

# Development of Phase Field Methods using OpenFOAM

## Part I: Method Development and Implementation

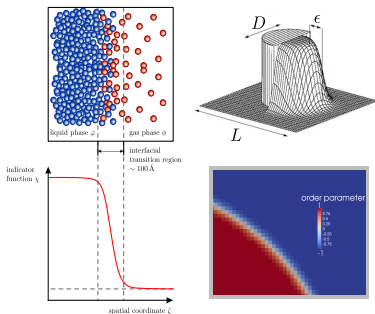


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Martin Wörner<sup>2</sup>, Olaf Deutschmann<sup>2</sup>

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Karlsruhe Institute of Technology

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10<sup>th</sup> OpenFOAM Workshop

June 29 – July 2, 2015 in Ann Arbor, Michigan, USA



Center of  
Smart Interfaces



### ► Today's Objectives

#### Executive Overview of

##### ► Numerical Modeling

(Allen-Cahn and Cahn-Hilliard in unified model framework)

- ▷ Consistent coupling to incompressible two-phase Navier-Stokes equations
- ▷ Enforcement of phase-volume conservation and boundedness (AC)
- ▷ Treatment of moving contact lines

##### ► Equation Discretization and Solution

- ▷ Enforcement of phase-volume conservation and boundedness (CH)
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##### ► Implementation into FOAM

##### ► Numerical Results

- ▷ Validation & Verification
- ▷ Wetting Physics (Xuan Cai, KIT Karlsruhe)



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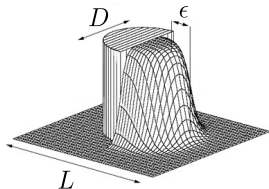
## Sharp vs. Diffuse Interface Modeling

### ► sharp interface models

- ▷ surface of zero thickness
- ▷ discontinuity/jump of material and transport quantities
- ▷ discontinuous phase indicator
- ▷ methods (main representatives):  
Volume-Of-Fluid / Level-Set  
Interface-Capturing, Arbitrary  
Lagrangian Eulerian Interface-Tracking,  
Front-Tracking Methods

### ► diffuse interface models

- ▷ surface of finite thickness
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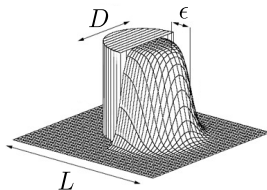


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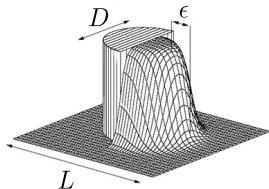


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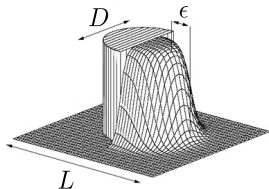
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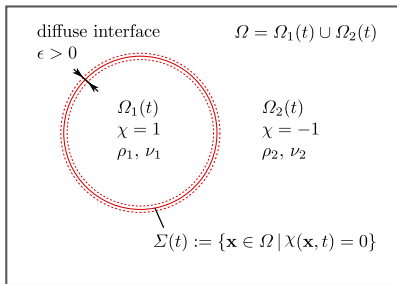


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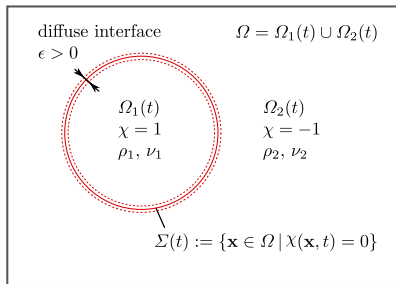


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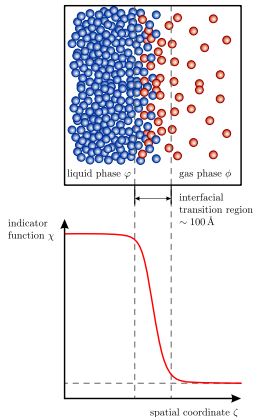
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  - ▷ connection to thermodynamics by a phenomenological free energy functional (model).
  - ▷ evolution of phase field governed by dissipative minimization of free energy.
- ▶ **Diffuse interface** represented as a finite thickness transition layer
  - ▷ characterized by capillary width  $\epsilon > 0$  (related to interfacial thickness)
  - ▷ diffusion of phase constituents within thin transition layer
  - ▷ fluid mixing (even for immiscible fluids) and interface evolution controlled by chemical potential
  - ▷ fluid properties vary rapidly but smoothly between fluids
- ▶ **Phase-field methods for two-phase flow**
  - ▷ pioneering work: Jacqmin <sup>[1]</sup>
  - ▷ two 'flavors': Cahn-Hilliard <sup>[2]</sup> or Allen-Cahn <sup>[3]</sup>



