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# Behavior of UO<sub>2</sub> and FISSIUM in Sodium Vapor Atmosphere at Temperatures up to 2800° C

H. Feuerstein, J. Oschinski Hauptabteilung Ingenieurtechnik Projekt Schneller Brüter

# Kernforschungszentrum Karlsruhe

#### KERNFORSCHUNGSZENTRUM KARLSRUHE Hauptabteilung Ingenieurtechnik Projekt Schneller Brüter

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H.Feuerstein, J.Oschinski

Kernforschungszentrum Karlsruhe GmbH, Karlsruhe

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BEHAVIOR OF UO<sub>2</sub> AND FISSIUM IN SODIUM VAPOR ATMOSPHERE AT TEMPERATURES UP TO 2800 °C \*

Abstract

\*

In case of a HCDA a rubble bed of fuel debris may form under a sodium pool and reach high temperatures. An experimental technique was developed to study the behavior of fuel and fission products in out-of-pile tests in a sodium vapor atmosphere.

Evaporation rates of  $UO_2$  were measured up to 2800 °C. The evaporation was found to be a complex process, depending on temperature and the 'active' surface.

Evaporation restructures the surface of the samples, however no new 'active' surface is formed.

 $\mathrm{UO}_{2}$  forms sometimes well shaped crystals and curious erosion

products. The efficiency of the used condenser/filter lines was higher than 99.99 % . In case of a HCDA all the evaporated substances will condense in the sodium pool.

Thermal reduction of the UO $_2$  reduces the oxygen potential of the system. The final composition at 2500 °C was found to be UO $_{1.95}$ .

The only influence of the sodium vapor was found for the diffusion of  $UO_2$  into the thoria of the crucible. Compared with experiments in an atmosphere of pure argon, the diffusion rate was reduced.

This paper was presented at the International Conference on Nuclear and Radiochemistry, Beijing, China, Sept.1-5,1986

VERHALTEN VON UO, UND FISSIUM IN EINER NATRIUMDAMPF-ATMOSPHÄRE

BEI TEMPERATUREN BIS ZU 2800 °C \*

Zusammenfassung

Im Falle eines HCDA kann sich eine Schüttung von Brennstoffstücken unter einem Natriumpool bilden, in der hohe Temperaturen vorkommen können. Es wurde eine Versuchstechnik entwickelt, um das Verhalten von Brennstoff und FISSIUM in einer Natriumdampf-Atmosphäre out-of-pile untersuchen zu können.

Die Verdampfungsraten von  $\rm UO_2$  wurden bis zu einer Temperatur von

2800 °C bestimmt. Die Verdampfung ist ein komplexer Prozeß, der von der Temperatur und der 'aktiven' Oberfläche der Probe abhängt.

Bei der Verdampfung wird die Oberfläche der Proben sehr stark restrukturiert, es wird jedoch keine neue 'aktive' Oberfläche gebildet.

Bei hohen Verdampfungsraten kondensiert das  $UO_2$  in Form von

gut ausgebildeten Kristallen, durch Erosion entstehen daraus oft kuriose Gebilde. Der Wirkungsgrad der gesamten Abscheidestrecke war höher als 99.99 % . Für den Fall eines HCDA bedeutet das, daß die verdampften Stoffe im Natriumpool vollständig absorbiert werden.

Das Sauerstoffpotential des Gesamtsystems wird durch thermische Reduktion verringert. Die Endzusammensetzung des Oxides betrug bei 2500 °C  $U0_{1.95}$ .

Nur für die Diffusion von UO<sub>2</sub> in Thoriumdioxid wurde ein

Einfluß von Natriumdampf beobachtet. Die Diffusionsgeschwindigkeit war geringer als bei Versuchen in reinem Argon.

\* Dieser Bericht basiert auf einem Vortrag auf der "International Conference on Nuclear and Radiochemistry", Peking, VR-China, 1.-5.September 1986

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#### 1. Introduction

One accident scenario for a liquid metal fast breeder reactor (LMFBR) assumes that the reactor core has suffered catastrophic disassembly with the rubble of reactor fuel and cladding covered with liquid metal coolant and some structural or core-catcher material (1). An important, yet unanswered question, is then how much heat must be extracted from the rubble (2).

