

# Development of Phase Field Methods using OpenFOAM® Part II: Application to Complex Wetting Physics

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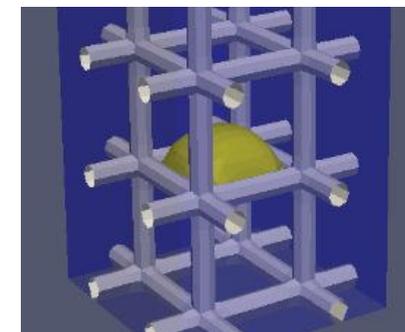
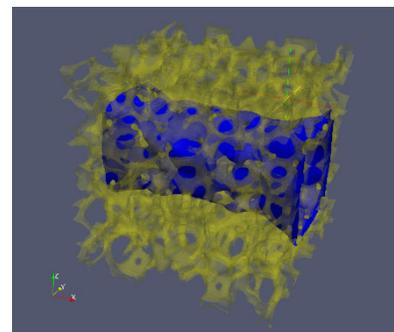
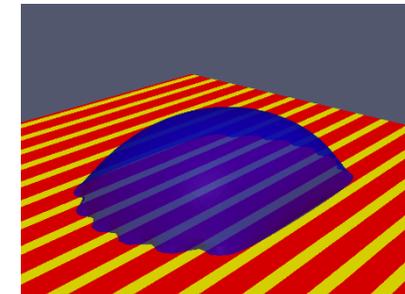
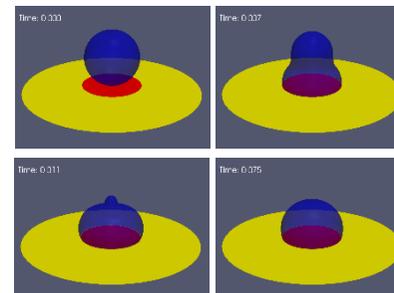
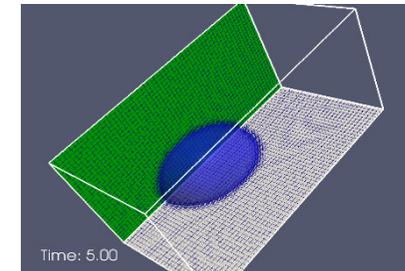
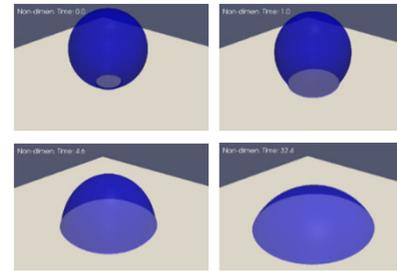
<sup>2</sup> Technische Universität Darmstadt, Germany

10th OpenFOAM® Workshop, June 29 – July 2, 2015 in Ann Arbor, Michigan, USA



# Outline

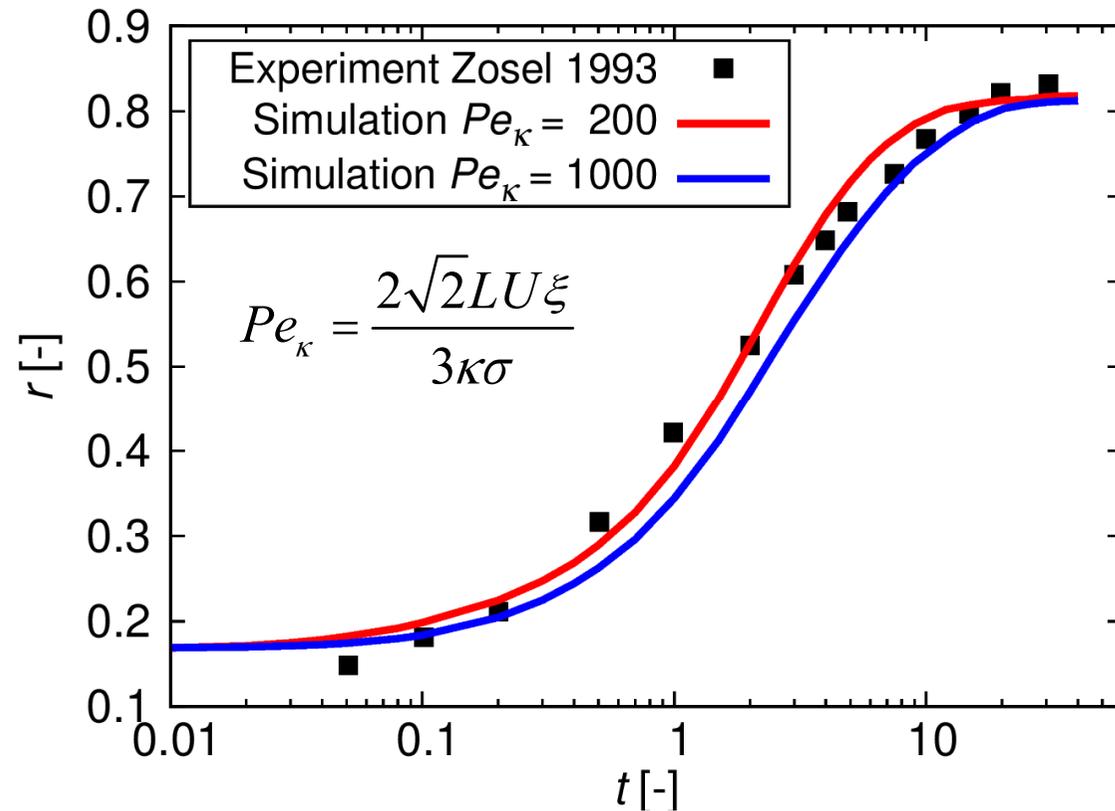
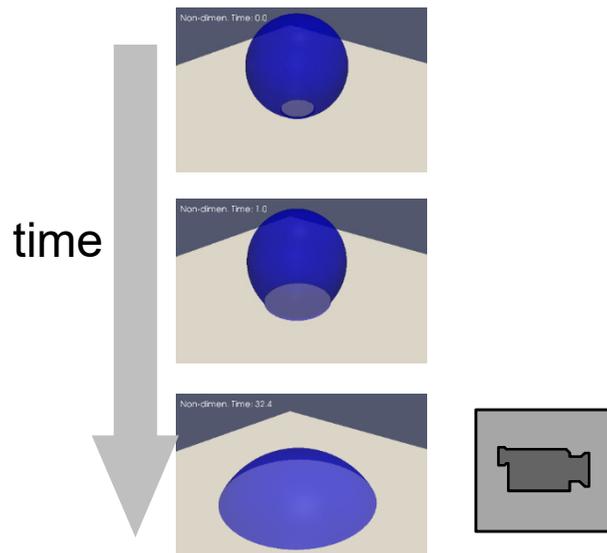
- Droplet spreading/sliding on flat/inclined surface
- Wetting on chemically heterogeneous surface
- Two-phase flows in sponge (foam) structure
- Rising bubble interacting with solid cell structure



# Droplet Spreading on Flat Surface

## Experiment by Zosel 1993

- PIB solution  $\mu = 25 \text{ pa}\cdot\text{s}$
- on smooth flat PTFE surface
- contact angle  $\theta_e = 58^\circ$
- $R_0 = 1.2 \sim 1.5 \text{ mm}$

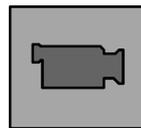


Zosel, A., Studies of the Wetting Kinetics of Liquid-Drops on Solid-Surfaces. Colloid Polym Sci, 1993. 271(7): p. 680-687.

# Rapid Wetting on Initial Spreading Stage

- Equilibrium contact angle BC

$$\mathbf{n} \cdot \nabla C + \frac{3}{4\lambda} \sigma \cos \theta_e (C^2 - 1) = 0$$



- Dynamic contact angle model for energy relaxation (Jacqmin 2000)

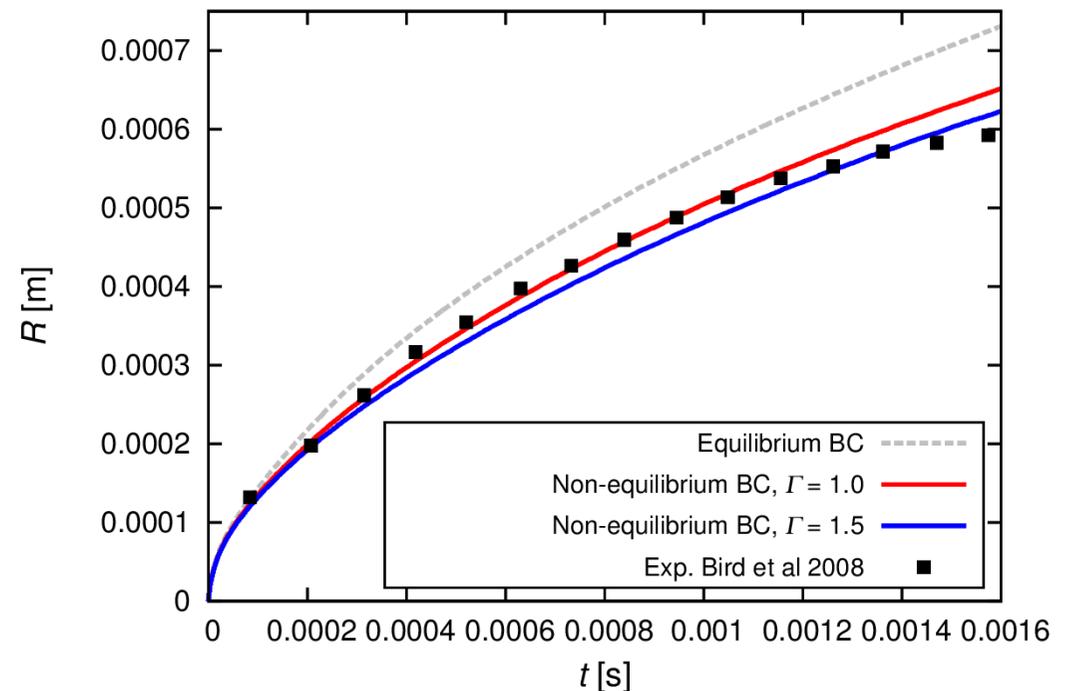
- Finite area method

$$\mathbf{n} \cdot \nabla C + \frac{3}{4\lambda} \sigma \cos \theta_e (C^2 - 1) = -\Gamma \left( \frac{\partial C}{\partial t} + \mathbf{u}_w \cdot \nabla C \right)$$

- Yue 2011 provides a guideline on how to choose  $\Gamma$

- $\Gamma = 1 \sim 1.5$  should produce best-fit with exp. data. → **Confirmed!**

