

Heavy Liquid Metal Summer School June 15–19, 2015 SCK•CEN Lakehouse, Mol, Belgium

# LIQUID-METAL CORROSION OF STEEL IN HLM

with emphasis on corrosion caused by liquid lead-bismuth eutectic (LBE)

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## Background



#### **Given Service Services of Service Activity of Servity of Service Activity of Service Activity of Service**

- □ High thermal conductivity and boiling point
- Reasonably low dynamic viscosity
- Some show minimum interaction with neutrons (e.g., sodium and lead)
- Liquid heavy metals release neutrons under proton irradiation (e.g., mercury, lead and bismuth)
- ...



- Efficient heat transfer medium/
- coolant for thermal energy conversion
- ---- Essential for fast neutron reactors
- Allows for sub-critical nuclear fuel in a proton-accelerator driven system
- Compatibility between liquid metals and steels?
  - Major steel elements are soluble in liquid metals
  - Formation of intermetallic phases
  - Degradation of mechanical properties
  - Prominent issue for lead alloys, especially lead-bismuth eutectic (LBE)

## In-service loadings on plant components





Some loadings are, however, interactive.

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## Some fundamentals of corrosion



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- Corrosion tends to achieve <u>global</u> thermodynamic equilibrium between material and corrosive medium.
  - Allows for identifying possible corrosion processes and estimating driving forces.
  - The fastest process is likely to dominate, especially in the initial stages.
  - The outcome of corrosion in the long run is, in general, hard to predict.
- Each corrosion process involves minimum one mass transfer across an interface and mass transport in the neighbouring phase.
  - The slowest elementary step is ratedetermining for the particular process.
  - Boundary conditions for mass transport (diffusion) follow from the assumption of <u>local</u> thermodynamic equilibrium at interfaces.

- The presence of a continuous and dense surface scale on the material is of particular importance.
  - Facilitated by the stability of solid corrosion products.
  - Spatial separation of material and corrosive medium increases the number of necessary transfer and transport processes.
  - Especially slow mass transport through <u>oxide scales</u> considerably reduces overall corrosion rates, may practically stop any further corrosion.
  - Such a surface oxide may be <<1 µm thick and exist on the material before first contact with the corrosive medium.
  - Passivation of so-called stainless steel is a prominent example.



Material	Composition*). Microstructure. Geometry.
Corrosive medium	Composition*). Available mass/volume per unit material surface area. Static or flowing.
Temperature	Thermo-physical and chemical properties, e.g., solubility limits and phase stabilities. Kinetics of corrosion processes or elementary steps like mass transfer and diffusion.
Temperature gradients	Local differences in characteristics mentioned above. Influence on long-range mass transfer or deposition.
Flow velocity	Mass transfer coefficients. Convective transport. Abrasion.

\*) Impurities may be as important as major constituents.

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# Solid metal in contact with liquid metal



Transfer of material elements onto the liquid metal as long as global saturation of the liquid is achieved



Causes for noticable recession of the material surface or loss of material

#### Liquid metal



Metallic material, polycrystalline



Surface interaction like adsorption, grain boundary grooving

Possible causes for degraded mechanical properties especially observed at relatively low temperature





Transfer of elements from the liquid onto the material, but mobility in the solid phase is comparatively low



**Chemical reaction** 

Formation of intermetallic compounds, depending on transport in the liquid metal or material, and stability of such new phases

# **Degradation of mechanical properties**





Fig. 2. Tensile load-strain diagrams of Armco iron specimens tested in bismuth (continuous lines) and in vacuum (dashed lines) at  $350^{\circ}C$  (1),  $400^{\circ}C$  (2), and  $550^{\circ}C$  (3).

Source: V.V. Popovich, I.G. Dmukhovskaya, Soviet materials science a transl. of Fiziko-khimicheskaya mekhanika materialov / Academy of Sciences of the Ukrainian SSR 14 (1978) 365–370.

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#### □ Iron–Bismuth:

- Hardening and embrittlement at 350°C.
- Softening and plastification at 550°C.
- Effects depend on the specific pair of solid and liquid metal.