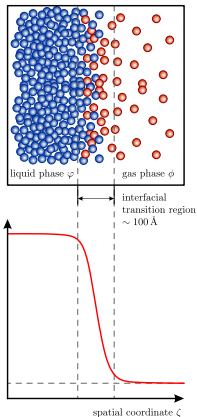
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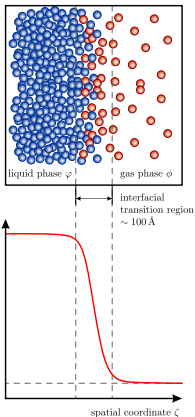
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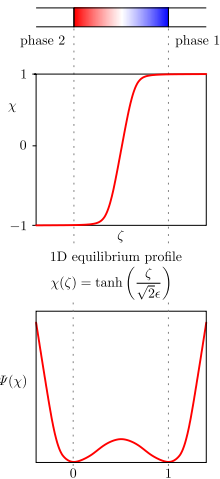
### ► Free energy

Free energy density model for mixing of the two-phase system

$$f(\chi) = \underbrace{\frac{\lambda}{2} |\nabla \chi|^2}_{\text{'gradient energy'}} + \underbrace{\frac{\lambda}{\epsilon^2} \Psi(\chi)}_{\text{bulk energy}}$$

where

- $\Psi(\chi) = (\chi^2 - 1)^2/4$ : bulk energy density (Ginzburg-Landau double-well functional)
  - $\Psi'(\chi) = \chi(\chi^2 - 1)$ : derivative of  $\Psi$  w.r.t.  $\chi$
  - $\Phi(\chi) = \delta F/\delta \chi$ , with  $F = \int_{\Omega} f dx$ : **chemical potential** (Cahn, 1961)
- Competition between bulk and capillary/interfacial (gradient) contribution 'controlling' surface tension and interfacial thickness.



# Introduction & Motivation V

## Diffuse Interface Models – Model Parameters



### ► Input model parameters (primary parameters)

- ▷ capillary width:  $\epsilon$
- ▷ mobility coefficient:  $\kappa$
- ▷ viscosities and densities:  $\bar{\rho}^\varphi$ ,  $\bar{\nu}^\varphi$
- ▷ surface tension coefficient:  $\sigma$

### ► Derived model parameters (secondary parameters)

- ▷ mixing energy parameter:  $\lambda = \frac{3}{2\sqrt{2}} \sigma \epsilon$ .
- ▷ relaxation time parameter:  $\gamma = \frac{\lambda \kappa}{\epsilon^2}$ .

```
-----
FoamFile
{
  version      2.0;
  format       ascii;
  class        dictionary;
  location     "constant";
  object       phaseFieldProperties;
}
// .....

diffuseInterface
{
  //- diffusion interface model
  type        CahnHilliard;
  type        AllenCahn;

  //- numerical method (CH only)
  method coupled;

  //- interfacial width
  epsilon     epsilon [ 0 1 0 0 0 0 0 ] 5e-5;

  //- mobility
  kappa       kappa [ -1 3 1 0 0 0 0 ] 10e-9;
}
// .....

}

gamma     gamma [ -1 3 1 0 0 0 0 ] 10e-9;
lambda    lambda [ 0 1 0 0 0 0 0 ] 5e-5;

```





- ▶ Starting Point: Generic structure of the phase-field equation [4,5]

$$\partial_t (\rho\chi) + \nabla \cdot (\rho\chi\mathbf{v} + \mathbf{J}_\chi) = \xi_\chi.$$

- ▶ This can be specified into Allen-Cahn- (AC) or Cahn-Hilliard-type (CH) models via choice of either the production rate  $\xi_\chi$  or flux  $\mathbf{J}_\chi$  being non-zero

$$\mathbf{J}_\chi \neq 0 \text{ and } \xi_\chi = 0 \text{ (CH)} \quad \text{and} \quad \mathbf{J}_\chi = 0 \text{ and } \xi_\chi \neq 0 \text{ (AC)}$$

- ▶ Volume-Averaging yields governing equations with  $C \equiv \bar{c} := \alpha_2 - \alpha_1$ .

[4] W. Dreyer, J. Giesselmann and C. Kraus, *Physica D: Nonlinear Phenomena* 273 (2014).

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$$\begin{aligned} \partial_t \bar{c} + \nabla \cdot (\bar{c} \bar{\mathbf{u}}) &= \frac{\lambda\kappa}{\epsilon^2} \nabla^2 \bar{c} - \frac{\lambda\kappa}{\epsilon^4} \Psi'(\bar{c}) && \text{in } \Omega \\ \partial_n \bar{c} &= -\frac{3}{4\lambda} \cos \theta_e (\bar{c}^2 - 1) \text{ and } \partial_n \Phi = 0 && \text{on } \partial\Omega \\ \bar{c}|_{t=0} &= \bar{c}_0 && \text{in } \Omega \text{ at } t = 0 \end{aligned}$$

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- ▶ Cahn-Hilliard phase-field equation

$$\partial_t \bar{c} + \nabla \cdot (\bar{c} \bar{\mathbf{u}}) = \kappa \nabla^2 \Phi(\bar{c}) \quad \text{with} \quad \Phi(\bar{c}) = \frac{\lambda}{\epsilon^2} \Psi'(\bar{c}) - \lambda \nabla^2 \bar{c} \quad \text{in } \Omega$$