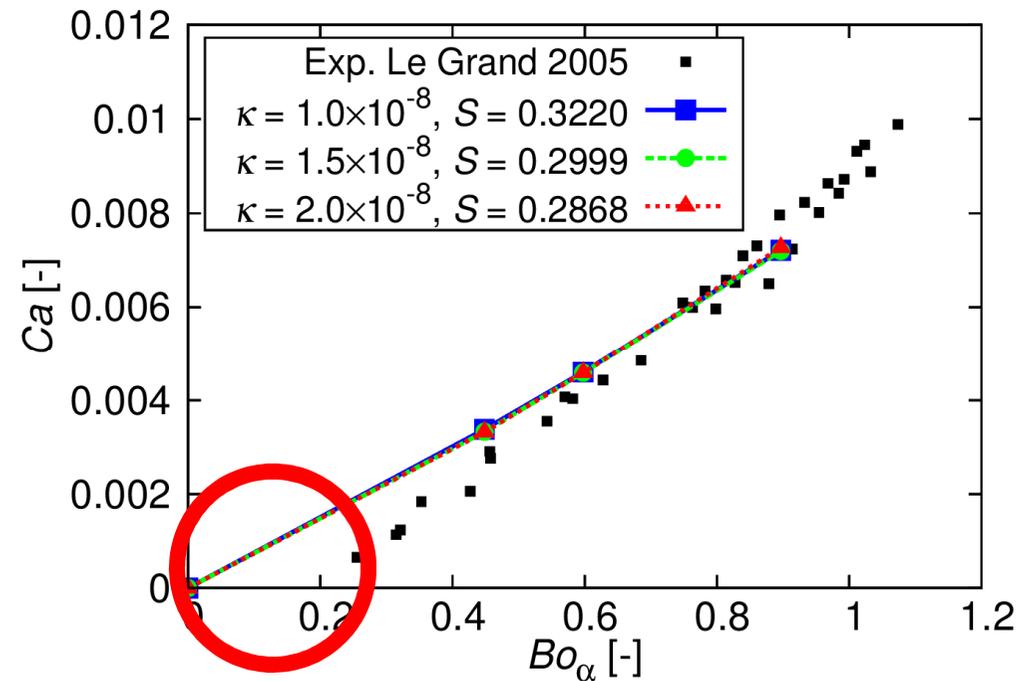
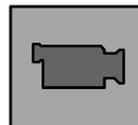
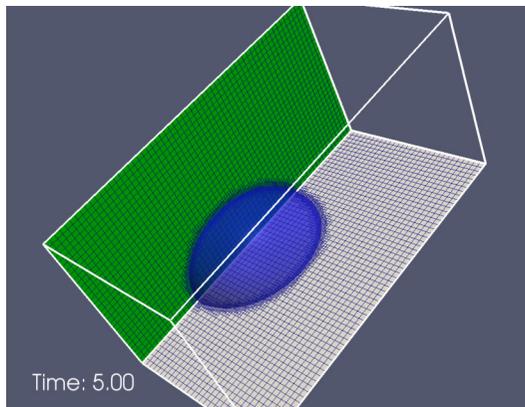
Sim. on 2D Axisymmetric Static Mesh



# Droplet Sliding on Inclined Surface

## ■ Experiment by Le Grand et al. 2005

- Droplet of silicon oil
- Surface is inclined ( $7^\circ < \alpha < 52^\circ$ )
- Contact angle  $\theta_e = 52^\circ$
- Droplet volume =  $6 \text{ mm}^3$



$$Ca = \frac{\eta U}{\sigma} \quad Bo_\alpha = V^{2/3} \left( \frac{\rho g}{\sigma} \right) \sin \alpha$$

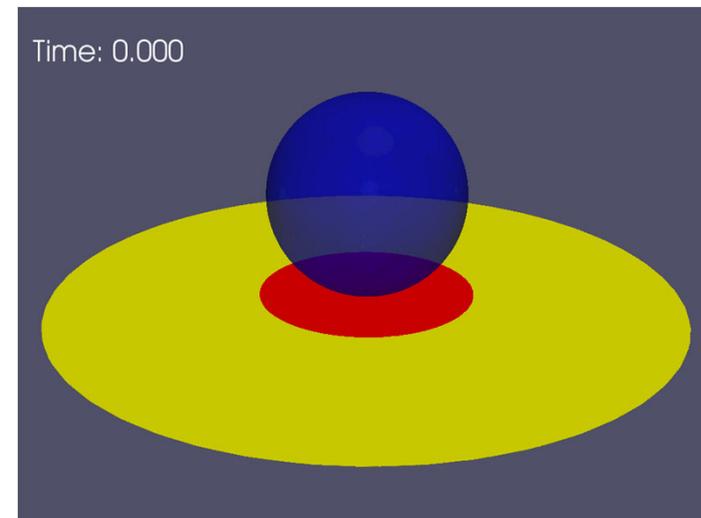
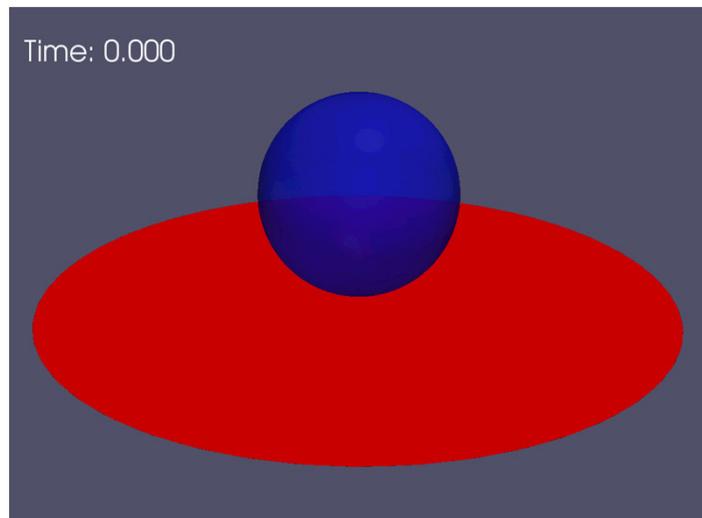
- Pinning effect (contact angle hysteresis)
- Our numerical modeling is under way

# Spreading on Chemically Heterogeneous Surface

- Water droplets (initial radius: 1 mm) jetted onto circular chemically-patterned surface:

$$\theta_e = 60^\circ \text{ Hydrophilic} \quad \theta_e = 120^\circ \text{ Hydrophobic}$$

- Effect of surface pattern (impact velocity: 0 m/s)



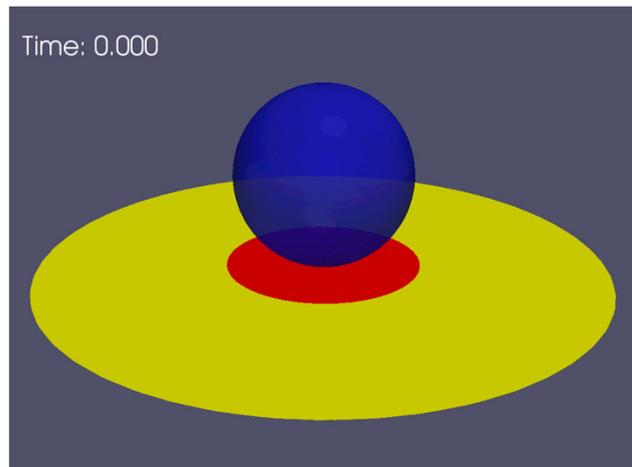
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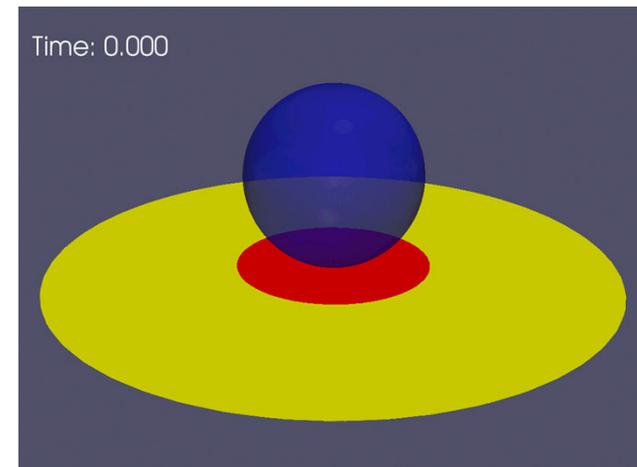
$\theta_e = 60^\circ$  Hydrophilic    $\theta_e = 120^\circ$  Hydrophobic

- Effect of droplet impact velocity ( $U_i$ )

$U_i = 0.5$  m/s



$U_i = 1.0$  m/s



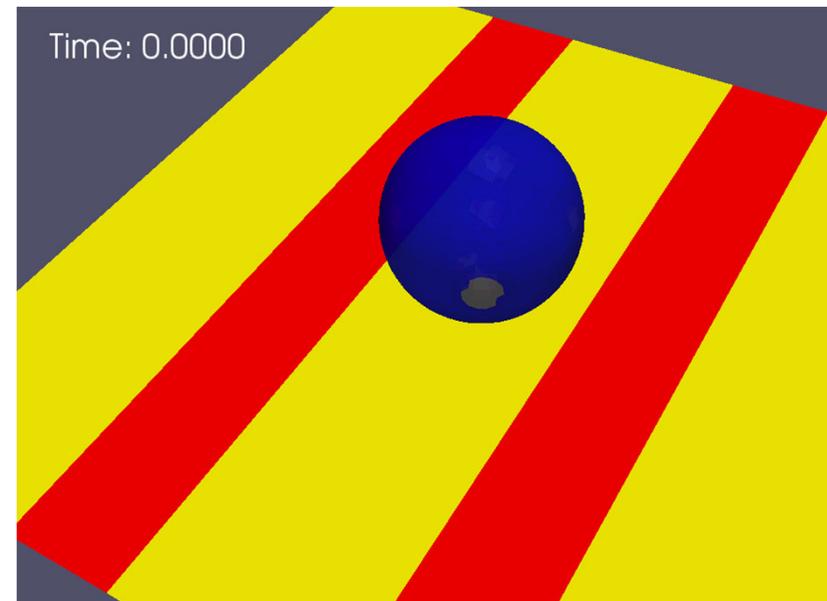
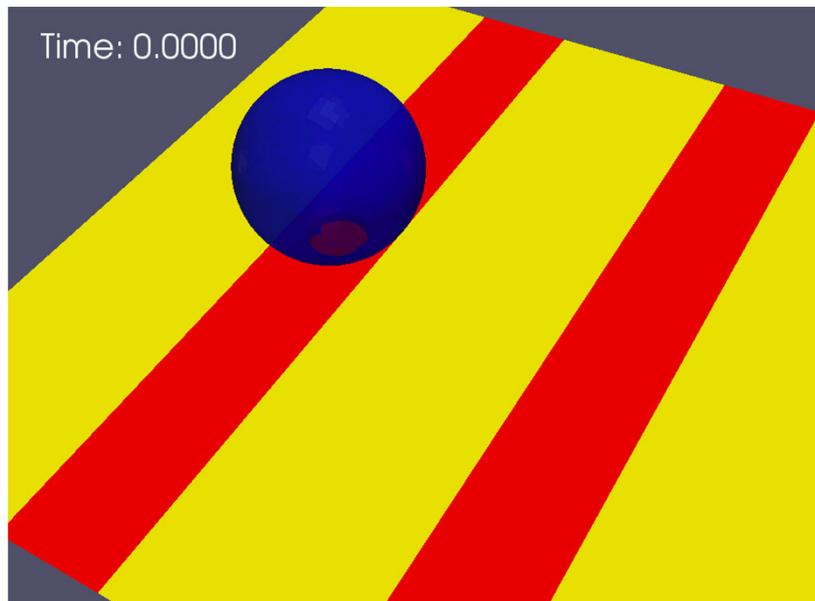
# Spreading on Chemically Heterogeneous Surface