The produced heat is the decay heat of the radioactive nuclides, mainly from the fission products. The temperatures in the rubble bed depend strongly on the total amount of these radioisotopes, and also from their distribution between the different liquid and solid phases. At least parts of the bed will dryout and reach high temperatures. Crusts will isolate this part of the bed against the underlying structures, and a sodium vapor layer will be between the rubble bed and the sodium pool.

An out-of-pile experimental program is under way at KFK to study the behavior of radionuclides and fuel under such conditions (3). The behavior of  $UO_2$ -fuel will be described in this report.

#### 2. Experimental facility

The facility SUSI is used for the experiments (4). It may be considered to consist mainly of a stainless steel vessel with a volume of 1100 liters, with a water cooled induction coil in the center part. Auxiliary systems are for evacuating to a pressure of  $10^{-3}$  mbar, inert-gas supply and to deliver liquid sodium at a rate of 0.5 to 10 grams per minute into the vessel. This

sodium supply system consists of a hydraulic press, squeezing solid sodium into a melting crucible. The transport gas for the molten sodium is Ar-6.0.

All of the experimental arrangement is build inside of the vessel. Fig.1 shows a photography of the arrangement. The atmosphere in the vessel was always Ar-6.0.

3. Experimental arrangement

## 3.1 High temperature part

Figure 2 shows the high temperature part of the arrangement. The lower part of a 30 cm long tungsten receptor is in the induction coil. This is the furnace to heat the samples. The samples are kept in thoria crucibles, which are in a protective tungsten cup.

The sodium is evaporated by heating to 1000 to 1100 °C and blown to the sample through a tantalum tube. In some tests Ar-6.0 is used instead of sodium, also pre-heated in the evaporator. For easier retrievability of condensed substances a thin walled tungsten cylinder is placed inside of the receptor.

In most of the experiments the receptor is used without any thermal shielding. Radiation losses limit the possible temperature to about 2600 °C. For higher temperatures granulated thoria isolation in an alumina beaker is used.

# 3.2 Temperature measurement

The temperature measurement is done by optical pyrometers from outside of the vessel at the receptor (fig.2). Two-wave-length-pyrometers were used, measuring at 440 and 653 nm, or at 850 and 1000 nm . The pyrometers got calibrated by the PTB-Braunschweig with tungsten lamps. Because in the experiments also a clean tungsten surface is seen in pure argon, the values are considered to be reliable. The temperature at the position of the sample of course is somewhat lower. It is obtained from special calibration experiments, by observing a W-sample from the top.

The temperature difference between the receptor wall and the sample position was not constant. For e.g. 2500 °C is was between zero and 120 °C. It was independent on a preheated gas stream through the Ta-tube. Probably temperatures from the top are influenced by thermal convection inside of the receptor.

Many attempts were made to solve the problem of the sample temperature. Measurements with W-Re-thermocouples were not successful for temperatures above 2100 °C. However good values were obtained from the total amount of evaporated tungsten (determination as described for other elements below). By using functions as given by Jehn (5) the calculated temperatures were always within  $\pm 50$  °C of the temperature measured at the receptor.

Finally it was assumed, that the receptor-wall temperature is also a good measure for the sample temperature. In this paper therefore always receptor temperatures are given. One should keep in mind however, that the real sample temperature could be somewhat lower.

3.3 Low temperature part

The low temperature part may be considered to begin at the evaporator, which has a constant inside temperature of 1050 to 1100  $^{\circ}$ C. Up to this part sodium will be in the vapor phase.

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From the sample evaporating substances get transported by the sodium vapor and the Ar-transport gas first to a condenser, and further to parallel filter lines. The filters consist of sintered stainless steel plates or cylinders with a pore size (nominal) of 0.5  $\mu$  (SUPRAMESH of PALL-company). In case of sodium experiments these filters are pre-heated to 350 °C to avoid clogging. The efficiency of a filter-line is better than 99.99 % . Parallel lines could be used by opening or closing ball valves at a manifold from outside of the SUSI-vessel.