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# Numerical Modeling II

## Coupling to Navier-Stokes Equation



- ▶ Cahn-Hilliard momentum equation with (non-standard) relative density flux due to diffusion of components [6,7]

$$\partial_t(\alpha_1 \bar{\rho}^k) + \nabla \cdot (\alpha_1 \bar{\rho}^k \bar{\mathbf{u}}) = -\nabla \cdot \mathbf{J}_k \quad \Leftrightarrow \quad \partial_t \alpha_1 + \nabla \cdot (\alpha_1 \bar{\mathbf{u}}) = -\nabla \cdot \left( \frac{\mathbf{J}_k}{\bar{\rho}^k} \right)$$

- ▶ From summation of the right equation for  $k = 1, 2$ , exploiting  $\alpha_1 + \alpha_2 \equiv 1$

$$\frac{\mathbf{J}_1}{\bar{\rho}^1} + \frac{\mathbf{J}_2}{\bar{\rho}^2} = 0, \quad \text{where } \mathbf{J}_k := \alpha_1 \bar{\rho}^1 (\bar{\mathbf{u}}^1 - \bar{\mathbf{u}}) + \bar{\mathbf{J}}_k,$$

i.e., insisting on volume conservation in the volume-averaged model, the volumetric diffusion fluxes are required to match – in the spirit of Cahn and Hilliard.

- ▶ Then, however, from summation of the left equation for  $k = 1, 2$ , the continuity equation becomes

$$\partial_t \bar{\rho} + \nabla \cdot (\bar{\rho} \bar{\mathbf{u}}) =: D_t \bar{\rho} = -\nabla \cdot (\mathbf{J}_1 + \mathbf{J}_2) \neq 0 \quad \text{in cases where } \bar{\rho}^1 \neq \bar{\rho}^2$$

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which allows for an objective <sup>[8]</sup> momentum flux tensor on r.h.s.

$$\sigma := \tilde{\sigma} + \bar{\mathbf{u}} (\mathbf{J}_1 + \mathbf{J}_2) = -p\mathbf{I} + \tau$$

- ▶ Then,

$$\partial_t(\bar{\rho} \bar{\mathbf{u}}) + \nabla \cdot (\bar{\rho} \bar{\mathbf{u}} \bar{\mathbf{u}}) - \bar{\mathbf{u}} [D_t \bar{\rho}] = -\nabla p + \nabla \cdot \tau - (\mathbf{J}_1 + \mathbf{J}_2) \cdot \nabla \bar{\mathbf{u}}$$

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$$\partial_t(\bar{\rho} \bar{\mathbf{u}}) + \nabla \cdot (\bar{\rho} \bar{\mathbf{u}} \bar{\mathbf{u}}) - \bar{\mathbf{u}} [D_t \bar{\rho}] = -\nabla p + \nabla \cdot \boldsymbol{\tau} - (\mathbf{J}_1 + \mathbf{J}_2) \cdot \nabla \bar{\mathbf{u}}$$

$$\Leftrightarrow \partial_t(\bar{\rho} \bar{\mathbf{u}}) + \nabla \cdot (\bar{\rho} \bar{\mathbf{u}} \bar{\mathbf{u}}) = -\nabla p + \nabla \cdot \boldsymbol{\tau} - \nabla \cdot (\bar{\mathbf{u}}(\mathbf{J}_1 + \mathbf{J}_2))$$

[8] H. Abels, H. Garcke and G. Grün, *Math. Models Methods Appl. Sci.* 22/3 (2012).





- ▶ Allen-Cahn phase-field equation with space-time dependent Lagrange multiplier concept [9] to enforce volume conserving property

$$\partial_t \bar{c} + \nabla \cdot (\bar{c} \bar{u}) = \gamma \Delta \bar{c} - \frac{\gamma}{\epsilon^2} \Psi'(\bar{c}) + \lambda(t) \Psi(\bar{c})$$

- ▷ Choose  $\lambda$  s.t. phase volumes are conserved, i.e.

$$\begin{aligned} \frac{d}{dt} \int_{\Omega} \bar{c} dx &= \int_{\Omega} \partial_t \bar{c} dx = 0 \\ &= \int_{\Omega} \left[ -\nabla \cdot (\bar{c} \bar{u}) + \gamma \Delta \bar{c} - \frac{\gamma}{\epsilon^2} \Psi'(\bar{c}) + \lambda(t) \Psi(\bar{c}) \right] dx \\ &= - \int_{\partial\Omega} \bar{c} \bar{u} \cdot \mathbf{n} ds + \gamma \int_{\partial\Omega} \mathbf{n} \cdot \nabla \bar{c} ds - \frac{\gamma}{\epsilon^2} \int_{\Omega} \Psi'(\bar{c}) dx + \lambda(t) \int_{\Omega} \Psi(\bar{c}) dx \end{aligned}$$

$$\Rightarrow \lambda(t) = \frac{\int_{\partial\Omega} \bar{c} \bar{u} \cdot \mathbf{n} ds - \gamma \int_{\partial\Omega} \mathbf{n} \cdot \nabla \bar{c} ds}{\int_{\Omega} \Psi(\bar{c}) dx} + \frac{\gamma/\epsilon^2 \int_{\Omega} \Psi'(\bar{c}) dx}{\int_{\Omega} \Psi(\bar{c}) dx}$$

[9] J. Kim, S. Lee and Y. Choi, *Int. J. Eng. Sci.* 84 (2014).



