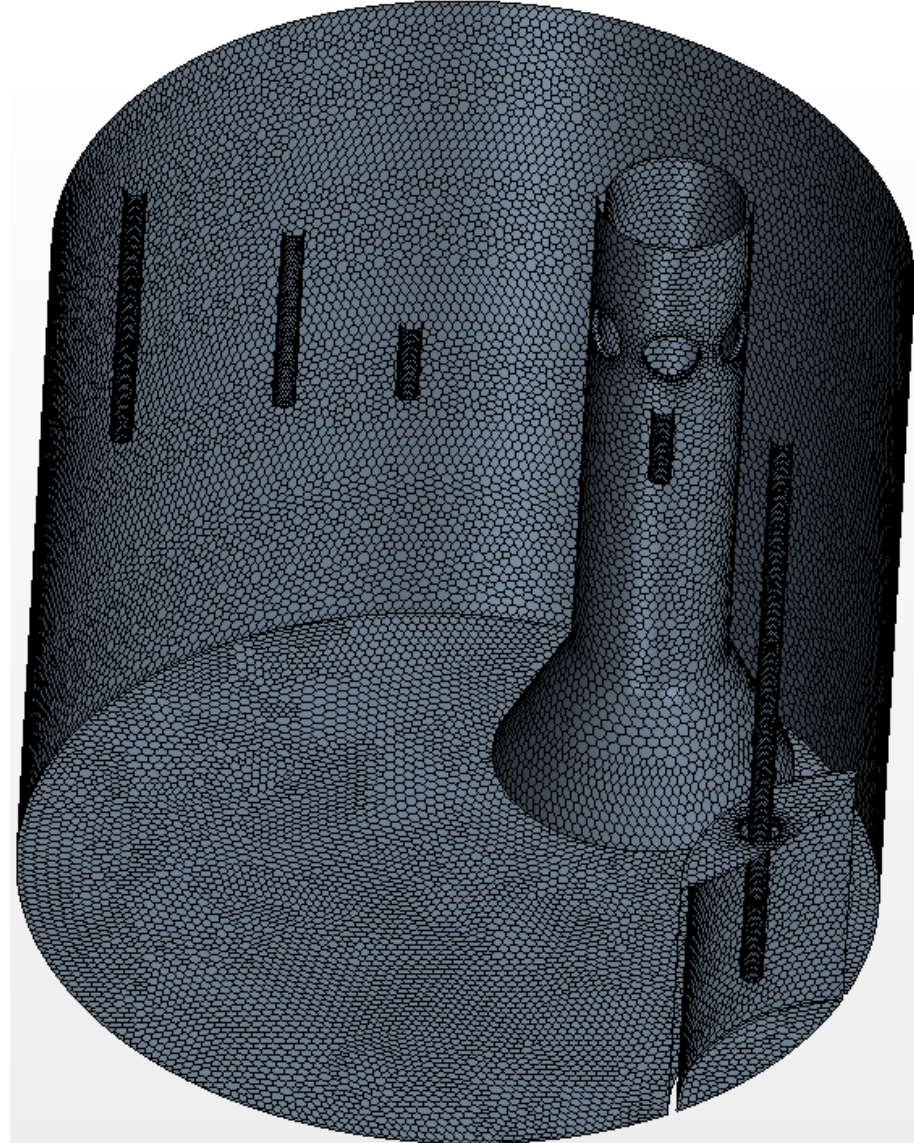
- Fluid: LBE with constant fluid properties at $T=400^{\circ}\text{C}$

