

**Analysis of Diffusion of Turbulent Kinetic Energy  
by Numerical Simulations of Natural Convection  
in Liquid Metals**

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# Introduction

- **Motivation**

**advanced liquid metal cooled reactors**

- **passive decay heat removal by natural convection**

**theoretical investigation of flow phenomena**

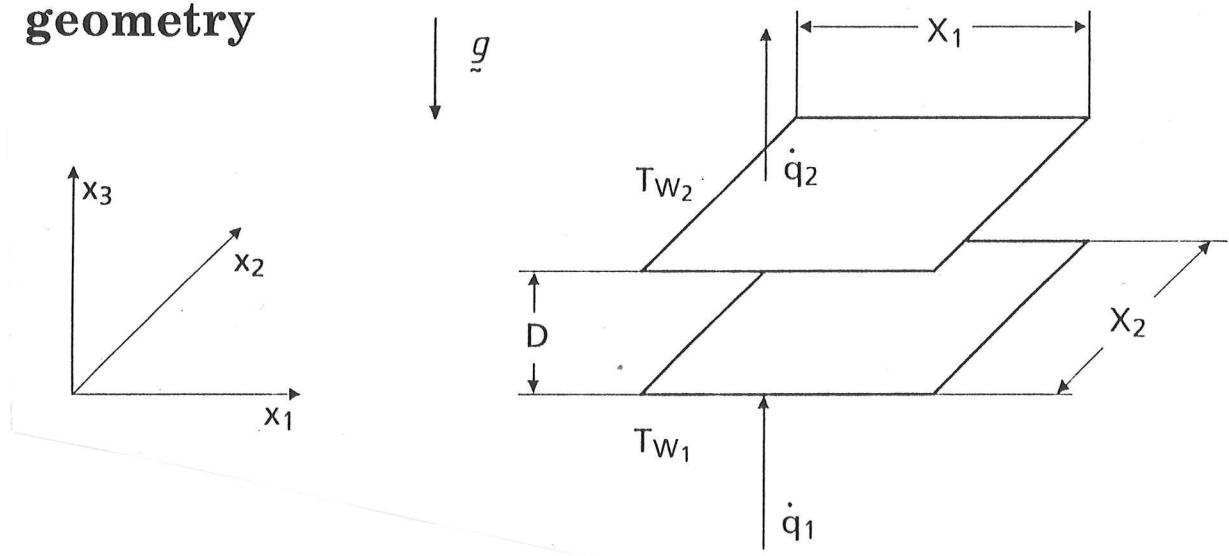
- **statistical turbulence models**  
e.g.:  **$k-\epsilon$  model  $v_t \sim k^2/\epsilon$**
- **transport equations for  $k$ ,  $\epsilon$**
- **closure of unknown correlations**

- **Objective**

- **detailed analysis of all terms in  $k$ -equation**
- **turbulent natural convection in liquid sodium**
- **evaluation of direct simulation results**

# Rayleigh-Bénard convection

- geometry



- dimensionless numbers

- Rayleigh-number:

$$Ra = \frac{g\beta(T_{W1} - T_{W2}) D^3}{\nu \kappa}$$

- Prandtl-number:  $Pr = \nu/\kappa$

liquid sodium:  $Pr = 0.006$

- Grashof number:  $Gr = Ra/Pr$

## Direct simulation method

- full conservation equations for
  - mass
  - momentum
  - energy
- three-dimensional, time-dependent
- resolve all scales
  - no model assumptions
  - no parameters

# Case specifications

Case	Pr	Ra	Gr	grid
A	0.006	3,000	$5 \cdot 10^5$	$128 \cdot 128 \cdot 31$
B	0.006	6,000	$10^6$	$200 \cdot 200 \cdot 31$
C	0.006	12,000	$2 \cdot 10^6$	$250 \cdot 250 \cdot 39$
D	0.006	24,000	$4 \cdot 10^6$	$250 \cdot 250 \cdot 39$