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$$\Rightarrow \lambda(t) = \frac{\int_{\partial\Omega} [\mathbf{n} \cdot (\bar{\mathbf{u}} \bar{c}) - \mathbf{n} \cdot \nabla \bar{c}] \, ds}{\int_{\Omega} \Psi(\bar{c}) \, d\mathbf{x}} + \frac{\gamma/\epsilon^2 \int_{\Omega} \Psi'(\bar{c}) \, d\mathbf{x}}{\int_{\Omega} \Psi(\bar{c}) \, d\mathbf{x}}$$

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# Equation Discretization and Solution I

## Enforcement of phase-volume conservation and boundedness (CH)



- ▶ approach: decompose 4<sup>th</sup> order Cahn-Hilliard phase-field transport equation into 2<sup>nd</sup> order Helmholtz-type equations and solve simultaneously.

- ▶ steps:

▶ use FEM's block-coupled matrix support

▶ approximate the phase-field transport equation

- ▶ starting point: semi-(time-)discretized form of Cahn-Hilliard transport equation [10,11]

$$\frac{\gamma_n \bar{c}^n - \gamma_o \bar{c}^o + \gamma_{oo} \bar{c}^{oo}}{\Delta t} + \nabla \cdot (\bar{c} \bar{u})^o$$
$$= \kappa \nabla^2 \left[ -\lambda \nabla^2 \bar{c}^n + \frac{\lambda}{\epsilon^2} ((\bar{c}^o)^2 - 1) \bar{c}^o + \gamma_n \frac{\lambda}{\epsilon^2} (\gamma_n \bar{c}^n - \gamma_o \bar{c}^o + \gamma_{oo} \bar{c}^{oo}) \right],$$

with the time-discretization dependent parameters  $\gamma_n = (1, 3/2)$ ,  $\gamma_o = (1, 2)$  and  $\gamma_{oo} = (0, 1/2)$  for Euler implicit and Gear's backward schemes, respectively.

[10] P. Yue et al., *J. Fluid Mech.* 515 (2004).

[11] S. Dong, *Comput. Methods App. Mech. Engrg.* 247–248 (2012).

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- ▶ Sorting: explicit (r.h.s.) and implicit (l.h.s.) terms

$$-\nabla^2 \left( \lambda \nabla^2 \bar{c}^n - \gamma_i \gamma_n \frac{\lambda}{\epsilon^2} \bar{c}^n \right) - \frac{\gamma_n}{\kappa \Delta t} \bar{c}^n = S_\Psi(\bar{c}^o, \bar{c}^{oo}),$$

where

$$S_\Psi(\bar{c}^o, \bar{c}^{oo}) := \frac{1}{\kappa} \left[ -\frac{\gamma_o}{\Delta t} \bar{c}^o + \frac{\gamma_{oo}}{\Delta t} \bar{c}^{oo} + \nabla \cdot (\bar{c} \bar{u})^o \right. \\ \left. - \frac{\lambda \kappa}{\epsilon^2} \nabla^2 \left( ((\bar{c}^o)^2 - 1 - \gamma_o \gamma_i) \bar{c}^o + \gamma_{oo} \gamma_i \bar{c}^{oo} \right) \right]$$

- ▶ Defining auxiliary variable for separation into two Helmholtz-type equations as

$$\Psi^n := \lambda \nabla^2 \bar{c}^n - \gamma_i \gamma_o \frac{\lambda}{\epsilon^2} \bar{c}^n,$$

we arrive at

PsiEqn :	$\nabla^2 \Psi^n + \frac{\gamma_o}{\kappa \Delta t} \bar{c}^n = -S_\Psi(\bar{c}^o, \bar{c}^{oo})$
CEqn :	$\nabla^2 \bar{c} - \frac{\Psi^n}{\lambda} = \frac{\gamma_i \gamma_o}{\epsilon^2} \bar{c}^n$



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### ► Assembling the coupled system

- improved implicitness compared to Dong<sup>[12]</sup> and Yue et al.<sup>[13]</sup> achieved by

$$S'_{\Psi}(\bar{c}^o, \bar{c}^{oo}) := \frac{1}{\kappa} \left[ -\frac{\gamma_o}{\Delta t} \bar{c}^o + (\gamma_i - 1/\Delta t) \gamma_{oo} \bar{c}^{oo} \right]$$

- finite volume notation of final coupled system

$$\left\{ \begin{array}{l} [\nabla \cdot (\nabla \{\Psi\})] + \left[ \frac{\gamma_n}{\kappa \Delta t} \{\bar{c}\} \right] \\ \quad + \left[ \nabla \cdot \left( \phi \{\bar{c}\}_{f(\phi, \Gamma, \gamma=0.75)} \right) \right] \\ \quad + [\nabla \cdot (\gamma(3\bar{c}^2 - 1 - \gamma_i \gamma_o) \nabla \{\bar{c}\})] = -S'_{\Psi} \\ [\nabla \cdot (\nabla \{\bar{c}\})] - \left[ \frac{1}{\lambda} \{\Psi\} \right] = \left[ \frac{\gamma_i \gamma_n}{\epsilon^2} \{\bar{c}\} \right] \end{array} \right.$$