# Liquid-metal/steel interactions

#### Corrosion

- Solution of steel elements with preferential (Ni, Cr) rather than general removal
- Surface recession and/or development of a nearsurface depletion zone
- Penetration of the depletion zone by liquid metal
- Formation of intermetallic phases on the steel surface or in a near-surface zone inside the steel

Observed on the µm-scale, accessible by light-optical microscopy (LOM), scanningelectron microscopy (SEM), energy-dispersive X-ray spectroscopy (EDX), X-ray diffraction (XRD) ...

Liquid-metal embrittlement (LME), softening, ....

#### **Degradation of mechanical properties**

- Damage accumulation at the surface due to corrosion
- Or arising from phenomena below the µm-scale:
  - Adsorption of liquid-metal elements
  - Subsequent processes affecting near-surface defects (dislocations, grain boundaries, cracks)
- Quantification by tensile, slow-strain rate, creep, fatigue, fracture-toughness tests performed either in or after exposure to the liquid metal



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#### Impact of oxygen solved on steel corrosion in liquid metals

#### "Absence" of oxygen

- Chemical oxygen potential too low for remarkable interactions with steel elements
- Steel elements dissolve in the liquid metal
- Absorption of liquid metal constituents by the steel
- Formation of intermetallic phases)

#### Low-oxygen conditions

- Solid oxides of steel elements are stable
- Amount of oxides formed too small for a continuous surface layer
- Concentration gradients that <u>promote</u> solution of steel elements may develop in the liquid metal

#### High-oxygen conditions

- Solid oxides of steel elements form a continuous surface layer
- Solution of steel elements still possible, but only after diffusion through solid oxide



#### Oxygen concentration in the bulk of the liquid metal $\longrightarrow$

Transition from solution-based to

 oxidation-based corrosion with increasing oxygen concentration

# Continuous oxide layer is the goal of deliberate oxygen addition (Pb, LBE)

Locally low-oxygen conditions even

 when oxygen concentration in the bulk of the liquid metal is high



### Effect of oxygen on the solution of steel elements

# Karlsruhe Institute of Technology

#### Unfavourable concentration gradients

- May establish if dissolving metal Me forms stable solid oxides
- Equilibrium concentration of solved Me then decreases with increasing c<sub>o</sub> (following from the solubility product of the solid oxide)
- Unfavourable gradient if c<sub>Me;eq</sub> decreases (due to increasing c<sub>O</sub>) with increasing distance from the steel surface





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## Effect of oxygen on the solution of steel elements





# Illustration of concentration profiles that are decisive for diffusion of Me in the liquid metal

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# **Corrosion testing in Pb or LBE**



COSTA		
Testing haracteristics Exposure to static liquid metal. Ceramic crucible containing 14 cm liquid metal. One specimen per crucible, partially submerged. Simultaneous exposure of several crucibles to flowing gas with controlled oxygen partial pressure in a glass tube. Homogeneous liquid metal temperature.		
Sample geometry	Typically, rectangular specimens with 5.6 cm <sup>2</sup> exposed to liquid metal.	
Determination of oxygen content	From equilibrium with oxygen-containing gas. Appropriate sensors under development.	

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# **Corrosion testing in Pb or LBE**



		Specimo
		Specifier
Testing characteristics	Exposure to static liquid metal. Ceramic crucible containing 70 cm <sup>3</sup> liquid metal. One specimen, partially submerged. Option to introduce oxygen-lean or -rich gas into the steel capsule that houses the crucible. Quasi-static when bubbling the gas through the liquid metal. Temperature gradient along the crucible height.	Gas outle
Sample geometry	Typically, cylindrical specimen with ~10 cm <sup>2</sup> exposed to liquid metal.	
Determination of oxygen content	Potentiometric oxygen sensor.	

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# **Corrosion testing in Pb or LBE**



CORRIDA		Locks of the test-sections Sensor 3 Heaters Oxygen- transfer device
Testing characteristics	Exposure to flowing LBE, typically 2 m/s. 1000 kg circulating LBE (5.3 kg/s). Several steel samples simultaneously exposed in vertical test-sections. Oxygen control via gas with variable oxygen partial pressure. Large internal steel surface in contact with the liquid metal. Temperature difference along the loop of ~100–150°C.	Air cooler Sensor 2 Sensor 4 Air cooler Flow Test-section 1 Counter-flow heat- exchanger Dump tank
Sample geometry	Typically, cylindrical specimen with 7.5 cm <sup>2</sup> exposed to liquid metal.	
Determination of oxygen content	Four potentiometric oxygen sensors distributed along the loop.	