4. Experimental conditions

#### 4.1 Samples

For the experiments artificial fuel with fission products (FISSIUM), and  $UO_2$  - pellets from the NUKEM-company, are used. It is not possible to use plutonium in our laboratory. FISSIUM is an artificial mixture of  $UO_2$  and fission products, simulating a burn-up of 10%, sintered at a temperature of 1500 °C for 2 hours. It was fabricated in the facility FIFA (6). For some fission product elements radioactive tracers are used, e.g. for Zr, Nb, Ce and Ru.

In addition pure  $UO_2$  pellets were fabricated by the same method as the FISSIUM and used in some experiments.

(To simulate the destroyed core, stainless steel 1.4970 was added in some experiments. Results of such experiments were not reported in this paper.)

The sample weight was between 10 and 70 grams. Normally standard size pellets were used. In some experiments however broken pellets were used to increase the surface.

## 4.2 Atmosphere

The experiments were performed at a total pressure of 1 bar. In the tests the atmosphere at the samples was either Ar-6.0 or an Ar-6.0/ Na-vapor mixture with a sodium partial pressure of 0.2 to 0.3 bars. The gas was blown to the surface with a rate of about 25 1/min. The gas stream is not hitting the surface directely. It is leaving the Ta-tube very turbulent and just filling the lower part of the receptor with 'stirred' gas. Fig.3 shows a photography of the sodium-vapor leaving the Ta-tube.

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The oxygen partial pressure may be an important parameter in the experiments. In case of no sodium attempts were made to measure it with an electrochemical analyzer (ENDOMESS). It has been always below 0.1 ppm by volume ( below  $10^{-7}$  bar). The coil of the evaporator is made of stainless steel, and traces of oxygen react probably with the chromium . In experiments with sodium the partial pressure could not be measured. The oxygen concentration of the used sodium was in the range of 10 ppm by weight. It can be assumed, that also in experiments with sodium, because of the reaction with the chromium of the steel, the oxygen partial pressure was below 0.1 ppm by volume.

( The fact that temperatures could be calculated from the tungsten evaporation rates (above) confirm the very low oxygen partial pressure.)

# 4.3 Procedure

The samples got heated to the wanted temperature with a heating rate of 50 °C per minute, then the temperature was kept constant for the predetermined time, and finally the cooling rate was 100 °C per minute. In some earlier experiments the temperature was raised stepwise. In experiments with sodium the sodium stream was started at a sample temperature of about 1400 °C. The temperature was kept at this level until a thermocouple at the evaporator showed that the sodium reached the receptor (usually after 2 to 3 minutes).

Figure 4 shows schematically the total procedure prior, during and after the experiment in the SUSI-vessel.

The most time consuming steps are after the heating. Sodium from all parts of the condenser and filter lines have to be converted to NaOH and NaNO<sub>3</sub>, using the technique of conversion by N<sub>2</sub>/steam or converting it with methyl-alcohol. All surfaces were washed with nitric acid and treated in an ultrasonic bath. Often large volumes of solutions were obtained, containing corrosion products from the used stainless steel parts as well. The solutions were prepared for the chemical analysis, which was done using an ICP-6000 of Perkin Elmer. Some elements had to be determined by neutron activation analysis, e.g. cesium. For some elements evaporation rates were too low and ICP-detection limits to high. For these elements radioactive tracers were used and gamma spectroscopy applied.

Uranium, which is the only element described in this report, was determined always by ICP.

### 4.4 Performed experiments, range of parameters

So far results could be obtained from 34 experiments, with temperatures between 1400 and 2800 °C. The other parameters were : with or without sodium and steel, flow rate of the atmosphere, heating and cooling rates, specific surfaces of the sample, the amount of the samples and the sample material (UO<sub>2</sub> of different type and FISSIUM).

5. Results

### 5.1 Density and open pores

Because of the fabrication process and the high concentration on fission products, the used FISSIUM had a geometrical density of 7.5 g/cm<sup>3</sup>, and contained 28 % open pores. Pellets of pure UO<sub>2</sub> were fabricated by the same process, they had a densy of 9.8 and only 2.7 % open pores. Comparative tests were done also with different types of UO<sub>2</sub> pellets from RBU, they had densities of 10.3 and less than 1 % open pores.