- Reynolds-Averaged Navier-Stokes Equations (RANS)
- Incompressible

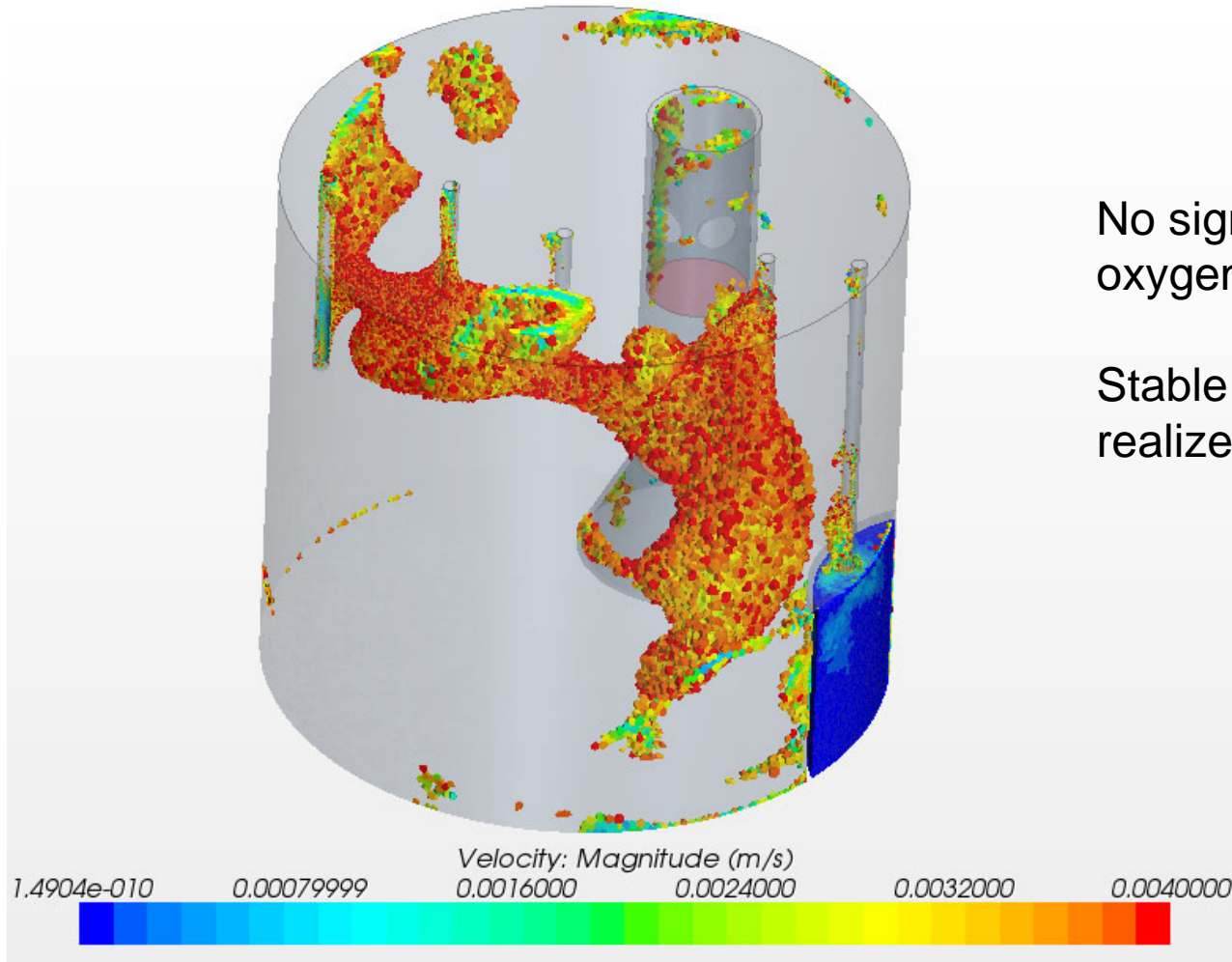
- Realizable two-layer k-epsilon turbulence model

Exemplary computational mesh

- 680,000 polyhedral cells



Main Flow Patterns, $T=400^{\circ}\text{C}$: Stable Large-Scale Low-Flow-Speed region



No significant change by
oxygen sensors

Stable stagnant region
realized by design

Only cells with velocity magnitude $< 4 \text{ mm/s}$ are shown (4 mm/s is $\sim 10\%$ of characteristic circumferential speed, the max. flow speed in the jets is $\sim 150 \text{ mm/s}$)