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## **Post-test examinations**



#### Corrosion phenomena

- Structure/composition of corrosion scales
- Topography of interfaces, e.g., instantaneous steel surface
- Assessment on the µm-scale by LOM, SEM+EDX, XRD, …
- AES, XPS or TEM required when submicron resolution is required

#### Quantification

- Gravimetry vs. metallography
- Full quantification required, i.e., loss of sound steel <u>and</u> thickness of corrosion scales
- Element transfer to the liquid metal may then be calculated
- Local assessment of corrosion needed

#### Mechanisms and kinetics

- Deeper understanding
- Increased reliability of predictions
- Input to corrosion models
- Transfer to in-plant conditions

# **Oxidation in oxygen-containing LBE**

of 9Cr ferritic/martensitic and austenitic steels

#### Protective scaling

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- Thin Cr- (Si-) rich oxide scale (thickness ~1 µm or less)
- Precursors of this scale are likely to be present already on the original material
- Insignificant growth in thickness with increasing exposure time
- Release of Fe, Ni and other steel elements to the liquid metal is likely to be negligible
- Local degradation gives way to faster corrosion processes
- Dominant oxidation process for Type 316 steels and 15-15Ti, especially at T≤ 450°C and  $c_0 \le 10^{-6}$  mass%





316L

# **Oxidation in oxygen-containing LBE**



of 9Cr ferritic/martensitic and austenitic steels

#### Accelerated oxidation

- Typical for and, finally, the general corrosion process of 9Cr steels, after failure of the thin Cr-rich scale
- Less frequent occurrence on austenitic steels, especially at T≤ 450°C and c<sub>0</sub>≤ 10<sup>-6</sup> mass%
- Comparatively thick scales generally consisting of Fe<sub>3</sub>O<sub>4</sub>, Fe–Cr spinel<sup>\*)</sup> and an internal oxidation zone
- Release of Fe to the LBE at the oxide scale surface
- Fe<sub>3</sub>O<sub>4</sub> is missing at high T and low c<sub>0</sub> or high flow velocity





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<sup>\*)</sup> Notation  $Fe(Fe_xCr_{1-x})_2O_4$  implies that the formed spinel is based on  $FeCr_2O_4$  (regular spinel structure) but deficient in Cr. Alternatively, the formed spinel may derive from  $Fe_3O_4$  (inverse spinel structure) with solved Cr, i.e.,  $Fe(Fe_{1-x}Cr_x)_2O_4$ .

## Solution-based corrosion in oxygen-containing LBE



#### **Type 316 steels, 15-15Ti**

- Selective leaching of Ni and Cr
- Formation of a ferritic depletion zone that is penetrated by the liquid metal
- Occasionally, oxide (precipitated) on the surface, but transfer of removed elements to the LBE dominates
- Starts locally from failure of the thin Cr-scale





- 9Cr ferritic/martensitic steel
  - Probably starts from penetration of LBE into the oxide scale formed during accelerated oxidation
  - Steel elements may be selectively (Cr) or generally removed, depending on local conditions
  - Predominance of steel element release over accumulation in oxides not always clear

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# A porous inner magnetite layer

- replaces the Fe–Cr spinel found in 9Cr steels
- Oxidation not significantly faster, but scale integrity poorer
- Magnetite scale detaches, buckles and finally fails more frequently than scales observed for 9Cr steels



### Solution-based corrosion

Underneath or in the absence of buckled scale

**Outer part** 

Inner part

Iron



## Performance of Fe in oxygen-containing LBE

### at 450°C, 2 m/s and 10<sup>-6</sup> mass% oxygen

#### No protective scaling

#### Accelerated oxidation







Pb and Bi

at the interface

10 µm

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## **Quantification of corrosion**



#### Goal of quantification

- Material loss, average of general corrosion and maximum of local corrosion
- Thickness of adherent (oxide) scale
- Overall change in dimensions, including the scale
- Frequency of occurrence of different corrosion modes
- Amount of metals transferred to the liquid metal

#### Metallographic method (cylindrical specimens)

Initial diameter from measurement in a laser micrometer (0.1 µm resolution)



by 90°

- Diameter of unaffected material and thickness of corrosion scales determined in a microscope (LOM) at minimum ×500 magnification, with 1 µm resolution
- Identification of corrosion modes
- Occurrence of different corrosion modes on opposing sides of the re-measured diameter is considered in the evaluation