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# Implementation into FOAM I

## Class overview and collaboration



- ▶ three main (base) classes
  - ▷ `diffuseInterfaceModels` holding `phaseFieldEquations`
  - ▷ `phaseContactAngle` holding `constantPhaseContactAngle` and `dynamicPhaseContactAngle`
  - ▷ `diffuseInterfaceProperties` providing mixture density and viscosity fields as well as derived (secondary) model parameters, i.e. mixing energy and relaxation time parameters
- ▶ Client point of view:
  - ▷ Top-Level Solver `phaseFieldFoam`
  - ▷ Dictionary `phaseFieldProperties`

```
=====
\ \ \ \ \ Field | foam-extend: Open Source CFD
\ \ \ \ \ Operation | For copyright notice see file Copyright
\ \ \ \ \ And
\ \ \ \ \ Manipulation
=====
FoamFile
{
    version      2.0;
    format       ascii;
    class        dictionary;
    location     "constant";
    object       phaseFieldProperties;
}
// .....

diffuseInterface
{
    //- diffusion interface model
    // type      CahnHilliard;
    // type      AllenCahn;

    //- numerical method (CH only)
    method coupled;

    //- interfacial width
    epsilon      epsilon [ 0 1 0 0 0 0 ] 5e-5;

    //- mobility
    kappa        kappa [ -1 3 1 0 0 0 ] 10e-9;
}
// .....
}

}
// .....
}
// .....
}
// .....
}
```



### Temporal Sub-cycling

- ▶ needed in segregated mode for solution of Cahn-Hilliard equation (chemical potential as auxiliary quantity):

$$\partial_t \bar{c} + \nabla \cdot (\bar{c} \bar{\mathbf{u}}) = \kappa \nabla^2 \Phi(\bar{c})$$

$$\text{with } \Phi(\bar{c}) = \frac{\lambda}{\epsilon^2} \Psi'(\bar{c}) - \lambda \nabla^2 \bar{c}$$

- ▶ mass-flux accumulation yields updated

$$\begin{aligned} F_m &\equiv \alpha_{1,f} \bar{\rho}^1 F_1 + \alpha_{2,f} \bar{\rho}^2 F_2 \\ &= \left( \frac{1 - \bar{c}}{2} \right)_f \bar{\rho}^1 F_1 + \left( \frac{1 + \bar{c}}{2} \right)_f \bar{\rho}^2 F_2 \\ &= \frac{\bar{\rho}^2 - \bar{\rho}^1}{2} (\bar{c})_f F_1 + \frac{\bar{\rho}^2 + \bar{\rho}^1}{2} F \end{aligned}$$

for discretized momentum equation (`rhoPhi`). Note:  $\alpha_{1,f} \bar{\rho}^1 F_1 \approx \alpha_{1,f} F$ .

implemented as

$$F_{m,\text{sum}} = \sum_{n_{\text{asc}}} \frac{\Delta t_{\text{asc}}}{\Delta t_{\text{total}}} F_{m,\text{asc}},$$

$$\text{with } \Delta t_{\text{asc}} \equiv \frac{\Delta t_{\text{total}}}{n_{\text{asc}}}$$



### Temporal Sub-cycling

- needed in segregated mode for solution of Cahn-Hilliard equation (chemical potential as auxiliary quantity):

$$\partial_t \bar{c} + \nabla \cdot (\bar{c} \bar{\mathbf{u}}) = \kappa \nabla^2 \Phi(\bar{c})$$

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# Implementation into FOAM II

## Top-level: Client/user interface



### Temporal Sub-cycling

- needed in segregated mode for solution of Cahn-Hilliard equation (chemical potential as auxiliary quantity):

$$\partial_t \bar{c} + \nabla \cdot (\bar{c} \bar{\mathbf{u}}) = \kappa \nabla^2 \Phi(\bar{c})$$

$$\text{with } \Phi(\bar{c}) = \frac{\lambda}{\epsilon^2} \Psi'(\bar{c}) - \lambda \nabla^2 \bar{c}$$

- mass-flux accumulation yields updated

$$\begin{aligned} F_{m,f} &\equiv \alpha_{1,f} \bar{\rho}^1 F_1 + \alpha_{2,f} \bar{\rho}^2 F_2 \\ &= \left( \frac{1 - \bar{c}}{2} \right)_f \bar{\rho}^1 F_1 + \left( \frac{1 + \bar{c}}{2} \right)_f \bar{\rho}^2 F_2 \\ &= \frac{\bar{\rho}^2 - \bar{\rho}^1}{2} (\bar{c})_f F_1 + \frac{\bar{\rho}^2 + \bar{\rho}^1}{2} F \end{aligned}$$

for discretized momentum equation (`rhoPhi`). Note:  $\alpha_{1,f} F_1 \approx \alpha_{1,f} F$ .