- Experiment by Léopoldès et al. 2003

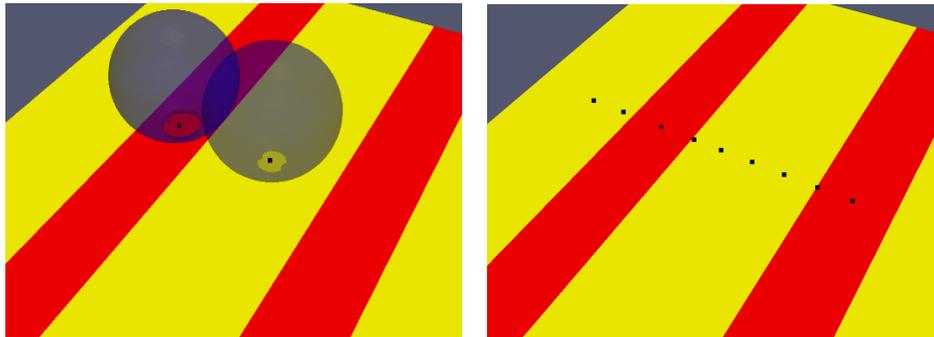
- Inkjet droplets (initial radius =  $11\ \mu\text{m}$ )

- released onto rectangular patterned surface:

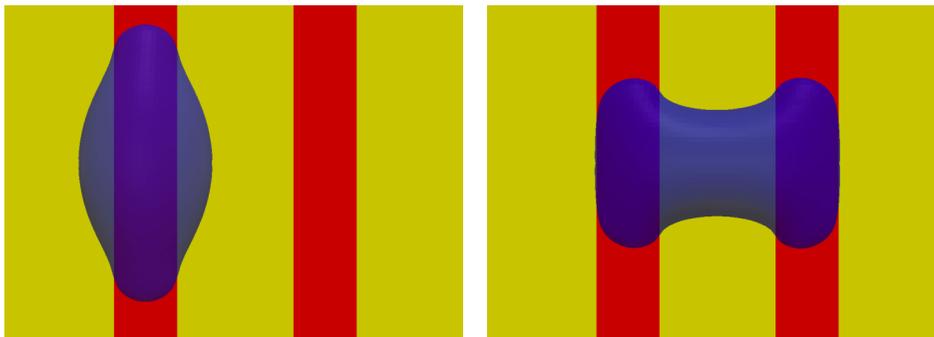
$\theta_e = 20^\circ$     $\theta_e = 64^\circ$



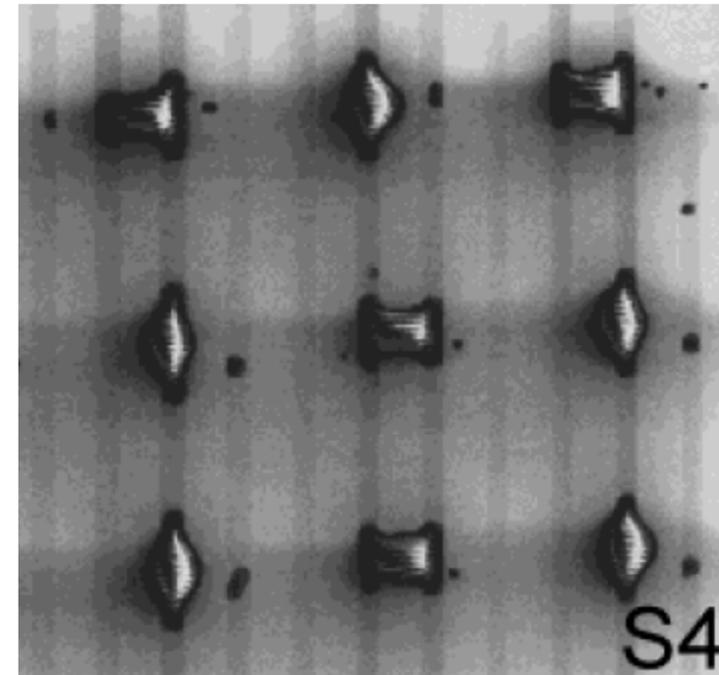
# Spreading on Chemically Heterogeneous Surface



Different initial impact points



Final droplet shapes

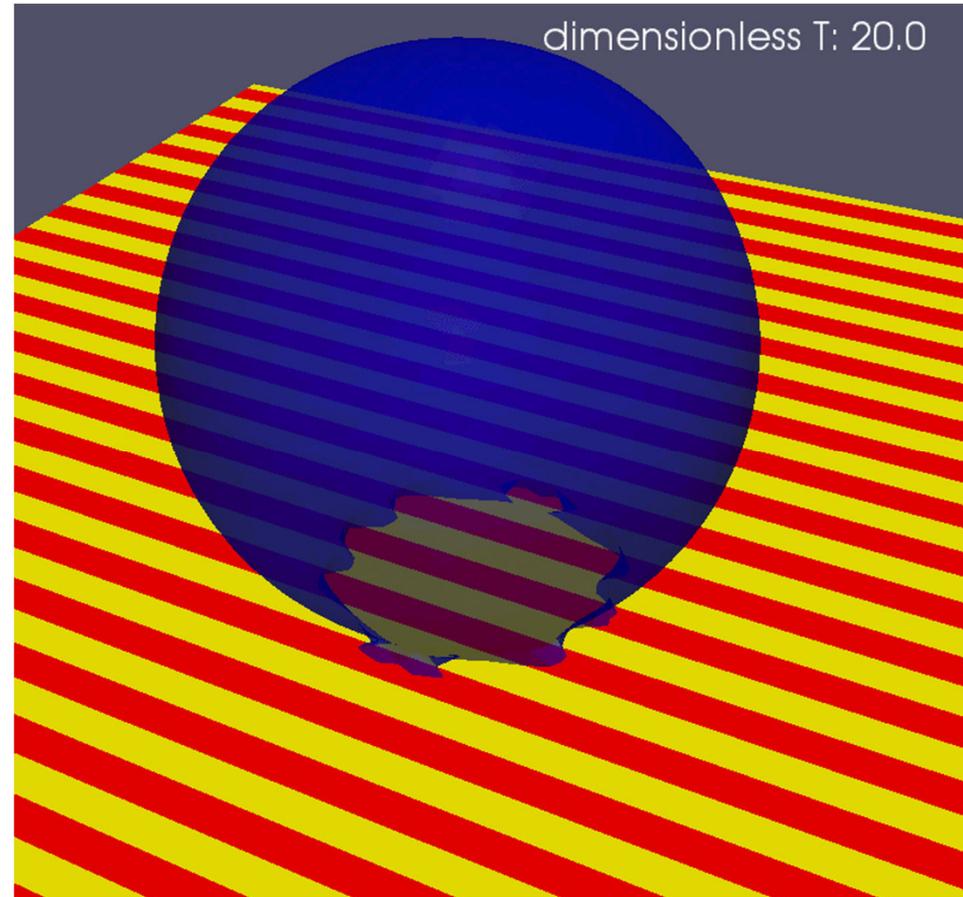
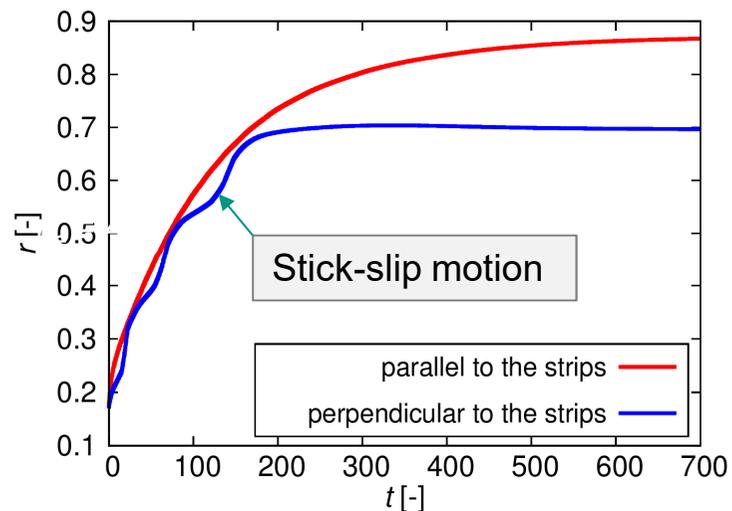


Experimental observation on final droplet shapes using scanning electron microscope (source: Léopoldès at al. 2003)

# Spreading on Chemically Heterogeneous Surface

- Experiment by Jansen et al. 2013
- Alternating stripes made of:

SiO <sub>2</sub> , $\theta_e = 40^\circ$
PFDTs, $\theta_e = 106^\circ$

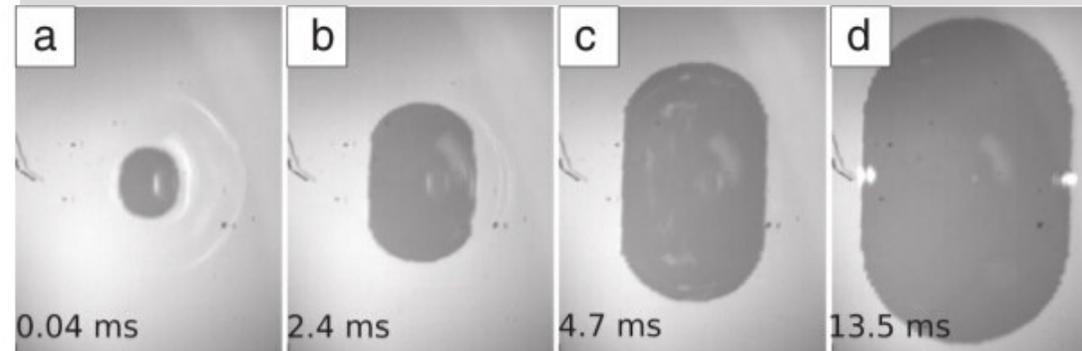


H.P. Jansen et al., Lattice Boltzmann modeling of directional wetting: comparing simulations to experiments, Phys. Rev. E 88 (2013) 013008–013017.