- **boundary conditions:**
  - periodic in horizontal direction ( $X_{1,2} = 8$ )
  - walls: no slip condition  
constant wall temperatures
- **initial conditions**
  - A, B, C: fluid at rest
  - D: final data of C

# Computer code TURBIT

- **finite volume method**
- **spatial discretization**
  - **finite differences**
  - **staggered grid**
- **time integration**
  - **momentum equation**
    - explicit Euler Leapfrog scheme**
    - projection method of Chorin**
  - **thermal energy equation**
    - semi-implicit Leapfrog-Crank-Nicholson scheme**
- **verified for natural and forced convection in various fluids**

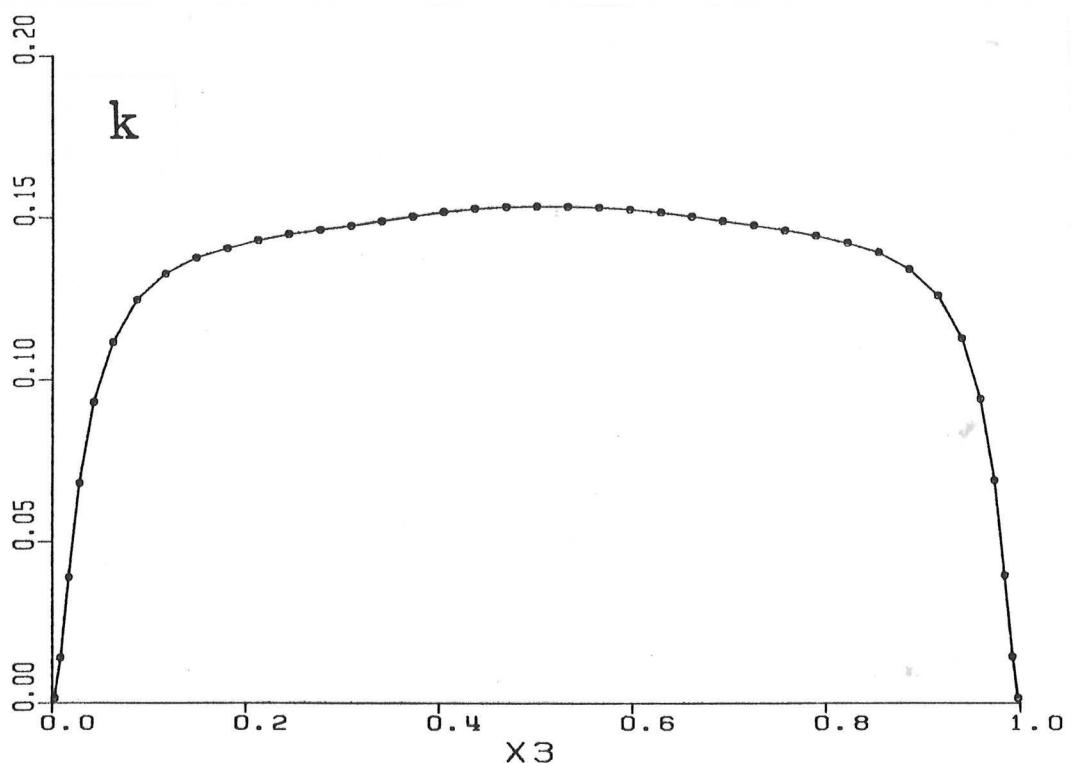
## Evaluation of numerical results

- 3d, time-dependent data for  $u_1, u_2, u_3, p, T$
- kinetic turbulence energy

$$k = \frac{1}{2} \overline{u_i' u_i'} = \frac{1}{2} \left( \overline{u_1'^2} + \overline{u_2'^2} + \overline{u_3'^2} \right)$$

where  $u_i' = u_i - \bar{u}_i$

- vertical profile of  $k$



## Transport equation for $k$

- turbulent Rayleigh-Bénard convection
  - no mean velocity  $\bar{u}_i = 0$
  - no gradients in horizontal directions
  - fully developed flow

$$0 = \frac{\partial}{\partial x_3} \underbrace{\left[ - \overline{u'_3 \frac{u'_i u'_i}{2}} - \overline{u'_3 p'} + \frac{1}{\sqrt{Gr}} \frac{\partial k}{\partial x_3} \right]}_D,$$