Within the error limits density and open pore volume did not change, regardless if or not sodium was used. This result has been surprizing and can not be explained completely, because the metallographic picture especially of the FISSIUM was drastically changed. Probably there are compensating effects of densification and creation of new pores by evaporation.

### 5.2 Rate of evaporation

Evaporation rates of  $UO_2$  at high temperatures were reported in the literature several times (e.g. 7 and 8). However the experimental conditions were always different from these in a HCDA.

In the described experiments rates were determined by two ways: weight loss determinations for pure UO<sub>2</sub> pellets, and determination of the total amount of evaporated uranium from all parts of the arrangement. The second method was the only one usable for FISSIUM.

Using the geometrical surface of the pellets or broken pellets,

the evaporation rates as shown in fig.5 are obtained.

In spite of the scattering of the values there is no influence to be seen by the sodium vapor. That means sodium vapor behaves like an inert gas. This was to be expected because at the temperatures of the experiments there are no chemical compounds between sodium and fuel stable enough to influence the evaporation rate; and for lower temperatures the evaporation rates were too small to be measured.

Furthermore within the investigated range of 0.9 to  $3 \text{ cm}^2/\text{g}$  there is no influence of the specific surface, and within 0.6 to 3 cm no influence of the high of the stacked pellets or particles.

An Arrhenius-fit gives the evaporation rate as a function of the temperature as

$$\log ER = 2.29 - 11100/T$$

With this the heat for the total evaporation process is obtained to

$$\Delta H_{ER} = -212 [kJ/mol]$$

In this function the evaporation rate ER is given in  $[mg/cm^{2} \circ s]$ and the temperature T is given in K.

## 5.3 Discussion of the rates of evaporation

The table compares measured values with such from the theory and the literature.

Using a Knudsen-function (9) for calculating maximum evaporation

rates, with vapor pressure data of Ackermann(10), calculated rates are in a rather good agreement with data measured by Felix (7) in vacuum. That means the evaporation rates in vacuum are controlled by the vapor pressure. The heat of evaporation of -610 kJ/mol is in agreement with other observations.

In a gas atmosphere evaporation rates are as expected smaller. Data from Matzke (8), obtained in 0.5 bar hydrogen, are included in the table. Matzke found a heat of evaporation of -440 kJ/mol. In this case the total process is composed of several steps.

	I										
	I		I	evaporation rate [mg/cm <sup>2</sup> •s]							
			I	603 684 883 88							
Т	1	vapor press.	I		ł		1				
°C		of UO2	١	calc.(max)		Felix	1	Matzke			
	1	[mbar]	l	(9)		(7)		(8)	r	esults	
	1	(10)	I	(vacuum)		(vacuum)	l	(0.5 bar)	(	1 bar)	
	_ _		_ _		_		_				
	1		I		۱		I				
2000	l	0.0076	۱	0.12	1	0.1	l	0.0017		0.0025	
2500		1.8	ļ	25	1	50		0.2		0.019	
2800		18.0	۱	240	1	780		1.5		0.048	
	I		1		ļ		I	I			

The evaporation rates from this paper are - with the exception of the lowest temperature- even smaller than the values of Matzke. Also the found heat of evaporation is much smaller.

Concerning to Aitken (11) the total evaporation rate above 2000 °C is controlled by the transport in the gas phase. He estimates viscose flow in tight channels, if the partial pressure difference on both sides is larger than 1 mbar (for argon gas). For 2400 °C he calculates a evaporation rate of 2•10<sup>-3</sup> [mg/cm<sup>2</sup>•s], a value which is even smaller than the value of this paper. On the other hand he estimates heats of evaporation between -50 and -100 [kJ/mol], which are actually energies for the diffusion process.

The experiments reported in this paper are therefore between the experiments of Matzke and the model of Aitken. For the case of a HCDA one has to assume, especially at higher temperatures, evaporation rates of the fuel which cannot be neglected.

Furthermore Felix found for the release of fission products from fuel at high temperatures, that the release rates were controlled by the fuel evaporation, and not any more by the diffusion inside of the fuel.