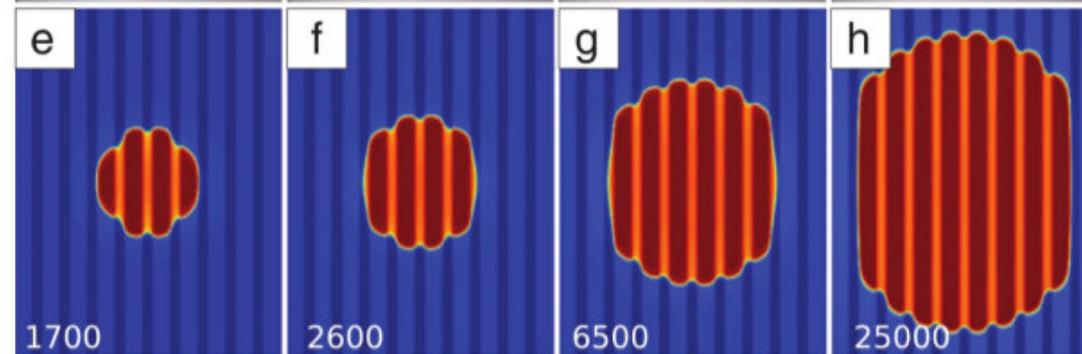
# Bottom View

Time

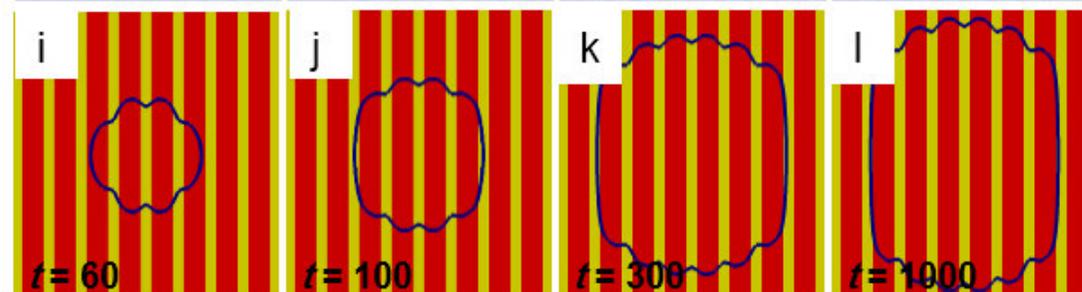
Experiment  
Jansen et al. 2013



Lattice-Boltzmann  
simulation  
Jansen et al. 2013

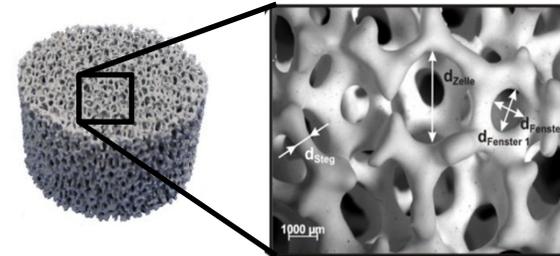


Our simulation  
(four cells per stripe)

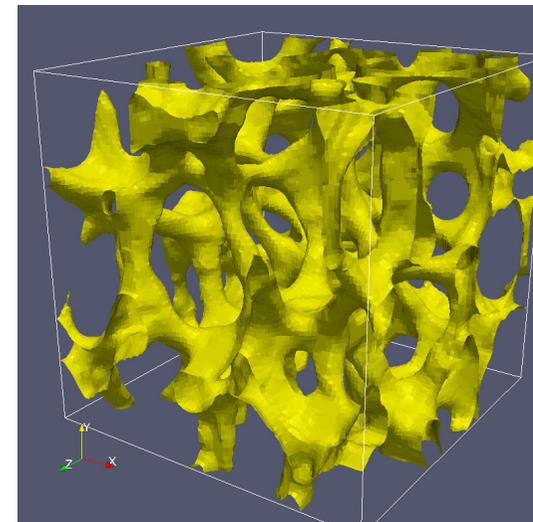


# Two Phase Flow in Sponge (Foam) Structure

- Institute of Thermal Process, KIT provides the sponge geometry
    - ( $\mu$ )CT scanings
    - reconstruction of sponge structure in MATLAB produces STL file
  - calculations on exemplary sponge sample type:
    - $\text{Al}_2\text{O}_3$
    - porosity = 80%
    - 20 pores per inch (ppi)
- investigations on SiSiC sponge ongoing
- *blockMesh* + *snappyHexMesh*



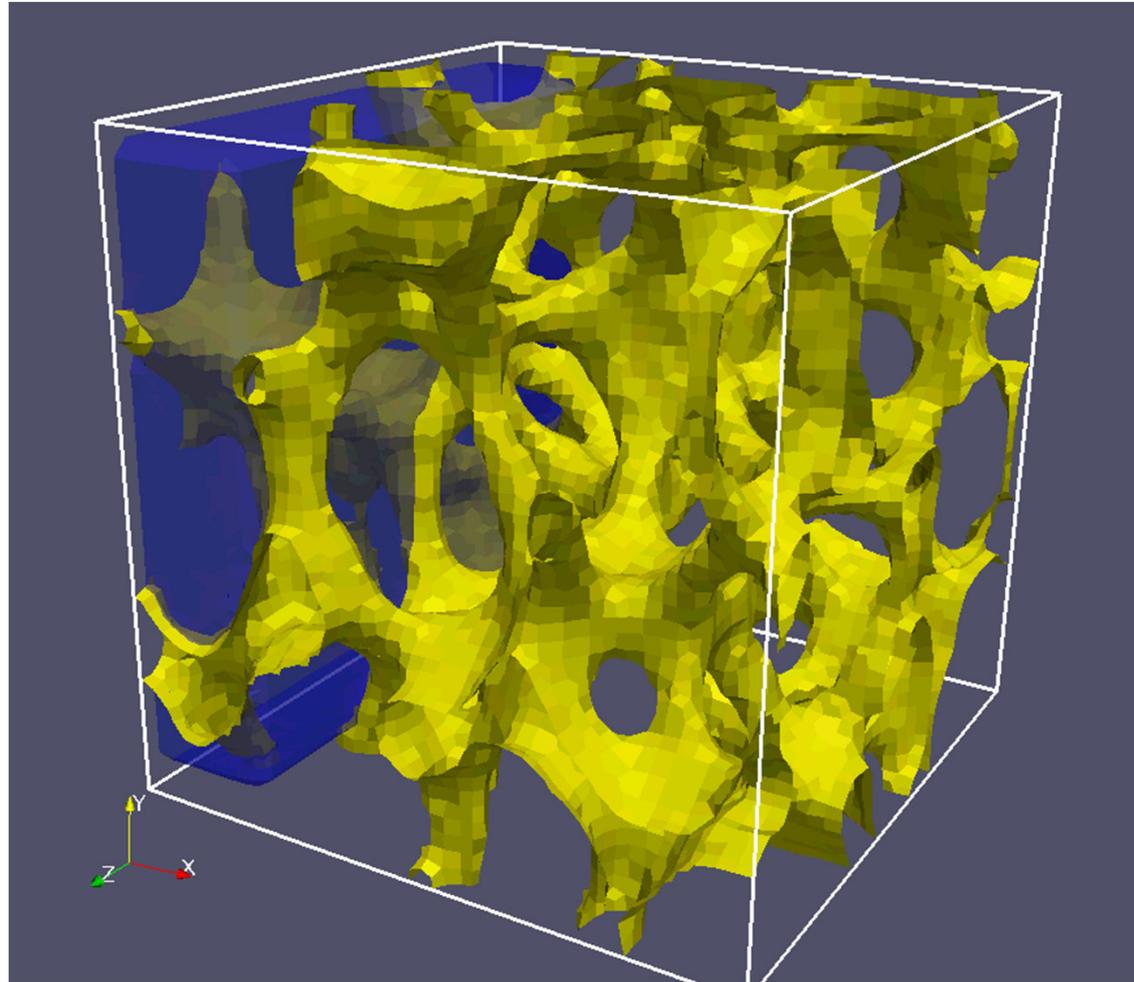
solid sponge chemical reactor



Representative Elementary  
Volume (REV) for CFD

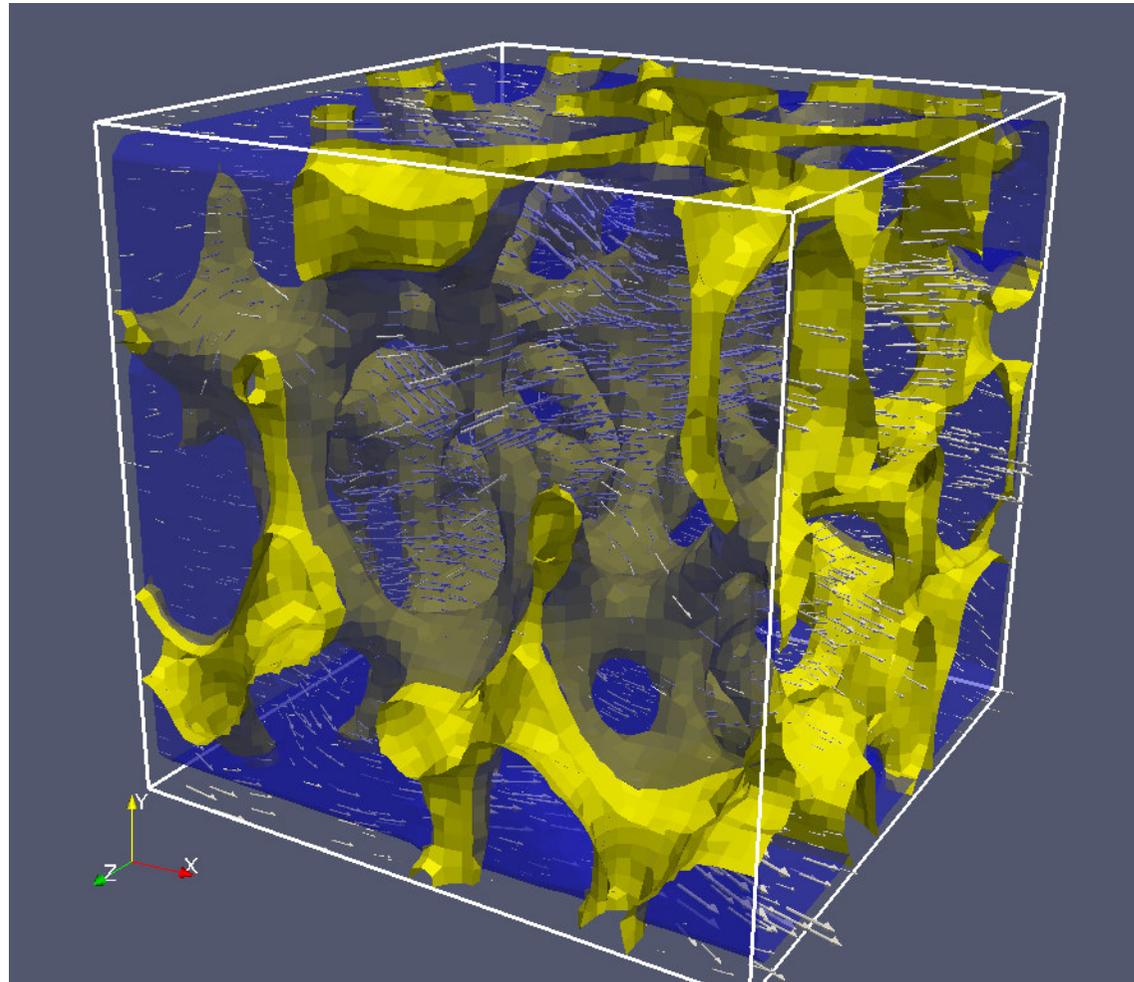
# Two Phase Flow in Sponge (Foam) Structure

- Blue iso-surface  
→ interface btw.  
liquid and gas
- Pressure-driven  
(from left to right)