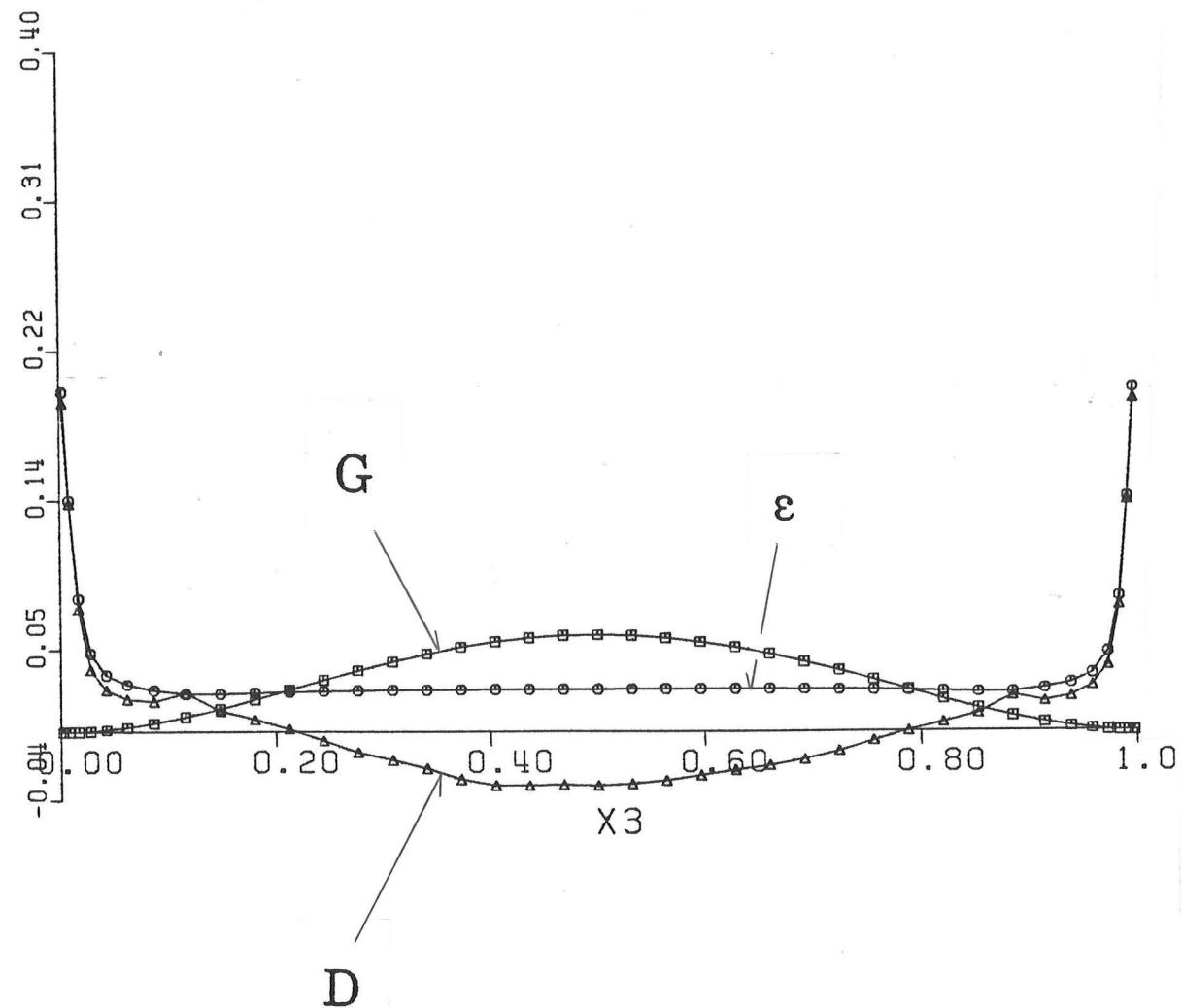
$$\underbrace{+ \overline{u'_3 T'}}_G$$

$$- \underbrace{\frac{1}{\sqrt{Gr}} \frac{\partial u'_i}{\partial x_l} \frac{\partial u'_i}{\partial x_l}}_\varepsilon$$