If in the case of a HCDA the fuel reaches high temperatures, evaporation of fuel has to be considered. Important for this process will be the active surface. In our experiments the large inner surface in the case of used FISSIUM was 'not active' for the evaporation, while in the rubble bed of 3 cm depth all the geometrical surface was 'active'. In a real case there is one more driving force : the temperature gradient in the fuel because of the intrinsic heat sources. With the model of Aitken and the observations in this work, the evaporation rate will be not increased.

# 5.4 Transport of evaporated U02

As described in the previous chapters evaporating  $UO_2$  will leave the surface of the pellets. A smaller fraction diffuses into the thoria material, an other fraction condenses in the crucibles, the remaining part gets plated out at the high temperature part of the arrangement or is transported to the filter lines. The fractions of the evaporated  $UO_2$  found in the various parts af the arrangement were very scattered from experiment to experiment.

# 5.4.1 Diffusion into thoria

The used thoria curcibles were obtained from the ZIRCOA -company, ordered as 'fine grains' with high density. The density measured in our laboratory was  $9.38 \text{ g/cm}^3$ , with less than 0.1 % open pores.

Diffusion in solids is a very complex process, even if one considers a nearly ideal systems like the  $\text{ThO}_2 - \text{UO}_2$  mixture (12). It was not the goal of this work to study this diffusion, some observations however are worth to be discussed.

The diffusion depends on the (chemical) activity of the two oxydes, which is proportional to their vapor pressures. Because the vapor pressure of thoria is much lower than this of  $UO_2$ , diffusion was only observed for  $UO_2$  into the thoria, and not for thoria into  $UO_2$ . (The latter was checked by chemical analysis of the samples after the experiments.)

After removing the pellets from the crucible, 'foot prints' can be seen (fig.6). The deepest colored part were at the pelletpositions. There the UO<sub>2</sub>-partial pressure in the space between the oxydes has the highest value. The density of the thoria at such position after an experiments was found to 9.59 g/cm<sup>3</sup>, clearly showing the influence of the UO<sub>2</sub>. The thoria surface at such positions was very rough if compared with areas apart of it.

If viewed by dark-field optical microscopy or with polarized light, cross sections of the crucible at such position show a penetration profile with a sharp boundary (fig.7).

Actually there is no really boundary, as seen by microprobe analysis. The seen boundary reflects only a certain concentration of uranium in thoria. Nevertheless this boundary is used for the further considerations, because it was found in all experiments.

The boundary moves into the thoria with the square root of the time as expected for diffusion controlled processes. Fig.8 shows the results for the temperature of 2450  $\pm$ 50 °C. No differences are seen between different types of UO<sub>2</sub>-pellets or FISSIUM.

It is remarkable from fig.8, that the penetration rate is higher in experiments without sodium compared to those with a sodium vapor atmosphere. Because the vapor pressure of UO<sub>2</sub> is the same in both atmospheres, surface effects are probably responsible for this behavior.

This was the only influence of the sodium vapor atmosphere seen so far in our experiments. If or not such an effect could have an influence on core-catcher materials is not sure, however it has to be taken into consideration.

# 5.4.2 UO<sub>2</sub> crystals and erosion products

Evaporation rates of  $UO_2$  get high at higher temperatures. In such cases, well shaped crystals are growing at the wall around the upper edge of the thoria crucible. Fig.9 shows some SEM-pictures. The crystals were condensed from the gas phase, sometimes they were up to 0.5 mm in size.

The crystals undergo obviously an erosion process. Edges were smoothed and finally very courious figures were found (fig.10).

Chemical analysis of the crystals and erosion products showed more than 95 % UO<sub>2</sub> and less than 1 % ThO<sub>2</sub>, and the concentration on fission products (in the case of FISSIUM pelltes) was neglectable. From this analysis it may be assumed that pure UO<sub>2</sub> was condensed.

### 5.4.3 Deposition at high temperatures

Above a temperature of 1000 °C the sodium remained in the vapor phase. This part of the arrangement is called 'high temperature part'. The most important section of it was the tungsten cylinder. Along this the temperature dropped from the sample temperature to the temperature of the sodium evaporator.  $31 \pm 24$  % of the evaporated UO<sub>2</sub> was found in this section, sometimes in a narrow band, sometimes smeared over the whole cylinder surface. No effect of the experimental conditions on this distribution was detected, and the sodium had no influence.