implemented as

$$F_{m,\text{sum}} = \sum_{n_{\text{asc}}} \frac{\Delta t_{\text{asc}}}{\Delta t_{\text{total}}} F_{m,\text{asc}},$$

$$\text{with } \Delta t_{\text{asc}} \equiv \frac{\Delta t_{\text{total}}}{n_{\text{asc}}}$$

```
phaseFieldEqn.H
{
    label nSubCycles
    (
        readLabel(piso.lookup("nSubCycles"))
    );

    if (nSubCycles > 1)
    {
        dimensionedScalar totalDeltaT = runtime.deltaT();
        surfaceScalarField rhoPhiSum = 0.0*rhoPhi;

        for
        (
            subCycle<volScalarField> CSubCycle(C, nSubCycles);
            !(++CSubCycle).end();
        )
        {
            // Solve the phase field equation
            // Update and return mass flux field
            rhoPhi = phaseField.solve(C, Phi);
            rhoPhiSum += (runtime.deltaT()/totalDeltaT)*rhoPhi;
        }
        rhoPhi = rhoPhiSum;
    }
    else
    {
        rhoPhi = phaseField.solve(C, Phi);
    }
}

diffuseInterface.updateProperties(rho, mu);
```

# Implementation into FOAM III

## Top-level: Client/user interface



- ▶ Relative density flux due to diffusion of components (with matching volumetric diffusion fluxes – in the spirit of Cahn and Hilliard) as consequence of solenoidal condition ( $\nabla \cdot \mathbf{u} = 0$ ):

$$\partial_t(\bar{\rho} \bar{\mathbf{u}}) + \nabla \cdot (\bar{\rho} \bar{\mathbf{u}} \bar{\mathbf{u}}) \\ = -\nabla p + \nabla \cdot \boldsymbol{\tau} - \nabla \cdot (\bar{\mathbf{u}}(\mathbf{J}_1 + \mathbf{J}_2))$$

- ▶ Consistency of the Allen-Cahn diffuse interface model requires a source term in the pressure equation.

part of UEqn.H

```
surfaceScalarField muf = diffuseInterface.muf();

fvVectorMatrix UEqn
(
    fvm::ddt(rho, U)
    + fvm::div(rhoPhi, U)
    - fvm::laplacian(mu, U)
    - (fvc::grad(U) & fvc::grad(mu))

    //-HM Relative density flux
    //- due to diffusion of components
    //- Abels et al. (arXiv:1011.0528, 2010)
    //- Ding et al. (JCOMP, 226, 2007)
    - phaseField.diffRhoPhi(U)

    //-HM Rhie-Chow interpolation practice
    //- buoyancy and surface tension term
    //- transferred to pressure equation
);
```

part of pEqn.H

```
for(int nonOrth=0; nonOrth<=nNonOrthCorr; nonOrth++)
{
    fvScalarMatrix pdEqn
    (
        fvm::laplacian(rUAF, pd)
        == fvc::div(phi) + phaseField.massSource(C)
    );

    //[...]
}
```

# Implementation into FOAM III

## Top-level: Client/user interface



- ▶ Relative density flux due to diffusion of components (with matching volumetric diffusion fluxes – in the spirit of Cahn and Hilliard) as consequence of solenoidal condition ( $\nabla \cdot \mathbf{u} = 0$ ):

$$\partial_t(\bar{\rho} \bar{\mathbf{u}}) + \nabla \cdot (\bar{\rho} \bar{\mathbf{u}} \bar{\mathbf{u}}) \\ = -\nabla p + \nabla \cdot \boldsymbol{\tau} - \nabla \cdot (\bar{\mathbf{u}} (\mathbf{J}_1 + \mathbf{J}_2))$$

- ▶ Consistency of the Allen-Cahn diffuse interface model requires a source term in the pressure equation.

part of UEqn.H

```
surfaceScalarField muf = diffuseInterface.muf();

fvVectorMatrix UEqn
(
    fvm::ddt(rho, U)
    + fvm::div(rhoPhi, U)
    - fvm::laplacian(mu, U)
    - (fvc::grad(U) & fvc::grad(mu))

    //-HM Relative density flux
    //- due to diffusion of components
    //- Abels et al. (arXiv:1011.0528, 2010)
    //- Ding et al. (JCOMP, 226, 2007)
    - phaseField.diffRhoPhi(U)

    //-HM Rhie-Chow interpolation practice
    //- buoyancy and surface tension term
    //- transferred to pressure equation
);
```

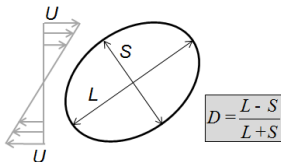
part of pEqn.H

```
for(int nonOrth=0; nonOrth<=nNonOrthCorr; nonOrth++)
{
    fvScalarMatrix pdEqn
    (
        fvm::laplacian(rUAf, pd)
        == fvc::div(phi) + phaseField.massSource(C)
    );

    //[...]
}
```

# Results: Validation & Verification I

## Test case I – Drop deformation in shear flow



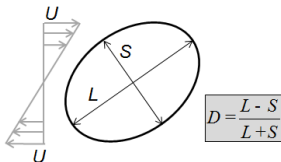
Drop deformation in shear flow

- ▶ Analytical solution <sup>[14]</sup> relates deformation parameter  $D$  to Capillary number  $Ca$ .  
(Assumptions: matching  $\nu$ ,  $\rho$  and creeping unbounded flow)
- ▶ Validation test for implementation of interfacial energy density (surface tension)
- ▶ Verification test for phase-volume conservation and boundedness

[14] G.I. Taylor, *Proc. R. Soc. London, Ser. A* 146 (1934).