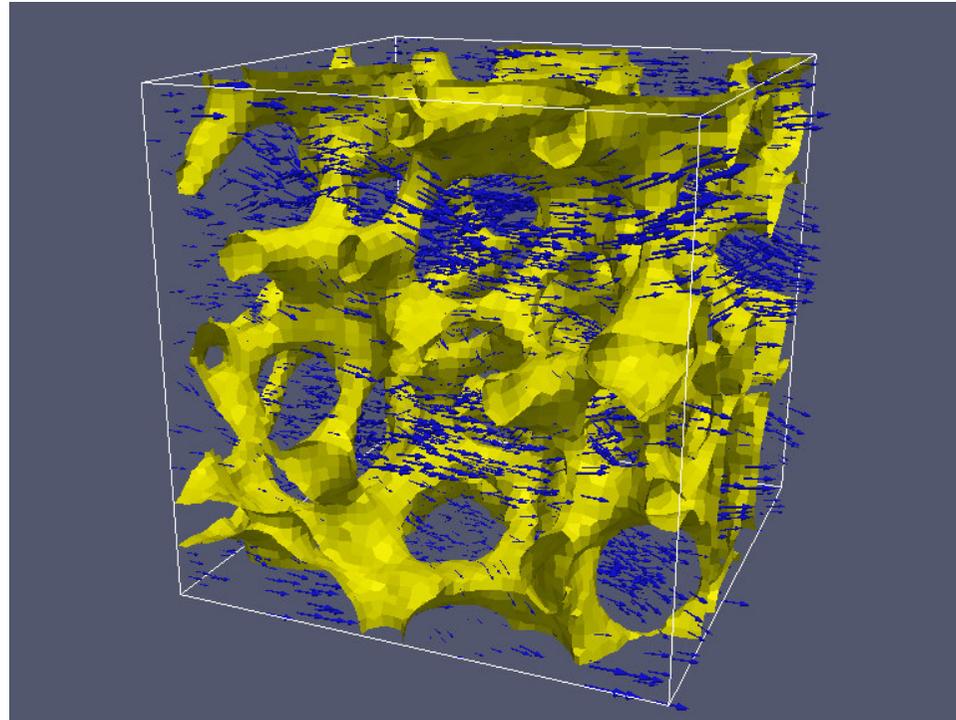
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# Validation for Hydrodynamics of Gas Flow

- Apply the solver for gas flow through sponge structure
- Compare simulated pressure drop versus superficial velocity against:
  - experimental results (Dietrich et al. 2009 [1])
  - CFD results using “simpleFoam” (Meinicke et al. 2014 [2])

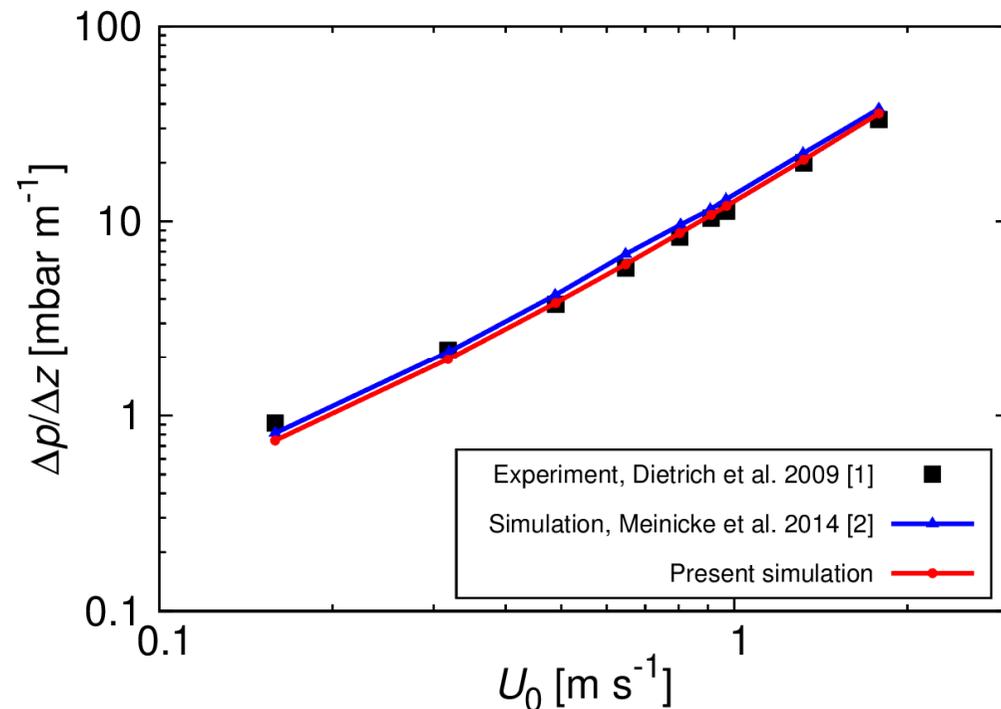


sample sponge type:  $\text{Al}_2\text{O}_3$ , 80% porosity, 20 ppi

- [1] B. Dietrich, W. Schabel, M. Kind, H. Martin. Pressure Drop Measurements of Ceramic Sponges - Determining the Hydraulic Diameter. Chem. Eng. Sci. 64 (16), 3633-3640. 2009
- [2] S. Meinicke, B. Dietrich, Th. Wetzels. CFD-Simulation der einphasigen Durchströmung fester Schwammstrukturen ProcessNet Fachausschuss CFD, Mischvorgänge u. Rheologie, Würzburg, 2014

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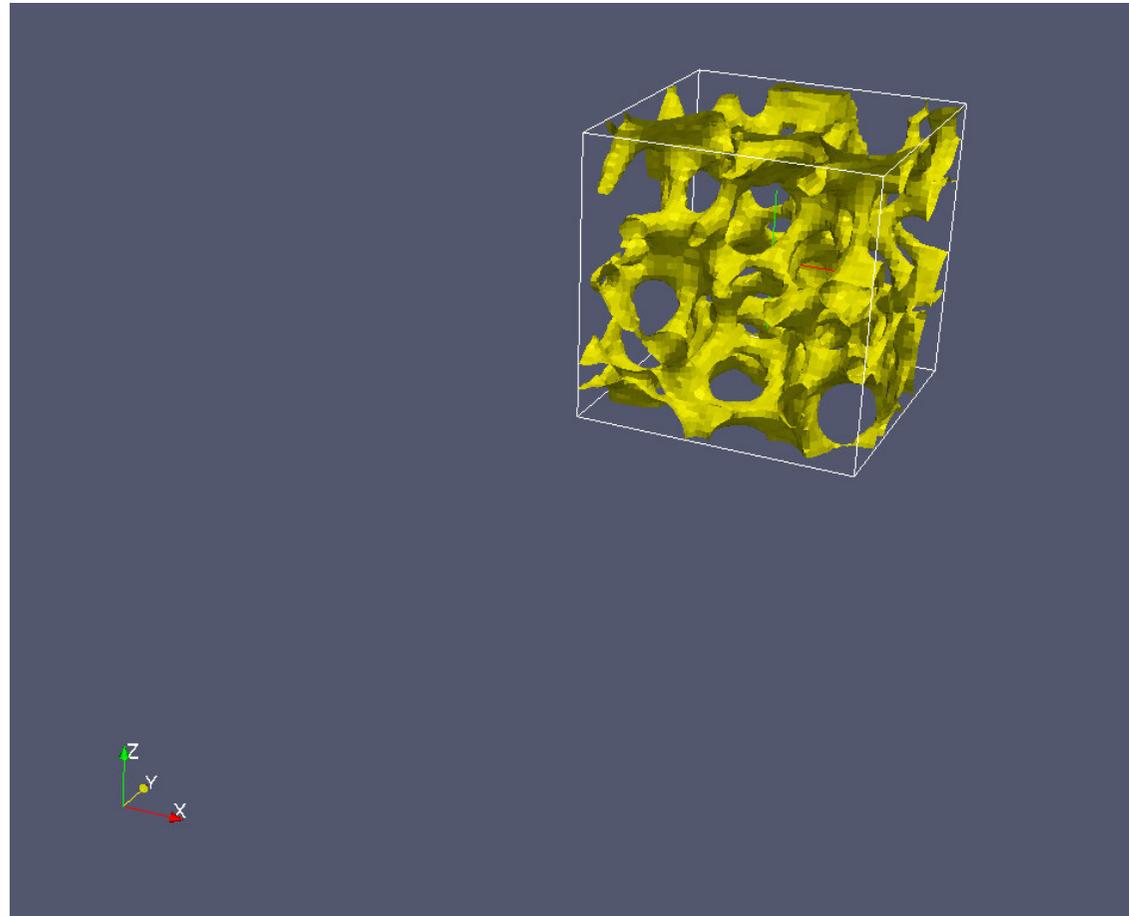


- $U_0$ : superficial gas velocity
- $\Delta p / \Delta z$ : pressure drop per unit length

- [1] B. Dietrich, W. Schabel, M. Kind, H. Martin. Pressure Drop Measurements of Ceramic Sponges - Determining the Hydraulic Diameter. Chem. Eng. Sci. 64 (16), 3633-3640. 2009
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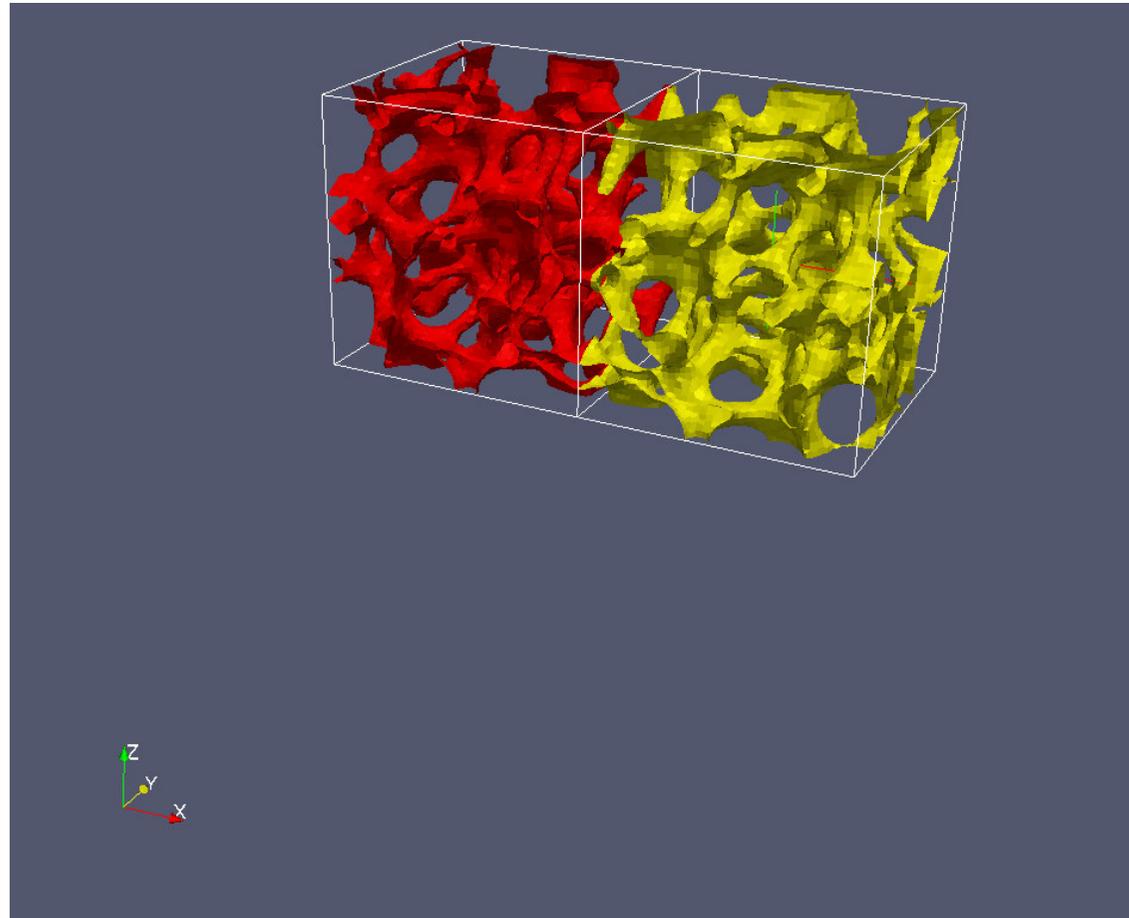
# Hydrodynamics of Two Phase Flows

- Exp. data will be provided by our project partner
- Representative domain → difficult to get inlet liquid distribution from exp.