Because no clear 'thermal gradient tube'-effect was found, and because the UO<sub>2</sub> in this part of the facility is already in a condensed form, aerosol deposition on the surface is considered to be responsible for the observations.

## 5.4.4 Transport into filter lines

On top of the evaporator (fig.2) and before the condenser there is a small space, where the temperature drops within less than 0.5 seconds to below 500 °C. In case of experiments with sodium, this is condensed in this area, probably starting at 'seeds' of other aerosols. 25  $\pm$ 15 % of the evaporated UO<sub>2</sub> was always found in this area, independent if or not sodium was used in the experiment.

The remaining  $\mathrm{UO}_2$  is found in the sintered metal filters.

# 5.5 Thermal reduction

Heating pure  $UO_2$  in an oxygen-free atmosphere will cause the loss of some oxygen from the oxide (13,14). Such an effect can be expected because of a relative high oxygen potential at high temperatures. If oxygen is lost the remaining oxygendeficient oxide has a lower oxygen potential. This may have an influence on the behavior of the nuclides.

In the experiments with FISSIUM this effect cannot be seen because of the many phases. In pure  $UO_2$  pellets however the oxygen deficient oxide is formed.

Metallographic specimen of samples, heated for 1 hour to 2500 °C in an argon or sodium/argon atmosphere, show the occurence of a metallic phase in form of bright spots with a diameter of 1 to 6  $\mu$  (fig.11). The pictures are comparable to those of Rothwell (13).

The original oxide was stoichiometric  $UO_{2.00}$ , the final composition was  $UO_{1.95}$  in the case of a LWR-specific pellet and  $UO_{1.96}$  in the case of a FBR-specific pellet. (These values were obtained by picture analysis). These are the final composition for a thermodynamic equilibrium , no further reduction is expected when heating for a longer time (11).

From the literature (13,14) one may expect a final composition of UO<sub>1.97</sub> for a temperature of 2500 °C. The found values are in the same range, the used method for the calculation however to coarse to allow a more precise evaluation

In any case thermal reduction has to be taken into account when considering the rubble bed of fuel. Especially the breeding blanket material, which will be one component of the rubble, will cause by this way a reduction of the overall oxygen-potential of the system.

## 5.6 surface structur

Evaporation of substances from solid bodies starts at sharp edges and corners, which gets smoothed by this process. In some cases even grain-boundaries may be startpoints for the evaporation.

Originally the surface of the used pelltes was smooth from the fabrication, even if the pellets were not grinded or polished. After an experiment the surfaces were completely restructured, consisting of small spheres and agglomerates, the spheres with diameters up to 100  $\mu$ . Fig.12 shows some examples. The new surface was formed at a temperature of 2400 °C within 10 minutes, at lower temperatures after a longer time. It was formed as well on FISSIUM and on UO<sub>2</sub> surfaces, independent on the used atmosphere.

The diameter of the spheres was the same at all temperatures and independent on the time. Sometimes however, especially at higher temperatures, columns of the same diameter were found on the surface.

Obviously the new structure is formed by evaporating oxide. The size of the spheres is larger than the grain size of the original material, which was in the case of FISSIUM 90% below 30  $\mu$ . Therefore it is assumed that the material is a condensate, especially if one considers the fact, that these spheres and agglomerates could easily be stripped away. Like the crystals described in chapter 5.4.2 the spheres consist of UO<sub>2</sub>.

The new formed surface is obviously much larger than the surface of the original pelltes. However it was not an active surface in the sense of chapter 5.3, and does not increase the evaporation rate. There were no signs for any influence of the new surface on the behavior of other nuclides. 6. Summary and discussion

An experimental arrangement was developed to study the behavior of UO<sub>2</sub> and FISSIUM in a sodium vapor atmosphere at temperatures just below the melting point of the UO<sub>2</sub>. Experiments were performed up to 2800 °C and up to 2 hours holding time. A maximum of 70 grams of sample materials was used in a 3 cm high stack.

Density and open pore volume did not change during an experiment. There were probably compensating effects of densification and creation of new pores because of evaporation of fission products and  $UO_2$ .