# Results: Validation & Verification I

## Test case I – Drop deformation in shear flow



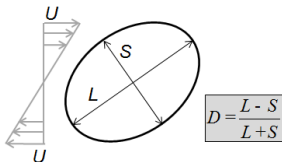
Drop deformation in shear flow

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[14] G.I. Taylor, *Proc. R. Soc. London, Ser. A* 146 (1934).

# Results: Validation & Verification I

## Test case I – Drop deformation in shear flow



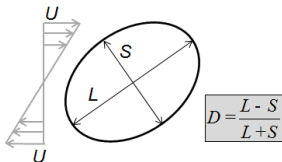
Drop deformation in shear flow

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- ▶ Validation test for implementation of interfacial energy density (surface tension)
- ▶ Verification test for phase-volume conservation and boundedness

[14] G.I. Taylor, *Proc. R. Soc. London, Ser. A* 146 (1934).

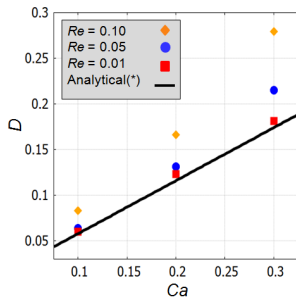
# Results: Validation & Verification I

## Test case I – Drop deformation in shear flow



Drop deformation in shear flow

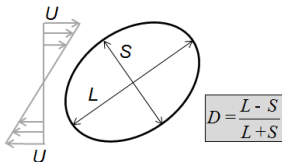
- ▶ Analytical solution <sup>[14]</sup> relates deformation parameter  $D$  to Capillary number  $Ca$ .  
(Assumptions: matching  $\nu, \rho$  and creeping unbounded flow)
- ▶ **Validation test for implementation of interfacial energy density (surface tension)**
- ▶ **Verification test for phase-volume conservation and boundedness**



[14] G.I. Taylor, *Proc. R. Soc. London, Ser. A* 146 (1934).

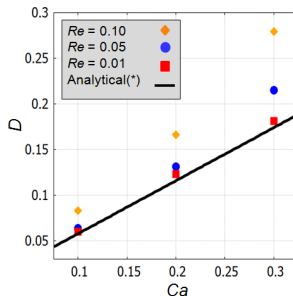
# Results: Validation & Verification I

## Test case I – Drop deformation in shear flow



Drop deformation in shear flow

- ▶ Analytical solution <sup>[14]</sup> relates deformation parameter  $D$  to Capillary number  $Ca$ .  
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- ▶ **Verification test for phase-volume conservation and boundedness**

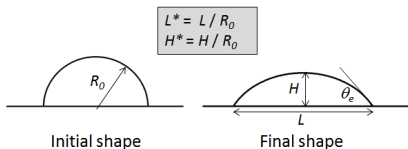


model / method	$\Delta e_b$	$\Delta e_v / \%$
Allen-Cahn	$0.000E-12$	$3.054E-09$
Cahn-Hilliard / segregated	$3.900E-03$	$1.211E-06$
Cahn-Hilliard / coupled	$3.149E-04$	$4.036E-06$

Tab.: Phase-volume conservation and bounded properties.

[14] G.I. Taylor, *Proc. R. Soc. London, Ser. A* 146 (1934).

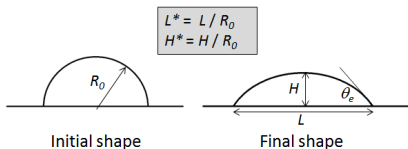




- ▶ Analytical solution [15,16] for  $E_0 \ll 1$  (droplet shape is controlled by the capillary force) and  $E_0 \gg 1$  (droplet shape is controlled by the gravity force)
- ▶ Validation test for implementation of (static) contact angle boundary condition
- ▶ Verification test for phase-volume conservation and boundedness

[15] Y. Chen, R. Mertz and R. Kulenovic, *Int. J. Multiphase Flow* 35/1 (2009).

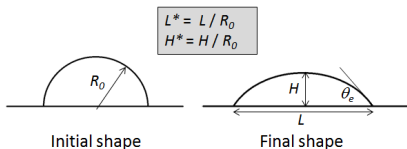
[16] J.-B. Dupont and D. Legendre, *J. Comput. Phys.* 229 (2010).



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[16] J.-B. Dupont and D. Legendre, *J. Comput. Phys.* 229 (2010).