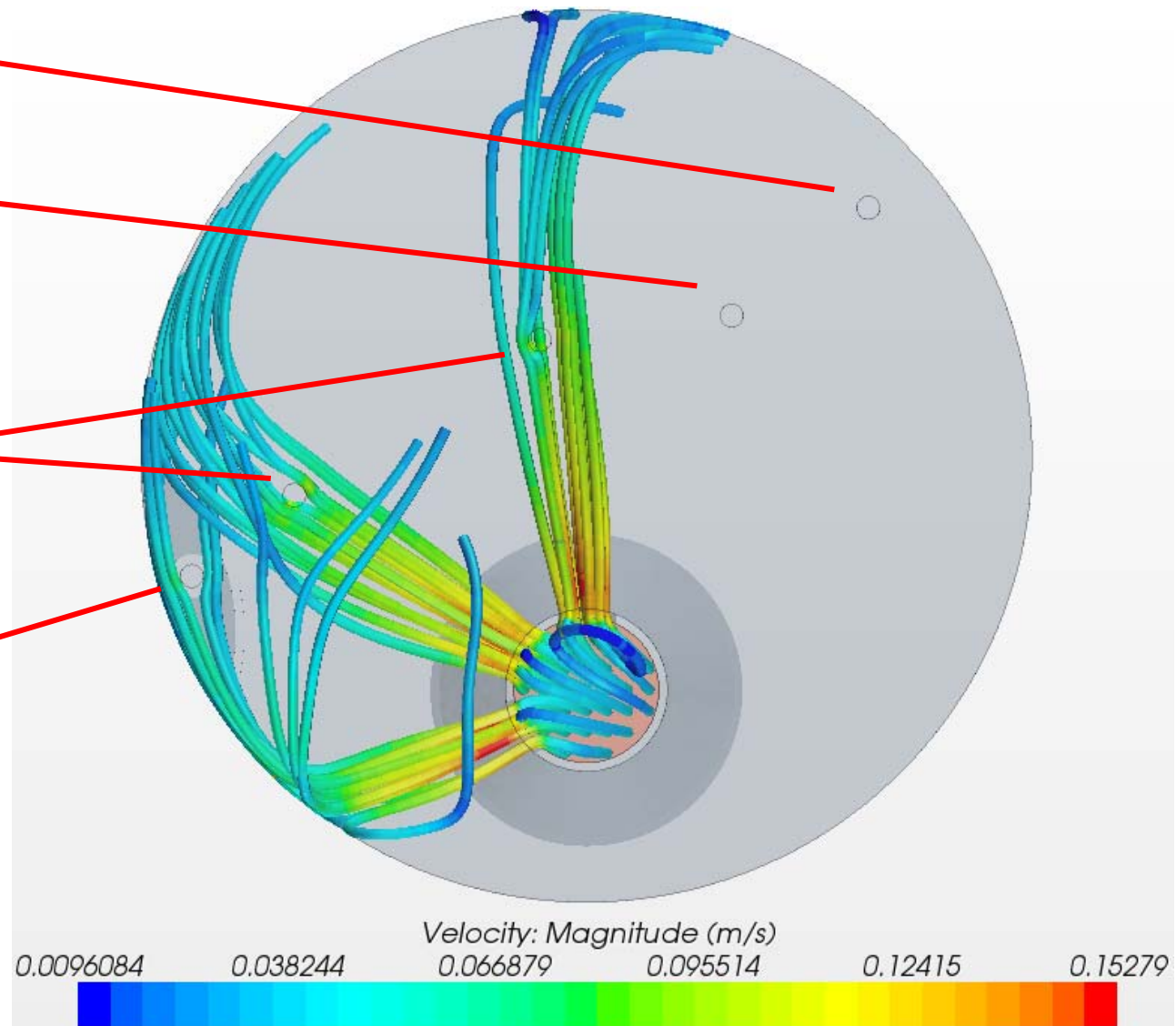
Main Flow Patterns, $T=400^{\circ}\text{C}$: Fast jets from orifices