# Budget of kinetic turbulence energy

- sodium,  $\text{Ra} = 24,000$

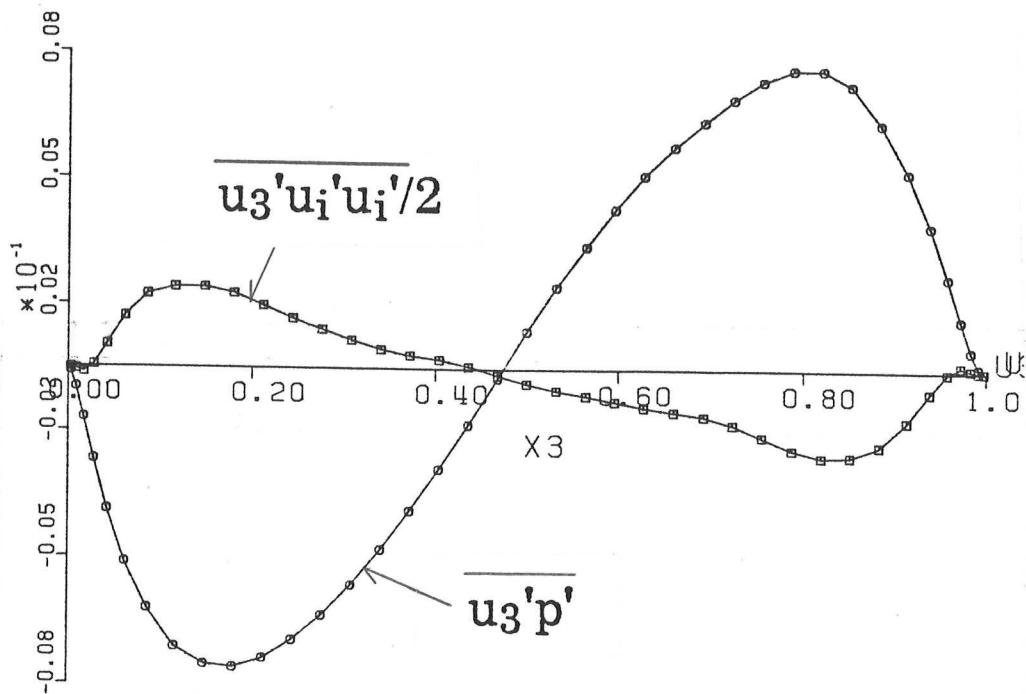
$$0 = G + D - \epsilon$$



## Analysis of diffusion of k

$$D = \frac{\partial}{\partial x_3} \left[ u'_3 \frac{u'_i u'_i}{2} + u'_3 p' - \frac{1}{\sqrt{Gr}} \frac{\partial k}{\partial x_3} \right]$$

- sodium, Ra = 24,000



- standard turbulence models
  - neglect molecular diffusion
  - neglect pressure diffusion
  - model triple correlation
- proposal of Lumley:  $\overline{u_3' p'} = -1/5 \overline{u_3' u_i' u_i'}$

# Conclusions

- Direct numerical simulation
  - turbulent Rayleigh-Bénard convection
  - liquid sodium
- Balance of kinetic turbulence energy
  - no local equilibrium  $G \neq \varepsilon$
  - redistribution of  $k$  by diffusion
  - turbulent diffusion mainly due to  $\overline{u_i' p'}$
- Standard turbulence models
  - neglect pressure diffusion