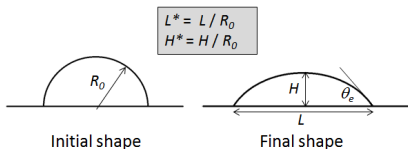
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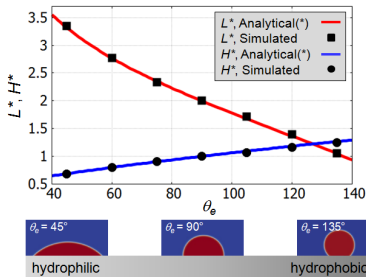
[16] J.-B. Dupont and D. Legendre, *J. Comput. Phys.* 229 (2010).

# Results: Validation & Verification II

## Test case II – Capillarity-driven Droplet Spreading / Dewetting



- ▶ Analytical solution [15,16] for  $Eo \ll 1$  (droplet shape is controlled by the capillary force) and  $Eo \gg 1$  (droplet shape is controlled by the gravity force)
- ▶ **Validation test for implementation of (static) contact angle boundary condition**
- ▶ Verification test for phase-volume conservation and boundedness

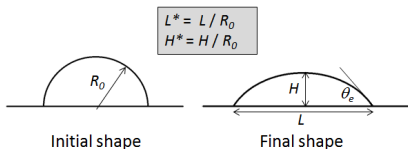


[15] Y. Chen, R. Mertz and R. Kulenovic, *Int. J. Multiphase Flow* 35/1 (2009).

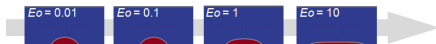
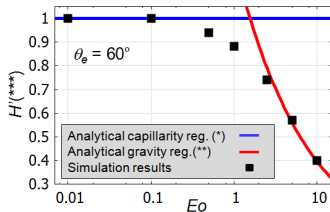
[16] J.-B. Dupont and D. Legendre, *J. Comput. Phys.* 229 (2010).

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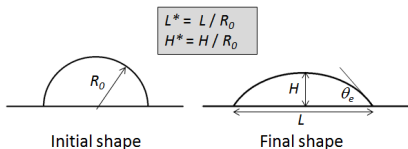


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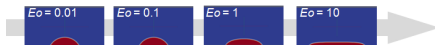
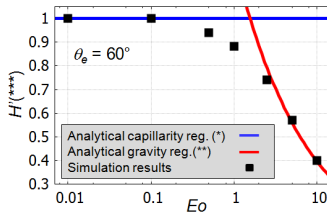
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# Results: Validation & Verification II

## Test case II – Capillarity-driven Droplet Spreading / Dewetting



- ▶ Analytical solution [15,16] for  $Eo \ll 1$  (droplet shape is controlled by the capillary force) and  $Eo \gg 1$  (droplet shape is controlled by the gravity force)
- ▶ Validation test for implementation of (static) contact angle boundary condition
- ▶ **Verification test for phase-volume conservation and boundedness**



model / method	$\Delta e_b$	$\Delta e_v / \%$
Allen-Cahn	$1.000E-11$	$1.076E-06$
Cahn-Hilliard / segregated	$2.577E-03$	$1.018E-09$
Cahn-Hilliard / coupled	$1.253E-03$	$8.230E-07$

Tab.: Phase-volume conservation and bounded properties.

[15] Y. Chen, R. Mertz and R. Kulenovic, *Int. J. Multiphase Flow* 35/1 (2009).

[16] J.-B. Dupont and D. Legendre, *J. Comput. Phys.* 229 (2010).



### Summary

- ▶ Consistent coupling to incompressible two-phase Navier-Stokes equations.
- ▶ Enforcement of phase-volume conservation and boundedness.
- ▶ Quantitative validation of phase-field methods based on Allen-Cahn and Cahn-Hilliard diffuse interface models.
- ▶ Quantitative verification on phase-volume conservation and boundedness properties (ongoing work).

### Outlook

- ▶ Release of the source to `foam-extend`.



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- ▶ **Prof. Dr. Hrvoje Jasak** and **Vuko Vukčević** (Faculty of Mechanical Engineering, University of Zagreb; Wikki Limited)
- ▶ **Klas Jareteg** (Department of Applied Physics, Chalmers University of Technology)
- ▶ **Ivor Clifford** (The Idaho National Laboratory, The Pennsylvania State University)
- ▶ **Helmut Abels** (Faculty of Mathematics, University of Regensburg)



## Closing II

### Acknowledgements...



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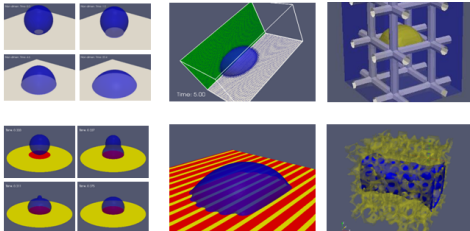
- ▶ **Prof. Dr. Hrvoje Jasak** and **Vuko Vukčević** (Faculty of Mechanical Engineering, University of Zagreb; Wikki Limited)
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- ▶ **Helmut Abels** (Faculty of Mathematics, University of Regensburg)

**Thank You for Your Attention!**

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## Thank You for Your Attention!





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