1 oxygen sensor in circumferential flow

1 oxygen sensor in core of global low-speed region

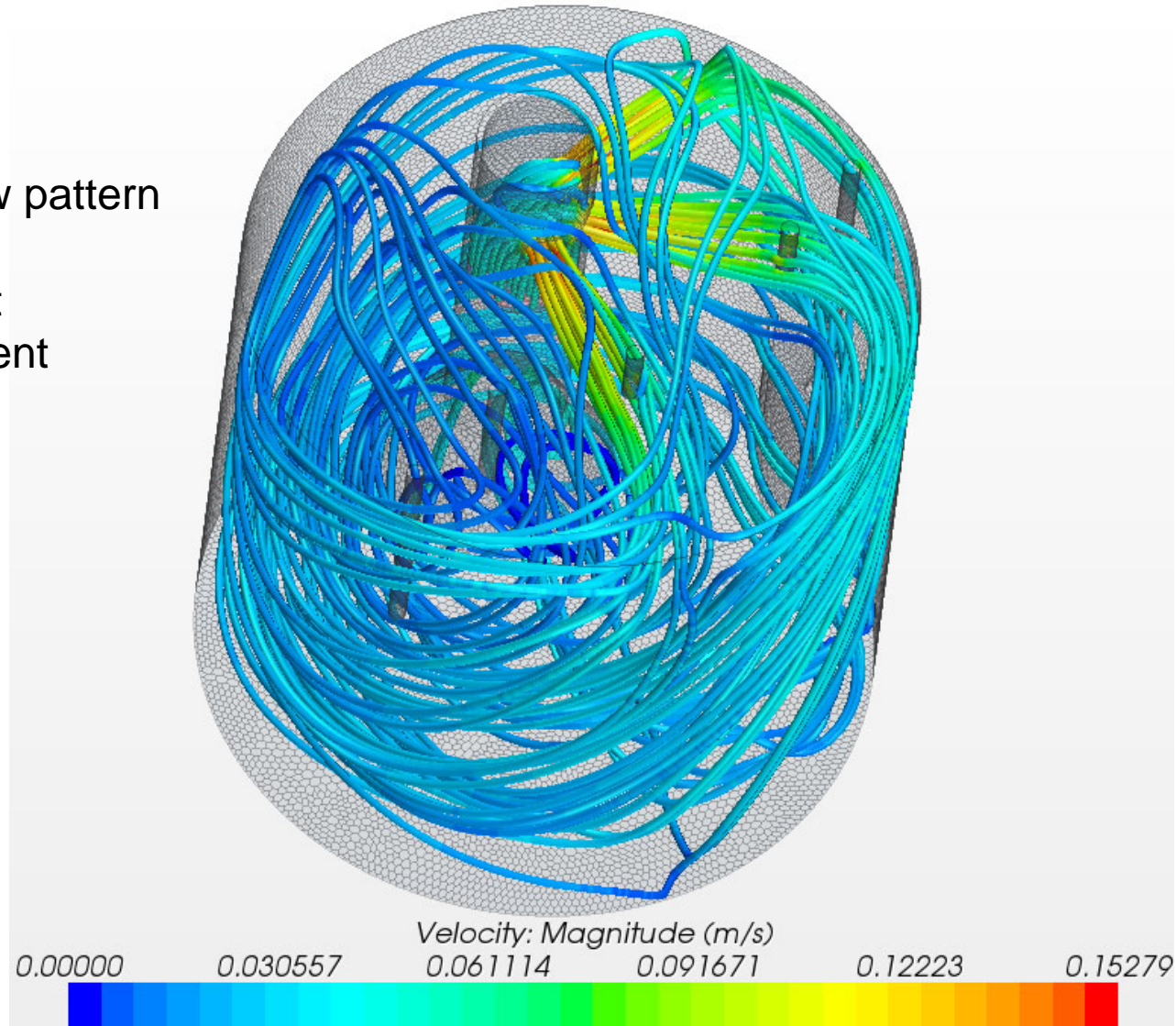
2 oxygen sensors in jets

1 oxygen sensor in dead water pocket



Main Flow Patterns, $T=400^{\circ}\text{C}$: Large scale circumferential flow structure