60°

Cross hairs

30°

0°

Direction of rotation

х

y

Mounting resin

Specimen

Marker at 270°



# **Example evaluation**



Oxide scale surface

Oxide/metal interface

8.000

10.000

#### Oxidation of Fe in LBE at 450°C, 2 m/s, 10<sup>-6</sup>% oxygen

#### Classification of local measurements

 Only diameters with oxidation on both sides useful for determining the recession of solid Fe

(url) x +20

+10

 $X_0 = 0$ 

-10

-20

 $\Delta x_{Ox} - \Delta x_{Ox;i}$ 

scale growth

Power law kinetics of

**Oxide/metal interface** 

2.000

from paralinear model.

4.000

Time (h)

6.000

 $-\Delta x_{Ox;i}$ 

 $-\Delta x_{Fe}$ 

 $\cap$ 

- Oxide scale thickness from any evaluated site that shows oxidation
- Quality of measurements?

#### Analysis of oxidation data

- Local scale thickness and recession of solid Fe as a function of time are compared with typical rate laws
- Amount of Fe solved by the liquid metal estimated from Fe mass balance (if not directly linked to a parameter of the kinetics of scale growth)
- Rate laws of scale growth, solution and Fe recession need to match each other
- Estimation of the position/movement of interfaces from the determined kinetics

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# **Kinetics of accelerated oxidation**



#### of 9Cr steel T91 in LBE at 450/550°C, 2 m/s, 10<sup>-6</sup>% oxygen



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#### **D** Parabolic approach $\Delta x^2 = k_2 t$

- Good approximation for short term data
- Overestimates steel recession and scale thickness in the long run

#### **D** Parabolic approach $\Delta x^2 = k_2 t + C_2$

- C<sub>2</sub> > 0 reflects initially fast progress
- Corresponds well with both steel recession and scale growth for long term data
- Believed to be more appropriate for data extrapolation than other power laws or logarithmic approach

```
D Paralinear approach \frac{d\Delta x}{dt} = \frac{k_p}{2\Delta x} + \frac{d\Delta x}{dt}
```

- Approximates the scale thickness
- Significantly overestimates metal recession

## **Kinetics of solution-based corrosion**



of Type 316 steels in LBE at 450/550°C, 2 m/s, 10<sup>-6</sup>% oxygen



#### □ In general, selective leaching of Ni and Cr

- Only few sites on investigated specimens may be affected
- Incubation times around 5000 and 1000 h at 450 and 550°C, respectively
- Maximum depth observed on the investigated cross section is evaluated
- Approximation of the kinetics by two linear rate laws so as to account for initially faster progress

#### In exceptional cases, non- selective removal of steel elements

- No kinetic analysis possible so far
- Non-selective removal apparently proceeds faster (in terms of depth of attack) than selective leaching

Mass transfer is likely to be equally fast for all steel elements, but limited transport of one or another element in the liquid metal may render the removal selective?

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## Mechanism of selective leaching from austenitic steel

#### Stage I

- Transfer of steel elements in proportion to their concentration in the steel
- Fe approaches saturation first, followed by Cr

#### Stage II

- Especially Fe partially re-precipitates as ferrite, alternatively to transport in the liquid metal
- A ferritic depletion zone establishes, with minimum driving force for Fe (Cr) transport inside this zone
- Further re-crystallisation of austenite into ferrite via intermittent solution in the liquid metal
- Ni is removed via diffusion in the liquid metal that accumulates in the depletion zone

#### Stage III

- Fe (Cr) still dissolves and is removed from the depletion zone surface
- Recession of the depletion zone surface

c<sub>Fe;S</sub>/ c<sub>Cr:S</sub>  $\mathbf{C}_{Ni;S}$  $C_{Fe;S}$ Liquid metal Ni Fe Cr. Ni Fe. Cr Boundary layer Austenitic steel Stage I Stage II Time Selective leaching is an intermittent step in the general, non-selective removal (solution) of steel elements

Qualitative concentration profiles

in the liquid metal

Selectivity gets increasingly lost, the faster Fe (Cr) transport in comparison to Ni diffusion