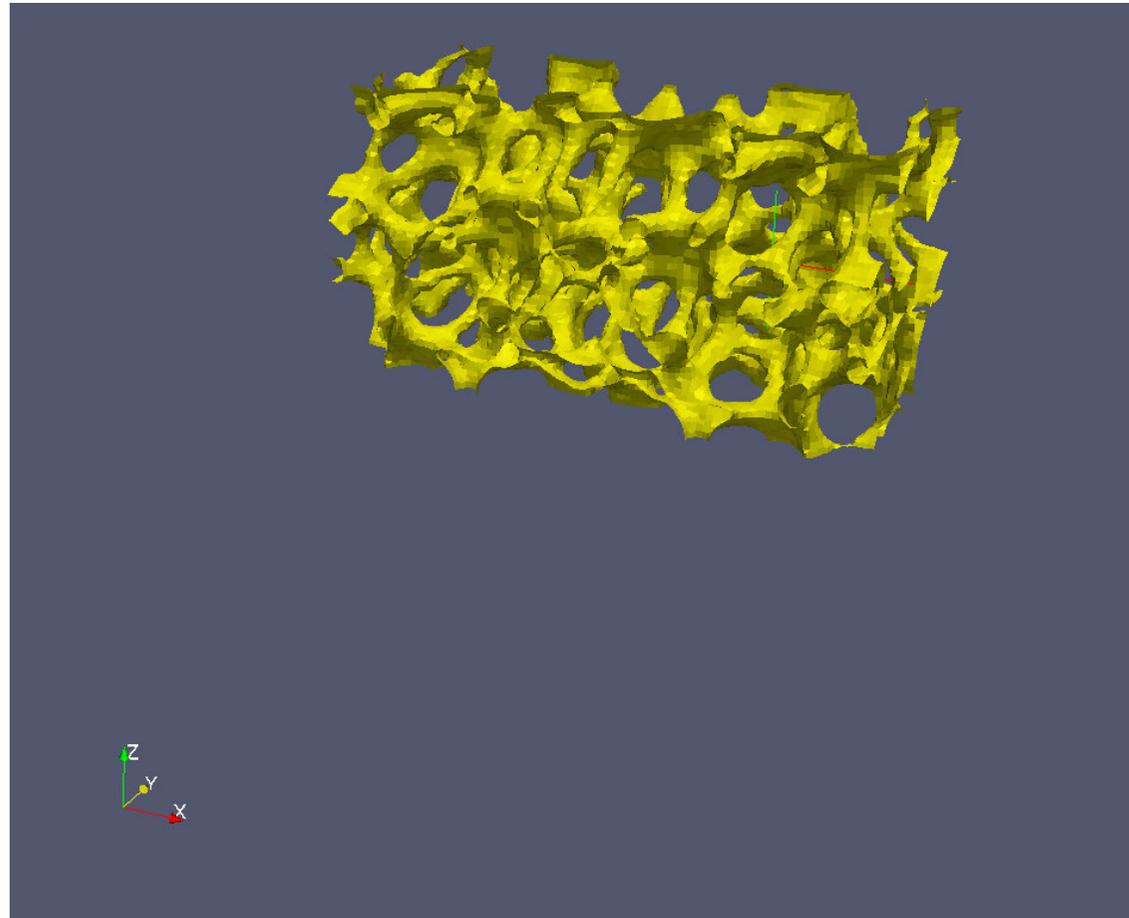
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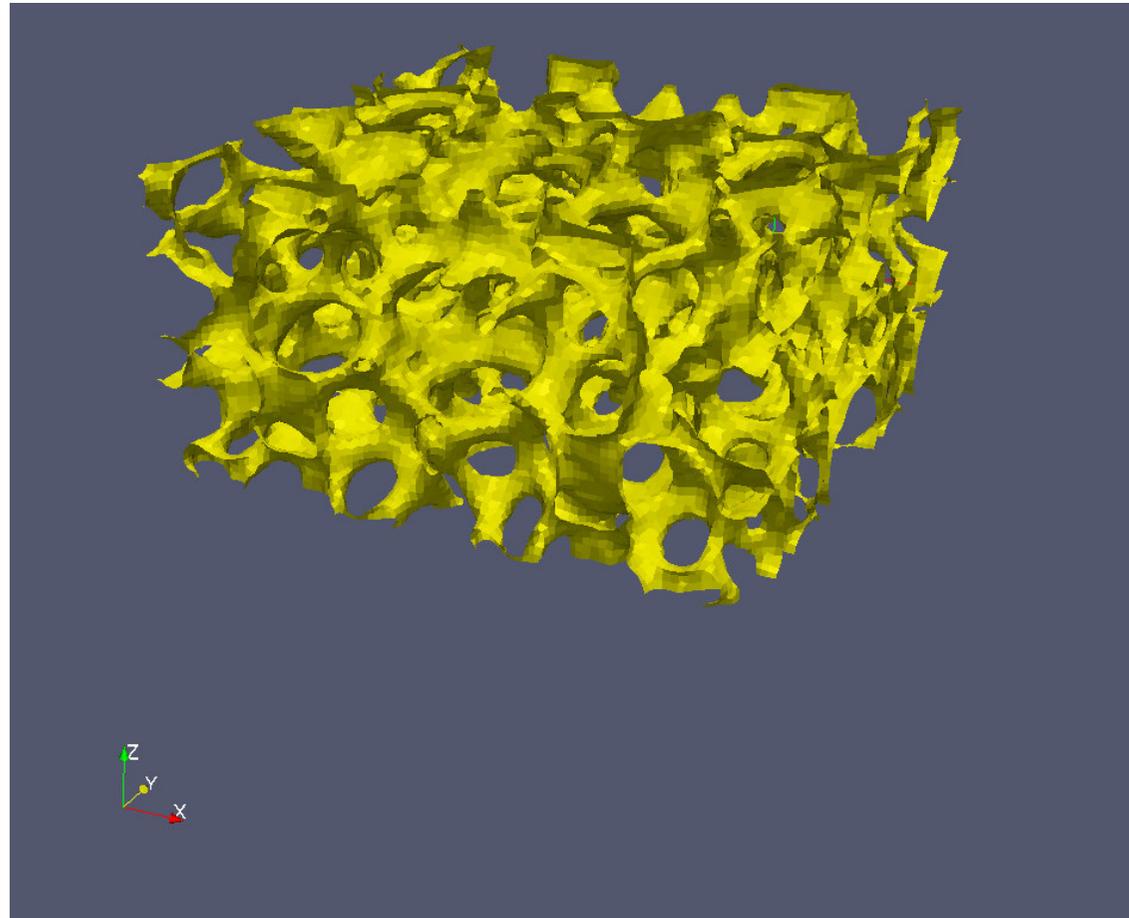
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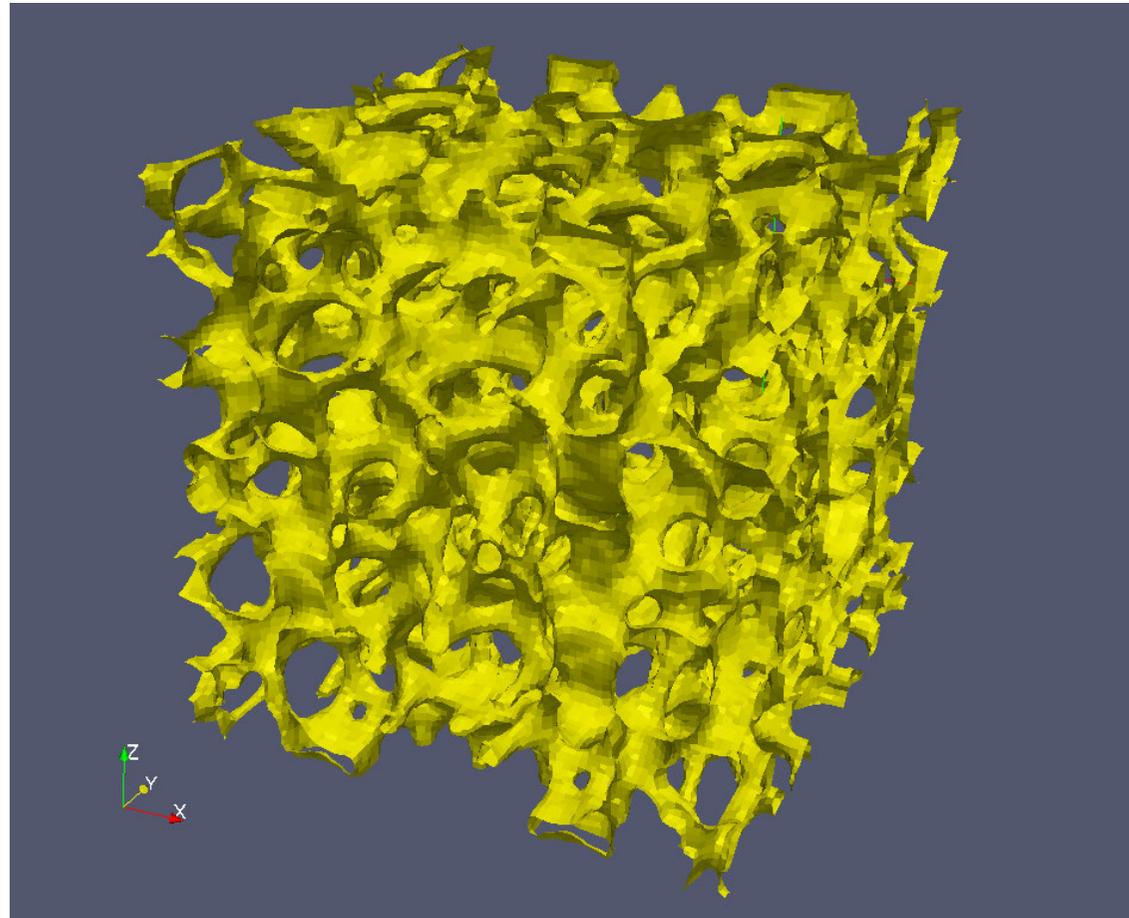
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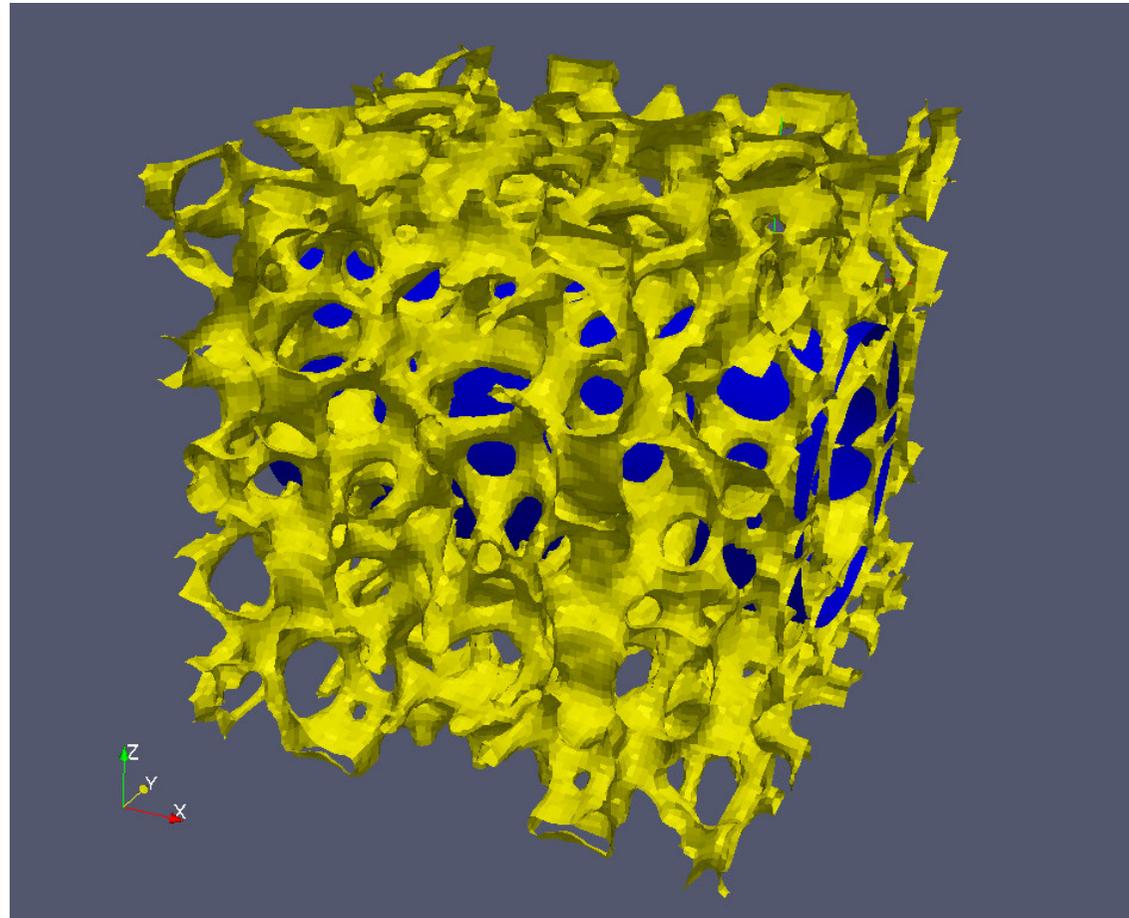
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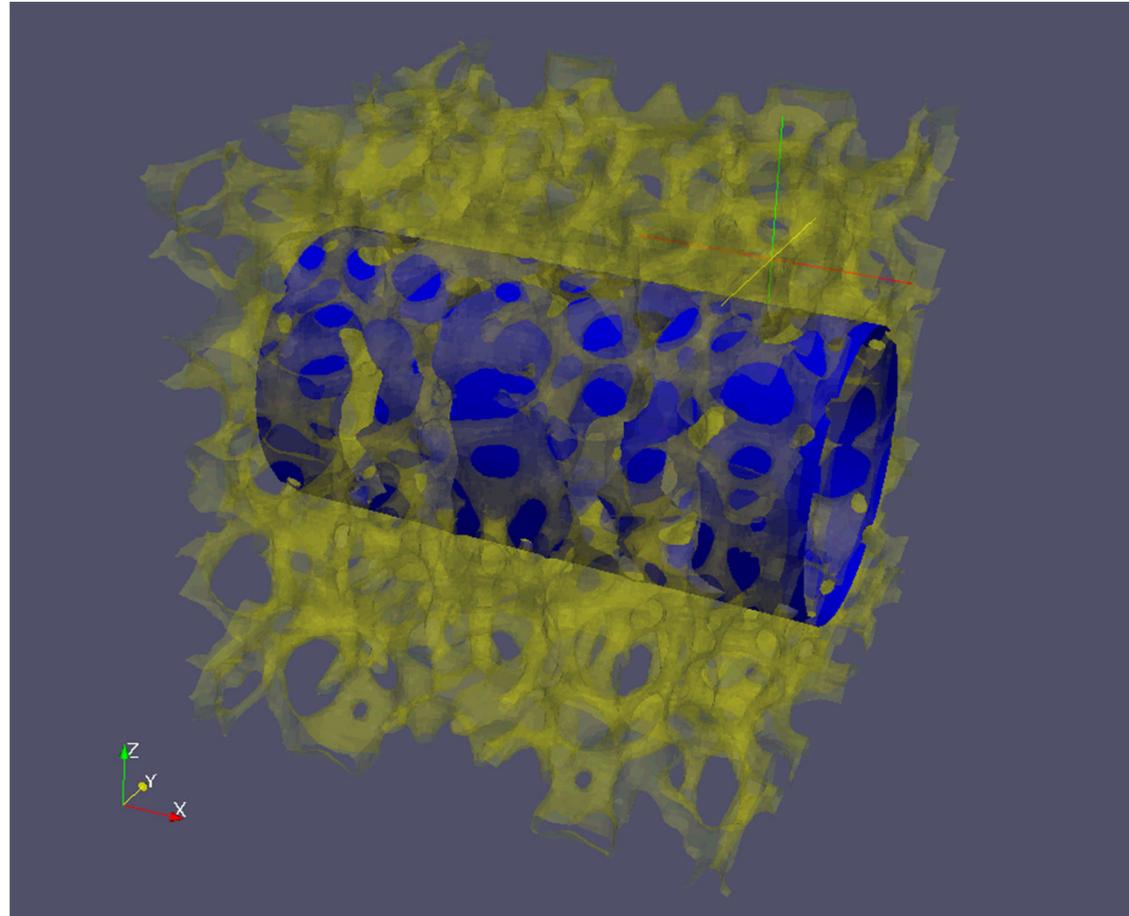
# Hydrodynamics of Two Phase Flows