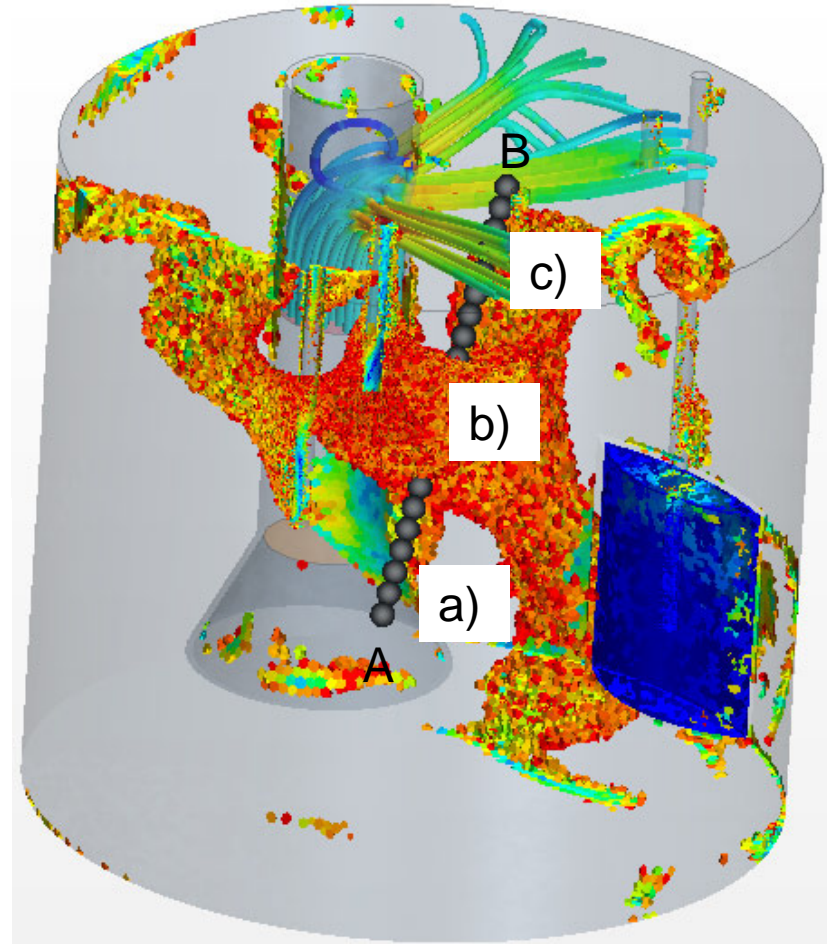
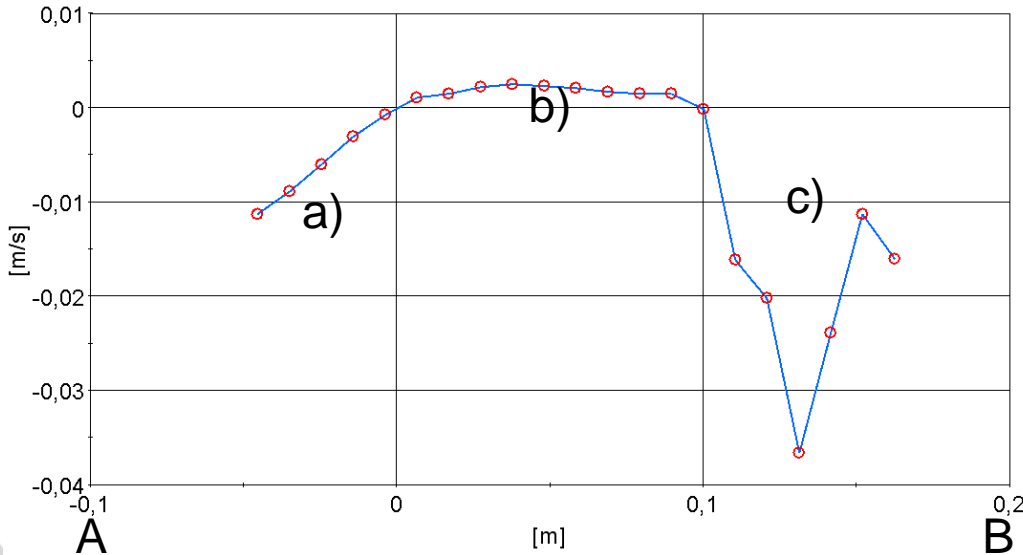
Stable circumferential flow pattern
Important for experiments
oxygen transport
Flow measurement
etc.



Main Flow Patterns, $T=400^{\circ}\text{C}$: Location of measurement lines of flow velocity by Ultrasonic Doppler Velocimetry UDV

Location of measurement line chosen according to following criteria:

- upwardly inclined direction (allowing escape of air bubbles)
- identification of
 - a) main circumferential flow velocity, direction is known
 - b) low speed region,
 - c) fast jet



Summary and next steps

- Pre-design ready - pots are manufactured
- CFD results in location of sensors and 1st design details
- „Internals“ can now be constructed

Next design relevant CFD calculations:

- Characterization of impeller and flow straightener:
homogeneity of flow, turbulence intensity, turbulent length scale
- Characterization of flow around oxygen sensors
(turbulent vortex street?)
- Unsteady simulations with time-resolved transport of dissolved species
from cover gas atmosphere
- Simulations including all internals and auxiliary hot tank with sacrificial
Ni probe

Thanks to my colleagues at KIT

C. Bruzzese – who did all the CFD calculations and prepared most of the slides,
A. Class, C. Schroer , F. Lang

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