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## **Modelling approaches**



#### Protective scaling

- Prediction of scale failure more important than scale growth
- Approach by point defect model (e.g., developed by Macdonald et al.) seems promising
- Experimentally observed incubation time of solution-based corrosion or accelerated oxidation may be used as quality criterion

#### Accelerated oxidation

- On the basis of experimental data and rate laws available for oxide growth and steel recession
- Overall "less-than-parabolic" kinetics due to vacancy accumulation and pore formation at interfaces (point defect model) or re-distribution of Cr in the formed Fe–Cr spinel (more difficult to model)
- Growth stress or mechanical failure of the thick scale to be considered in addition to chemical failure

#### □ Solution-based corrosion, especially selective leaching

- Modification of simple mass transfer models by introducing the re-precipitation of solved steel elements in metallic form or as oxides
- Re-precipitation of ferrite in the depletion zone based on models developed for solid-state phase transformations

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# **Corrosion protection of steels**



### Optimum oxygen addition to liquid Pb or LBE

- □ In order to keep up protective scaling
- Promote accelerated oxidation rather than solution-based corrosion if the protective scale fails
- Required c<sub>o</sub> tends to increase with increasing temperature (and flow velocity)
- Adverse effect of oxygen if solutionbased corrosion actually occurs?

### Optimised steel composition and microstructure

- High content in Cr, (Si) or Al and finegrained microstructure promote oxidation, especially protective scaling
- Low Ni content, so that the optimised steel would be ferritic (bcc structure) rather than austenitic (fcc structure)

- However, the bcc structure seems more prone to embrittlement in case of oxide scale failure
- Any modification of existing steels requires time-intensive mechanical testing and qualification procedures

### Protective coatings

- With minimum solubility in Pb or LBE
- With optimised oxidation performance and applying oxygen addition at the same time
- Properties of the steel substrate remain unaffected as long as interdiffusion at the coating/steel interface is low
- Requires appropriate coating process
- Additional effort to be spent into manufacturing of coated components

## **Surface modification**



Surface alloying with strong oxide formers (AI) by pulsed electron beams provides corrosion protection in oxygen-containing Pb alloys at up to 700°C



GESA:

FeCrAl layer Volumetric heating: rate: < 10<sup>9</sup> K/s time: < 40 µs

LPPS sprayed



Melt layer:

depth:  $< 100 \ \mu m$ cooling:  $< 10^7 \ K/s$ (heat conduction)



Surface alloyed layer

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# Summary (1)



- Materials of construction, especially steels, are, in general, not stable in the service environment.
  - Possible interactions or transformations and associated driving forces follow from equilibrium thermodynamics.
  - Actually dominating mechanisms and kinetics of degradation are hard to predict, identification requires input from previous operating experience or experiments.
  - Surface scales play an important role for the observed kinetics and, therefore, applicability of the material.
  - Such scales may form in-situ or already exist before first exposure to the operating environment.
  - Influence of other in-service loading must be considered.

- In the presence of liquid metals, steels are prone to being solved or mechanical properties may degrade.
  - In the case of Pb or LBE, oxygen addition is considered an appropriate remedy for both principal degrading processes.
  - Modes of oxidation observed are protective scaling or accelerated oxidation—is the latter tolerable?
  - However, formed oxide scales tend to fail locally, and solved oxygen may then adversely affect steel solution.
  - 9Cr steels typically show accelerated oxidation rather than protective scaling.
  - Type 316 steels: primarily protective scaling, but comparatively short incubation of solution-based attack (selective leaching).

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# Summary (2)



#### Strategy accounting for interactions with LBE (Pb), for a particular steel under consideration:

- Define ranges of temperature and concentration of solved oxygen so that oxidation is tolerable and incubation of solution-based corrosion takes longer than the anticipated service time (ideal case).
- Prove that sufficient mechanical properties are maintained at contact of liquid metal with the steel after oxide scale failure.
- Consider surface alloying for improved oxidation performance, or other protective coating if limitations to operating conditions are too tight.

 On the basis of empirical
kinetics, derived mechanisms and corrosion models

Mechanical tests at simultaneous exposure to liquid metal, e.g., low oxygen content for investigating fundamental issues, target oxygen content for qualifying the materials

In principle, same tests as for uncoated materials, but special emphasis on interdiffusion between coating and substrate



# Thank you for your attention!

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