- Specify initial liquid distribution along x
- Mesh Info
  - Background: 80\*80\*80
  - Two-level mesh refinement near solid surface



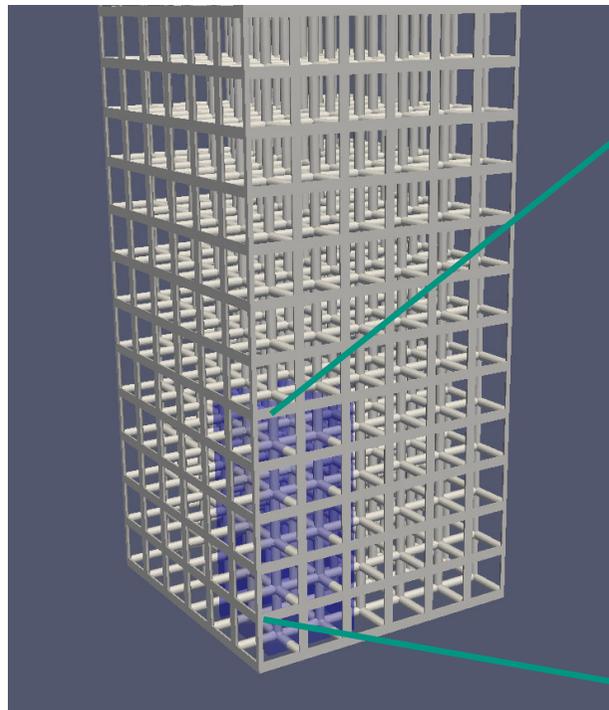
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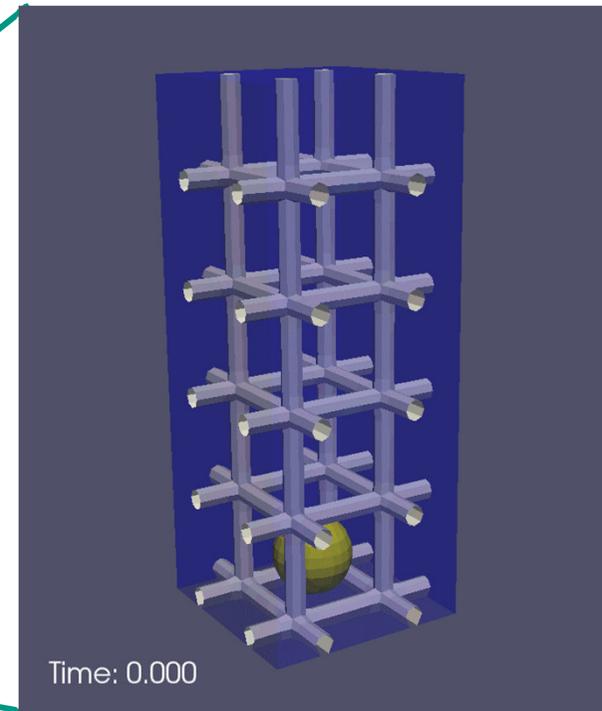


# Bubble Rise in Periodic Open Cell Structure (POCS)

- POCS as internals in bubble column reactor can enhance gas-liquid mass transfer (by disturbing/renewing the liquid concentration boundary layer)
  - Cooperation with Institute of Multiphase Flows, TU Hamburg-Harburg, Germany



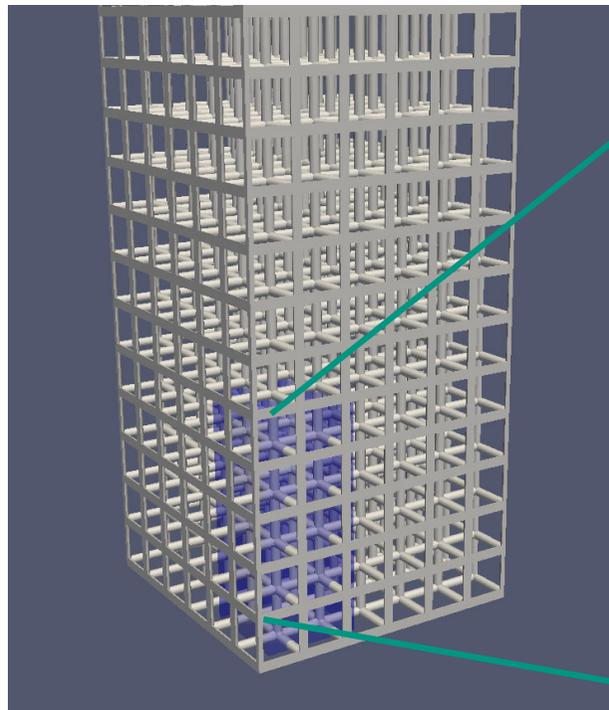
Windows size: 4mm; Grid Angle: 90°  
**Manufactured at FAU Erlangen, Germany**  
**Geometry provided by TUHH, Germany**