The evaporation rate of UO<sub>2</sub> was high at higher temperatures and reached 0.1 [mg/cm<sup>2</sup>•s] at 2800 °C. Only an 'active' geometrical surface participated in this process, no evaporation occured from inner pores (inspite of 28 % open pores in the case of FISSIUM).However in a 'rubble bed' of smaller pieces of broken pellets, all the geometrical surface was active.

The obtained evaporation rates were between values measured by Matzke (8) and evaluated by Aitken (11). Also the found heat for the total evaporation process of -212 [kJ/mol] was smaller than values of Matzke, but larger then these of Aitken. That means that in a small rubble bed the evaporation rate is not only controlled by the diffusion in the gas phase, but also by the evaporation itself.

For a rubble bed of a HCDA-reactor evaporation rates as described in this paper have to be expected. Near the melting point of the  $UO_2$  the rate is 0.07 [mg/cm<sup>2</sup>•s].

Evaporation of UO, creates a new pellet surface, consisting

of small spheres and agglomerates of pure UO<sub>2</sub>. However no new 'active' surface is formed.

Evaporated  $UO_2$  is transported away from the oxide surface. A small fraction diffuses into the thoria of the crucible. Inspite of no or very small temperature gradients one other small fraction condenses inside of the crucible. In case of high temperatures well shaped  $UO_2$  crystals, as well as curiously shaped erosion products of such crystals were found. No such particles were found inside of a bed of  $UO_2$  pieces.

One third of the evaporated UO<sub>2</sub> was plated out on surfaces with temperatures higher than 1000 °C. In this part of the experimental arrangement the sodium is still in the vapor phase, aerosol deposition may be assumed.

In the area after this high temperature part the temperature drops to below 500  $^{\circ}$ C within less than 0.5 seconds. Here around 25 % of the evaporated UO<sub>2</sub> was always found. Finally sintered stainless steel filters, SUPRAMESH of the Pall-company, removed more than 99.99 % of the oxide aerosol from the sweep-gas stream. In the case of experiments with a sodium vapor atmosphere, the filters were heated to about 350  $^{\circ}$ C to avoid clogging. The efficiency has been the same.

For the case of a HCDA-reactor therefore one can expect, that all of the evaporated fuel will be condensed within the sodium pool. Release to the environment can only occure together with the release of sodium or during a sodium fire.

The oxygen-potential of the fuel may influence the release of radionuclides and fuel. It was found, that under the conditions of an LMFBR - accident core a thermal reduction with the effect of reducing this potential occures. The final composition was found for 2500 °C to be  $UO_{1-95}$ .

All results described so far in this summary were obtained independent if or not the experiments were performed in a pure argon or an argon/sodium-vapor atmosphere. An influence of the sodium was only seen for the diffusion of UO<sub>2</sub> into the thoria of the crucible. In the case of sodium vapor, the diffusion rate was reduced. This effect will have to be considered when studying core catcher questions.

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Fig.1: Experimental arrangement in the SUSI-Vessel



Fig.2: High temperature part of the experimental arrangement



Fig.3: Beam of sodium vapor leaving the tantalum tube (about 2x)



Fig.4: Schematic diagram of the investigations prior and after the heating







<u>Fig.6:</u> 'Foot prints' of  $UO_2$ -pellets in the thoria crucible ( about 2x)



<u>Fig.7</u>: Diffusion zone of UO<sub>2</sub> into thoria; 1 hour at  $2500^{\circ}$ C, sodium vapor atmosphere. (100 x)



















 $\underline{\text{Fig.9 and 10:}}$  Crystals of  $\text{UO}_2$  , condensed inside of the thoria crucible. Lower two figures erosion products.



Fig.11: Thermal reduction of UO<sub>2</sub>. Upper two figures FBR-specific pellets, lower two figures LWR-specific pellets. Left two figures before, right after heat treatment for 60 minutes to 2500<sup>o</sup>C. (Polarized light, 250x), white inclusions are metal rich phases.



Fig.12:Surface structure of  $UO_2$  pellets after exposure<br/>to sodium or argon for 15 minutes $2400^{\circ}C.$