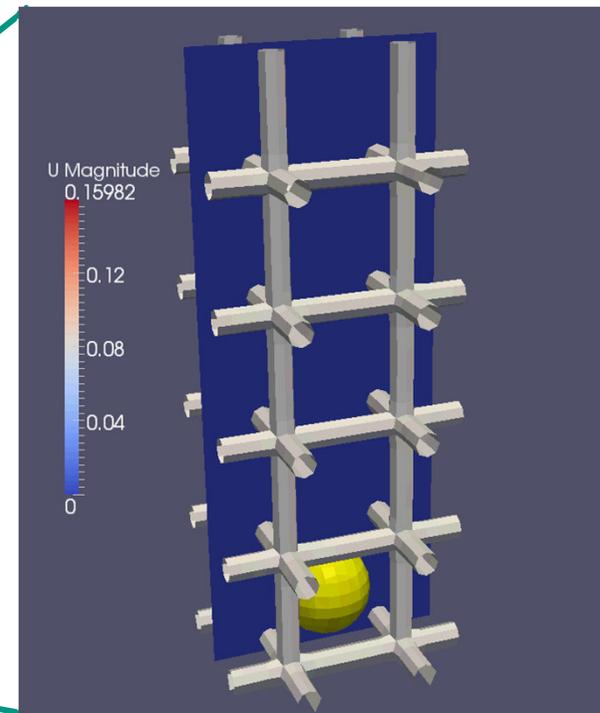
Subdomain for CFD simulation  
A gas bubble ( $D = 4\text{mm}$ ) in stagnant water  
Surface Wettability:  $\theta_e = 90^\circ$

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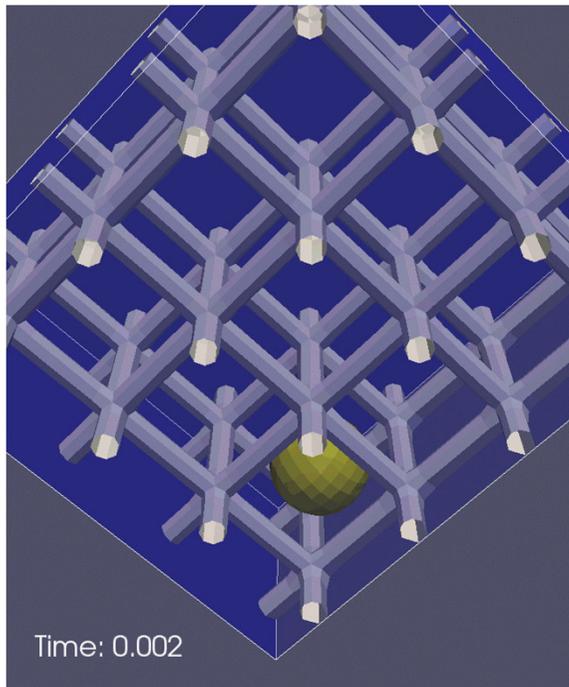


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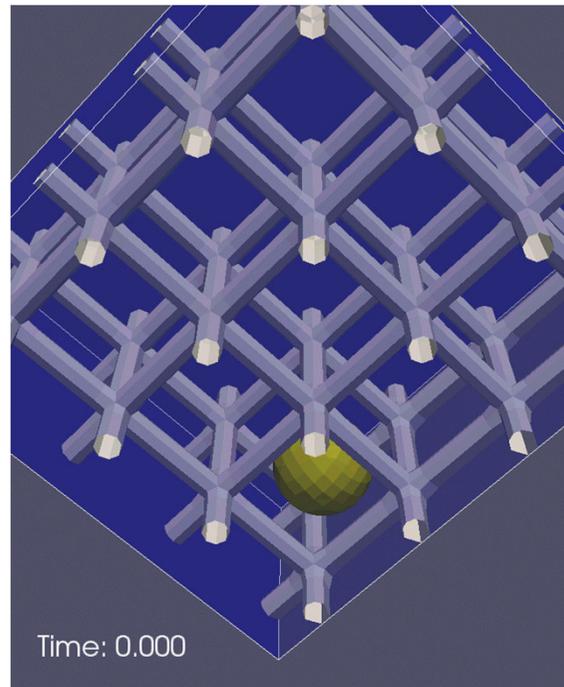
# Bubble Rising in Periodic Open Cell Structure

- Wettability effect on interaction of rising bubble with cell structure

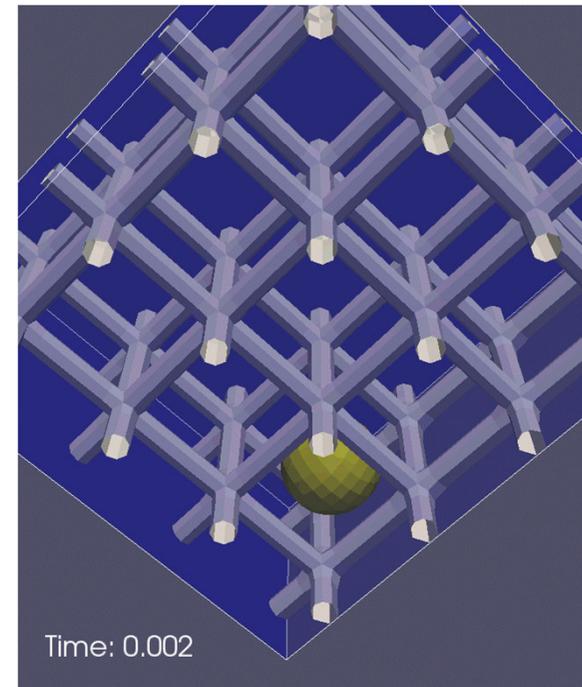
$$\theta_e = 0^\circ$$



$$\theta_e = 90^\circ$$

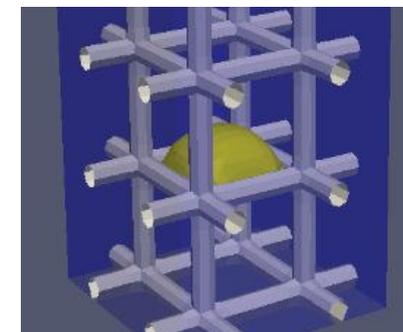
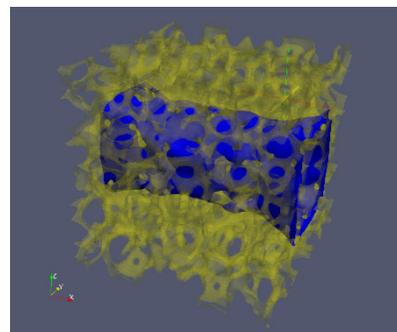
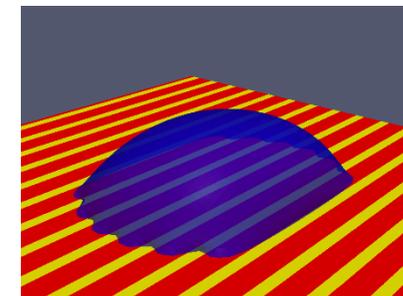
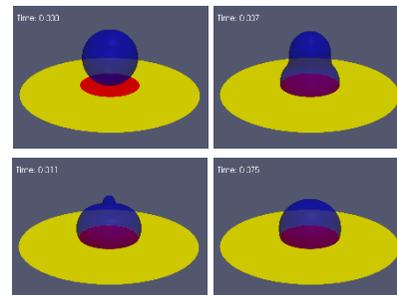
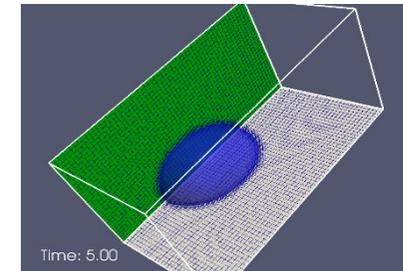
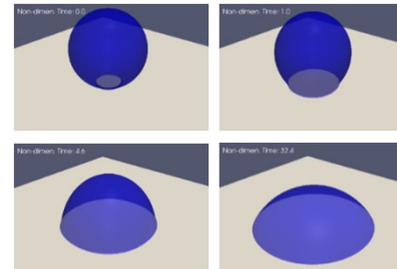


$$\theta_e = 135^\circ$$



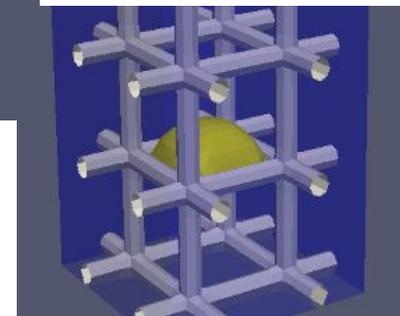
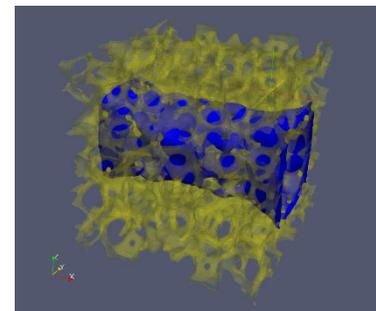
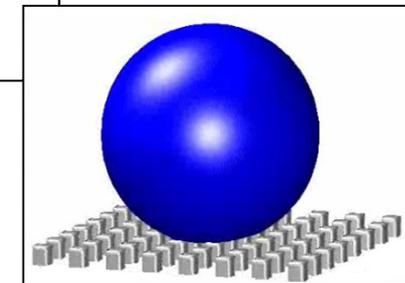
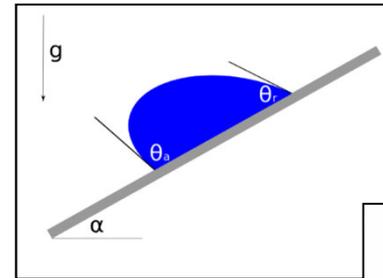
# Summary

- Droplet spreading/sliding on flat/inclined surface
- Wetting on chemically heterogeneous surface
- Two-phase flows in sponge (foam) structure
- Rising bubble interacting with solid cell structure



## Outlooks

- Pinning effect of droplet on inclined surface (contact angle hysteresis)
- Droplet wetting on topologically heterogeneous surface
- Provide closure relation (e.g. interfacial area) for Euler-Euler simulation for sponge structure
- Coupling hydrodynamics with heat transfer, mass transfer and chemical reactions ...



# Acknowledgement

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## ■ Partners:

- Dr. B. Dietrich, S. Meinicke (KIT-TVT, Germany)
- Prof. M. Schlüter, C. Möller (TU Hamburg-Harburg, Germany)
- Prof. M. Grünewald, C. Hecht (Ruhr Uni. Bochum, Germany)
- Prof. P. Yue (Virginia Tech, USA)
- Prof. H. Alla (USTO, Oran, Algeria)

